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1 **Selective carbon sources and salinities enhance enzymes and extracellular polymeric**
2 **substances extrusion of *Chlorella* sp. for potential co-metabolism**

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15

16 **Abstract**

17 This study investigated the extracellular polymeric substance (EPS) and enzyme extrusion of
18 *Chlorella* sp. using seven carbon sources and two salinities for potential pollutant co-
19 metabolism. Results indicated that the levels of biomass, EPS and enzymes of microalgae
20 cultured with glucose and saccharose outcompeted other carbon sources. For pigment
21 production, glycine received the highest chlorophyll and carotene, up to 10 mg/L. The EPS
22 reached 30 mg/L, having doubled the amount of protein than carbohydrate. For superoxide
23 dismutase and peroxidase enzymes, the highest concentrations were beyond 60 U/ml and 6
24 nmol/d.ml, respectively. This amount could be potentially used for degrading 40%
25 ciprofloxacin of concentration 2000 µg/L. When increasing salinity from 0.1% to 3.5%, the
26 concentrations of pigment, EPS and enzymes rose 3 to 30 times. These results highlighted

27 that certain carbon sources and salinities could induce *Chlorella* sp. to produce EPS and
28 enzymes for pollutant co-metabolism and also for revenue-raising potential.

29 Keywords: *Chlorella* sp., extracellular polymeric substance, superoxide dismutase,
30 peroxidase, co-metabolism.

31 1. Introduction

32 Microalgae can remediate various types of pollutants including nutrients, organic compounds,
33 heavy metals and micropollutants which differ greatly from concentration, characteristic to
34 toxicity level (Chan et al., 2014; Vadlamani et al., 2019). Microalgae use the pollutants as
35 primary substrates for cell growth and trigger enzymes production, so-called the metabolism.
36 However, most organic pollutants present in wastewater at minor concentration (e.g.
37 antibiotic, pesticide). For example, acetaminophen presents in sewage system and water
38 reservoir of many countries from 20 to 100 µg/L (Phong Vo et al., 2019). They are unable to
39 be used as sole carbon source since the obtained metabolic energy from micropollutants is
40 insufficient to microorganism's demand. Therefore, the co-metabolism for removing
41 pollutant is necessary. Cometabolism is the transformation of a non-growth substrate (e.g.,
42 organic pollutants) primed by microalgae using a growth substrate or another biodegradable
43 compound (e.g., glucose, saccharose, acetate). Microalgae can extrude extracellular
44 polymeric substances (EPS) and several types of enzymes to the culturing environment (Lv et
45 al., 2019). Positively, those EPS and enzymes catalysed the pollutant co-metabolism of
46 microalgae. Thus, microalgae can degrade long-chain organic pollutants in a more efficient
47 manner. Example enzymes are superoxide dismutase (SOD) and peroxidase (POX). The SOD
48 (EC 1.15.1.1) catalyses the dismutation (or partitioning) of the superoxide (O_2^-) radical into
49 either ordinary molecular oxygen (O_2) or hydrogen peroxide (H_2O_2). POX (EC 1.11.1.x) is a

50 large group of enzymes that can catalyse the reaction of H_2O_2 and organic compounds by
51 using them as electron donor and acceptor (Eq. 1 and 2), so-called the co-metabolism.

52 $2\text{HO}_2 \rightarrow \text{O}_2 + \text{H}_2\text{O}_2$ (Eq. 1)

53 $\text{ROOR}' + 2\text{e}^- + 2\text{H}^+ \xrightarrow{\text{Peroxidase}} \text{ROH} + \text{R}'\text{OH}$ (Eq. 2)

54 In practice, wastewater in the treatment plant contained various organic pollutants and carbon
55 sources. For instance, atrazine, carbamazepine, diclofenac, sulfamethoxazole are among
56 hundreds of micropollutants are detected in wastewater treatment plant (Luo et al., 2014).
57 The wastewater is discharged from domestic, pharmaceutical, alcoholic, cassava, sugar
58 refinery industries which possess high nutrient level of methanol, ethanol, acetate and sugar
59 carbon sources (Bhattacharya et al., 2017). In the latest investigations, several researchers
60 have studied the effects of different feeding carbon sources on microalgae (Lin and Wu,
61 2015; Zhang et al., 2014). Their experimented carbon sources were glucose, saccharose,
62 acetate and sodium bicarbonate (Moon et al., 2013; Tu et al., 2018; Vergnes et al., 2019;
63 Wang et al., 2016). Some important carbon sources are not fully explored, such as methanol,
64 ethanol and glycine. Also, those studies focus on the impact of carbon sources on protein,
65 carbohydrate and lipid yield in microalgae cells, but not the pollutant co-metabolism (Yew et
66 al., 2019). It is known widely the growth and pigment production of microalgae are
67 determined strongly by the type of feeding carbon source. However, still little is known with
68 insightful elaboration on the biochemical effect of the carbon source towards the pollutant co-
69 metabolism of microalgae. This is useful and applicable for using microalgae towards organic
70 pollutants cometabolism and nutrient recovery in wastewater treatment plant and industry
71 discharge. Another factor influencing microalgae is salinity. By entering microalgae cells,
72 substantial amounts of sodium and chloride ions of high salinity alter the biochemical
73 function of microalgae and interfere the remediation process (Pérez et al., 2016). Through

74 literature, only limited studies have explored the effect of different carbon sources between
75 fresh water (salinity 0.1%) and sea water (salinity 3.5%), towards pollutant co-metabolism.
76 Therefore, it was hypothesized that salinity and type of carbon source potentially alter the
77 EPS and enzyme concentration extruded by microalgae and influence the pollutant co-
78 metabolism efficiency. To address the identified gaps, this study investigated the effect of
79 different carbon sources on microalgae cultured in salinities 0.1% and 3.5%, with a focus on
80 EPS and enzymes extrusion for potential pollutant co-metabolism. Up to our knowledge, this
81 study was the first one encountered insightfully the impacts of various carbon sources and
82 salinities on the pollutant co-metabolism of microalgae.

83 In the previous work, the *Chlorella* sp. has demonstrated that it could adapt better to the
84 salinities from 0.1 to 3% than other strains (i.e., *Stichococcus* sp. and *Chlorella vulgaris*) (Vo
85 et al., 2019). In detail, the *Chlorella* sp. can accumulate 60-80% TOC while the *Stichococcus*
86 sp. only hands on less than 60%. The elemental analysis demonstrates that the C percentage
87 in the *Chlorella* sp. and cells reaches to 20%; on the other hand, the values of *Chlorella*
88 *vulgaris* and *Stichococcus* sp. stay at 9 to 15%. Hence, in this work, *Chlorella* sp. was
89 experimented in the mixotrophic condition using six organic carbon sources (i.e., methanol,
90 ethanol, glucose, saccharose, glycine, acetate) and photoautotrophic one with inorganic
91 sodium bicarbonate. Apart from the biomass and pigment, the bound and soluble EPS, SOD
92 and POX in the two selected salinities were analysed to evaluate the cometabolism potential.
93 In addition, the advanced technology such as Scanning Electron Microscope (SEM) was used
94 to explore the effect of salinity on microalgae. By clarifying those, *Chlorella* sp. would be
95 better characterised for sustainable applications in industrial wastewater to recover nutrients
96 and to increase the pollutant co-metabolism process.

97 2. Materials and methods

98 2.1 Microalgae and wastewater

99 The *Chlorella* sp. (CS-436) stock was supplied by the National Algae Supply Service
100 (Tasmania, Australia). The stock was cultured in cyanobacterial growth media MLA
101 (AusAqua, Australia) at $20 \pm 1^\circ\text{C}$ and 4.35 ± 0.03 klux. The cultured microalgae was
102 illuminated by a LED light bulb (11 W, 220–240 V) (Philip, Australia). The illumination
103 intensity was measured by a light meter, model QM1584 (Digitech, Australia). The
104 microalgae stock was renewed per fortnight.

