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1 **High-Performance Mild Annealed CNT/GO-PVA Composite Membrane for Brackish Water**  
2 **Treatment**

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15  
16 **Abstract**

17 Two-dimensional (2D) graphene oxide (GO)-based materials with tunable physicochemical  
18 properties have enormous potential for developing next-generation desalination  
19 membranes. Nevertheless, weak interlamellar interactions result in poor selectivity towards  
20 small ions, limiting the wide applicability of GO membranes. Controlling the swelling of the  
21 GO membrane while maintaining high permeability and selectivity is a significant scientific  
22 and technological challenge. To address the issues above, we used one-dimensional (1D)  
23 carbon nanotubes (CNT) as a nano-spacer and polyvinyl alcohol (PVA) as an adhesive.  
24 Synergistic ionic complexation between 1D-CNT, 2D-GO, and PVA was studied using various  
25 analytical techniques. The intercalation of CNT between GO nanosheets and the cross-linking  
26 of CNT/GO-PVA significantly improved the separation performance. Pressure-assisted  
27 filtration was used to coat the CNT/GO-PVA on hydrophilic mixed cellulose esters (MCE)  
28 support with pore size 0.22  $\mu\text{m}$  to obtain a highly ordered laminated structure. Five minutes  
29 of mild annealing at 80  $^{\circ}\text{C}$  narrowed the laminar channels of the GO nanosheets by  
30 transforming the oxygen-containing functional groups. In a dead-end filtration unit, the

31 CNT<sub>5</sub>/GO<sub>15</sub>-PVA<sub>0.5</sub> composite membrane exhibits a high rejection of 94.2% to sodium sulphate  
32 (Na<sub>2</sub>SO<sub>4</sub>) and 85.86% to sodium chloride (NaCl), accompanied by a high permeate rate of 14.2-  
33 13.45 LMH at 5 bar operating pressure. The salt rejection studies were evaluated for  
34 continuous operation for 72 hours for all membranes. Due to the synergistic effect of CNT,  
35 GO, and PVA, prepared membranes demonstrated the potential for practical water  
36 separation applications with desired permeability and selectivity.

37 **Keywords:** graphene oxide, carbon nanotube, swelling, membrane separation, desalination

## 38 **1. Introduction**

39 Nanofiltration (NF) technology applications for hard water softening, resource recovery and  
40 desalination processes are numerous [1, 2]. Polymeric NF membranes were widely used for  
41 ions separation at relatively low pressure and demonstrated high efficiency in removing  
42 divalent ions and, to a less extent, monovalent ions [2, 3]. Despite the several advantages of  
43 NF membranes, polymeric NF membranes experience some drawbacks, such as limited water  
44 flux, membrane fouling, and low rejection of monovalent ions [4, 5]. Researchers suggested  
45 incorporating nanomaterials in polymeric NF membranes to improve their filtration  
46 characteristics and fouling propensity [6].

47 Graphene-based materials are state-of-the-art with potential applications in batteries,  
48 composite materials, and separation and purification technologies due to their excellent  
49 physicochemical properties [7-9]. The intertwined nanochannels formed by the stacking of  
50 2D graphene-based nanosheets in graphene-based membranes result in a zigzag route for the  
51 permeation of water molecules [10]. Graphene oxide (GO) membranes are gaining wide  
52 attention in the preparation of NF membranes due to the ease of fabrication via various  
53 methods, e.g. pressure-assisted filtration [11], inkjet printing [12], vacuum, and dip-coating  
54 method [13]. Among all the methods mentioned above, pressure-assisted filtration is widely  
55 applied to obtain GO membranes' highly ordered laminar structure [11, 14]. One of the GO-  
56 based membrane limitations is that polar functional groups of the GO sheets increase the  
57 interlayer spacing to about 7 nm when exposed to an aqueous environment [15]. Previous  
58 studies showed that the reduction in membrane thickness (< 100 nm) effectively increases  
59 the permeability of the GO membrane but compromises its selectivity [11, 16, 17]. The  
60 selectivity of the GO-based membranes is governed by the surface charge and the frictionless

