1	Potable water reuse through advanced membrane technology
2	Chuyang Y. Tang ^{a,*} Zhe Yang ^a , Hao Guo ^a , Jason Wen ^b , Long D. Nghiem ^c , Emile
3	Cornelissen ^{d,e,f,*}
4	^a Haking Wong Building, Department of Civil Engineering, the University of Hong Kong, Pokfulam Road,
5	Hong Kong, China
6	^b Department of Water Resources, City of Lakewood, California, USA
7	° Centre of Technology in Water and Wastewater, University of Technology Sydney, Sydney NSW 2007
8	^d KWR Watercycle Research Institute, 3433 PE Nieuwegein, Netherlands
9	^e Singapore Membrane Technology Centre, Nanyang Environment and Water Research Institute, Nanyang
10	Technological University, Singapore 637141, Singapore
11	^f Particle and Interfacial Technology Group, Ghent University, Coupure Links 653, B-9000 Ghent, Belgium
12	
13	* Corresponding Author. Tel: +852 2859 1976, Fax: +852 2559 5337, E-mail address: tangc@hku.hk
14	(CYT); Emile.Cornelissen@kwrwater.nl (EC)

16 Abstract

17 Recycling water from municipal wastewater offers a reliable and sustainable solution to 18 cities and regions facing shortage in conventional water supply. Places including 19 California and Singapore have developed advanced water reuse programs as an integral 20 part of their water management strategy. Membrane technology, particularly reverse 21 osmosis, has been playing a key role in producing high quality recycled water. This 22 feature paper highlights the historical development, current status and future perspectives 23 of advanced membrane processes to meet both indirect and direct potable reuse. Recent 24 advances in membrane materials and process configurations are presented and 25 opportunities and challenges are identified in the context of water reuse.

27 INTRODUCTION

28 Potable water reuse has become an important indispensable component of the water 29 infrastructure in many cities and regions around the world to address water scarcity. As a 30 notable example, water supply of Southern California traditionally relied heavily (about 31 two-thirds) on imported water, whose availability has shrunk significantly over the last 32 four decades due to more upstream demand, stringent environmental regulations and 33 multi-year droughts. Severe overdraft of groundwater since 1940s caused declining 34 groundwater levels and seawater intrusion that contaminated freshwater aquifers.¹ In the 1970s, Orange County Water District in Southern California started its Water Factory 21 35 (WF21), which employed advanced treatment processes to produce high quality recycled 36 water for direct injection to the drinking water aquifers.² Since 2008, a new Groundwater 37 Replenishment System (GWRS) has replaced WF21 to produce 70 MGD of highly 38 purified water using reverse osmosis (RO) technology.³ This world's largest advanced 39 40 wastewater reclamation system for potable reuse has expanded its production to 100 41 MGD in 2015, with an ultimate capacity of 130 MGD to be completed by 2023.

42

43 Membrane technology, particularly RO, has played a key role in producing highly 44 purified recycled water for potable reuse. Compared to alternative technologies such as 45 activated carbon adsorption and soil aquifer treatment, RO provides better assurance for 46 safe potable applications thanks to its ability to simultaneously remove a broader range of 47 contaminants including total dissolved solids, pathogenic agents, and organic 48 micropollutants [ref.]. Advancement in membrane technology in recent years has 49 increased the number of water reuse projects worldwide (Figure 1). In California alone,

several additional major projects have been implemented or planned, including the 50 51 40-MGD Edward C. Little Water Recycling Facility,⁴ a potential 150-MGD Regional Recycled Water Program in Metropolitan Water District of Southern California,⁵ and a 52 scheduled Groundwater Reliability Improvement Project (GRIP)⁶ to produce recycled 53 54 water in 2018. Water reuse has gone far beyond any single region or country, stretching 55 from the United States, Singapore in the Far East, South and Western Europe to Australia 56 in the southern hemisphere. In Singapore, the five NEWater plants provide a total of 170 MGD, or 40% of the nation's water supply.⁷ This number is scheduled to be increased to 55% 57 by 2060. Other notable examples include: the 20 MGD Beenvup plant commissioned in 58 Perth, Western Australia in 2016, which is the first RO plant in Australia for indirect 59 60 potable reuse; ... In Belgium (Europe) the Intermunicipal Water Company of Veurne-Ambacht (IWVA) treats secondary wastewater effluent at the Torreele facility for 61 indirect potable reuse via groundwater recharge in the dune water catchment of St. André.⁸ 62 63 This 2 MGD has been in operation since 2002 and has brackish water reverse osmosis at its 64 core for high quality water production. In Australia, after a successful full scale trial over 5 years, in 2016, the Beenyup Advanced Water Recycling plant was officially opened in 65 Perth as the first indirect potable reuse scheme in the country. In conjunction with aquifer 66 67 storage and recovery, the Beenvup plant can produce 20 MGD of recycled water, which is 68 enough to supply up to 100,000 households in Perth.



70 Figure 1. Historical developments of membrane-based wastewater reuse. The lower part of the 71 figure shows notable examples of wastewater reuse plants together with their treatment schemes. 72 The size of the sphere represents the relative size of a plant. The upper part of the figure presents 73 the development of new desalting membranes. The respective years of first appearance of 74 aquaporin, graphene, MOF and MoS₂ membranes are based on Refs ⁹⁻¹². The images of the 75 membranes in the upper part of the figure are reprinted with copyright permissions: CA and TFC 76 membranes from Ref. ¹³, CNT membrane from Ref. ¹⁴, biomimetic membrane from Ref. ¹⁵, TFN 77 membrane from Ref. ¹⁶, graphene membrane from Ref. ¹⁷, MOF membrane from Ref. ¹⁸ and MoS₂ 78 membrane from Ref. 19.

79

80 With water scarcity becoming an increasingly serious threat globally,²⁰ the thirst for

81 water reuse is growing. This feature paper examines the evolution of membrane-based

82 water reuse technology and highlights future opportunities and challenges in this field.