105 This study used artificial wastewater for experiment which was spiked with selective carbon
106 sources. Seven carbon sources were employed separately to prepare seven wastewater types
107 including: methanol (CH_3OH), ethanol ($\text{C}_2\text{H}_5\text{OH}$), saccharose ($\text{C}_{12}\text{H}_{22}\text{O}_{11}$), glucose
108 ($\text{C}_6\text{H}_{12}\text{O}_6$), sodium acetate (CH_3COONa), glycine ($\text{C}_2\text{H}_5\text{NO}_2$), and sodium bicarbonate
109 (NaHCO_3). The MLA media was also spiked in the wastewater at dosing as advised from the
110 supplier. It served as background for microalgae growth since the MLA media contained vital
111 elements (e.g., Mg^{2+} , Mn^{2+} , Cu^{2+} , Zn^{2+}). The nitrogen and phosphorus sources were from
112 NaNO_3 and KH_2PO_4 , respectively. The concentrations of total carbon (TC), NO_3^- -N and
113 PO_4^{3-} -P were fixed at 300, 30 and 5 mg/L, respectively. The concentration of carbon, nitrogen
114 and phosphorus was studied and optimized in the previous work and also to maximize the
115 nutrient recovery capacity of microalgae (Vo et al., 2019). The spiked trace vitamins were
116 supplied by AusAqua Company (Australia) and the applied dose of trace vitamins followed
117 the supplier's instructions. All the chemicals were purchased from Merck (Australia) to
118 ensure the analytical grade quality.

119 2.2 Experimental design

120 Eight sealed glass bottles (1 L each) were used as the experimental photobioreactors. Seven
121 photobioreactors contained one type of carbon source each as previously described. One
122 photobioreactor served as the control, feeding MLA media only. The initial microalgae
123 concentration cultured in the photobioreactor was retained at 50 mg/L. The illumination
124 intensity and temperature for those photobioreactors were similar to the stock solution.
125 Following this the cultured solutions were gently mixed at 50 rpm. The experimental period
126 lasted for 10 d. Biomass concentration of microalgae was measured every 2 d. Other
127 parameters including pigment, EPS, enzymes and efficiencies in removing pollutants, were
128 checked on day 10th.

129 2.2.1 Biomass yield analysis

130 The biomass yield of microalgae was obtained by measuring the cell density at 680 nm using
131 a spectrophotometer (DR1900, Hach). Then, the value of cell density was converted to the
132 biomass yield by Eq (3):

$$133 \quad y = (x - 0.0222)/0.0021 \quad (R^2=0.95) \quad (\text{Eq. 3})$$

134 Where:

135 x : cell density

136 y : biomass yield (mg/L)

137 2.2.2 Chlorophyll and carotene analysis

138 The pigment (chlorophyll and carotene) was analysed according to methods used in the
139 previous studies (Vo et al., 2019; Xiong et al., 2017a). In brief, a 10 ml sample was
140 centrifuged at 9000 rpm for 10 min. The supernatant was disposed and the pellet was
141 suspended in 10 ml of 90% acetone. The sample was sonicated in 5 min at 4°C and incubated

142 in 24 h in darkness. It was re-centrifuged at 4°C, 4000 rpm for 15 min. The supernatant was
143 checked at various wavelengths with a spectrophotometer. The chlorophyll and carotenoid
144 concentrations were calculated as follows:

$$145 \text{ Chlorophyll (mg/L)} = 11.64*(A_{663}-A_{750}) - 2.16*(A_{647} - A_{750}) + 0.1*(A_{630} - A_{750}) \text{ (Eq. 4)}$$

$$146 \text{ Carotene (mg/L)} = (1000 A_{470} + 243.1*A_{661} - 1267.1*A_{645})/214 \text{ (Eq. 5)}$$

147 Where

148 A_{λ} : cell density at wavelength λ (nm).

149 2.2.3 Extracellular polymeric substances

150 The EPS extraction procedure was modified from Deng et al. (2016). Firstly, a 30 mL sample
151 was collected and then centrifuged at 3000 rpm for 30 min. The supernatant was re-
152 centrifuged at 3000 rpm for another 30 min and filtered through a 0.45 μm Phenex-NY
153 (Nylon) syringe filter to receive soluble EPS. The pellets in the centrifuge tube were
154 suspended in phosphorus buffer solution to 30 mL, and mixed with cation exchange resin for
155 2 h at 900 rpm. By filtering the resin and liquid through a 1.2 μm Phenex-GF (Glass fiber)
156 syringe filter, the bound EPS was retained. Both the soluble and bound EPS were analysed
157 for protein and polysaccharide using the modified Lowry method (Sigma, Australia) and
158 Anthrone-sulphuric acid method, respectively (Deng et al., 2016).

159 2.2.4 Superoxide dismutase and peroxidase enzymes

160 The SOD and POX activity was analyzed by using enzyme test kits (Sigma-Aldrich,
161 Australia). At first, a 20 ml sample was collected and centrifuged at 4500 rpm for 15 min at
162 4°C. The cellular pellet and supernatant were utilised for the enzymatic activity assay in cells
163 and culturing environment, respectively. The SOD and POX analysis was conducted

164 according to the manufacturer's instructions. One SOD unit was defined as the amount of
165 enzyme exhibiting 50% dismutation of the superoxide radical. The unit U/ml (nmol/min.ml)
166 served to measure SOD activity while the unit nmol/d.ml was applied for POX activity.

167 2.2.5 Total carbon, nitrate and phosphate analysis

168 The total carbon (TC) level was analysed by Multi N/C 3100 (Analytikjena, Germany). The
169 NO_3^- -N and PO_4^{3-} -P concentrations were measured by the test kits, coded 114942 and
170 100798 of Merck (Australia), respectively. The Photometer Nova 60 (Merck, Australia) was
171 employed for NO_3^- -N and PO_4^{3-} -P analysis.

172 2.2.6 Scanning electron microscope

173 The surface morphology of microalgae cells were analysed using SEM (Zeiss Supra 55VP,
174 Carl Zeiss AG). The microalgae samples were filtered by glass fiber filter paper GF/C
175 (Whatman, Australia), dehydrated for 24 h at 105 °C, and coated by Au/Pd. The SEM was
176 operated at 10 kV as accelerating voltage and multiple magnifications. The SEM was used to
177 explore the effect of salinity on microalgae.

178 2.3 Model analysis of biomass yield

179 To understand the effect of different carbon sources and salinities on biomass yield, the
180 Gompertz model (Eq. 6) was applied to describe the biomass growth. Data were retrieved
181 from experimental measurement described in section 2.3.1.

$$182 \quad y = a.e^{-\exp(-k(x - x_c))} \quad (\text{Eq. 6})$$

183 Where, y is the estimated biomass yield (mg/L), a is the maximum biomass yield (mg/L), k is
184 the biomass yield per day (mg/L.d), x is the cultured time (d), x_c is the lag time of biomass
185 yield (d). The a, k and x_c values are kinetic parameters and can be achieved using Origin 8.0
186 software.

187 2.4 Statistic analysis

188 The analysis of variance (ANOVA) was used for statistical purposes. Specifically, the
189 repeated measures of ANOVA examined the difference of biomass yield which was
190 influenced by salinities and carbon sources, according to the cultured time. For other
191 parameters, the factorial ANOVA was applied to investigate the difference of pigment, EPS,
192 enzymes and pollutants removal efficiencies impacted by salinities and carbon sources. All
193 the data were presented as mean value \pm standard deviation (Mean \pm SD) with duplicated
194 samples.

195 3. Results and discussion

196 3.1 Biomass yields feeding by different carbon sources and salinities

197 Both organic and inorganic carbon sources and salinity can affect the growth of *Chlorella* sp.
198 (Vo et al., 2019). The *Chlorella* sp. was cultured in seven types of carbon sources using two
199 salinities: fresh water (0.1%) and sea water (3.5%). As shown in Fig. 1, biomass
200 concentrations feeding with different carbon sources and salinities were significantly
201 different ($p < 0.01$). For salinity 0.1%, the glucose and saccharose yielded the highest biomass
202 reaching beyond 600 mg/L at day 10. Other carbon sources, namely ethanol, glycine, sodium
203 acetate and sodium bicarbonate achieved smaller amounts (400 - 500 mg/L). The methanol
204 emerged the least effective carbon source for biomass growth, which was not significantly
205 different to the control, around 100 mg/L ($p > 0.01$). Its biomass concentration was five-fold
206 less than those cultured in glucose and saccharose.