61 capillary channels for mass transport [18]. The post-treatment process and fabrication  
62 technique determine the formation of capillary channels and the microstructure order in GO  
63 membranes [18, 19]. Numerous strategies were developed to combat the swelling and  
64 instability of the GO membrane, such as chemical modification, reduction, and cross-linking  
65 of GO, enhancing the practical implementation of GO membranes in water and wastewater  
66 treatment [17]. Nevertheless, the partial reduction of polar functional groups of GO  
67 membranes could offer a stable NF membrane of a high rejection rate [20, 21].

68 Reduced graphene oxide (rGO) membranes are still under development and require more  
69 research to improve the permeability and rejection rate of the membrane. [22]. The rGO  
70 membranes resemble the properties of graphene materials with a lattice parameter of  $3.5\text{\AA}$ ,  
71 which can potentially block salt ions by size exclusion [21]. Remarkably, tuning the interlayer  
72 spacing of graphene sheets using nanoparticles becomes an effective method for increasing  
73 the membrane's permeability. Laminated rGO membranes were obtained in previous studies  
74 by post-treatment of the GO membranes at a thermal temperature above  $120\text{ }^{\circ}\text{C}$ , but a  
75 decrease in membrane selectivity was reported due to the development of microstructural  
76 defects [23, 24]. Thus, a mild reduction of GO membranes is suggested to lower the  
77 transformation of polar functional groups with microstructure evolution at  $80\text{ }^{\circ}\text{C}$ . It is also  
78 postulated that the narrow interlayer space of graphene-based membranes is the main  
79 reason for its low water flux. Researchers investigated inorganic [25, 26], organic [19, 27, 28],  
80 and nanotubes-based frameworks [29, 30] nanoparticles for tuning the interlayer spacing in  
81 the GO membranes. Carbon nanotube (CNT) is considered the most promising material  
82 among all materials mentioned above due to its high compatibility [31]. For instance, Gao et  
83 al. [29] developed a graphene-based NF membrane intercalated with a multiwalled carbon  
84 nanotube (MWCNT) to improve salt rejection. The permeability coefficient of the developed  
85 membranes was  $11.3\text{ Lm}^{-2}\text{h}^{-1}\text{bar}^{-1}$  with a rejection rate of sodium sulfate ( $\text{Na}_2\text{SO}_4$ ) and sodium  
86 chloride (NaCl) equal to 83.5% and 51.4%, respectively [29]. Another study by Jin et al. [30]  
87 prepared GO membranes intercalated with single-walled carbon nanotube (SWCNT). They  
88 have achieved water permeability up to  $660\text{--}720\text{ Lm}^{-2}\text{h}^{-1}\text{bar}^{-1}$  and a rejection rate of 97.4%  
89 to 98.7% to rhodamine B and coomassie brilliant blue dyes, respectively [30]. Fan et al.  
90 prepared loose NF membranes using rGO/CNT using block copolymers (BCPs) to disperse CNT  
91 for the removal of organic dyes and achieved 97.3% rejection for methyl orange (MO) dye

92 [32]. In another study, Huang et al. prepared rGO/CNT composite membranes for  
93 pharmaceuticals and personal care products (PPCP) [33]. They have achieved over 76%  
94 removal efficiency for PPCP with clean water permeability (4454 LMH/Bar) [33]. The rejection  
95 rate of rGO/CNT membrane to monovalent and divalent ions was not investigated in the  
96 previous studies. Future research should focus on improving the selectivity and stability of  
97 graphene-based membranes for desalination processes with enhanced antifouling  
98 performance.