83

84 • EVOLUTION OF MEMBRANE-BASED WATER REUSE

85 Reverse osmosis (RO) is a well-established technology that can be used in combination

86 with other complementary processes (for pretreatment to remove particulate matter and posttreatment to ensure the destruction of any remaining micropollutants ²¹⁻²⁴ and 87 88 remineralization in the case of potable reuse) to produce high quality recycled water 89 (Figure 1 and Figure 2). WF21 in Southern California introduced the first RO plant in the world in 1977 to purify reclaimed water to meet drinking water standards.² This 5 MGD 90 91 RO plant was used to reduce the total dissolved solids of secondary effluent after 92 pretreatment by conventional lime clarification, recarbonation, and multimedia filtration 93 (Figure 2a). In modern potable reuse plants, conventional pretreatment is often replaced 94 by a single microfiltration (MF) process (Figure 2b), which is more compact and efficient 95 for the removal of particulates. In addition, downstream low pressure-high intensity 96 ultraviolet light with hydrogen peroxide (UV/H₂O₂) is typically used to ensure adequate 97 destruction of small molecular weight micropollutants such as N-nitrosodimethylamine 98 (NDMA), N-nitrosodiethylamine (NDEA), and 1,4=Dioxane that cannot be completely removed by RO membranes.²⁵ This advanced MF-RO-UV/H₂O₂ treatment scheme has 99 100 been widely adopted in many potable reuse plants, such as the grand-scale GWRS in Southern California³, the Bedok and Kranji NEWater plants in Singapore⁷, the Beenvup 101 102 plant in Australia (ref?), and the Toreele Reuse plant in Belgium (ref?). A further 103 significant improvement is the direct treatment of membrane bioreactor (MBR) effluent 104 by RO (Figure 2c). In this new treatment scheme, the MBR achieves simultaneous roles of bioreactor, biomass separation, and RO pretreatment.^{26, 27} The elimination of further 105 106 RO pretreatment using the particulate-free MBR effluent translates into additional 107 savings of space, energy, and cost, which prompts Changi NEWater Plant in Singapore to adopt the MBR-RO-UV/ H_2O_2 scheme.⁷ 108



109 110

Figure 2. Evolution of membrane-based water reuse: (a) conventional pre-treatment of secondary 111 effluent followed by RO; (b) MF pre-treatment of secondary effluent followed by RO, where an 112 additional UV/H₂O₂ post-treatment may be used for the further removal of organic micropollutants; 113 (c) MBR-RO treatment, where an additional UV/H₂O₂ post-treatment may be used for the further 114 removal of organic micropollutants; and (d) OMBR with an optional draw solution re-concentration 115 unit. Some OMBR applications (e.g., using fertilizer-based draw solution) do not require the 116 re-concentration unit.

Alternative membrane processes such as forward osmosis (FO)²⁸⁻³¹ have also been 118 119 explored for water reuse. FO-based processes, in which water transports through a dense 120 semi-permeable membrane using a high osmotic pressure draw solution, are interesting 121 due to their better ability to deal with difficult-to-treat waste streams (e.g., with high organic loading).³² One key challenge for FO is the energy-intensive re-concentration of 122 draw solution for clean water production.³¹ To overcome this issue, Shon and co-workers 123 ³³ developed a fertilizer-drawn FO process, in which the FO permeate water can be 124 reused for fertigation. Other applications that do not require draw solution 125 re-concentration, such as osmotic dilution of seawater or brine with wastewater ^{34, 35}, are 126 127 also gaining more attention. Nevertheless, economic benefits of water reuse through osmotic dilution are yet to be proven.²⁹ 128

An osmotic membrane bioreactor (OMBR) patented in 2005 ³⁶ is an innovative MBR 130 131 technique for the reclamation of wastewater, which combines activated sludge treatment and forward osmosis in a single unit process (Figure 2d).^{37, 38} Compared to the MBR-RO 132 133 scheme, OMBR can be potentially more compact and less energy intensive for niche 134 applications where draw solutions do not need to be re-concentrated (e.g., by using 135 fertilizer draw solutions). Other potential for osmotic membrane bioreactors include the high rejection of micropollutants ³⁹ and the simultaneous recovery of water, mineral, and 136 nutrient ^{40, 41}. Recent extension to anaerobic OMBRs further allow the recovery of energy 137 in the form of biomethane.⁴² Nevertheless, challenges of membrane fouling ⁴³, salinity 138 accumulation in the bioreactor ⁴⁴, and membrane stability ⁴⁵ need to be further addressed 139 140 to enable its full scale applications.

141

142 • TOWARDS BETTER PERFORMANCE MEMBRANES

143 Membranes play a critical role in RO-based water reuse. The quest for high-permeability 144 and high-selectivity RO membranes is summarized in Figure 1. The first-generation RO 145 membranes are of cellulose acetate with an asymmetrical structure. With the development 146 of more permeable and more selective thin film composite (TFC) polyamide membranes 147 in the 1970s, existing commercial RO membranes are largely dominated by the latter.⁴⁶ A 148 typical TFC RO membrane consists of a polyamide rejection layer of several tens to 149 hundreds of nanometers in thickness, which is formed by an interfacial polymerization 150 reaction of an amine monomer (typically m-phenylenediamine or MPD) and an acyl chloride monomer (typically trimesoyl chloride) on an ultrafiltration support substrate.⁴⁶ 151 152 Commercial TFC polyamide membranes have a wide range of pH tolerance (pH 2-11),

153 excellent mechanical stability (up to several MPa of applied pressure), high salt rejection 154 (e.g., NaCl rejection of up to 99.7%) and yet a moderate water permeability (e.g., 1-8 $L/(m^2h^1bar^1)$).^{47, 48} Unlike seawater desalination whose energy consumption (~ 4 kWh/m³) 155 156 is mainly dictated by the high osmotic pressure of seawater (~ 2.7 MPa), the energy consumption in RO-based water reuse (~ 1 kWh/m³ with approximately 0.555 kWh/m³ 157 for RO⁸) is governed mostly by membrane resistance and fouling. Tripling membrane 158 159 water permeability can potentially reduce the energy consumption for potable reuse by half.⁴⁹ Thus, developing low-pressure RO membranes with high permeability and good 160 161 antifouling performance deserves to be a top research priority.

162

163 Nanocomposite membranes. A new type of RO membranes, known as thin film nanocomposite (TFN) membranes, were developed by Hoek and coworkers in 2007.¹⁶ In 164 165 this novel approach, zeolite nanoparticles of defined pore size are included into the 166 polyamide rejection layer during an interfacial polymerization (Figure 3a). The inclusion 167 of porous zeolite nanoparticles enhances the resulting membrane permeability while 168 maintaining its salt rejection. The ease of fabricating TFN membranes at relatively cheap cost allows its commercial scale up.⁵⁰ In the meantime, many other materials, such as 169 170 nanoparticles of silver, silica, or zinc oxide, have been extensively studied for the synthesis of TFN membranes ^{51, 52}, although the majority of the studies were performed at 171 172 bench scale.