207 For salinity 3.5%, the biomass yield decreased by 200 mg/L for most carbon sources
208 compared to salinity 0.1%. Only the sodium acetate carbon maintained a comparable biomass
209 yield between 400 and 500 mg/L in both salinities. Similar to salinity 0.1%, both glucose and
210 saccharose presented the highest biomass yield in salinity 3.5% (400 - 500 mg/L). The

211 methanol and the control samples possessed the lowest biomass level, less than 100 mg/L.
212 Other carbon sources received biomass from 250 to 400 mg/L.

213 [Insert Fig. 1]

214 To elaborate the impact of carbon sources and salinities on biomass yield, the Gompertz
215 model was applied to validate the results of experimental parts. In this model, the three
216 kinetic parameters, including maximum biomass yield (a), biomass growth rate (k) and lag
217 time of biomass yield (x_c), were calculated. Overall, most of the models well-fitted the
218 experimental data, confirming by high R^2 values. The biomass growth rates of glucose and
219 saccharose surpassed five-fold other carbon sources. Furthermore, in salinity 3.5%, the
220 biomass growth rate reduced 20 – 30% than in salinity 0.1%. This coincided the results of
221 experimental data. It can be seen that biomass feeding by glucose and saccharose reached
222 stationary phase at day 4. Other carbon sources likely performed stationary phase since day
223 10 of the cultured period in salinity 0.1%, but not in salinity 3.5%.

224 The effects of carbon sources such as glucose, saccharose, sodium acetate and sodium
225 bicarbonate to microalgae's biomass have been studied by several researchers (Lin and Wu,
226 2015; Vo et al., 2019; Zhang et al., 2014). These particular organic carbon sources were
227 implemented in mixotrophic mode and the sodium bicarbonate was examined in
228 photoautotrophic mode. However, the effects of methanol, ethanol and glycine were not
229 investigated adequately. In this study, the biomass yields were higher than those of other
230 studies. Several technical conditions could explain this discrepancy but the most important
231 one was due to the experimented microalgae strain. The *Chlorella* sp., a highly productive
232 strain of this work, could adapt to both fresh water and sea water environments. In the
233 previous study, *Chlorella* sp. could well tolerate salinity from 0.1 to 3.5% (Vo et al., 2019).
234 For instance, the received biomass yield was 600 to 800 mg/L and the sugar-based carbon

235 sources of others achieved biomass from 350 to 450 mg/L (Moon et al., 2013; Zhang et al.,
236 2014). In details, the *Chlorella* sp. Y8-1 and *Botryococcus braunii* were fed carbon levels
237 from 500 to 12000 mg/L, that 2 to 40 times higher than in our experiment (i.e., 300 mg/L).
238 Another evidence was the *Chlamydomonas reinhardtii*. Although a comparable biomass
239 concentration (i.e., 400 mg/L) to our results has been achieved, the feeding acetate
240 concentration (i.e., 1 – 10 g/L) was 3 to 30 times higher than ours (Moon et al., 2013). This
241 further emphasised the distinct characteristics of *Chlorella* sp. For methanol, ethanol and
242 glycine carbon sources, the literature is limited for making an adequate comparison.
243 Technically, the alcohol carbon sources required microalgae more time to adapt and grow
244 (Choi et al., 2011). For example, Choi et al. (2011) cultured *Chlorella* sp. in 1% methanol
245 and eventually obtained 4.2 g biomass/L after 45 d. It can be seen from Fig. 1 that, at salinity
246 3.5%, most biomass growth curves still happened on log phase after 10 d. In practice,
247 culturing for 45 d is time-consuming and potentially reduces revenue. In contrast, *Chlorella*
248 sp. feeding ethanol and glycine carbon sources herein could grow to 250-500 mg/L within 10
249 d under both salinities. This is very comparable to the sugar-based feedstocks used in other
250 studies (Moon et al., 2013; Zhang et al., 2011; Zhang et al., 2014).

251 3.2 Pigment production under different carbon sources and salinities

252 While consuming carbon sources and necessary nutrients, *Chlorella* sp. can produce pigment
253 such as chlorophyll and carotene. High chlorophyll and carotene levels demonstrate the
254 adaptation and growth of microalgae to the culturing environment (Singh et al., 2018). The
255 concentration of chlorophyll and carotene associated to the seven carbon sources and two
256 salinities were different significantly ($p < 0.01$) (Fig. 2).

257 The chlorophyll production of this microalgae strain ranged from 0.3 to 5 mg/L for all carbon
258 sources and salinities after 10 d. At salinity 0.1%, *Chlorella* sp. generated chlorophyll below

259 0.5 mg/L, the exception being glycine. The *Chlorella* sp. feeding glycine produced 4.1 mg
260 chlorophyll/L, which was 10 times more than other carbon sources. However, *Chlorella* sp.
261 performed differently in salinity 3.5%. Most carbon sources could generate chlorophyll 3 to
262 30 times more than salinity 0.1%. The *Chlorella* sp. culturing by ethanol, saccharose, glucose
263 and sodium acetate yielded chlorophyll from 2 to 5 mg/L. The saccharose one achieved
264 around 5 mg/L as the highest chlorophyll concentration. The exception was also glycine that
265 its chlorophyll level in salinity 0.1% tripled the amount in salinity 3.5%. Only the methanol
266 and bicarbonate-feeding microalgae performed insignificant change in both salinities. The
267 chlorophyll concentration of microalgae culturing in those carbon sources received less than
268 0.3 mg/L.

269 The *Chlorella* sp. yielded carotene from 0.1 to 1.5 mg/L, which was three times less than the
270 corresponding amount of chlorophyll. In salinity 0.1%, most carbon sources achieved low
271 carotene concentration, less than 0.5 mg/L, apart from glycine. In turn, at salinity 3.5%, the
272 level of carotene increased 10-fold to 1.5 mg/L, typically for the saccharose and glucose
273 carbon sources. Other carbon sources still created the carotene level below 0.5 mg/L which
274 was not significantly different from the control unit. However, *Chlorella* sp. feeding glycine
275 was again exceptional because it generated more carotene in salinity 0.1% than salinity 3.5%.
276 It can be seen that glycine was the most effective carbon source for chlorophyll and carotene
277 production. In turn, methanol and bicarbonate achieved the least pigment content. The reason
278 was elaborated in Section 3.6. In short, the photoautotrophic mode exhibited less pigment
279 production at least 10 times than the mixotrophic one.

280

[Insert Fig. 2]

281 3.3 Extracellular polymeric substances production

282 The EPS are excreted by *Chlorella* sp. to the culturing environments when they consume
283 carbon sources. They consist mostly soluble/bound protein and polysaccharide. By adding
284 different carbon sources, this impacts on the EPS extrusion of *Chlorella* sp. as shown in Fig.
285 3. For salinity 0.1%, the produced EPS differed significantly amongst carbon sources
286 ($p < 0.01$); nevertheless, the level of EPS was always below 15 mg/L. The ethanol and glycine
287 ones possessed the highest EPS concentrations, ca. 13 mg/L. The follow-up carbon sources
288 included glucose, saccharose and bicarbonate, producing around 10 mg EPS/L. Other carbon
289 sources produced less than 6 mg EPS/L. Of the EPS's components, protein concentration
290 dominated at least double the amount of polysaccharide. For example, the glycine-induced
291 protein concentration exceeded the polysaccharide concentration eight-fold. However, for the
292 saccharose and glucose carbon sources, the levels of protein and polysaccharide were close.
293 Regarding the bound and soluble forms, their concentrations were almost equal, both for
294 protein and polysaccharide.

