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1 **Factors governing microalgae harvesting efficiency by flocculation using cationic**
2 **polymers**

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18 **Abstract**

19 This study aims to elucidate the mechanisms governing the harvesting efficiency of
20 *Chlorella vulgaris* by flocculation using a cationic polymer. Flocculation efficiency increased
21 as microalgae culture matured (i.e. 35–45, 75, and >97% efficiency at early, late exponential,
22 and stationary phase, respectively). Unlike the negative impact of phosphate on flocculation in
23 traditional wastewater treatment; here, phosphorous residue did not influence the flocculation
24 efficiency of *C. vulgaris*. The observed dependency of flocculation efficiency on growth
25 phase was driven by changes in microalgal cell properties. Microalgal extracellular polymeric
26 substances (EPS) in both bound and free forms at stationary phase were two and three times
27 higher than those at late exponential and early phase, respectively. Microalgae cells also
28 became more negatively charged as they matured. Negatively charged and high EPS content
29 together with the addition of high molecular weight and positively charged polymer could
30 facilitate effective flocculation via charge neutralisation and bridging.

31 **Keywords:** Algal extracellular polymeric substances; *Chlorella vulgaris*; Growth phase;
32 Phosphorous; Zeta potential.

33 **1. Introduction**

34 Microalgae are an emerging feedstock for third-generation biofuel, which can address the
35 imminent depletion of fossil fuel and the increasing threat of global warming (Nagarajan et
36 al., 2020; Rajesh Banu et al., 2020). The first-generation (i.e. food crops) and second-
37 generation (i.e. lignocellulosic biomass) biofuel are more environmentally friendly than fossil
38 fuel, but they also have inherent drawbacks especially as they compete with food security and
39 have low conversion efficiency (Nagarajan et al., 2020; Rajesh Banu et al., 2020). As
40 phytoplankton, microalgae are fast-growing photosynthesizing microscopic organisms that
41 can be cultivated without any requirement for arable land and with minimal input of
42 resources. Large-scale microalgae production has been demonstrated in the desert or even on
43 the ocean surface. Microalgae are rich in carbohydrates, proteins, and lipids. These
44 compounds are valuable substrates for the production of renewable fuel such as biodiesel,
45 biomethane, and green hydrogen (Rajesh Banu et al., 2020).

46 The harvesting process remains a major challenge in the microalgae supply chain. The
47 current high cost of harvesting reduces the competitiveness of large-scale biofuel production
48 from microalgae (Khoo et al., 2020; Yin et al., 2020). Microalgae harvesting is the process of
49 recovering a concentrated algal slurry (10 – 25% dry biomass) from the diluted algal
50 suspension (0.02 – 0.05% dry biomass) and reuse the cultivation solution for subsequent
51 algae production. In the current microalgae industry, the harvesting process accounts for 20
52 to 30% of the total algal biomass production cost (Singh & Patidar, 2018). Current
53 microalgae harvesting methods include centrifugation, filtration, flocculation, [flotation](#),
54 [electrocoagulation](#), [bioflocculation](#), and [magnetic separation](#) (Ananthi et al., 2021; Yin et al.,
55 [2020](#)). Comprehensive reviews of the pros and cons of these methods [have highlighted](#)
56 [flocculation](#) as the most promising technology for low-cost harvesting of microalgae biomass
57 for biofuel production (Ummalyma et al., 2017; Yin et al., 2020).

58 Microalgae flocculation using synthetic cationic polymer is a promising technique to
59 overcome the current constraints of algal harvesting. It has been shown to effectively
60 flocculate over 90% of freshwater and seawater microalgae at low doses with a simple and
61 fast operation (Gerchman et al., 2017; Nguyen et al., 2019; Udom et al., 2013; Vu et al.,
62 2020a; Vu et al., 2021). Charge neutralisation and bridging effects have been shown to be the
63 mechanisms behind cationic polymer flocculation, although there are still questions as to how
64 these mechanisms and the flocculation efficiency may be influenced under different algal
65 culture conditions. [Labeeuw et al. \(2021\)](#) reported that the growth phases (i.e. early
66 exponential, late exponential, and stationary) of microalgae influenced the flocculation
67 efficiency using a highly charged cationic polymer. Three algal species (cyanobacteria
68 *Synechocystis sp.*, freshwater *Chlorella vulgaris*, and marine diatom *Phaeodactylum*
69 *tricornutum*) showed different responses to polymer flocculation at three growth phases.
70 Flocculation by cationic polymer addition was 98% effective at flocculating *Synechocystis sp.*
71 regardless of the growth phase, whereas it was 50% less effective for *C. vulgaris* and *P.*
72 *tricornutum* at early stationary phase (Labeeuw et al., 2021). This variation may be attributed
73 to differences in biomass concentration and algal biochemical composition at each growth
74 phase. Thus, it is necessary to delineate the factors that may affect the polymer flocculation
75 of microalgae at different growth phases. This will help to gain further knowledge of algal
76 flocculation and identify the strategies to optimise algal harvesting using cationic polymer.

