DOMESTIC WASTEWATER TREATMENT EMPLOYING A NOVEL BAFFLED OSMOTIC MEMBRANE BIOREACTOR-MICROFILTRATION HYBRID SYSTEM

by

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A Thesis submitted in fulfilment for the degree of

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- Pathak, N., Li, S., Kim, Y., Chekli, L., Phuntsho, S., Jang, A., Ghaffour, N., Leiknes, T. & Shon, H.K. 2018, Assessing the removal of organic micropollutants by a novel baffled osmotic membrane bioreactor-microfiltration hybrid system, Bioresource Technology, vol. 262, pp. 98-106.
- 3. Pathak, N., Chekli, L., Wang, J., Kim, Y., Phuntsho, S., Li, S., Ghaffour, N., Leiknes, T. & Shon, H. 2017, Performance of a novel baffled osmotic membrane bioreactor-microfiltration hybrid system under continuous operation for simultaneous nutrient removal and mitigation of brine discharge, Bioresour Technol, 240, pp. 50-8.
- Wang, J., <u>Pathak, N.,</u> Chekli, L., Phuntsho, S., Kim, Y., Li, D. & Shon, H. 2017,
 Performance of a Novel Fertilizer-Drawn Forward Osmosis Aerobic Membrane
 Bioreactor (FDFO-MBR): Mitigating Salinity Build-Up by Integrating
 Microfiltration, Water, 9 (1) 21.
- Chekli, L., <u>Pathak, N.</u>, Kim, Y., Phuntsho, S., Li, S., Ghaffour, N., Leiknes, T., Shon, H. 2018, Combining high performance fertiliser with surfactants to reduce the reverse solute flux in the fertiliser drawn forward osmosis process, Journal of Environmental Management, Vol.226, pp. 217-225.

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LIST OF ABBREVIATIONS

AL-DS Active layer facing draw solution

AL-FS Active layer facing feed solution

AOB Ammonia oxidizing bacteria

AS Activated sludge

BNR Biological nutrient removal

CEOP Cake-enhanced osmotic pressure

CLSM Confocal laser scanning microscopy

COD Chemical oxygen demand

CP Concentration polarization

CTA Cellulose triacetate

DI Deionised

DOC Dissolved organic carbon

DS Draw solution

ECP External concentration polarization

EDGs Electron donating groups

EDX Energy dispersive X-ray spectroscopy

EPS Extracellular polymeric substances

EWGs Electron withdrawing groups

FDFO Fertilizer drawn forward osmosis

FS Feed solution

HA Humic acid

HRT Hydraulic retention time

ICP Internal concentration polarization

LC-MS Liquid chromatography mass spectroscopy

LC-OCD Liquid chromatography-organic carbon detection

LMH Litres per square meter per hour

MBR Membrane bioreactor

MD Membrane distillation

MF Microfiltration

MLE Modified Ludzak–Ettinger (MLE)

MLSS Mixed liquor suspended solids

NaOAc Sodium acetate

NF Nanofiltration

NOB Nitrite oxidizing bacteria

OCT Optical coherence tomography

OLR Organic loading rate

OMBR Osmotic membrane bioreactor

OMBR-MF Osmotic membrane bioreactor-microfiltration

OMPs Organic micro-pollutants

PA Polyamide

PAOs Phosphorous accumulating organisms

PES-MF Polyether sulfone-microfiltration

PPCPs Pharmaceutical and personal care products

PRO Pressure retarded osmosis

RO Reverse osmosis

RSF Reverse salt flux

RSFS Reverse salt flux selectivity

SBR Sequencing batch reactor

SEM Scanning electron microscopy

SMP Soluble microbial products

SND Simultaneous nitrification and denitrification

SOA Ammonium sulphate

SOUR Specific oxygen uptake rate

SRSF Specific reverse salt flux

SRT Solid retention time

SWRO Seawater reverse osmosis

TDS Total dissolved solids

TDS Total dissolved solids

TFC Thin-film composite

TN Total nitrogen

TOC Total organic carbon

TP Total phosphorous

TrOCs Trace organic contaminants

TS Total solids

UF Ultrafiltration

Abstract

A novel baffled osmotic membrane bioreactor microfiltration (OMBR-MF) hybrid system was proposed for the domestic wastewater treatment with specific focus on nutrient and organic micropollutant (OMPs) removal. This baffled OMBR-MF hybrid system was first applied in laboratory scale conditions to treat simulated wastewater. Insertion of baffles in the aerobic reactor, created separate oxic and anoxic zones. In particular, simultaneous nitrification and denitrification (SND) was achieved in a single baffled OMBR-MF hybrid system. Thus, this reactor design enables both aerobic and anoxic processes reduce the process footprint and energy costs associated with pumping the mixed liquor in-between the oxic and anoxic tanks and chemical dosing costs for pH adjustment. The bioreactor was operated under four different oxic-anoxic cycle time at constant flux operation employing thin film composite-forward osmosis (TFC-FO) and polyether sulfone-microfiltration (PES-MF) membranes. At 65 d sludge retention time (SRT) 86-92 % COD, 63-76 % TN and 57-63 PO₄-P % removal was achieved during Run 1 to Run 4 in a bioreactor. The oxic-anoxic cycle time of 0.5-1.5 h appeared to be an appropriate choice for the process. Incorporation of MF membrane effectively alleviated salinity build up in the reactor, allowing stable operation of the system.