99 In this study, mild annealed reduced graphene oxide (MrGO) membranes were prepared for  
100 water desalination at 80 °C. The fabricated membrane was cross-linked with optimal polyvinyl  
101 alcohol (PVA) concentration to stabilise the process and prevent membrane swelling. CNT was  
102 used to provide frictionless capillary channels for enhanced water permeability. The  
103 concentration of CNT in the graphene-based membranes was optimised for the trade-off  
104 between permeability and selectivity. Deionized (DI) water was used to prepare the GO/CNT-  
105 PVA dispersions for membrane fabrication. The GO/CNT-PVA membranes were tested for  
106 2000 ppm sodium sulfate ( $\text{Na}_2\text{SO}_4$ ) and sodium chloride (NaCl) rejection at 5 bar hydraulic  
107 pressure.

## 108 **2. Materials and methods**

### 109 **2.1. Chemicals required**

110 All chemicals used in this study were of analytical grade and used as received without any  
111 further purification. Brownish-yellow powder of high surface area GO of  $\geq 99\%$  purity with  
112 lateral size of 1-5  $\mu\text{m}$ , and thickness of 0.8-1.2 nm was purchased from ACS Material, LLC,  
113 USA. The obtained GO has 51.26 and 40.78 wt. % of carbon and oxygen content, respectively.  
114 Multiwalled carbon nanotube (MWCNT) of  $\geq 99\%$  purity (Average diameter: 8.7-10 nm,  
115 Surface area: 216  $\text{m}^2/\text{g}$ , and Trace metals analysis  $\leq 20000$  ppm). Polyvinyl alcohol (PVA) with  
116 an average molecular weight of 47 kDa,  $\text{Na}_2\text{SO}_4$  and, NaCl chemicals were obtained from  
117 Merck, Australia. Hydrophilic mixed cellulose esters (MCE) MF-Millipore membrane filter  
118 (Pore size: 0.22  $\mu\text{m}$ , Diameter: 47 mm, and Lot: R9NA98005) was supplied by Sigma Aldrich  
119 Australia.

### 120 **2.2. MrGO/CNT-PVA membrane fabrication**

121 In the beginning, 5 g of PVA was dissolved in 100 mL DI water for 24 hours at 60 °C with  
 122 constant stirring. The resulting viscous solution was sonicated for an hour to remove any  
 123 trapped air bubbles. Next, aqueous GO and CNT (25 mg/l) were prepared using an  
 124 ultrasonication bath for 2 hours with 60 °C temperature at 40 kHz. Terminology and the  
 125 composition of all the prepared solutions for coating are in **Table 1**. The GO/CNT-PVA  
 126 composite membranes were prepared using a pressure-assisted filtration technique, as  
 127 depicted in **Figure 1**. The solutions were passed through hydrophilic mixed cellulose esters  
 128 (MCE) filters with 0.22  $\mu\text{m}$  pore size at 5 bar pressure for 3 hours. The obtained membranes  
 129 were dried overnight at room temperature ( $23 \pm 1.5$  °C) and thermally reduced at 80 °C for 5  
 130 min to obtain MrGO. Finally, the obtained membranes were characterised using various  
 131 analytical instruments listed in **Table 2**. Before conducting the performance studies, the  
 132 obtained GO/CNT-PVA composite membranes were stored in plastic Petri dishes.