77 Phosphorous is an essential nutrient for microalgal growth, especially for the synthesis of
78 biomolecules such as phospholipids, adenosine triphosphate, and deoxyribonucleic acids in
79 the algal cells. Phosphorus is present in the algal medium as orthophosphates and decreases
80 in concentration gradually with culture age. Residual phosphorous has been reported to
81 impact coagulation and flocculation in wastewater treatment (Liu & Liss, 2007; Morgan,
82 1958; Park et al., 2016). The presence of phosphorous as phosphates in wastewater hindered

83 the flocculation and sedimentation processes (Morgan, 1958). A higher flocculant dose and a
84 longer settling time were required to overcome the interference caused by phosphate
85 compounds (Morgan, 1958; Park et al., 2016). Conversely, the gravitational settling velocity
86 of sludge flocs was enhanced for wastewater with reduced phosphorous concentration (Liu &
87 Liss, 2007). This improvement was attributed to larger and more compact flocs formed under
88 phosphorous limited conditions. In other words, a lower phosphorous concentration can lead
89 to a higher flocculation efficiency in a wastewater matrix. However, it is still unknown if
90 these findings are also applicable to a microalgal culture with a very different matrix
91 compared to wastewater.

92 As microalgae grow, they also secrete metabolites (e.g. carbohydrates and proteins) that
93 surround the cells, known as algal extracellular organic matter, or extracellular polymeric
94 substances (EPS). EPS can influence the surface properties of algal cells as well as promoting
95 or inhibiting floc formation (Henderson et al., 2010; Roselet et al., 2017; Sano et al., 2011;
96 Vandamme et al., 2012; Zhang et al., 2012). Algal EPS can act as a polymer aid at low
97 concentration, as it frequently contains biopolymers that can bridge the cells and/or with
98 hydroxide precipitates to form large flocs (Gonzalez-Torres et al., 2017). On the other hand,
99 EPS can decrease the efficiency of the coagulation-floation process as EPS can form
100 complexes with the coagulant and thereby increasing the required coagulant dose to floc algal
101 cells (Bernhardt et al., 1985; Roselet et al., 2017; Vandamme et al., 2012). Given these
102 effects of EPS on algal harvesting, the concentration and composition of algal EPS would
103 likely influence the flocculation efficiency using cationic polymer at different growth phases.

104 This study aims to elucidate the underlying [factors affecting the flocculation efficiency of](#)
105 [Chlorella vulgaris at different growth phases \(i.e. early exponential, late exponential and](#)
106 [stationary phase\)](#). Factors including residual phosphorus concentration, surface charge of
107 microalgal cells, and cell EPS content are examined at each growth phase. Results presented

108 here are useful for further optimisation of microalgae harvesting by flocculation using
109 organic polymers.

110 **2. Materials and methods**

111 2.1. *Chlorella vulgaris* cultivation

112 The freshwater microalgae *Chlorella vulgaris* (CS-41) was obtained from Australian
113 National Algae Culture Collection at CSIRO Microalgae Research (Hobart, TAS, Australia).
114 The stock culture was maintained in 0.22 µm filtered autoclaved freshwater MLA medium
115 (Algaboost; Wallaroo, SA, Australia). [The main nutrient composition of this MLA medium](#)
116 [includes approximately 49 mg/L of MgSO₄·7H₂O, 170 mg/L of NaNO₃, 35 mg/L of K₂HPO₄,](#)
117 [and 2 mg/L of H₃BO₃, respectively \(Bolch & Blackburn, 1996\).](#)

118 *C. vulgaris* culture was prepared in three steps from 1 L bottle to 350 L photobioreactor
119 (Supplementary data Fig. 1S). The stock culture was first cultivated in a 1 L bottle, then
120 transferred to a 10 L bottle for further cultivation until the early stationary phase. Finally, the
121 10 L culture was used to inoculate two identical 350 L photobioreactors (i.e. two biological
122 replicates). The 350 L photobioreactors were maintained at 25 °C, 100-400 µmol
123 photons/m²/s light in a 16:8 light:dark cycle, and air supply through air lines. These
124 photobioreactors were also sparged with 100% CO₂ for 1 min/day to provide carbon and
125 maintain the pH below 9.3. Microalgal growth was monitored daily by optical density
126 measurement. Microalgae suspensions from these two photobioreactors were extracted at the
127 same time of the day for flocculation and determination of extracellular polymeric substances
128 (EPS).