Based on outstanding SND performance using baffled OMBR-MF hybrid system test at different oxic-anoxic conditions long-term OMBR-MF hybrid system performance was evaluated at optimum oxic-anoxic (0.5-1.5 h) cycle time. The process performance was evaluated in terms of water flux, salinity build up in the bioreactor, organic and nutrient removal and microbial activity using synthetic reverse osmosis (RO) brine as draw solution (DS). The incorporation of MF membrane was effective in maintaining a

reasonable salinity level (612–1434 mg/L) in the reactor which resulted in a much lower flux decline (i.e. 11.48–6.98 LMH) as compared to previous studies. An average of 8.56 LMH FO flux was achieved during 38 days of continuous operation. The stable operation of the osmotic membrane bioreactor–forward osmosis (OMBR-FO) process resulted in an effective removal of both organic matter (97.84%) and nutrient (phosphate 87.36% and total nitrogen 94.28%), respectively. The dissolved oxygen profile during aerobicanoxic cycle confirmed < 0.5 mg/L oxygen favourable for denitrification.

To further investigate novel baffled OMBR-MF system performance in particular the efficiency of OMPs removal under unique redox environment (oxic-anoxic conditions) were evaluated. The performance of OMBR-MF system was examined employing three different draw solutes (DS), and three model OMPs. The DS employed in this study were sodium chloride (NaCl), potassium chloride (KCl) and sodium acetate (CH₃COONa). Three model organic micropollutants used were caffeine, atenolol and atrazine respectively. The highest forward osmosis (FO) membrane rejection was attained with atenolol (100%) due to its higher molar mass and positive charge. With inorganic DS caffeine (94–100%) revealed highest removal followed by atenolol (89–96%) and atrazine (16–40%) respectively. All three OMPs exhibited higher removal with organic DS as compared to inorganic DS. Significant anoxic removal was observed for atrazine under very different redox conditions with extended anoxic cycle time. This can be linked with possible development of different microbial consortia responsible for diverse enzymes secretion. Overall, the OMBR-MF process showed effective removal of carbonaceous matter, nutrient and organic micropollutants (OMPs).

Membrane biofouling is an inevitable phenomenon in any membrane process. Therefore real-time membrane fouling characterization without affecting continuous operation

would be helpful in devising efficient antifouling strategy. Further, real wastewater exhibits entirely different foultants and very diverse bacterial community. So, it would be more interesting to study foulant and microbial interaction with membrane employing real wastewater. So, in order to study the biofouling development on forward osmosis membranes optical coherence tomography (OCT) technique was employed. On-line monitoring of biofilm growth on a flat sheet cellulose triacetate forward osmosis (CTA-FO) membrane was conducted for 21 days with three different draw solutes. Further, the process performance was evaluated in terms of water flux, organic and nutrient removal, microbial activity in terms of soluble microbial products (SMP) and extracellular polymeric substance (EPS), and floc size. The measured biofouling layer thickness was in the order sodium chloride (NaCl) > ammonium sulfate (SOA) > potassium dihydrogen phosphate (KH₂PO₄). Very high organic removal (96.9 \pm 0.8%) and reasonably good nutrient removal efficiency (85.2 \pm 1.6% TN) was achieved. The sludge characteristics and biofouling layer thickness suggest that less EPS and higher floc size were the governing factors for less fouling.

Osmotic membrane bioreactor for wastewater treatment is very attractive and emerging process. It has shown very promising results for organic, nutrient and trace organics removal. With current technological advances, employing hybrid OMBR-MF have potential to produce fresh water at less cost than conventional desalination/water recovery technologies (i.e. ultrafiltration/RO systems). Main benefits of using baffled OMBR-MF hybrid system are better removal efficiency in terms of nutrient and micropollutants, saving in energy and pH adjustment costs, reduced process piping costs as SND takes place in single reactor and more flexible treatment unit.

The major challenges of OMBR to be a techno-economically viable technology are developing a high performance low cost forward osmosis membrane with higher flux and high selectivity with less internal concentration polarization (ICP) effect, and the availability of suitable draw solutions (to explore other divalent organic DS with lower RSF and lower fouling propensity and to compare their performance in baffled OMBR-MF system). It would be interesting to address microbial community dynamics in oxic and anoxic zone in the baffled bioreactor to elucidate its impact on nutrient and OMPs removal.

Besides, most of studies of OMBR have been performed at lab-scale. Therefore, more studies both in pilot and in full-scale plants are necessary to gain knowledge to achieve a better OMBR performance. In order to commercialise OMBR, full scale benchmarking and efficient process controls intensification are major challenges. Looking to the present progresses in FO membrane development (outer selective hollow fiber and nanomaterials made) in order to meet similar flux of existing porous membranes and very high performance of FO membranes in rejection of nutrients and micropollutants as compared to MF/UF membranes, OMBR can become techno- economically viable alternative for waster reuse applications in near future.

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