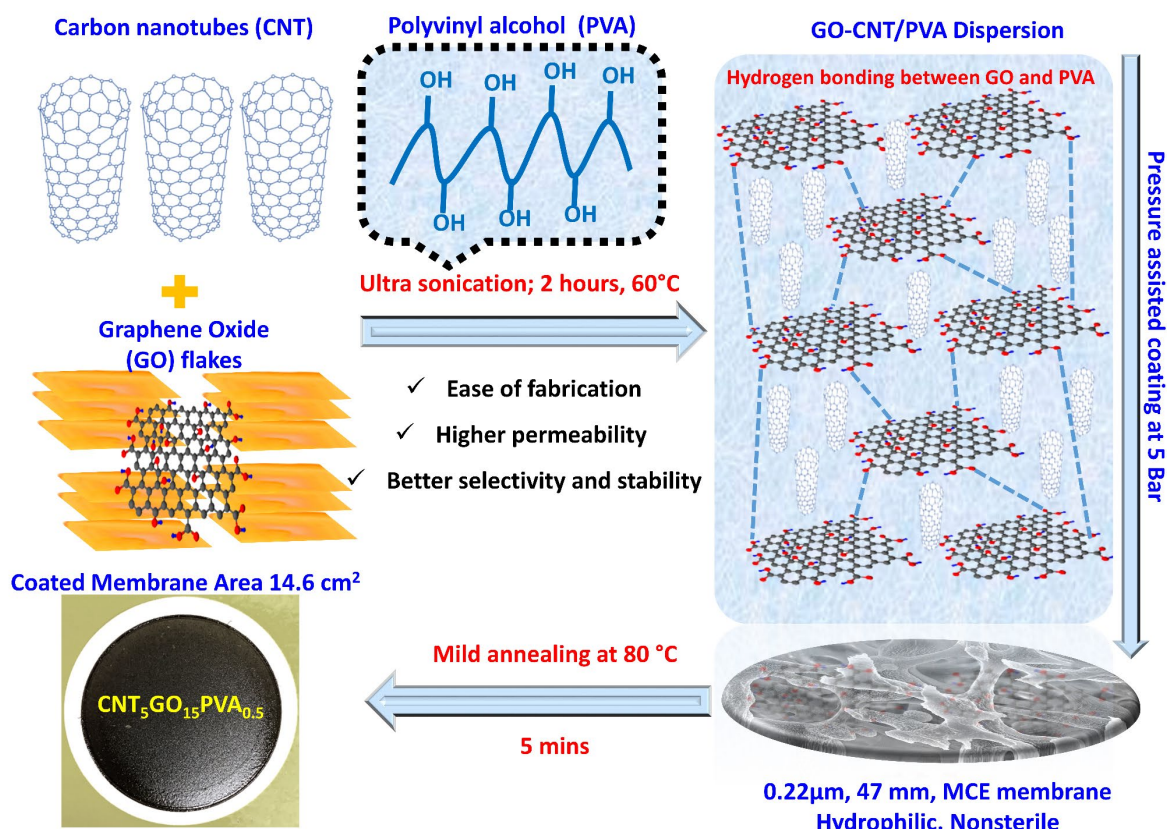
133 **Table 1:** Composition of GO, CNT and PVA in the various coating solutions to prepare GO/CNT-  
 134 PVA composite membranes.

Membrane code	CNT		GO		PVA (5 wt% (mL))	
	Aq sol, mL	Volume ratio (%)	Aq sol, mL	Volume ratio (%)	5 wt% (mL)	Volume ratio (%)
CNT <sub>5</sub> GO <sub>15</sub> PVA <sub>0.5</sub>	5	24.39	15	73.17	0.5	2.44
CNT <sub>10</sub> GO <sub>10</sub> PVA <sub>0.5</sub>	10	48.78	10	48.78	0.5	2.44
CNT <sub>15</sub> GO <sub>5</sub> PVA <sub>0.5</sub>	15	73.17	5	24.39	0.5	2.44
GO <sub>20</sub> PVA <sub>0.5</sub>	-	-	20	97.56	0.5	2.44
CNT <sub>20</sub> PVA <sub>0.5</sub>	20	97.56	-	-	0.5	2.44
CNT <sub>20</sub>	20	100	-	-	-	-

135

136

137



138

139 **Figure 1:** Schematic illustration for the fabrication of GO/CNT-PVA composite membranes.

140 **Table 2:** Analytical instruments used to study the physicochemical properties of GO/CNT-PVA  
 141 composite membranes.