129 2.2. Microalgae flocculation

130 2.2.1. Materials

131 A cationic polyacrylamide polymer (FO3801) was purchased from SNF (SNF Pty Ltd;
132 Corio, VIC, Australia). The polymer is highly charged (75 mV by zeta potential) with a high
133 molecular weight (over 15 MDa) and a charge density of 80%. A stock polymer solution (2
134 g/L) was prepared in Milli-Q water under mixing for 60 min using a magnetic stirrer. The
135 stock solution was used for the flocculation experiment within one day to avoid any polymer
136 hydrolysis during long-term storage.

137 *C. vulgaris* suspension (10 L) at early exponential, late exponential and stationary phase
138 was collected from the two 350 L photobioreactors (section 2.1) for the flocculation
139 experiment.

140 To investigate the impact of residual phosphorous in the algal culture on flocculation
141 efficiency, dipotassium phosphate (K_2HPO_4) was added to *C. vulgaris* suspensions at
142 stationary phase to achieve the phosphate (PO_4^{3-}) concentration of 10, 20, 30, and 40 mg/L.
143 *C. vulgaris* suspension at stationary phase without K_2HPO_4 addition was used as the control.
144 The phosphate concentration of this control suspension was 3.7 mg/L. After K_2HPO_4 was
145 completely dissolved in the suspensions, algae flocculation was performed with FO 3801 at
146 35 mg polymer/g dry biomass.

147 2.2.2. Experimental protocols

148 Flocculation test took place in 250 mL glass beakers containing 100 mL of microalgal
149 culture. Polymer solution was dosed at 35 mg/g dry algal biomass. This dose was the optimal
150 dose for *C. vulgaris* flocculation as reported in a previous study (Labeeuw et al., 2021). After
151 polymer dosing, the microalgae suspensions were rapidly mixed for 1 minute at 200 rpm,
152 followed by slow mixing for 5 minutes at 50 rpm. The suspensions were allowed to settle for

153 10 minutes. Then 10 mL aliquot was pipetted at a height between one- and two-third from the
154 bottom of the beaker. Optical density of this aliquot sample was measured to determine the
155 flocculation efficiency (Section 2.3.3).

156 2.3. Analytical methods

157 2.3.1. Microalgae growth analysis

158 Two samples of 100 mL (i.e. two technical replicates) are taken from each of the two 350
159 L photobioreactors every second day for measurements of dry weight, optical density, pH,
160 residual phosphorous concentration, and zeta potential.

161 The dry weight of *C. vulgaris* culture (i.e. dry biomass concentration) was determined
162 gravimetrically by filtering 100 mL solution through a 1.1 µm pre-weighed glass fibre filter
163 paper. After 12 h of oven drying at 60 °C, the weight of the filter paper with retained biomass
164 was used to calculate the dry algal biomass concentration.

165 The optical density of the microalgal culture was measured by a spectrophotometer
166 (Shimadzu UV 6000) at a wavelength of 680 nm. The residual phosphorous concentration in
167 the algal culture was determined using Phosphorous TNTplus Vial Test high range (1.5-15.0
168 mg/L PO₄³⁻) and a spectrometer (DR3900, Hach Pacific, Australia). Samples of the algal
169 culture were filtered through 0.45 µm Nylon syringe filters to remove microalgal cells before
170 applying the vial test to the supernatant. The zeta potential of the algal culture was measured
171 using the zeta instrument (Zetasizer Nano ZS Zen 3600, Malvern, UK).

172 2.3.2. Flocculation efficiency

173 The optical density and zeta potential of the microalgal culture before and after polymer
174 flocculation was measured as outlined in Section 2.3.1. The flocculation efficiency was
175 determined using Equation 1:

176
$$\text{Flocculation efficiency (\%)} = \left(\frac{OD_i - OD_f}{OD_i} \right) \times 100 \quad (\text{Equation 1})$$

177 where OD_i and OD_f imply the optical density of the microalgal culture before and after
178 flocculation.