295 Of the salinity 3.5%, *Chlorella* sp. produced excessive EPS than in salinity 0.1%. Particularly
296 for the saccharose, glucose, glycine and sodium bicarbonate, EPS value doubled the one in
297 salinity 0.1%. The amount of protein in salinity 3.5% also doubled in salinity 0.1%, while the
298 level of polysaccharide was similar. It implied that increasing salinity would enhance protein
299 production of microalgae. The largest increase in the EPS component related to the bound
300 protein. The glycine carbon source facilitated *Chlorella* sp. producing the highest EPS of 31
301 mg/L. The saccharose, glucose and sodium bicarbonate generated 20 mg EPS/L; the others
302 produced below 10 mg EPS/L. It can be seen each carbon source influenced EPS generation
303 in different ways. Unlike protein, polysaccharide was produced at a lower level at either
304 salinities. The concentration of carbohydrate did not exceed 10 mg/L in most cases and
305 preferably stayed below 5 mg/L. In salinity 0.1%, there was no significant difference between

306 the bound and soluble carbohydrate concentration. However, in salinity 3.5%, the bound
307 carbohydrate increased significantly than the soluble one, especially of the saccharose,
308 glucose, glycine and bicarbonate carbon sources.

309 [Insert Fig. 3]

310 3.4 Superoxide dismutase and peroxidase production

311 As *Chlorella* sp. was stressed by carbon sources and salinities, it started producing a number
312 of enzymes such as SOD and POX in both cells and the culturing environment. Those
313 enzymes alleviated the stress of biotic and abiotic factors and also functioned the biochemical
314 processes in microalgae. The levels of SOD and POX were affected by both carbon sources
315 and salinities as illustrated in Fig. 4. Overall, for most cases, the SOD level in microalgae
316 cells was two to three times higher than in the culturing environments. The *Chlorella* sp.
317 extruded SOD below 20 U/ml to the culturing environments while it generated 30 to 60 U/ml
318 in the cells. For all carbon sources, glucose recorded the highest value (60 U/ml) in the
319 culturing environment. Comparing the two salinities, microalgae extruded SOD to the
320 culturing liquid in salinity 3.5% double in salinity 0.1%. Nevertheless, SOD concentrations in
321 cells of microalgae were comparable in the two salinities. For instance, in the microalgae
322 cells the SOD values mostly varied from 50 to 60 U/ml.

323 POX activity in *Chlorella* sp. for most carbon sources and salinities ranged from 1 to 2
324 nmol/d.ml, which is comparable to the control samples, except for glucose and saccharose in
325 salinity 0.1%. Those produced POX in microalgae cells from 5 to 6 nmol/d.ml which was
326 double the POX activity of other carbon sources. The increase of POX in sugar carbon
327 sources rooted from the POX activity in microalgae cell. It indicated that the sugar carbon
328 sources affected the biochemical and metabolic pathways of microalgae more significantly
329 than other carbon sources. Further discussion was given in section 3.6. On the other hand,

330 other carbon sources received a consistent POX concentration in both cell and culturing
331 environment, around 1 nmol/d.ml. There was no distinct discrepancy between the two
332 salinity. In salinity 3.5%, the saccharose and glucose carbon sources received lower POX
333 concentration than in salinity 0.1%. Their POX concentration was comparable to other carbon
334 sources.

335 [Insert Fig. 4]

336 3.5 Nutrient removal influenced by different carbon sources and salinities

337 Carbon, nitrogen and phosphorus are nutritious elements and promote the growth of
338 *Chlorella* sp., and furthermore produce pigment, EPS and enzymes. As shown in Fig. 5, those
339 compounds reduced significantly after 10 d. The total carbon decreased 30 to 90%. Methanol,
340 ethanol and sodium bicarbonate carbon sources were used below 50%. The saccharose,
341 glucose and acetate ones were removed from 70 to 90%. For glycine, it was a particular case
342 given *Chlorella* sp. removed 91% in salinity 0.1% and 55% in salinity 3.5%. This result was
343 closely linked to the larger amount of chlorophyll and carotene produced in salinity 0.1%
344 when compared to salinity 3.5%. Total carbon removal of methanol in salinity 3.5% also
345 surpassed 50% in salinity 0.1%.

346 The nitrogen removal efficiencies varied from 70 to 99%, which were superior to the carbon
347 removal efficiencies. In salinity 0.1%, the nitrogen was removed from 85 to 89% for all
348 carbon sources. In salinity 3.5%, these values ranged more widely from 70 to 99%. The
349 glucose and saccharose carbon sources exhibited the highest nitrogen consumption (99%)
350 which were 20% better than others. For phosphorus, *Chlorella* sp. consumed 65 to 75% in
351 salinity 0.1%. In turn, in salinity 3.5%, it fluctuated from 30 to 75% given that the
352 phosphorus removal efficiency of the corresponding carbon sources impaired two times than

353 in salinity 0.1%. Nonetheless, the glucose and saccharose carbon sources did not follow this
354 trend as the phosphorus removal efficiencies persisted at 70%.

355 [Insert Fig. 5]

356 3.6 Effects of carbon sources and metabolic pathways on *Chlorella* sp.

357 The interesting question in this research was how and to what degree the carbon sources
358 impacted on *Chlorella* sp., since the biomass, pigment, EPS and enzyme levels related to
359 those carbon sources were different (Fig. 1-4). There were two possible explanations and they
360 originated from the chemical structure of carbon sources and the responses of microalgae.
361 Firstly, it was known that those carbon sources possessed different energy content. For
362 instance, glucose comprised more energy in its chemical structure and could produce 2.8 kJ
363 energy/mol compared to 0.8 kJ/mol of acetate (Perez-Garcia et al., 2011). In addition,
364 saccharose could create 4.2 kJ/mol. Therefore, glucose and saccharose resulted in the highest
365 biomass yield being produced. In contrast, the alcohol-based carbon sources, methanol and
366 ethanol, containing a low energy outputs of 0.1 kJ/mol and 0.5 kJ/mol, respectively, could
367 also toxify microalgae more severely than the sugar-based and inorganic carbon sources
368 (Cardol et al., 2011). Such facts are consistent with their low biomass yield (Fig. 1).

369 Secondly, regarding microalgae, those carbon sources were consumed by different metabolic
370 pathways. For instance, microalgae transformed glucose through the hexose/H⁺ symport
371 system, then glucose was converted by the Embden–Meyerhof Pathway (EMP) and entered
372 the tricarboxylic acid (TCA) cycle for ATP production. Of the saccharose, microalgae
373 consumed it via two possible pathways: direct accumulation by specific carriers or
374 degradation by particular enzymes, such as sucrase, to monomers including glucose and
375 fructose (Wang et al., 2016). The monosaccharides are subsequently uptaken via the EMP
376 and TCA cycle. The EMP was an ATP economical pathway since the cells only invested one

377 ATP molecule per sugar molecule for transportation (Perez-Garcia et al., 2011). By using less
378 ATP pools, cells could yield more pigment, EPS and enzyme products for co-metabolism.
379 Microalgae also transform the supplied glucose into stored energy efficiently in the
380 phosphoanhydride bonds of ATP (12%). This explained the highest biomass, pigment, EPS
381 and enzyme levels of microalgae feeding by saccharose and glucose.

382 Of the sodium acetate, it is transported by the monocarboxylic/proton of monocarboxylic
383 molecules in the cell membrane. Inside the cells, sodium acetate is assimilated for the
384 acetylation of coenzyme A to form acetyl coenzyme A and participated in the Glyoxylate
385 Cycle. Unlike glucose, acetate encountered in the Glyoxylate Cycle, principally for lipid
386 production prior to entering the TCA cycle. This reduces the amount of acetate available for
387 biomass production. Previously, Bouarab et al. (2004) reported that glucose donates 38 moles
388 ATP and acetate donates 12 moles for microalgae growth, indicating glucose outcompeted
389 acetate for cell build-up. This explains the biomass and products of microalgae feeding by
390 acetate are lower than glucose and saccharose.