Analytical instrument	Physicochemical properties studied
Fourier-transform infrared spectroscopy (FTIR)	To identify the functional groups and chemical bonds
Raman spectroscopy	To study the phonon properties of CNT and GO and to detect vibrational and rotational states in a molecular system
Scanning electron microscopy (SEM)	To investigate the morphology of the resultant membranes
X-ray diffraction (XRD)	To analyse the effective channel size (interlayer space) of the membranes
X-ray photoelectron spectroscopy (XPS)	To identify the chemical bonding and structure of the resultant membranes

Water contact angle studies	To study the hydrophilicity of the resultant membrane
Surface zeta ( $\zeta$ ) potential measurements	To measure the magnitude of the electrostatic or charge repulsion/attraction at the interface

142

### 143 2.3. Membrane performance studies

144 Membrane performance studies (pure water flux and salt rejection) were conducted using  
 145 HP4750 Sterlitech cell at  $23 \pm 1.5$  °C temperature and  $\sim 48 \pm 4$  % humidity. The HP4750  
 146 Sterlitech cell had an active membrane area (A) of  $0.00146 \text{ m}^2$ , and the cell was filled with  
 147 feed every 12 hours. The first 30 minutes of operation were used to stabilise the system prior  
 148 to taking the readings. All experiments were carried out at a constant hydraulic pressure of 5  
 149 bar supplied by compressed air. Using an electronic weighing balance, permeate flux was  
 150 calculated every three hours for the first 12 hours of operation and then every 12, 24, and 24  
 151 hours. The permeate flux ( $J$ ) and salt rejection rate were calculated using equations 1 and 2,  
 152 respectively. In the Equations,  $V$  denotes the volume of permeate in litres (L), and  $t$  denotes  
 153 the time in hours.  $C_p$  and  $C_f$  represent the salt concentrations in permeate and feed,  
 154 respectively, as determined by the LAQUA PC210 conductivity metre. Each experiment was  
 155 carried out three times, with the average value reported.

$$156 \quad J = \frac{V}{A \times t} \quad (1)$$

$$157 \quad \text{Rejection (\%)} = \left(1 - \frac{C_p}{C_f}\right) \times 100 \quad (2)$$

## 158 3. Results and discussions

### 159 3.1. Physicochemical properties of the GO/CNT-PVA composite membranes

160 A significant challenge in designing and fabricating GO-based membranes is to ensure that  
 161 molecular transport occurs entirely within the nanochannels and would not occur via  
 162 membrane cracks or pores [34]. **Figure S1** shows the surface morphology of the MCE  
 163 substrate. The top-surface morphologies of the GO/CNT-PVA composite membranes are  
 164 shown in **Figure 2a**. Since CNT lack polar functional groups, agglomeration of CNT can be  
 165 observed in the CNT<sub>20</sub> and CNT<sub>20</sub>PVA<sub>0.5</sub> membranes. Both membranes exhibited microscale