Figure 3. Novel RO membranes. Polyamide membranes include (a) a thin-film nanocomposite 175 176 membrane with nanomaterials embedded into polyamide rejection layer,¹⁶ (b) a molecular 177 layer-by-layer (mLBL) membrane fabricated by repeated cycles of interfacial polymerization of 178 MPD with TMC,⁵³ and (c) a sub-10-nm-thick polyamide rejection layer fabricated by performing 179 interfacial polymerization reaction on a sacrificial nanostrand interlayer.⁵⁴ Examples of emerging 180 materials for high performance membranes include: (d) aquaporins,¹⁵ (e) artificial water channel,⁵⁵ 181 (f) carbon nanotubes,⁵⁶ (g) metal-organic frameworks,¹⁸ (h) nanoporous graphene monolayers,⁵⁷ (i) 182 graphene oxide frameworks.¹⁷ and molybdenum disulfide (MoS₂) frameworks.¹⁹ All figures are 183 reprinted with copyright permissions from the respective references. 184

185 **Ultrathin membranes.** Another effective way to increase the membrane permeability is 186 by reducing the thickness of the polyamide rejection layer. Gu and co-workers introduced a molecular layer-by-layer (mLBL) membrane.⁵³ In their approach, an ultrathin 187 188 polyamide rejection layer was prepared by alternative soaking of a substrate in 189 low-concentration MPD and TMC solutions for repeated cycles (Figure 3b). A mLBL 190 membrane of 20-25 nm in thickness was prepared, which show 75% improvement in 191 water permeability and similar NaCl rejection compared to a control TFC membrane 192 prepared by conventional interfacial polymerization with rejection layer thickness of 110 nm. Livingston and co-workers ⁵⁴ prepared an ultrathin polyamide membrane by 193

194 performing interfacial polymerization reaction on a sacrificial layer of nanostrands. The 195 presence of nanostrand layer significantly reduced the diffusion of MPD monomers, 196 which resulted in an ultra-thin and smooth polyamide rejection layer of less than 10 nm 197 in thickness (Figure 3c). Though the resultant membrane had excellent water 198 permeability of more than two orders of magnitude higher than a commercial benchmark 199 and similar selectivity, this method is unfortunately difficult to scale up. By 200 electrospraying MPD and TMC monomer solutions into microdroplets for subsequent 201 interfacial polymerization, Tang and co-workers demonstrated finely controlled growth of a polyamide rejection film at 1 nm/min.⁵⁸ This electrospray-assisted additive interfacial 202 203 polymerization approach, a method that can be more easily scaled up, was able to prepare 204 uniform ultrathin polyamide membranes of four to a few tens of nm in thickness.

205

206 Next generation desalting materials and membranes. In recent years, novel materials 207 have emerged as potential candidates for preparation of high performance RO membranes.^{15, 59} One type of promising material is aquaporins (Figure 3d), or water 208 209 channel proteins, that are found in cellular membranes for delivering water across 210 biological cells with permeabilities of 2-3 orders of magnitude higher than the best 211 commercially available RO membranes and with nearly complete rejection of solutes including H⁺.⁶⁰⁻⁶² Synthetic channels and porous materials have also been investigated for 212 213 their use in synthesizing ultra-permeable membranes; some of the most notable examples 214 include self-assembled artificial water channels 55, carbon nanotubes (CNTs) 10, 14, 56, microporous metal-organic frameworks (MOFs) ^{50, 63, 64}, and graphene ⁵⁷, graphene oxide 215 ⁶⁵⁻⁶⁷, and MoS₂ ^{68, 69} (Figure 3e-j). Their intrinsic ultra-fast water transport rates can 216

potentially half the energy consumption for water reuse.⁴⁹ Nevertheless, a recent review highlights the challenges of defects prevention (for achieving high rejection) and scaling up (for commercial scale production).⁵⁹ Indeed, most of the reported membranes prepared by these novel desalting materials have NaCl rejections of only \sim or < 90%, which are significantly below commercial benchmarks. A compromise approach is to incorporate these materials in a thin film nanocomposite structure, which can effectively maintain salt rejection at the expense of water permeability.⁵⁹

224

225 Antifouling membranes. Developing membranes that are resistant to fouling, 226 particularly biofouling, is a priority research area in the context of membrane-based water 227 reuse. Various strategies have been developed to enhance antifouling performance of 228 membranes, which often involves surface coating, grafting, and immobilization of anti-adhesion and/or biocidal agents.⁷⁰ These approaches are generally designed to 229 230 modify a membrane's hydrophilicity, surface charge, and/or roughness, or to impart 231 antimicrobial moieties. Some notable examples of anti-fouling enhancement include polyvinyl alcohol grafting ⁷¹, polydopamine coating ⁷², zwitterionic grafting ⁷³ and 232 silver/copper nanoparticles immobilization ⁷⁴⁻⁷⁶. 233

234

235 • DEALING WITH ORGANIC MICROPOLLUTANTS

The presence of micropollutants in wastewater is a significant issue for membrane-based water reuse. NDMA is a notorious disinfectant byproduct and a human carcinogen that is frequently detected in RO permeate.^{25, 77} California has set a Public Health Goal of 3 ng/L and a notification level of 10 ng/L for this suspected carcinogen.⁷⁸ NDMA rejection by

RO membranes is in the range from 20 to 80%.77, 79, 80 Post-treatment by advanced 240 241 oxidation processes, such as UV treatment, is effective in destructing NDMA. 242 Nevertheless, it generally requires a very high UV intensity (e.g., 1000 mJ/cm²), a dosage of an order of magnitude higher than that used for UV disinfection.⁷⁷ Besides NDMA. 243 244 other micropollutants of concern include endocrine disruptors and pharmaceutically active compounds.⁸¹⁻⁸³. Recent issues in the Netherlands with discharge of 245 246 perfluorpolymers and pyrazole in surface water bodies challenged Dutch drinking water facilities. While perflourpolymer rejection by RO membranes is very high (>95%)⁸⁴, the 247 pyrazole rejection is low (approximately 35%)⁸⁵ depending on the type of RO membrane 248 249 resulting in the need of a post UV/peroxide treatment.

250

251 Due to their historical roots in desalination, commercial thin film composite polyamide 252 RO membranes have been highly optimized for salt rejection and water permeability, yet 253 they are often not adequate for the removal of micropollutants, particularly small polar 254 organic compounds. In recent years, researchers have started to realize the need for 255 designing membranes specifically for micropollutants removal. Tailoring membrane surface properties by surface coating/grafting show some promising results.⁸⁶⁻⁸⁹ For 256 257 instance, a hydrophilic polydopamine coating can effectively half the passage of hydrophobic EDCs through a polyamide membrane.⁸⁸ To reduce the adverse effect on 258 water permeability, materials of high selectivity to micropollutants are needed.⁹⁰ In this 259 260 regard, some of the novel desalting materials such as aquaporins and MOFs are of great 261 interest due to their highly defined pore structure and high specificity for water. Recent 262 studies on aquaporin-embedded polyamide membranes showed improved rejection rates to a wide range of micropollutants.^{91, 92} Graphene oxide sheets that are capable of
 forming highly hydrophilic water channels have also demonstrated great potential for
 micropollutants removal.⁹³⁻⁹⁵

266

267 • **BRIDGING THE GAP**

268 The challenge of implementing water reuse is not confined solely to the technical domain. 269 Public acceptance is a complex and thorny issue, one that has derailed a number of water reuse projects in the past.^{96, 97} A particular high profile case is that of Toowoomba in 270 271 Australia, where intense debate about a proposed indirect potable reuse scheme led to a referendum.⁹⁸ As the result of the referendum, in which 60% of the participants opposed 272 the scheme, it was abandoned.⁹⁸ Toowoomba has been seen as the trigger point for the 273 274 Oueensland government in Australia to abandon the Western Corridor Recycled Water project, which was completed in 2009 but has never been used as intended. The fallout 275 276 from Toowoomba underscores the need to fully understand the connection between 277 public perception about water reuse and technological innovation.