179 2.3.3. EPS extraction and determination

180 EPS consists of soluble EPS and bound EPS. Microalgal suspension of 35 mL was
181 centrifuged at 3,500 g and 4 °C for 30 min. The supernatant was then filtered through a 0.45
182 μm Nylon syringe filter to obtain soluble EPS. The algal pellet was re-suspended to a volume
183 of 35 mL in a phosphate buffer solution (10 mM NaCl, 1.2 mM KH_2PO_4 , and 6 mM
184 Na_2HPO_4). The re-suspended algal suspension was subjected to low-strength sonication for
185 40 s. The sample was centrifuged again at 9,000 g and 4 °C for 15 min. Filtered supernatant
186 contained bound EPS. Carbohydrate and protein concentration of the soluble and bound EPS
187 were determined using the phenol-sulfuric acid method (Nielsen, 2010) and Lowry method
188 (Lowry et al., 1951), respectively.

189 2.3.4. Statistical analysis

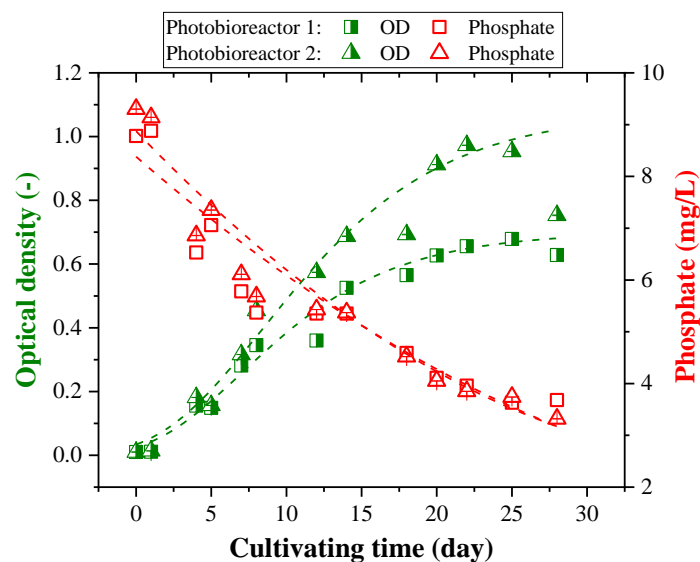
190 Statistical analysis of flocculation efficiency and biomass quality measurements was
191 performed using Student's t -test (OriginPro 2019). Appropriate assumptions (i.e. data sets are
192 normally distributed and have equal variances) were checked before statistical analysis.

193 3. Results and Discussion

194 3.1. Biomass production and nutrient profile in pilot-scale photobioreactors

195 Batch autotrophic cultivation of *Chlorella vulgaris* in the 350 L pilot-scale
196 photobioreactor showed a typical S-shape growth curve with three distinctive phases (Fig. 1)
197 similar to that reported in the literature (e.g. Do et al. (2020); dos Santos et al. (2016); Klin et
198 al. (2020)). The duration of each algal growth phase in this study is similar to the growth of
199 *C. vulgaris* in a previous study under the same condition (Labeeuw et al., 2021). In the early

200 exponential growth phase (day zero to six), cells were adapting to the new environment. Once
 201 fully adapted, algal cells started to rapidly multiply. The culture entered the exponential
 202 phase at day seven. At the end of the exponential phase (day 18), cell growth reached its limit
 203 as defined by the availability of nutrients, light, and carbon source. The culture entered the
 204 stationary phase when the production of new cells was gradually offset by cell death.
 205 Samples were taken on day seven (i.e. early exponential), day 18 (i.e. late exponential), and
 206 day 28 (i.e. stationary) for subsequent flocculation experiments.