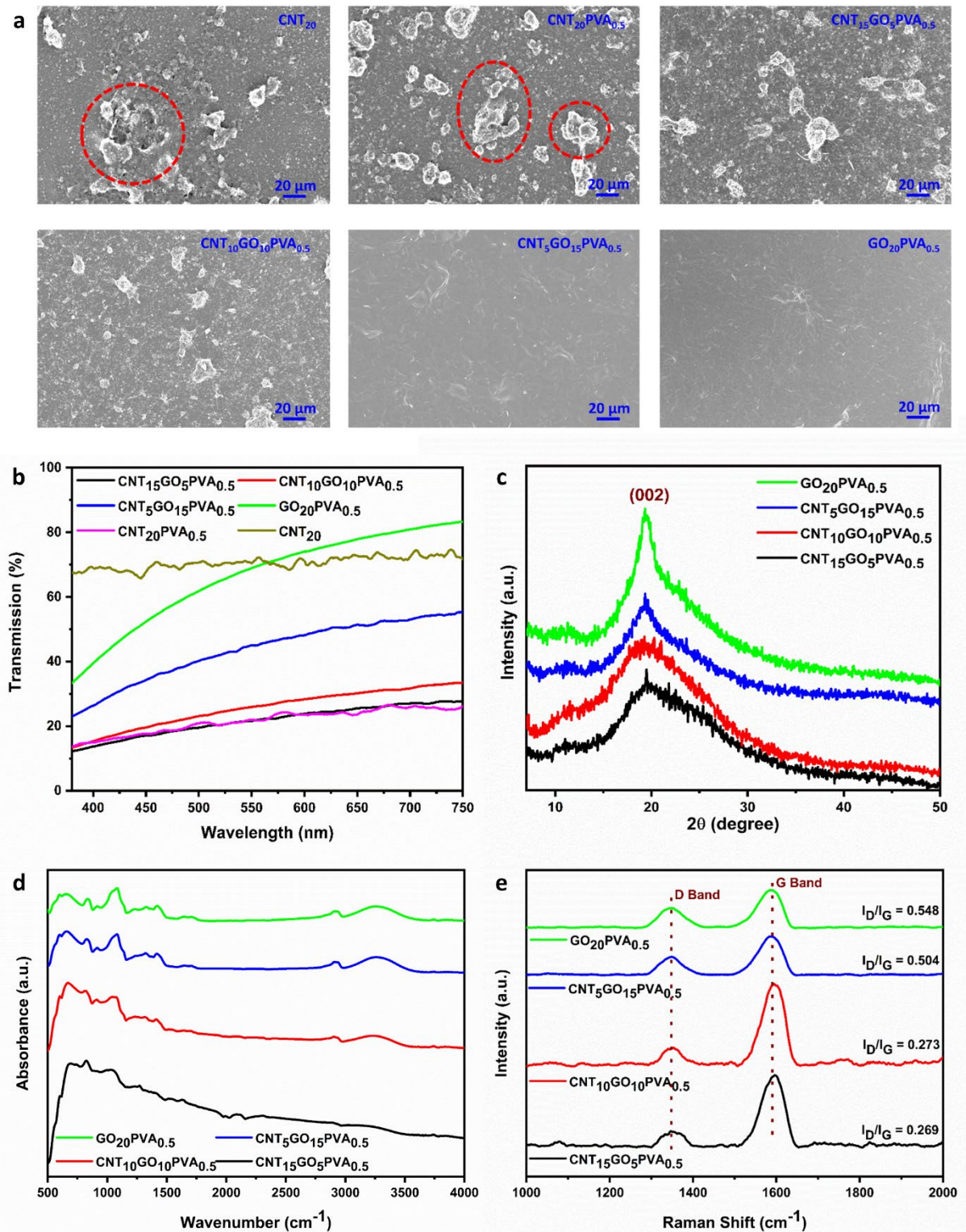
166 defects, indicating a lack of selectivity. Due to the non-uniform coating on CNT<sub>20</sub> and  
167 CNT<sub>20</sub>PVA<sub>0.5</sub> membranes, they were excluded from the performance studies. The surface  
168 morphology of the CNT<sub>5</sub>GO<sub>15</sub>PVA<sub>0.5</sub> membrane is nearly identical to that of the GO<sub>20</sub>PVA<sub>0.5</sub>  
169 membrane, but the GO<sub>20</sub>PVA<sub>0.5</sub> membrane exhibits a few more wrinkles. On the other hand,  
170 CNT<sub>10</sub>GO<sub>10</sub>PVA<sub>0.5</sub> and CNT<sub>15</sub>GO<sub>5</sub>PVA<sub>0.5</sub> membranes exhibited a mixture of morphologies,  
171 including i) a few agglomerated CNT on the top surface and ii) wrinkles caused by the GO and  
172 PVA. The wrinkles on CNT<sub>5</sub>GO<sub>15</sub>PVA<sub>0.5</sub> and GO<sub>20</sub>PVA<sub>0.5</sub> might be due to the trapped air or water  
173 molecules between GO nanosheets during membrane fabrication. The cross-section of all the  
174 prepared membranes is shown in **Figure S3**. It is worth noting that the membrane thickness  
175 significantly impacts the selectivity and permeability characteristics, as a thinner coating layer  
176 promotes high water flux. Although increasing the GO content increased the thickness of  
177 membranes CNT<sub>5</sub>GO<sub>15</sub>PVA<sub>0.5</sub> and GO<sub>20</sub>PVA<sub>0.5</sub>, these membranes still showed slightly higher  
178 water permeability compared to membranes CNT<sub>10</sub>GO<sub>10</sub>PVA<sub>0.5</sub> and CNT<sub>15</sub>GO<sub>5</sub>PVA<sub>0.5</sub>  
179 membranes. The increased water permeability could be due to the positive effect of  
180 increasing the hydrophilicity and improved membrane surface properties that transcended  
181 the negative impact of the increased hydraulic resistance caused by a thicker membrane. This  
182 discrepancy can be attributed to the different ratios of the CNT and GO nanosheets used,  
183 which alter the interaction between water and nanosheets during the drying process, thereby  
184 altering how these nanosheets stack in dried membranes.