278

Public acceptance. Since Toowoomba, significant efforts often by collaborations between social scientists and engineers, and practitioners in the water sector have been made to positively influence public perception about water reuse. These efforts have resulted in better awareness by the public about the reliability and efficiency of membrane separation and other technologies used for water reclamation, and hence, a gradual shift in public acceptance and a growing number of successful water reuse schemes in recent years. For examples, the City of San Diego reported an increase in public support of potable water reuse from 26% in 2004 to 73% in 2012 after sustained
investment in research and public engagement activities.⁹⁶

288 The legitimacy of potable reuse. Recent socio-psychological studies have also added 289 considerable depth to our understanding of the complex interactions amongst factors that 290 can influence public acceptance of water reuse. Through an experiment with 1000 Australian correspondents, Dolnicar et al. 100 conclusively observed that providing 291 292 information about the treatment processes significantly increased public acceptance of 293 water reuse. Proactively working with the media is also an important component of 294 public engagement activities. Ormerod and Silvia analysed 158 newspaper articles about 295 potable water reuse in the Orange County Water District from 2000 to 2016 and did not 296 identify any negative coverage. While some of these articles were positive, the majority 297 was neutral and uncommitted about potable water reuse. These results echo previous findings from Hurlimann and Dolnicar 101 who observe concluded that the media 298 299 coverage of potable water reuse can often be characterized by lack of inclusion of views, 300 a low level of support statements with scientific evidence, a low level of impartiality, and 301 a high level of hedging language. The implicit uncertainty about the reported information 302 in newspaper coverage highlights the need for better engagement between key 303 stakeholders of potable water reuse and the.

304

305 Improving public knowledge alone may not be sufficient to change public perception. In 306 the context of water reuse, there is a pre-cognitive and irrational perception that prevents 307 many people from separating the final product (clean water) and its contaminated source 308 (human excreta).⁹⁶ This is despite the fact that no traces of the original contamination

309 exists and that no incident on human health due to water reuse has ever been reported 310 albeit the many intentionally and unintentionally (unplanned) potable water reuse 311 schemes that have been in operation, in some cases, for several decades. One effective 312 strategy to overcome the challenge of irrational public perception provide experiential 313 activities such as field visits, tasting opportunities, using reused water for public 314 swimming pools and water splash pads. As a notable example, strong public support to 315 water reuse in Singapore can be attributed, at least in part, to a very concerted and 316 systematic public engagement program that includes the attractive NEWater Visitor 317 Centre at the Bedok plant.⁷ The centre has effectively become a tourist attraction, where 318 the public can book a tour for free to learn about how Singapore copes with their water 319 supply problem and be given a bottle of NEWater (reused water) as souvenir or for 320 tasting.

321 Effort to garner public support to potable reuse has evolved beyond simple marketing 322 activities. Harris-Lovett et al., have recently proposed a framework based on societal 323 legitimacy for engaging the public on issues of potable water reuse. On the same vein, 324 Binz et al., point out that technological innovation is incongruous with established social 325 rules. Thus, given the perceived unprecedented nature of potable water reuse, it is often 326 confronted with strong skepticism and a lack of societal legitimacy. Harris-Lovett et al., 327 argued that establishing legitimacy for potable water reuse involves embedding RO, 328 advanced oxidation, and other new technologies in the shared social belief system, moral 329 standards and cultural conventions through a set of strategies that go beyond traditional 330 public relations and educational outreach.

331 **Public trust and technical reliability.** A key component of the legitimacy framework

332 proposed by Herris-Lovett et al., is reliable risk management procedures. A promising 333 strategy is to make key innovation in potable water reuse namely membrane separation 334 and other advanced technologies more understandable by relating to standards and 335 procedures that have already gained legitimacy in other established sectors. Online 336 monitoring is essential not only for establishing a safety record but also effective risk 337 management. Indeed, while acknowledging the central role of technology innovation, Lee 338 and Tan accredited Singapore's success in supplying NEWater for potable use to an 339 extensive data acquisition program to demonstrate the safety record of potable water 340 reuse. Prior to the NEWater, the Singapore Public Utility Board collected some 20,000 341 test results from different sampling locations in a demonstration plant, covering about 342 190 physical, chemical and microbiological parameters. The results were benchmarked 343 again the WHO and USEPA drinking water standards to demonstrate the credibility of 344 potable water reuse.

346 With a focus on public safety, real-time monitoring has been a crucial strategy for 347 assurance and risk management of potable water reuse. Real-time monitoring offers an 348 opportunity to engage with the public as well as quickly detect and rectify failure. Given 349 the central role of RO in potable water reuse, several highly sensitive sensors have been 350 developed to monitor chemical and microbial contaminants on a real-time or near 351 real-time basis for membrane integrity assurance. In addition to traditional surrogate 352 parameters such as conductivity, total organic carbon, and sulfate which can be readily 353 monitored online, several new surrogates specific to potable water reuse have been added 354 in recent years. They include UV254 or fluorescence for monitoring organic 355 micropollutants and multi-able light scattering or measurement of adenosine triphosphate 356 for monitoring microbial contaminants.

357 Of a particular note, Fujioka et al., have successfully developed an analytical technique 358 consisting of high-performance liquid chromatography followed by photochemical 359 reaction and chemiluminescence detection (HPLC PR-CL) for online monitoring of 360 N-nitrosodimethylamine (NDMA) and several other N-nitrosamines in secondary treated 361 effluent and RO permeate. The detection limit of their technique (0.3 - 2.7 ng/L) is 362 comparable to the regulated concentrations of these organic micropollutants in most 363 potable water reuse guidelines or standards. The HPLC PR-CL developed by Fujioka et 364 al., marks a significant milestone as this is the first time target organic micropollutants 365 can be monitored in near real-time. Further development in online monitoring of RO 366 performance can be expected and will help to bridge the gap between technology 367 innovation and public confidence in potable water reuse.

369 • AUTHOR INFORMATION

370 Corresponding Author

- 371 *Phone: (+852) 2859 1976; e-mail: tangc@hku.hk
- **372** Notes
- 373 The authors declare no completing financial interest.
- 374

375 • ACKNOWLEDGMENTS

- 376 The study receives financial support from the General Research Fund of the Research
- 377 Grants Council (Project # 17207514) of Hong Kong. The partial funding support from
- 378 Seed Fund for Strategic Interdisciplinary Research at the University of Hong Kong is also
- appreciated.

381 • References

Zektser, S.; Loáiciga, H. A.; Wolf, J. T., Environmental impacts of groundwater
 overdraft: selected case studies in the southwestern United States. *Environ. Geol.* 2005,
 47, (3), 396-404.