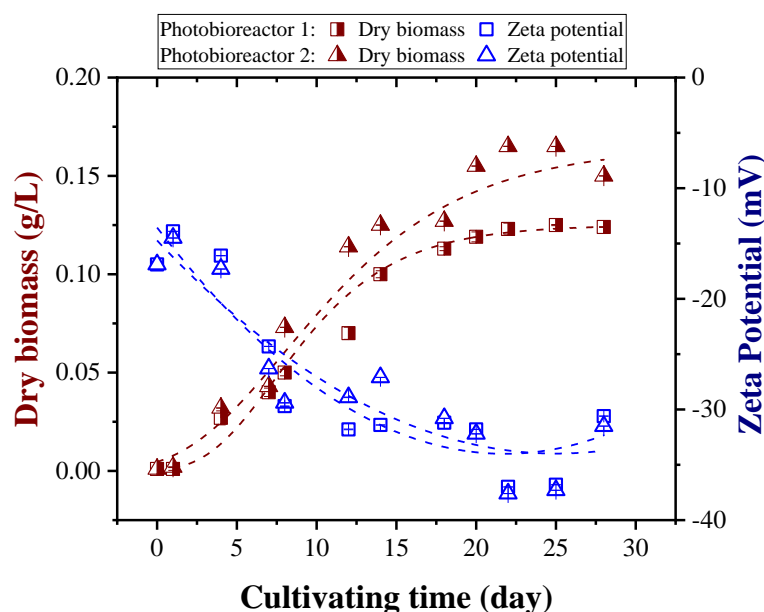


207

208 **Figure 1:** Change in optical density and phosphate concentration of *C. vulgaris* culture
 209 during 28-day cultivation. Values and error bars represent mean and standard deviation from
 210 two technical replicate measurements ($n = 2$), respectively.

211 As microalgal biomass was produced (i.e. increase in optical density and dry weight),
 212 phosphorous content in the culture decreased over time (Figs. 1 and 2). Microalgal cells
 213 uptake nutrients for growth and synthesis of intracellular proteins, lipids, and carbohydrates
 214 (Anto et al., 2019; Chu et al., 2013). Over 28 days of cultivation, phosphorous concentration
 215 decreased from 9.0 mg/L PO_4^{3-} (day zero) to 5.8, 4.6, and 3.7 mg/L PO_4^{3-} for early
 216 exponential, late exponential and stationary phase, respectively. This represents a final 60%

217 reduction in phosphorous availability during *C. vulgaris* growth (Fig. 1). The phosphorous
 218 reduction is low in this study compared to previous studies whose aim is to remove
 219 phosphorous from wastewater (Vu et al., 2020b). However, our data (optical density, dry
 220 algal biomass concentration, phosphate depletion, and zeta potential) are consistent between
 221 the two biological replicates (i.e. two photobioreactors) (t -test, $p > 0.05$), indicating the
 222 experimental reproducibility. The low phosphorous uptake was probably due to both light
 223 and carbon source limitations in our photobioreactor cultivation system. Nevertheless, the
 224 change in residual phosphorous will facilitate the investigation regarding its impact on
 225 microalgal harvesting (Section 3.3).



226

227 **Figure 2:** Change in dry biomass concentration and zeta potential of *C. vulgaris* culture
 228 during 28-day cultivation. The culture pH was fluctuating within the range of pH 8 to 9.
 229 Value and error bars represent mean and standard deviation from two technical replicate
 230 measurements ($n = 2$), respectively.

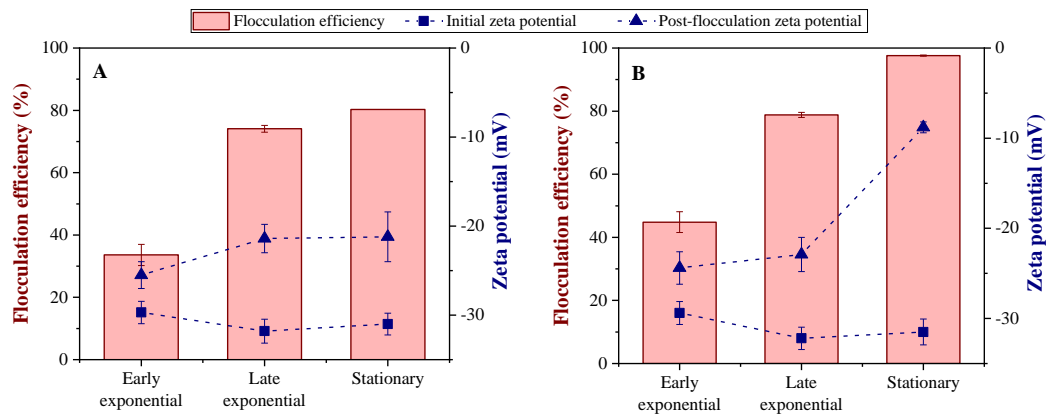
231 The surface charge of microalgal cells became more negative as the culture solution
 232 matured over time (Fig. 2). Microalgae cells are negatively charged so that they repel one

233 another by electrostatic interaction to stay dispersed in suspension. This maximises access to
234 sunlight for photosynthesis by individual microalgal cells. The net negative charge of the cell
235 surface is derived from the carboxylic groups on the cell membrane (Vandamme et al., 2013).
236 In this study, the algal culture pH was slightly basic at pH 8-9, thus, these carboxylic groups
237 dissociated to attain a negative charge for each microalgal cell. The increase in surface charge
238 was significant within the early exponential growth phase (day zero to six) (Fig. 2). Changes
239 in surface charge from the early exponential growth phase to the stationary phase were
240 discernible but not statistically significant.