391 Glycine is the simplest amino acid which contains amino group (-NH₂). This makes glycine a
392 unique carbon source in this study. Glycine would be involved in the transcript encoding and
393 form a precursor of chlorophyll and carotene (Cecchin et al., 2018). By adding glycine, the
394 activity of uroporphyrinogen-III synthase, coproporphyrinogen III oxidase and magnesium
395 chelatase enzymes upregulated and resulted in the increase of chlorophyll level. This
396 confirms that by feeding glycine directly in salinity 0.1%, the *Chlorella* sp. generated more
397 chlorophyll than microalgae cultured in other carbon sources. For carotene, the carotenoid
398 biosynthetic pathway performed differently as a carotenoid oxygenase decreased in the
399 mixotrophic condition (Cecchin et al., 2018). This finding was in contrary to the one of this
400 study. However, Cecchin et al. (2018) insisted that the function of carotenoid oxygenase

401 remained unclear. In addition, the experimented microalgae strains were a case by case basis
402 (i.e., *Chlorella* sp. and *Chlorella sorokiniana*).

403 In comparison, the mechanism of methanol and ethanol accumulation were still unclear. It
404 was speculated that microalgae tend to avoid consuming them due to high toxicity of alcohols
405 as a self-defence mechanism. Consequently, the total carbon removal efficiencies of
406 methanol and ethanol were consistently poor. Also, microalgae compensate ATP energy in
407 order to repair the damage caused by alcoholic carbon sources, which accounts for 45–82%
408 of the total ATP produced (Yang et al., 2000). This explained the low products yield of
409 *Chlorella* sp. when fed by alcohol carbon sources.

410 Regarding inorganic carbon, it is common knowledge that inorganic carbon operated under
411 photoautotrophic mode resulted in less productivity than the organic carbon under
412 mixotrophic mode (Yeh and Chang, 2012). The Calvin cycle in the autotrophic mode
413 consumes 70% of the ATP stock in the cells and subsequently produces 3.11 g biomass/mmol
414 ATP, rather than 19.3 g biomass/mmol ATP of the heterotrophic and mixotrophic conditions
415 (Yang et al., 2000). By the transcript encoding, in the mixotrophic condition, 285 transcripts
416 encoding of 259 different proteins shifted, while, in the autotrophic one, 721 transcripts
417 corresponding to 620 proteins diminished. Those transcript encoding exhibited the
418 metabolisms of photosynthesis, chlorophyll, carotenoid, photorespiratory pathway,
419 carbohydrates, fatty acids and amino acids metabolism, sulphur, nitrogen, phosphate
420 assimilation (Cecchin et al., 2018). Thus, the inorganic carbon-feeding microalgae yield
421 biomass and other products less than most organic carbon sources (Fig. 1-4).

422 3.7 Effects of salinities on *Chlorella* sp.

423 Salinity is able to influence the behaviour of *Chlorella* sp. by altering biomass concentration,
424 pigment, EPS, enzyme concentrations and pollutants removal efficiencies (Fig. 1-4). The

425 mechanisms and reasons for these changes can be elaborated as follows. Firstly, increasing
426 salinity causes stress in microalgae cells with surplus sodium and chloride ions penetrating
427 into the cells. It will induce the hydroxyl radical groups substantially and interfere the PSI,
428 PSII and other metabolic pathways of *Chlorella* sp. (Vo et al., 2019). To alleviate the stress,
429 *Chlorella* sp. respond in several ways. For example, to balance the osmotic regulation,
430 microalgae accumulate compounds such as soluble carbohydrates to tolerate salinity. Sugars
431 reduce the stress conditions and trigger the functions of osmoprotection, osmotic adjustment,
432 carbon storage, and radical scavenging (Khosh Kholgh Sima et al., 2012). Also, microalgae
433 yield more chlorophyll and carotene. Those pigments are antioxidant compounds and they
434 can cope the stress conditions. Microalgae concurrently produce more enzymes and EPS in
435 the cells, extruding to the culturing environment in order to neutralise the hydroxyl radical
436 groups. Thus, it was observed that concentration of SOD enzyme and EPS was shifted to the
437 higher level in salinity 3.5% (Fig. 3 and 4). However, less phosphorus was consumed in high
438 salinity due to the decline in H_2PO_4^- activity (Khosh Kholgh Sima et al., 2012). By saving
439 material pool to produce more EPS and enzymes, the biomass in higher salinity reduced
440 accordingly. The phosphorus consumption of sugar-feeding microalgae (i.e., glucose and
441 saccharose) in salinity 3.5% were still comparable to the one in salinity 0.1%. As explained,
442 the sugar-based carbon sources could alleviate the salinity stress to microalgae better than
443 other carbon sources; possibly, they consume phosphorus in the same manner in both
444 salinities.

445 For salt stress, as previously mentioned, twice the amount of protein in EPS was produced
446 compared to the carbohydrate. The reason for this could be due to the particular *Chlorella* sp.
447 strain. For instance, Xiao and Zheng (2016) reported the protein level extruded by microalgae
448 would vary case by case. In their review, the green microalgae produced protein from 0.5 to
449 10 mg/L, which was significantly less than the *Chlorella* sp. in this study (10-30 mg/L).

450 Regarding enzyme, similarly, Singh et al. (2018) found that *Chlorococcum humicola* and
451 *Chlorella vulgaris* augmented 55% SOD enzyme activity in salinity 3.5%. This outcome
452 agreed with our findings that SOD concentration rose with salinity for most cases (Fig. 4).
453 Regarding the POX enzyme, its activities were stable in most carbon sources and salinities,
454 except for saccharose and glucose. POX depended less on carbon sources and salinities, and
455 was low compared to SOD. The reason was still inconclusive but it was interpreted that the
456 POX-producing system within microalgae was less developed than that of SOD and it reacted
457 insignificantly against salinity. The POX system was more sophisticated in plants rather than
458 microalgae. For example, Soltani Nezhad and Mansouri (2019) found that POX in the plant
459 *Robinia pseudoacacia* increased to 40 U/mg at salinity 4M. Very few studies have reported
460 POX produced by microalgae so far.

461 In salinity 3.5%, although microalgae extruded more EPS and enzyme, it did not imply that
462 the pollutants were removed in a better manner. It might get worse. For example, salinity
463 diminished the $H_2PO_4^-$ activity and reduced phosphorus accumulation efficiency of
464 microalgae as previously mentioned (Khosh Kholgh Sima et al., 2012). Another evidence
465 was organic pollutants. In salinity 1%, the *Scenedesmus obliquus* removed 93.4%
466 levofloxacin of concentration 1 mg/L (Xiong et al., 2017b). Increasing salinity to 3% and 5%
467 impaired the levofloxacin removal efficiency to below 10%. However, the *Scenedesmus*
468 *obliquus* only removed 4% and 80% at salinity 0% and 0.3%, respectively, that less than the
469 value in salinity 1%. This indicated each strain preferred a particular salinity. Choosing an
470 appropriate salinity range for microalgae was critical as excessive salinity could face several
471 challenges. One of the problem was salt layer forming on microalgae cells which captured by
472 the SEM. This layer could hinder the pollutant assimilation process and reverse pollutant to
473 culturing environment. Apart from the salt layer, EPS could deposit on microalgae cell as

474 well. The thickness of EPS layer ranged up to 4 μm which further impaired the pollutant
475 assimilation (Vergnes et al., 2019).