385 2. Orange County Water District (OCWD); Water Factory 21.
386 https://www.ocwd.com/media/2451/water-factory-21-brochure.pdf

- 387 3. Orange County Water District (OCWD); Groundwater Replenishment System
 388 (GWRS). https://www.ocwd.com/gwrs/
- 389 4. West Basin Municipal Water District; Edward C. Little Water Recycling Facility.
 390 <u>http://www.westbasin.org/water-supplies-recycled-water/facilities</u>
- 391 5. Metropolitan Water District of Southern California; Regional Recycled Water
 392 Program. <u>http://www.mwdh2o.com/DocSvcsPubs/rrwp/index.html#home</u>
- 3936. Water Replenishment District of Southern California (WRD); Groudwater Reliability394ImprovementProject(GRIP)
- 395 <u>http://www.wrd.org/content/groundwater-reliability-improvement-project-grip</u>
- 396 7. Public Utilities Board (PUB). <u>www.pub.gov.sg/</u>
- 8. Van Houtte, E., Verbauwhede, J., Long-time membrane experience at Torreele's
 water re-use facility in Belgium. *Desalination and Water Treatment* 2013, *51*, (22-24),
 4253-4262.
- 400 9. Kumar, M.; Grzelakowski, M.; Zilles, J.; Clark, M.; Meier, W., Highly permeable
 401 polymeric membranes based on the incorporation of the functional water channel protein
 402 Aquaporin Z. *Proc. Natl. Acad. Sci.* 2007, *104*, (52), 20719-20724.
- 403 10. Manawi, Y.; Kochkodan, V.; Hussein, M. A.; Khaleel, M. A.; Khraisheh, M.; Hilal,
 404 N., Can carbon-based nanomaterials revolutionize membrane fabrication for water
 405 treatment and desalination? *Desalination* 2016, *391*, 69-88.
- 406 11. Qiu, S.; Xue, M.; Zhu, G., Metal–organic framework membranes: from synthesis to 407 separation application. *Chem. Soc. Rev.* **2014**, *43*, (16), 6116-6140.
- 408 12. Splendiani, A.; Sun, L.; Zhang, Y.; Li, T.; Kim, J.; Chim, C.-Y.; Galli, G.; Wang, F., 409 Emerging photoluminescence in monolayer MoS2. *Nano lett.* **2010**, *10*, (4), 1271-1275.
- 410 13. Gerstandt, K.; Peinemann, K.-V.; Skilhagen, S. E.; Thorsen, T.; Holt, T., Membrane
 411 processes in energy supply for an osmotic power plant. *Desalination* 2008, *224*, (1-3),
 412 64-70.
- 413 14. Hinds, B. J.; Chopra, N.; Rantell, T.; Andrews, R.; Gavalas, V.; Bachas, L. G., 414 Aligned multiwalled carbon nanotube membranes. *Science* **2004**, *303*, (5654), 62-65.
- 415 15. Werber, J. R.; Osuji, C. O.; Elimelech, M., Materials for next-generation desalination 416 and water purification membranes. *Nat. Rev. Mater.* **2016**, *1*, 16018.
- 417 16. Jeong, B.-H.; Hoek, E. M.; Yan, Y.; Subramani, A.; Huang, X.; Hurwitz, G.; Ghosh,
- 418 A. K.; Jawor, A., Interfacial polymerization of thin film nanocomposites: a new concept
- 419 for reverse osmosis membranes. J. Membr. Sci. 2007, 294, (1), 1-7.
- 420 17. You, Y.; Sahajwalla, V.; Yoshimura, M.; Joshi, R. K., Graphene and graphene oxide
 421 for desalination. *Nanoscale* 2016, *8*, (1), 117-119.
- 422 18. Denny Jr, M. S.; Moreton, J. C.; Benz, L.; Cohen, S. M., Metal-organic frameworks
- 423 for membrane-based separations. *Nat. Rev. Mater.* **2016**, *1*, 16078.
- 424 19. Sun, L.; Huang, H.; Peng, X., Laminar MoS 2 membranes for molecule separation.
- 425 *Chem. Commun.* **2013**, *49*, (91), 10718-10720.

- 426 20. United Nations Department of Economic and Social Affaires 427 <u>http://www.un.org/waterforlifedecade/scarcity.shtml</u>
- 428 21. Drewes, J. E.; Reinhard, M.; Fox, P., Comparing microfiltration-reverse osmosis and
- soil-aquifer treatment for indirect potable reuse of water. *Water Research* 2003, 37, (15),
 3612.
- 431 22. Côté, P.; Masini, M.; Mourato, D., Comparison of membrane options for water reuse
- 432 and reclamation. *Desalination* **2004**, *167*, (1-3), 1-11.
- 433 23. Wintgens, T.; Melin, T.; Schäfer, A.; Khan, S.; Muston, M.; Bixio, D.; Thoeye, C.,
 434 The role of membrane processes in municipal wastewater reclamation and reuse.
 435 *Desalination* 2005, *178*, (1-3 SPEC. ISS.), 1-11.
- 436 24. Bennett, A., Potable water: New technology enables use of alternative water sources.
 437 *Filtration + Separation* 2011, *48*, (2), 24-27.
- 438 25. Fujioka, T.; Khan, S. J.; Poussade, Y.; Drewes, J. E.; Nghiem, L. D., N-nitrosamine
- 439 removal by reverse osmosis for indirect potable water reuse A critical review based on
- 440 observations from laboratory-, pilot- and full-scale studies. *Separation and Purification*
- 441 *Technology* **2012**, *98*, 503-515.
- 442 26. Lay, W. C. L.; Lim, C.; Lee, Y.; Kwok, B. H.; Tao, G.; Lee, K. S.; Chua, S. C.; Wah,
 443 Y. L.; Ghani, Y. A.; Seah, H., From R&D to application: Membrane bioreactor
- technology for water reclamation. *Water Practice and Technology* **2017**, *12*, (1), 12-24.
- 27. Qin, J.-J.; Kekre, K. A.; Tao, G.; Oo, M. H.; Wai, M. N.; Lee, T. C.; Viswanath, B.;
 Seah, H., New option of MBR-RO process for production of NEWater from domestic
 sewage. *Journal of Membrane Science* 2006, *272*, (1), 70-77.
- 448 28. Cath, T. Y.; Childress, A. E.; Elimelech, M., Forward osmosis: Principles, 449 applications, and recent developments. *Journal of Membrane Science* **2006**, *281*, (1-2), 450 70-87.
- 451 29. Shaffer, D. L.; Werber, J. R.; Jaramillo, H.; Lin, S.; Elimelech, M., Forward osmosis:
 452 Where are we now? *Desalination* 2015, *356*, 271-284.
- 453 30. Zhao, S.; Zou, L.; Tang, C. Y.; Mulcahy, D., Recent developments in forward 454 osmosis: Opportunities and challenges. *Journal of Membrane Science* **2012**, *396*, 1-21.
- 455 31. Lutchmiah, K.; Verliefde, A. R. D.; Roest, K.; Rietveld, L. C.; Cornelissen, E. R.,
- 456 Forward osmosis for application in wastewater treatment: A review. *Water Research* 2014,
 457 58, 179-197.
- 458 32. Li, X. M.; Chen, G.; Shon, H. K.; He, T., Treatment of high salinity waste water from
- shale gas exploitation by forward osmosis processes. In *Forward Osmosis: Fundamentals and Applications*, 2015; pp 339-362.
- 461 33. Phuntsho, S.; Shon, H. K.; Hong, S.; Lee, S.; Vigneswaran, S., A novel low energy
- 462 fertilizer driven forward osmosis desalination for direct fertigation: Evaluating the 463 performance of fertilizer draw solutions. *Journal of Membrane Science* **2011**, *375*, (1-2),
- 464 172-181.
- 465 34. Boo, C.; Elimelech, M.; Hong, S., Fouling control in a forward osmosis process
 466 integrating seawater desalination and wastewater reclamation. *Journal of Membrane*467 *Science* 2013, 444, 148-156.
- 468 35. Valladares Linares, R.; Li, Z.; Sarp, S.; Bucs, S.; Amy, G.; Vrouwenvelder, J. S.,
- 469 Forward osmosis niches in seawater desalination and wastewater reuse. *Water Research*470 2014, 66, 122-139.
- 471 36. Wessels, L. P.; Cornelissen, E. R. Operation and apparatus for treating waste water of