241 Increasing surface charge leads to stronger electrostatic repulsion to prevent the
242 agglomeration of algal cells (Zheng et al., 2019). Thus, it is useful to examine if changes in
243 cell surface charge would affect flocculation efficiency.

244 3.2. Flocculation efficiency at different growth phases

245 The flocculation efficiency of FO 3801 was dependent upon the growth phase of *C.*
246 *vulgaris* (Fig. 3). This observation agrees with previous studies (Labeeuw et al., 2021; Zhang
247 et al., 2018). There is some variation in flocculation efficiency as well as the zeta potential of
248 the initial and post-flocculation microalgae at the three growth phases between the two
249 biological replicates (i.e. two independent photobioreactors) as can be seen in Fig. 3. *These*
250 *differences could have been due to the random biological variation of the two*
251 *photobioreactors, despite the efforts to operating them in the same conditions.* However, the
252 overall pattern is same and the difference in absolute value is also small.



253

254 **Figure 3:** Flocculation efficiency and the increase in zeta potential of *C. vulgaris* culture

255 at 35 mg polymer/g dry biomass of two biological replicates: (A) photobioreactor 1 and (B)

256 photobioreactor 2. Flocculation was conducted at three different growth phases: early

257 exponential, late exponential, and stationary. Values and error bars represent mean and

258 standard deviation from two technical replicate measurements ($n = 2$), respectively.

259 Charge neutralisation is an important flocculation mechanism and can partially, but not

260 fully explain the increase in flocculation efficiency as the microalgae culture progressed from

261 the early exponential to the stationary growth phase (Fig. 3). Results in Fig. 3 show that the

262 highly charged cationic polymer FO3801 could significantly reduce the cell surface charge.

263 However, complete charge neutralisation did not occur even at the stationary phase when the

264 highest flocculation efficiency of 97% was achieved. Previous studies have suggested that

265 complete charge neutralisation is not necessary to achieve high (>95%) flocculation

266 efficiency (Nguyen et al., 2019). It is noteworthy that in Fig. 3 the same polymer dose was

267 applied to all flocculation experiments and that the differences in the initial zeta potential

268 between the late exponential and stationary growth phase were negligible (t -test, $p > 0.05$).

269 Thus, the initial surface charge is not the only factor governing the dependency of

270 flocculation efficiency on growth phase. As the microalgae culture continued to mature, the

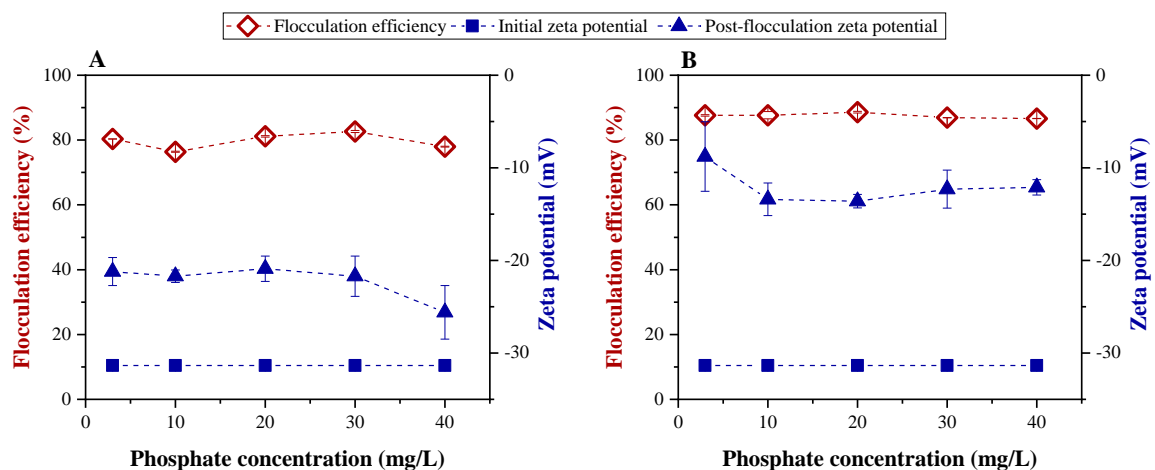
271 composition of the media and physiochemical properties of the algal cells also changed. The

272 possible influence of media matrix (in terms of phosphate content) and cell properties on the

273 effectiveness of polymer flocculation at different growth phases will be elucidated in
274 subsequent sections.