476 3.8 Implications for green pollutant co-metabolism process

477 Overall, the results of this study delivered a basis for further research and practical
478 applications. Industries such as molasses, vinegar, pharmaceuticals, aquaculture and cattle
479 discharge large amounts of wastewater into sewerage systems. Such waste streams contain
480 sufficient carbon sources (i.e., sugar, acetate, alcohol) for microalgae cultivation
481 (Bhattacharya et al., 2017). According to our results, wastewater containing glucose and
482 saccharose would receive the highest amount of removed pollutants, EPS and enzyme levels.
483 Hence, nutrients and valuable pigments such as chlorophyll and carotene could be recovered,
484 up to 10 mg/L. It indicated a sustainable revenue-raising potential. Also, enzymes and EPS in
485 the cultured effluent encountered significant amounts of organic pollutants as a co-
486 metabolism process (Bilal et al., 2019; Ufarté et al., 2015). After harvesting microalgae, the
487 cultured effluent could be reused for removing organic pollutants. Containing up to 30 mg
488 EPS/L, the cultured effluent possessed strong antioxidant properties and could catalyse the
489 degradation of pesticides, plastics and antibiotics (Xiao et al., 2019; Xiong et al., 2017a).
490 Several studies have reported the feasibility of EPS in the cometabolism of organic
491 pollutants, such as 2-chloro-N-(2,6-diethylphenyl)-N-(methoxymethyl) acetamide, toluene
492 and trichloroethylene (Ahmad, 2020; Yang et al., 2019). Apart from the organic pollutants,
493 EPS could absorb heavy metals, such as Cr (VI) (Johnson et al., 2020). By binding the heavy
494 metal in the EPS, cells exposed less to heavy metal and, consequently, it reduced toxicity
495 causing to the cells. It increased the biodegradation of organic pollutants. This conditions the
496 cometabolism of mg 1,4-Dioxane/L up to 100%. Based on the sustainable criteria, the
497 application of cultured liquid for pollutant co-metabolism was proposed as following (Fig. 6):

498

[Insert Fig. 6]

499 EPS from microalgae has been applied to agricultural crops to alleviate salt stress (Arroussi et
500 al., 2018). The EPS-incubated crops increased their protein levels by 31.5% compared to
501 non-incubated ones. In addition, the SOD and POX levels decreased by 30%, thus indicating
502 salt stress was less severe when implementing EPS-incubation. Apart from glucose and
503 saccharose, glycine yields significant amounts of chlorophyll, carotene and EPS. Also,
504 acetate can increase the carotene yield in salinity 3.5% (1.5 mg/L). In addition, the sodium
505 acetate could stimulate microalgae degrading ciprofloxacin three times higher to 40%, using
506 initial ciprofloxacin 2000 $\mu\text{g/L}$ and those microalgae produced enzyme level similarly to our
507 result (Xiong et al., 2017a). The algae-producing industry can reuse wastewater containing
508 glycine for mass production purposes. Glycine and acetate are part of the amine-rich
509 wastewater that is released from the degradation of amine-based adsorbents (Dong et al.,
510 2019). By culturing microalgae in amine-rich wastewater, the wastewater is detoxified,
511 nutrients are recovered and pigments are harvested. It can be seen that this work has solved to
512 the two major issues for microalgae-based sustainability: gaining revenue and remediating
513 pollutant by co-metabolism.

514 In practice, this work implied potential improvement. Bacteria in wastewater might compete
515 with microalgae and consume nutrients at the same time. Knowing how to harmonize and
516 combine microalgae and bacteria when using those carbon sources was important. For
517 example, purple bacterium was a prominent candidate because it functioned as a notable
518 pollutant remover in saline wastewater (Hülßen et al., 2019). Another issue was that sugar-
519 based carbon sources likely favoured microalgae rather than any others. However, in
520 wastewater, various carbon sources co-existed and it was anticipated that the competition
521 amongst carbon sources might occur. This is a problem that needs to be addressed.

522 4. Conclusion

523 Overall, the effects of seven carbon sources under two salinities on the cultivation of
524 *Chlorella* sp. were comprehensively studied. The sugar-based carbon sources achieved the
525 highest EPS and enzymes concentration. The produced EPS mainly comprised protein rather
526 than carbohydrate. When assessing the influence of salinity, EPS and enzymes concentrations
527 in salinity 3.5% rose by 3 to 30 times. The increasing EPS and enzymes concentration
528 suggested that the EPS and enzyme increased co-metabolism for degrading pollutants. In
529 EPS, there would be a number of enzyme types involved in the cometabolism which required
530 further address.

531 E-supplementary data of this work can be found in online version of the paper.

532

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659

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660 Figure captions

661 Fig. 1. Biomass concentrations of *Chlorella* sp. feeding with different carbon sources under
662 two salinities, fitted Gompertz model. The symbols demonstrate experimental measurements
663 and dash lines demonstrate model fit. All measures showed significant differences ($p < 0.01$)
664 amongst carbon sources and between the two salinities.

665 Fig. 2. Chlorophyll (A) and carotene (B) of *Chlorella* sp. at day 10th feeding with different
666 carbon sources under two salinities. All measures showed significant differences ($p < 0.01$)
667 amongst carbon sources and between the two salinities

668 Fig. 3. EPS of *Chlorella* sp. at day 10th feeding with different carbon sources under two
669 salinities. All measures showed significant differences ($p < 0.01$) amongst carbon sources and
670 between the two salinities.

671 Fig. 4. SOD (top) and POX (bottom) concentration of *Chlorella* sp. at day 10th feeding with
672 different carbon sources. All measures of SOD showed significant differences ($p < 0.01$)
673 between the two salinities. The POX concentration of the two salinities were insignificant
674 difference ($p > 0.01$).

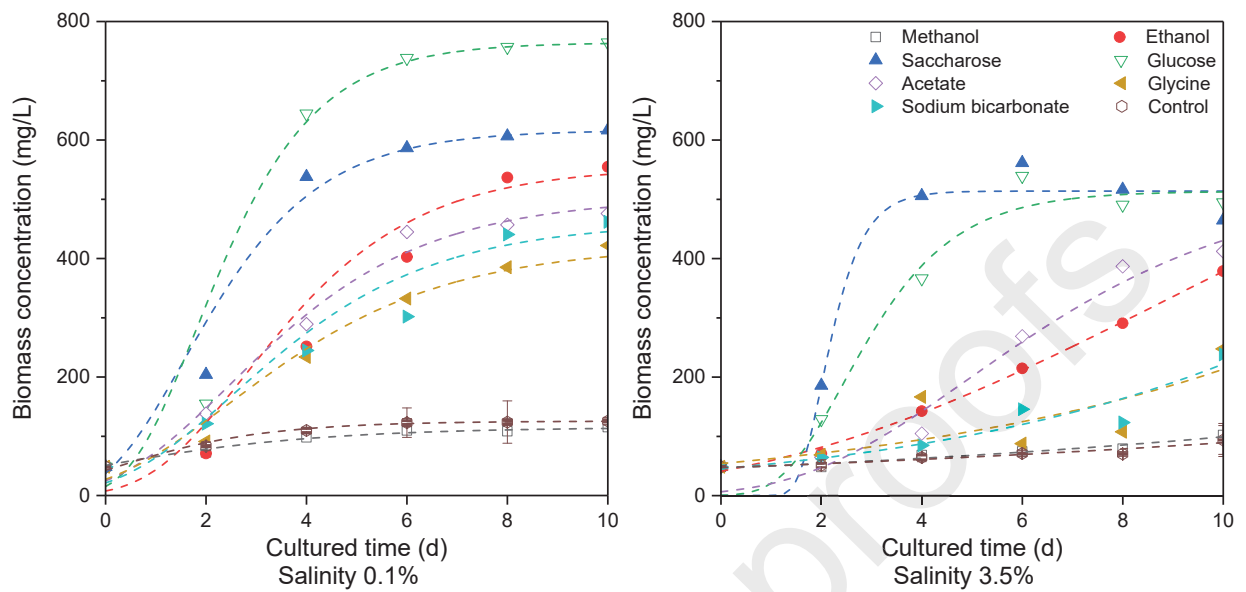
675 Fig. 5. Total carbon, nitrate and phosphate removal efficiencies of *Chlorella* sp. at day 10th
676 feeding with different carbon sources under two salinities. All measures showed significant
677 differences ($p < 0.01$) amongst phosphorus removal between the two salinities. The removal
678 efficiencies of total carbon and nitrate were insignificant difference ($p > 0.01$).