- a bioreactor in a membrane filtration unit (NL1028484). 8-3-2005, 2005.
- 473 37. Achilli, A.; Cath, T. Y.; Marchand, E. A.; Childress, A. E., The forward osmosis
 474 membrane bioreactor: A low fouling alternative to MBR processes. *Desalination* 2009,
 475 238, (1-3), 10-21.
- 476 38. Cornelissen, E. R.; Harmsen, D.; de Korte, K. F.; Ruiken, C. J.; Qin, J. J.; Oo, H.;
- 477 Wessels, L. P., Membrane fouling and process performance of forward osmosis 478 membranes on activated sludge. *Journal of Membrane Science* **2008**, *319*, (1-2), 158-168.
- 478 membranes on activated sludge. *Journal of Membrane Science* 2008, *319*, (1-2), 158-168.
 479 39. Alturki, A.; McDonald, J.; Khan, S. J.; Hai, F. I.; Price, W. E.; Nghiem, L. D.,
- 479 39. Alturki, A.; McDonald, J.; Khan, S. J.; Hai, F. I.; Price, W. E.; Nghiem, L. D., 480 Performance of a novel osmotic membrane bioreactor (OMBR) system: Flux stability and
- 481 removal of trace organics. *Bioresource Technology* **2012**, *113*, 201-206.
- 482 40. Wang, X.; Chang, V. W. C.; Tang, C. Y., Osmotic membrane bioreactor (OMBR) 483 technology for wastewater treatment and reclamation: Advances, challenges, and 484 prospects for the future. *Journal of Membrane Science* **2016**, *504*, 113-132.
- 485 41. Holloway, R. W.; Achilli, A.; Cath, T. Y., The osmotic membrane bioreactor: A 486 critical review. *Environmental Science: Water Research and Technology* **2015**, *1*, (5), 487 581-605.
- 488 42. Chen, L.; Gu, Y.; Cao, C.; Zhang, J.; Ng, J.-W.; Tang, C., Performance of a 489 submerged anaerobic membrane bioreactor with forward osmosis membrane for 490 low-strength wastewater treatment. *Water Research* **2014**, *50*, (0), 114-123.
- 491 43. Qin, J. J.; Kekre, K. A.; Oo, M. H.; Tao, G.; Lay, C. L.; Lew, C. H.; Cornelissen, E.
- R.; Ruiken, C. J., Preliminary study of osmotic membrane bioreactor: Effects of draw
 solution on water flux and air scouring on fouling. *Water Science and Technology* 2010,
 62, (6), 1353-1360.
- 495 44. Qiu, G.; Ting, Y. P., Osmotic membrane bioreactor for wastewater treatment and the 496 effect of salt accumulation on system performance and microbial community dynamics.
- 497 *Bioresource Technology* **2013**, *150*, 287-297.
- 498 45. Luo, W.; Xie, M.; Hai, F. I.; Price, W. E.; Nghiem, L. D., Biodegradation of cellulose
 499 triacetate and polyamide forward osmosis membranes in an activated sludge bioreactor:
 500 Observations and implications. *Journal of Membrane Science* 2016, *510*, 284-292.
- 501 46. Petersen, R. J., Composite reverse-osmosis and nanofiltration membranes. *Journal of* 502 *Membrane Science* **1993**, *83*, (1), 81-150.
- 503 47. Li, D.; Wang, H., Recent developments in reverse osmosis desalination membranes. 504 *J. Mater. Chem.* **2010**, *20*, (22), 4551-4566.
- 505 48. Tang, C. Y.; Kwon, Y.-N.; Leckie, J. O., Effect of membrane chemistry and coating 506 layer on physiochemical properties of thin film composite polyamide RO and NF
- 507 membranes II. Membrane physiochemical properties and their dependence on polyamide 508 and coating layers. *Desalination* **2009**, *242*, (1-3), 168-182.
- 509 49. Cohen-Tanugi, D.; McGovern, R. K.; Dave, S. H.; Lienhard, J. H.; Grossman, J. C.,
- 510 Quantifying the potential of ultra-permeable membranes for water desalination. *Energy & Environmental Science* **2014**, *7*, (3), 1134-1141.
- 512 50. Pendergast, M. M.; Hoek, E. M., A review of water treatment membrane 513 nanotechnologies. *Energy Environ Sci.* **2011**, *4*, (6), 1946-1971.
- 514 51. Yin, J.; Deng, B., Polymer-matrix nanocomposite membranes for water treatment. *J.* 515 *Membr. Sci.* **2015**, *479*, 256-275.
- 516 52. Lau, W.; Gray, S.; Matsuura, T.; Emadzadeh, D.; Chen, J. P.; Ismail, A., A review on
- 517 polyamide thin film nanocomposite (TFN) membranes: History, applications, challenges