275 3.3. Impact of phosphorous residue on flocculation

276 In this study, residual phosphorous in the algal media did not show any influence on
277 flocculation (Fig. 4). The variation in flocculation efficiency of the control sample and the
278 samples with added K_2HPO_4 (i.e. 10 to 40 mg/L PO_4^{3-}) was negligible (t -test, $p > 0.05$). In
279 addition, there was no observed correlation between algal cell zeta potential after flocculation
280 and phosphorous concentration. Charge neutralisation of the cultures with 10 to 40 mg/L
281 PO_4^{3-} was comparable to that of the control culture for both photobioreactors (t -test, $p >$
282 0.05). These observations conclusively affirm that the variation in flocculation efficiency of
283 *C. vulgaris* at different growth phases (Section 3.2) was not induced by residual phosphorous
284 in the culture media.

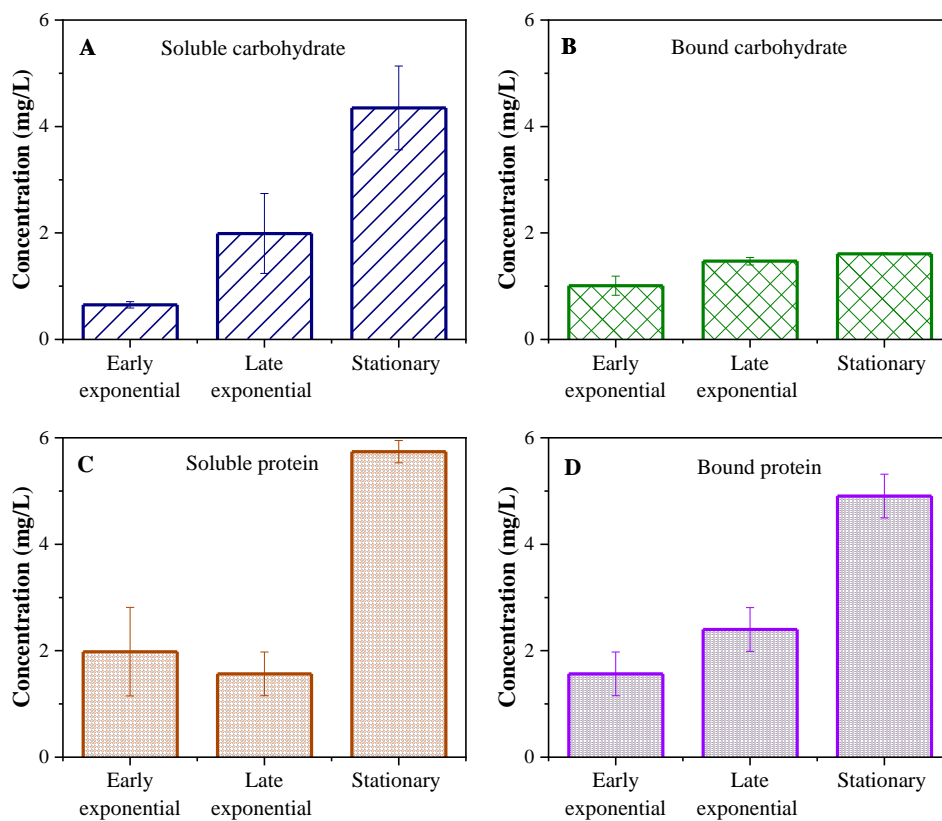


285

286 **Figure 4:** Flocculation efficiency and charge neutralisation of *C. vulgaris* culture at
287 various concentrations of phosphate in the media during the stationary phase for (A)
288 photobioreactor 1 and (B) photobioreactor 2. The polymer dose was 35 mg FO 3801/g dry
289 biomass. Value and error bars represent mean and standard deviation from two technical
290 replicate measurements ($n = 2$), respectively.