679 Fig. 6. Proposed application of culturing liquid for pollutant co-metabolism.

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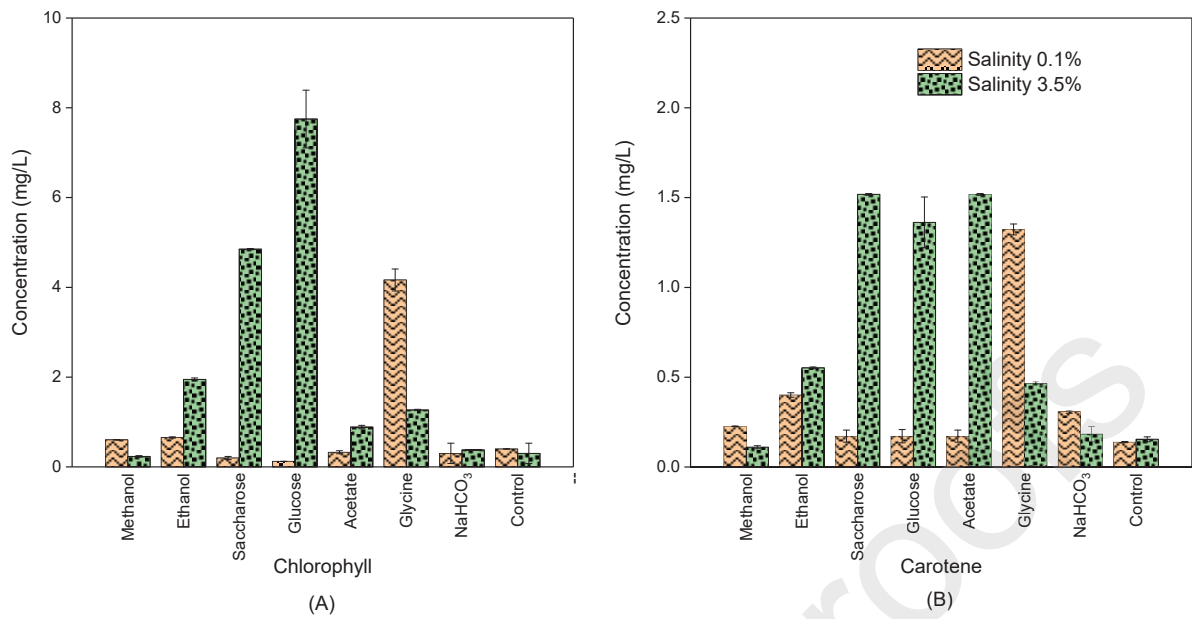
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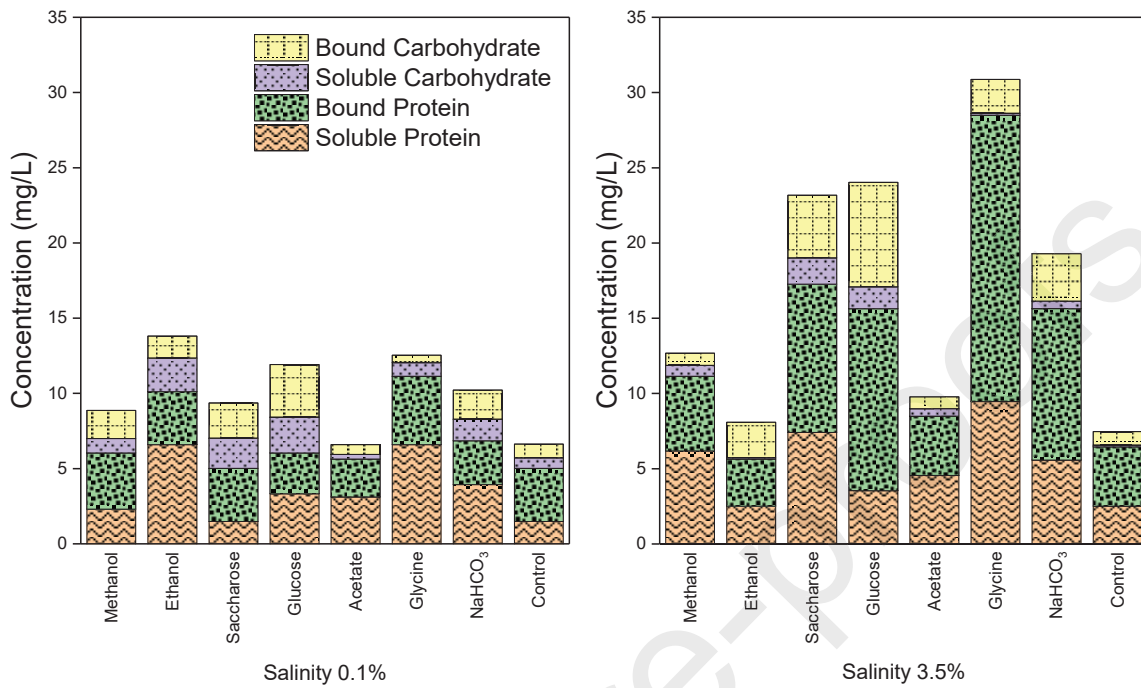
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Fig. 3. EPS of *Chlorella* sp. at day 10th feeding with different carbon sources under two