- 518 and approaches. *Water Res.* **2015**, *80*, 306-324.
- 519 53. Gu, J. E.; Lee, S.; Stafford, C. M.; Lee, J. S.; Choi, W.; Kim, B. Y.; Baek, K. Y.; Chan,
- 520 E. P.; Chung, J. Y.; Bang, J.; Lee, J. H., Molecular layer-by-layer assembled thin-film 521 composite membranes for water desalination. *Adv. Mater.* **2013**, *25*, (34), 4778-82.
- 522 54. Karan, S.; Jiang, Z.; Livingston, A. G., Sub-10 nm polyamide nanofilms with
- 523 ultrafast solvent transport for molecular separation. Science 2015, 348, (6241),
- 524 1347-1351.
- 525 55. Barboiu, M.; Gilles, A., From natural to bioassisted and biomimetic artificial water 526 channel systems. *Acc. Chem. Res.* **2013**, *46*, (12), 2814-2823.
- 527 56. Das, R.; Ali, M. E.; Hamid, S. B. A.; Ramakrishna, S.; Chowdhury, Z. Z., Carbon 528 nanotube membranes for water purification: a bright future in water desalination. 529 *Desalination* **2014**, *336*, 97-109.
- 530 57. Cohen-Tanugi, D.; Grossman, J. C., Water desalination across nanoporous graphene. 531 *Nano Lett* **2012**, *12*, (7), 3602-8.
- 532 58. Ma, X.-H.; Yang, Z.; Yao, Z.-K.; Guo, H.; Xu, Z.-L.; Tang, C. Y., Interfacial
- 533 Polymerization with Electrosprayed Microdroplets: Toward Controllable and Ultrathin
- 534 Polyamide Membranes. Environmental Science & Technology Letters 2018, DOI:
 535 10.1021/acs.estlett.7b00566.
- 536 59. Yang, Z.; Ma, X.-H.; Tang, C. Y., Recent development of novel membranes for desalination. *Desalination* **2018**.
- 538 60. Tang, C.; Wang, Z.; Petrinić, I.; Fane, A. G.; Hélix-Nielsen, C., Biomimetic 539 aquaporin membranes coming of age. *Desalination* **2015**, *368*, 89-105.
- 540 61. Tang, C.; Zhao, Y.; Wang, R.; Hélix-Nielsen, C.; Fane, A., Desalination by
 541 biomimetic aquaporin membranes: Review of status and prospects. *Desalination* 2013,
 542 308, 34-40.
- 543 62. Shen, Y.-x.; Saboe, P. O.; Sines, I. T.; Erbakan, M.; Kumar, M., Biomimetic 544 membranes: A review. *J. Membr. Sci* **2014**, *454*, 359-381.
- 545 63. Sorribas, S.; Gorgojo, P.; Téllez, C.; Coronas, J.; Livingston, A. G., High flux thin 546 film nanocomposite membranes based on metal–organic frameworks for organic solvent
- 547 nanofiltration. J. Am. Chem. Soc. 2013, 135, (40), 15201-15208.
- 548 64. Liu, X.; Demir, N. K.; Wu, Z.; Li, K., Highly water-stable zirconium metal-organic
- framework UiO-66 membranes supported on alumina hollow fibers for desalination. J. *Am. Chem. Soc.* 2015, 137, (22), 6999-7002.
- 551 65. Hu, M.; Mi, B., Enabling graphene oxide nanosheets as water separation membranes. 552 *Environ. Sci. Technol.* **2013**, *47*, (8), 3715-3723.
- 553 66. Nair, R.; Wu, H.; Jayaram, P.; Grigorieva, I.; Geim, A., Unimpeded permeation of 554 water through helium-leak-tight graphene-based membranes. *Science* **2012**, *335*, (6067), 555 442-444.
- 556 67. Hegab, H. M.; Zou, L. D., Graphene oxide-assisted membranes: Fabrication and 557 potential applications in desalination and water purification. *J. Membr. Sci.* 2015, 484, 558 95-106.
- 559 68. Xu, G.-R.; Xu, J.-M.; Su, H.-C.; Liu, X.-Y.; Zhao, H.-L.; Feng, H.-J.; Das, R.,
- 560 Two-dimensional (2D) nanoporous membranes with sub-nanopores in reverse osmosis
- 561 desalination: Latest developments and future directions. *Desalination* **2017**.
- 562 69. Hirunpinyopas, W.; Prestat, E.; Worrall, S. D.; Haigh, S. J.; Dryfe, R. A.; Bissett, M.
- 563 A., Desalination and Nanofiltration through Functionalized Laminar MoS2 Membranes.

- 564 ACS Nano **2017**.
- 565 70. Lee, K. P.; Arnot, T. C.; Mattia, D., A review of reverse osmosis membrane materials 566 for desalination—development to date and future potential. J. Membr. Sci. 2011, 370, (1), 567 1-22.
- 568 71. Hu, Y.; Lu, K.; Yan, F.; Shi, Y.; Yu, P.; Yu, S.; Li, S.; Gao, C., Enhancing the 569 performance of aromatic polyamide reverse osmosis membrane by surface modification 570
- via covalent attachment of polyvinyl alcohol (PVA). J. Membr. Sci. 2015, 501, 209-219.
- 571 72. Kasemset, S.; Lee, A.; Miller, D. J.; Freeman, B. D.; Sharma, M. M., Effect of 572 polydopamine deposition conditions on fouling resistance, physical properties, and 573 permeation properties of reverse osmosis membranes in oil/water separation. J. Membr. 574 Sci. 2013, 425-426, 208-216.
- 575 73. Mi, Y.-F.; Zhao, Q.; Ji, Y.-L.; An, Q.-F.; Gao, C.-J., A novel route for surface 576 zwitterionic functionalization of polyamide nanofiltration membranes with improved 577 performance. J. Membr. Sci. 2015, 490, 311-320.
- 578 74. Yin, J.; Yang, Y.; Hu, Z.; Deng, B., Attachment of silver nanoparticles (AgNPs) onto 579 thin-film composite (TFC) membranes through covalent bonding to reduce membrane 580 biofouling. J. Membr. Sci. 2013, 441, (Supplement C), 73-82.
- 581 75. Ben-Sasson, M.; Lu, X.; Bar-Zeev, E.; Zodrow, K. R.; Nejati, S.; Qi, G.; Giannelis, E.
- 582 P.; Elimelech, M., In situ formation of silver nanoparticles on thin-film composite reverse 583 osmosis membranes for biofouling mitigation. Water Res. 2014, 62, 260-70.
- 584 76. Zhang, A.; Zhang, Y.; Pan, G.; Xu, J.; Yan, H.; Liu, Y., In situ formation of copper 585 nanoparticles in carboxylated chitosan layer: Preparation and characterization of surface 586 modified TFC membrane with protein fouling resistance and long-lasting antibacterial properties. Sep. Purif. Technol. 2017, 176, 164-172. 587
- 588 77. Mitch, W. A.; Sharp, J. O.; Trussell, R. R.; Valentine, R. L.; Alvarez-Cohen, L.; 589 Sedlak, D. L., N-Nitrosodimethylamine (NDMA) as a Drinking Water Contaminant: A 590 Review. Environmental Engineering Science 2003, 20, (5), 389-404.
- 591 78. State Water Resources Control of California Board 592 https://www.waterboards.ca.gov/drinking water/certlic/drinkingwater/NDMAhistory.sht 593 ml
- 594 79. Steinle-Darling, E.; Zedda, M.; Plumlee, M. H.; Ridgway, H. F.; Reinhard, M., 595 Evaluating the impacts of membrane type, coating, fouling, chemical properties and 596 water chemistry on reverse osmosis rejection of seven nitrosoalklyamines, including
- 597 NDMA. Water Research 2007, 41, (17), 3959.
- 598 80. Fujioka, T.; Khan, S. J.; McDonald, J. A.; Roux, A.; Poussade, Y.; Drewes, J. E.;
- 599 Nghiem, L. D., N-nitrosamine rejection by nanofiltration and reverse osmosis membranes: 600 The importance of membrane characteristics. *Desalination* **2013**, *316*, 67-75.
- 601 81. Levine, A. D.; Asano, T., Peer reviewed: recovering sustainable water from 602 wastewater. Environ. Sci. Technol. 2004, 38, (11), 201A-208A.
- 603 82. Schwarzenbach, R. P.; Escher, B. I.; Fenner, K.; Hofstetter, T. B.; Johnson, C. A.; Von
- 604 Gunten, U.; Wehrli, B., The challenge of micropollutants in aquatic systems. Science 605 2006, 313, (5790), 1072-1077.
- 83. Luo, Y.; Guo, W.; Ngo, H. H.; Nghiem, L. D.; Hai, F. I.; Zhang, J.; Liang, S.; Wang, 606
- 607 X. C., A review on the occurrence of micropollutants in the aquatic environment and their
- 608 fate and removal during wastewater treatment. Sci. Total Environ. 2014, 473, 619-641.
- 609 84. Loi-Brügger, A., Panglisch, S., Hoffmann, G., Buchta, P., Gimbel, R., Nacke, C.-J.,

