

Design, Modelling and Experimental Evaluation of Energy Recovery Indirect Evaporative Cooling System

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Thesis submitted in fulfilment of the requirements for the degree of

Doctor of Philosophy

under the supervision of Associate Professor Dr. Guang Hong And Dr. Lee "Mickey" Clemon

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CERTIFICATE OF ORIGINAL AUTHORSHIP

I, Ahmed Y Taha Al-Zubaydi declare that this thesis is submitted in fulfilment of the

requirements for the award of Doctor of philosophy, in the Mechanical engineering at the

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Abstract

Design, Modelling and Experimental Evaluation of Energy Recovery Indirect Evaporative Cooling System

Heating, ventilating and air conditioning systems (HVAC) are essential for providing a comfortable and healthy indoor environment for human beings and required conditions for manufacturing and operations in industrial sectors. Maximizing energy efficiency and minimizing the environmental impact of HVAC systems has become more and more important to address the issues of sustainability and environmental protection. With the recent climate warming, the demand for air conditioning is expected to hit a new high. The dilemma of high demand while simultaneously reducing energy consumption requires a full-scale campaign to develop new technologies for HVAC systems.

Recovering wasted energy is one way to reduce the energy consumption in HVAC systems. In a modern building, the energy lost through ventilation can be more than 50% of the total thermal losses. In this study, two advanced technologies were investigated, the air-to-air heat recovery ventilation (HRV) and the indirect evaporative cooler (IEC). The energy wasted by the exhaust air was recovered by pre-cooling the supply air as the heat was transfer from the fresh air to the exhaust air in an HVAC system.

A test rig was designed, manufactured, modified and calibrated to meet the special aims of this research. It is a cost-effective and inventive test facility with the flexibility to be used for both dry (HRV) and wet (IEC) operation modes.

The experimental study of the HRV was conducted by testing two polymer heat exchangers with two different plate geometries, one with a flat plate and the other with a

dimpled surface plate. The key aims were to understand the effect of the surface geometry of the plates on the performance of the air-to-air heat exchanger. Regarding the performance of the HRV, the sensible efficiency of the heat exchanger with the dimpled surface was 50% to 60% higher than that of the heat exchanger with flat surface plate at lower air velocity and higher air initial temperatures. The highest COP of the heat exchanger with dimpled surface heat was 6.6; achieved under primary air operating temperature of 32.6 °C.

In the investigation of the IEC system, the main aim was to find the effect of water spray arrangement on the performance. Experiments were conducted with three water spray modes: (1) external spray, (2) internal spray and (3) mixed internal and external sprays. An ANSI/ASHRAE Standard 143-2015 evaluation indices with changing the primary air condition parameter (Primary air inlet temperature and velocity) were applied to evaluate the system performance with water spraying variation. The results show that the internal spraying mode performs better than the external spraying mode does in terms of the wetbulb efficiency, cooling capacity and the COP of IEC. The mixed-mode improves the performance further but increases the water evaporation rate. The innovative internal spray system benefits the sensible heat transfer in the IEC system. The cooling load capacity increases by 12.5% with the internal spray mode and 25% with the mixed mode. The COP varies in a wide range under different water spraying modes and operating conditions with the highest of 19.12 achieved in the mixed-mode.

CFD modelling was also performed to further investigate the IEC system. An Eulerian-Lagrangian 3-D numerical model was developed which was capable of simulating a representative IEC system with realistic nozzles in the mixed-mode operation. A solid-cone spray representation in Eulerian-Lagrangian numerical models was applied in order to replicate real nozzles characteristics in the simulation. The model was verified by

experimental results. The verified model was employed to study the effects of primary air temperature, humidity ratio and velocity on the performance of the indirect evaporative heat exchanger (IEHX). Operating under variable inlet air temperature and humidity conditions, simulated results showed that the wet-bulb effectiveness for the mixed mode ranged from 68%% to 80% with a primary air supply temperature near dewpoint temperature at primary air temperature lower than 28 °C and velocity less than 1.5 m/s.