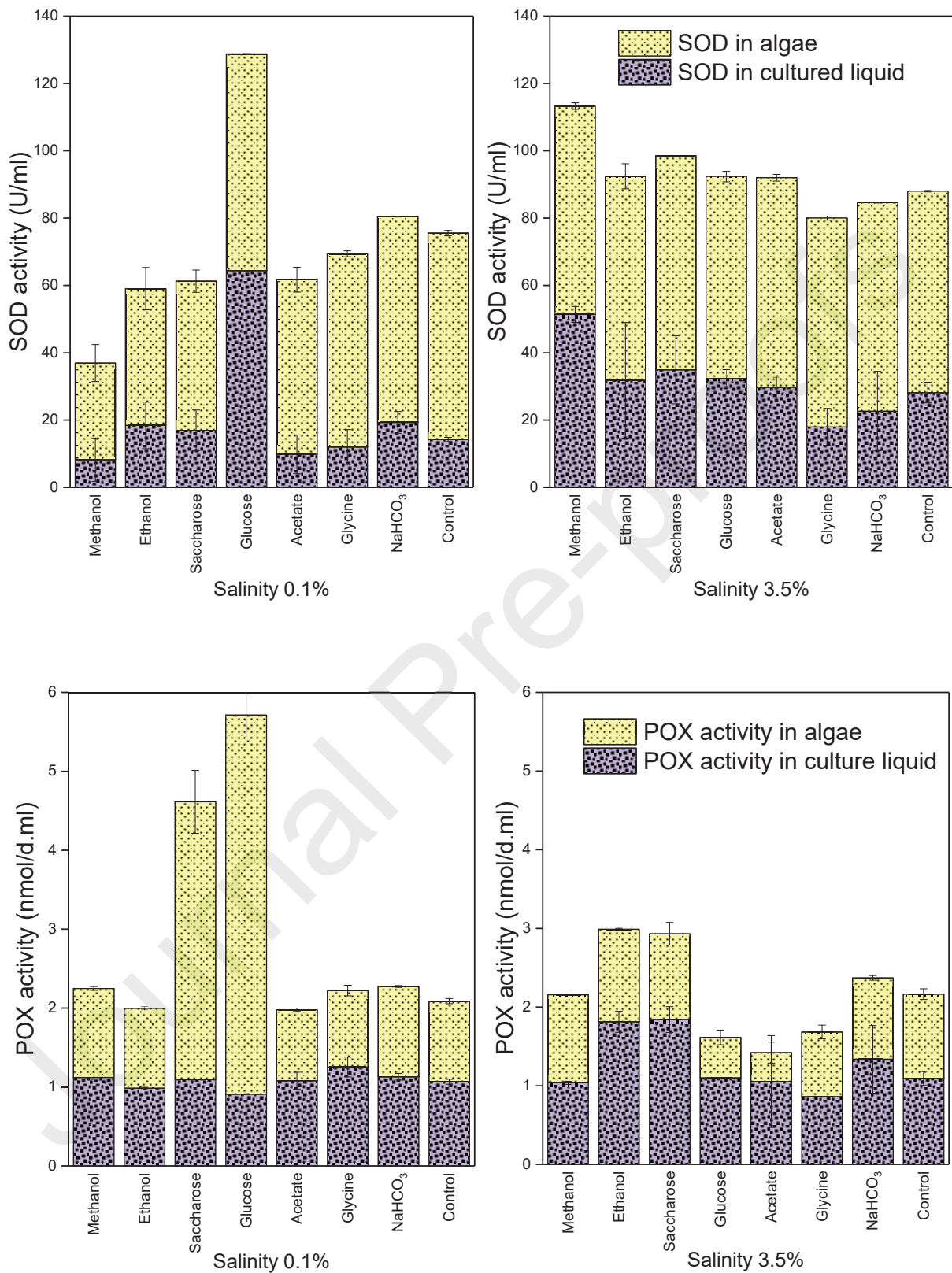
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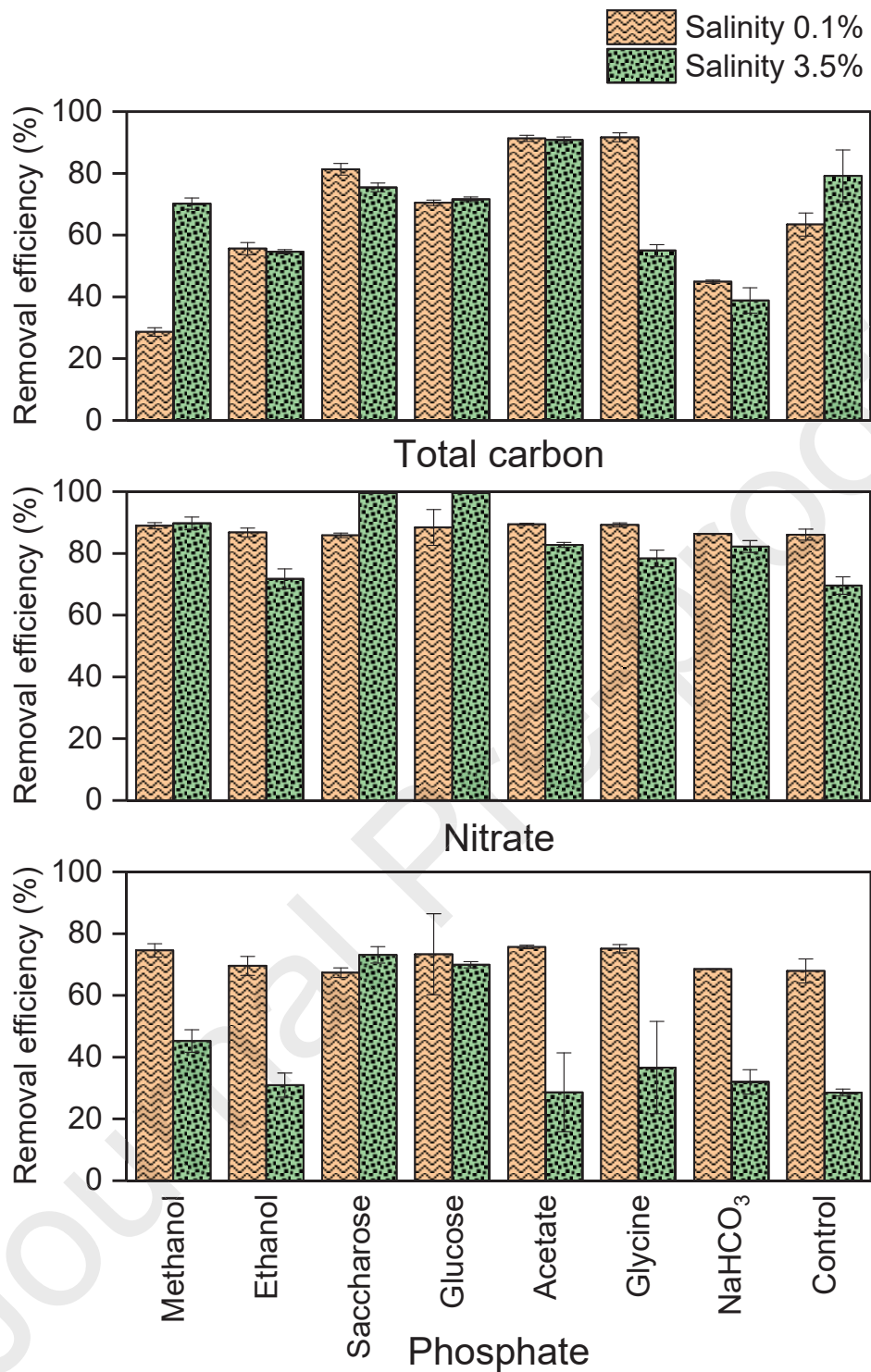
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702 Fig. 4. SOD (top) and POX (bottom) concentration of *Chlorella* sp. at day 10th feeding with703 different carbon sources. All measures of SOD showed significant differences ($p < 0.01$)

704 between the two salinities. The POX concentration of the two salinities were insignificant
705 difference ($p>0.01$).

Journal Pre-proofs



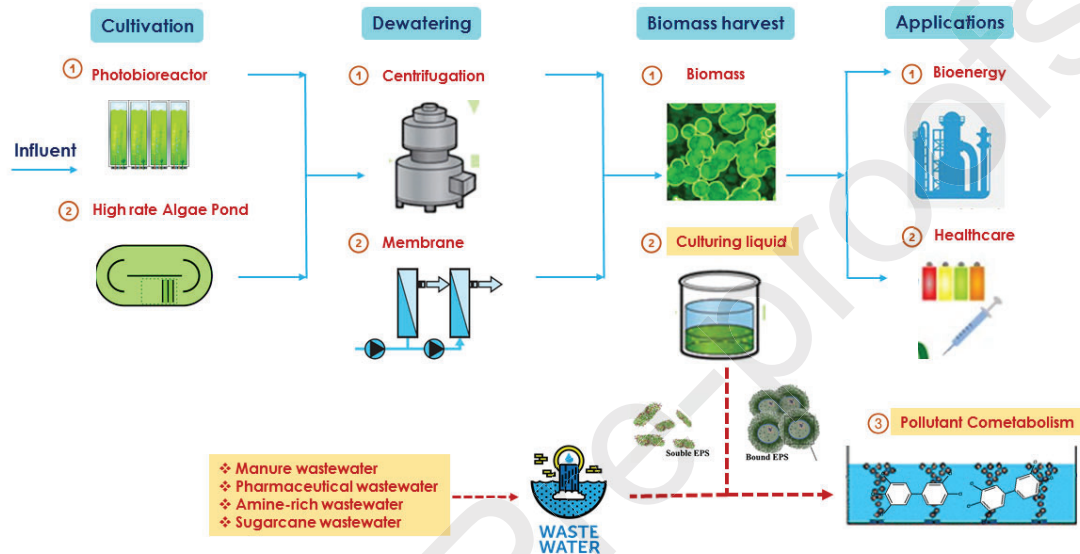
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707 Fig. 5. Total carbon, nitrate and phosphate removal efficiencies of *Chlorella* sp. at day 10th
 708 feeding with different carbon sources under two salinities. All measures showed significant

709 differences ($p < 0.01$) amongst phosphorus removal between the two salinities. The removal
 710 efficiencies of total carbon and nitrate were insignificant difference ($p > 0.01$).

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714 Fig. 6. Proposed application of culturing liquid for pollutant co-metabolism.

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Author Contribution Statement

Hoang Nhat Phong Vo: investigation, writing - original draft, methodology, formal analysis, data curation

Huu Hao Ngo: supervision, investigation, project administration, conceptualization, review & editing

Wenshan Guo: supervision, investigation, review & editing

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