- 610 Removal of trace organic substances from river bank filtrate Performance study of RO
- and NF membranes. *Water Science and Technology: Water Supply*, **2008**, *8*, (1), 85-92.
- 85. Bertelkamp, C.; Hijnen, W.; Siegers, W.; Hofman-Caris, R.; Leer, R. v. d. *Verwijdering van Pyrazool in drinkwaterzuiveringsprocessen, H2O*; 2016.
- 614 86. Kim, J.-H.; Park, P.-K.; Lee, C.-H.; Kwon, H.-H., Surface modification of
- 615 nanofiltration membranes to improve the removal of organic micro-pollutants (EDCs and 616 PhACs) in drinking water treatment: graft polymerization and cross-linking followed by
- 616 PhACs) in drinking water treatment: graft polymerization and cross-linking followed by 617 functional group substitution. *J. Membr. Sci.* **2008**, *321*, (2), 190-198.
- 618 87. Ben-David, A.; Bernstein, R.; Oren, Y.; Belfer, S.; Dosoretz, C.; Freger, V., Facile 619 surface modification of nanofiltration membranes to target the removal of 620 endocrine-disrupting compounds. *J. Membr. Sci.* **2010**, *357*, (1), 152-159.
- 621 88. Guo, H.; Deng, Y.; Tao, Z.; Yao, Z.; Wang, J.; Lin, C.; Zhang, T.; Zhu, B.; Tang, C. Y.,
- 622 Does Hydrophilic Polydopamine Coating Enhance Membrane Rejection of Hydrophobic
- 623 Endocrine-Disrupting Compounds? *Environmental Science & Technology Letters* **2016**, *3*, 624 (9), 332-338.
- 625 89. Guo, H.; Yao, Z.; Yang, Z.; Ma, X.; Wang, J.; Tang, C. Y., A one-step rapid assembly 626 of thin film coating using green coordination complexes for enhanced removal of trace 627 organic contaminants by membranes. *Environmental Science & Technology* **2017**, *51*,
- 628 (21), 12638-12643.
- 90. Park, H. B.; Kamcev, J.; Robeson, L. M.; Elimelech, M.; Freeman, B. D.,
 Maximizing the right stuff: The trade-off between membrane permeability and selectivity. *Science* 2017, *356*, (6343), eaab0530.
- 632 91. Madsen, H. T.; Bajraktari, N.; Hélix-Nielsen, C.; Van der Bruggen, B.; Søgaard, E.
- 633 G., Use of biomimetic forward osmosis membrane for trace organics removal. *J. Membr.* 634 *Sci.* **2015**, *476*, 469-474.
- 635 92. Xie, M.; Luo, W.; Guo, H.; Nghiem, L. D.; Tang, C. Y.; Gray, S. R., Trace organic
 636 contaminant rejection by aquaporin forward osmosis membrane: Transport mechanisms
 637 and membrane stability. *Water Res.* 2017.
- 638 93. Zhang, Y.; Zhang, S.; Chung, T.-S., Nanometric graphene oxide framework
 639 membranes with enhanced heavy metal removal via nanofiltration. *Environ. Sci. Technol.*640 2015, 49, (16), 10235-10242.
- 641 94. Jiang, Y.; Wang, W.-N.; Liu, D.; Nie, Y.; Li, W.; Wu, J.; Zhang, F.; Biswas, P.; Fortner,
- 642 J. D., Engineered crumpled graphene oxide nanocomposite membrane assemblies for
- 643 advanced water treatment processes. *Environ. Sci. Technol.* **2015**, *49*, (11), 6846-6854.
- 644 95. Oh, Y.; Armstrong, D. L.; Finnerty, C.; Zheng, S.; Hu, M.; Torrents, A.; Mi, B., 645 Understanding the pH-responsive behavior of graphene oxide membrane in removing 646 ions and organic micropollulants. *J. Membr. Sci.* **2017**, *541*, 235-243.
- 647 96. Smith, H. M.; Brouwer, S.; Jeffrey, P.; Frijns, J., Public responses to water reuse –
- 648 Understanding the evidence. *Journal of Environmental Management* **2018**, *207*, 43-50.
- 649 97. Kelly S. Fielding, S. D. a. T. S., Public acceptance of recycled water: state-of-the-art 650 review. *International Journal of Water Resources Development* in press.
- 651 98. Hurlimann, A.; Dolnicar, S., When public opposition defeats alternative water 652 projects - The case of Toowoomba Australia. *Water Research* **2010**, *44*, (1), 287-297.
- 653 99. Hartley, T. W., Public perception and participation in water reuse. *Desalination* **2006**, 654 *187*, (1-3), 115-126.
- 655 100. Dolnicar, S.; Hurlimann, A.; Nghiem, L. D., The effect of information on public

- acceptance The case of water from alternative sources. *Journal of Environmental Management* 2010, 91, (6), 1288-1293.
- Hurlimann, A.; Dolnicar, S., Newspaper coverage of water issues in Australia. *Water Research* 2012, *46*, (19), 6497-6507.
- 660 102. Dolnicar, S.; Hurlimann, A.; Grün, B., What affects public acceptance of
- recycled and desalinated water? *Water Research* **2011**, *45*, (2), 933-943.

664 • TOC