291 3.4. EPS content and impact on flocculation efficiency

292 Soluble and bound EPS content of *C. vulgaris* increased as the microalgal culture
293 sequentially transited through the three growth phases (Fig. 5). The concentration of soluble
294 EPS in terms of both carbohydrate and protein reached the highest value at the stationary
295 phase (Fig. 5A and 5C). This value is approximately two and three times the total soluble
296 EPS of late exponential and early exponential phase, respectively. Likewise, algal culture
297 media at the stationary phase had the highest bound EPS content (6.5 mg/L), followed by late
298 exponential (3.9 mg/L) and early exponential (2.5 mg/L) phase (Fig. 5B and 5D).



299

300 **Figure 5:** Accumulation of EPS in terms of (A) soluble carbohydrate, (B) bound
301 carbohydrate, (C) soluble protein, and (D) bound protein in the *C. vulgaris* culture media at
302 the early exponential, late exponential and stationary growth phases. Value and error bars
303 represent mean and standard deviation from two biological replicate measurements ($n = 2$),
304 respectively.

305 A similar trend of increasing EPS content as the microalgal culture continued to mature
306 has been reported for other microalga species such as *Asterionella formosa*, *C. vulgaris*,
307 *Microcystis aeruginosa*, and *Ettlia texensis* (Henderson et al., 2008; Salim et al., 2013; Zhang
308 et al., 2018). Algal cells were actively dividing and excreting metabolites (i.e. carbohydrates
309 and proteins) during the exponential growth phase. Thus, a higher EPS content was observed
310 at the late exponential phase than the early exponential phase. Although growth in the
311 stationary phase ceased, algal cells continued releasing metabolites, partly due to cell
312 autolysis. As a result, the EPS components at the stationary phase were influenced by the
313 algal intracellular contents (i.e. the biochemical composition). This explains the significant
314 increase in protein content of soluble and bound EPS at stationary phase (Figs. 5C and 5D) as
315 *C. vulgaris* is a protein-rich microalga. The solubilisation of the bound EPS fraction formed
316 during the exponential phase also contributed to the increase in soluble EPS content of algal
317 culture media at the stationary phase (Henderson et al., 2008). Therefore, the increase in EPS
318 content with culture age appears to be a key factor influencing *C. vulgaris* flocculation and
319 can elucidate its growth-phase dependent flocculation efficiency (section 3.2.1).

320 Microalgal EPS are dominated by hydrophobic proteins and hydrophilic carbohydrates
321 (Henderson et al., 2008). These biopolymers can contribute to the bridging mechanism,
322 which facilitates flocculation. In other words, these biopolymers from the algal cells and the
323 added cationic polymer can form EPS-cell-polymer networks via electrostatic interaction to
324 induce the flocculation process (Rao et al., 2021). As discussed in section 3.2, electrostatic
325 attraction is expected between the negatively charged algal cell surface and the positively
326 charged cationic FO3801 polymer to form large EPS-cell-polymer networks (i.e. flocs) via a
327 combination of charge neutralisation and bridging effects (Gonzalez-Torres et al., 2017; Rao
328 et al., 2021). Results from Fig. 5 are consistent with the dependence of flocculation efficiency
329 on growth phase.

330 Previous studies have established the dependency of flocculation efficiency on culture
331 maturity. Results from this study reveal for the first time underlying mechanisms governing
332 the relationship between flocculation efficiency and culture maturity. The results are
333 significant for optimising microalgae cultivation and harvesting. Microalgal EPS production
334 is species dependent. Thus, further work is necessary to corroborate findings from this study
335 to other microalgae species.

336 **4. Conclusions**

337 Flocculation efficiency of *Chlorella vulgaris* using cationic polymer increased with
338 microalgae culture maturity. The highest flocculation efficiency (>97%) was achieved with
339 the algal culture at stationary phase. Phosphorous residue in the culture did not affect *C.*
340 *vulgaris* flocculation and cell surface charge, contrary to its negative impacts on flocculation
341 in wastewater treatment application. The dependency of flocculation efficiency on growth
342 phase was induced by changes in cell properties (e.g. EPS and surface charge). High EPS
343 content with negative charges surrounding algal cells interacted with cationic polymer to
344 form polymer-EPS-cell networks via charge neutralisation and bridging, thus promoting the
345 flocculation process.

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349 **6. Declarations**

350 The authors declare that there is no conflict of interest regarding the publication of this
351 article.

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