Dedication

First to the memory of my father, Yassin Al-Zubaydi

To my mother Natheera Abdul-Baki, my wife Sarab Mansoor, my daughters Basma and Tanya and all my family

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This work would not have been possible without the financial support of the Australian Government Research Training Program Scholarship and the help of the University of Technology Sydney – School of Mechanical and Mechatronic Engineering. I am especially indebted to my principal supervisor, Associate Professor Dr Guang Hong, for her continuous support. As my supervisor and mentor, she was the best example of how the researcher and academic should be. I appreciate all her contributions of time, ideas, and assistance to make my PhD experience productive and inspiring. The enthusiasm she has for her research was contagious and motivational for me during hard times in the PhD study.

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List of Publications

- Al-Zubaydi, A.Y.T., G. Hong, and W.J. Dartnall. 2016, CFD Modelling and Analysis of Different Designs Plate Heat Exchangers. In 10th Australasian Heat & Mass Transfer Conference. Brisbane, QLD.
- Al-Zubaydi, A.Y.T. and G. Hong, 2018. Experimental investigation of counter flow heat exchangers for energy recovery ventilation in cooling mode, International Journal of Refrigeration. 93: p. 132-143.
- Al-Zubaydi, A.Y.T. and G. Hong, 2019. Experimental study of a novel water-spraying configuration in indirect evaporative cooling, Applied Thermal Engineering. 151: p. 283-293.

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Abbreviation

3-D Three Dimensional Geometry

AHRI Air-Conditioning, Heating and Refrigeration Institute

AHU Air-Handling Unit

ANSI American National Standards Institute

ASHRAE The American Society of Heating, Refrigerating and Air-Conditioning

Engineers

BOM Bureau of Metrology

CAD Computer Aided Design

CFD Computational Fluid Dynamic

CSIRO Commonwealth Industrial and Scientific Research Organisation

DEC Direct Evaporative Cooling

DIEC Direct-Indirect Evaporative cooler

DNS Direct Numerical Simulation

DOEE Department of Environmental and Energy - Australia

DPM Discrete Phase Modelling

HFC hydrofluorocarbons

HMX Heat and Mass Exchange

HRV Heat Recovery Ventilation

HVAC Heating, Ventilation and Air-Conditioning)

HX Heat Exchanger

IEA International Energy Agency

IEC Indirect Evaporative Cooling

IEHX Indirect Evaporative Heat Exchanger

LDPE Low-Density Polyethylene

LMTD Logarithmic mean temperature difference

M-Cycle Maisotsenko Cycle

NGER National Greenhouse and Energy Reporting

NTU Number of Transfer Units method

PETG Polyethylene Terephthalate Glycol

PHE Plates Heat Exchanger

PVC Polyvinyl Chloride

RANS Reynolds-Averaged Navier-Stokes

R-IEC Regenerative Indirect Evaporative Cooling

ε-NTU Effectiveness-Number of Transfer Units

Nomenclature

A : Area, m²

b : Gap between two plates, mm

 c_{pa} : Specific heat of air, J/kg. °C

COP : Coefficient of performance

 $eff._S$: Sensible efficiency, %

h : Enthalpy of air, J/kg

H: Height of Plate, mm

L : Length of Plate, mm

 l_{fg} : Latent heat of vaporization of water, J/kg

 \dot{m} : Mass flow rate, kg/s

N : Number of plates

p : Precision

P : Power, W

 \dot{Q} : Heat Transfer Rate, W

RH : Relative Humidity, %

 S_{arphi} : The source term for the continuous phase

 $S_{p\varphi}$: The additional source due to the interaction between air and water droplets

t: Temperature, °C

u(x): The absolute uncertainty of directly measured variable, %

v : Air velocity, m/s

 \dot{V} : Volumetric flow rate, m³/s

 V_w : Water evaporation rate, kg/hr

X : Total Width, mm

y : The indirectly measured variable

Z The differential pressure across the orifice plate, mmH₂O

Greek Letters

 β : The sum of bias error

 δ : The total uncertainty error, %

ε : Effectiveness

 ϕ : Flow variable

 Γ_{φ} : The diffusion coefficient

 ρ : Air density, kg/m³

t: Temperature depression, °C

ω : Relative humidity/moisture content of air, g/kg

 Δx : The instrument accuracy

 ΔP : Pressure variation, Pa

 Δy : The absolute uncertainty, %

 Δz : Plate thickness, mm

Subscripts

1 : Inlet

2 : Outlet

p : Primary air

s : Secondary air

DB : Dry-Bulb

WB : Wet-Bulb