185 The CNT/GO-PVA composite membranes were prepared using aqueous suspensions of  
186 CNT/GO-PVA (**Figure S2**). Due to the presence of polar functional groups, a completely  
187 dispersed yellowish-brownish solution was obtained for GO<sub>20</sub>PVA<sub>0.5</sub>. The UV-visible  
188 spectrometer was used to determine the transparency of all coating solutions (**Figure 2b**).  
189 The GO<sub>20</sub>PVA<sub>0.5</sub> solution exhibited greater than 84% transparency in the 380-750 nm  
190 wavelength range. Pristine CNT are hydrophobic and tend to agglomerate in DI water;  
191 therefore, almost a straight line was seen for the CNT<sub>20</sub> solution. However, when GO and PVA  
192 were added, the solution became darker, and thus partial transparency for CNT/GO-PVA  
193 aqueous solutions was observed. This could be due to the Van der Waals interactions  
194 between CNT and PVA, as shown in **Figure 3a** [35]. Additionally, prolonged ultra-sonication of  
195 CNT solution reduces the aspect ratio of CNT, resulting in partial fragmentation of CNT. Thus,  
196 Van der Waals interactions between CNT and PVA, hydrogen bonding between GO and PVA,

197 and donor-acceptor  $\pi$  interactions between GO and CNT contribute to the stability of the  
198 aqueous solution CNT<sub>15</sub>GO<sub>5</sub>PVA<sub>0.5</sub>, CNT<sub>10</sub>GO<sub>10</sub>PVA<sub>0.5</sub>, CNT<sub>5</sub>GO<sub>15</sub>PVA<sub>0.5</sub> and, GO<sub>20</sub>PVA<sub>0.5</sub>. The  
199 typical GO membrane exhibits an intense (001) peak near 10.5 ° and an interlayer spacing of  
200 8.4 Å [36]. The peak for CNT/GO-PVA composite membranes shift to 19.3 ° after prolonged  
201 ultra-sonication and mild annealing during the membrane fabrication process (**Figure 2c**).  
202 Apart from this, all (002) peaks in CNT/GO-PVA composite membranes are weak and have  
203 broad curves compared to the pristine GO membrane. This observation indicates a degraded  
204 crystalline structure following mild annealing, resulting from a partial reduction of polar  
205 functional groups. Hence, these XRD results confirm the structural changes caused by mild  
206 annealing, which further aids in enhanced water permeability.

207 The FT-IR was used to identify changes in chemical bonding in CNT/GO-PVA composite  
208 membranes. The FT-IR spectrum of CNT/GO-PVA composite membranes is shown in **Figure**  
209 **2d**. The broad and stronger peaks for polar functional groups are visible for CNT<sub>10</sub>GO<sub>10</sub>PVA<sub>0.5</sub>,  
210 CNT<sub>5</sub>GO<sub>15</sub>PVA<sub>0.5</sub> and, GO<sub>20</sub>PVA<sub>0.5</sub> membranes, such as hydroxyl (-OH group) vibration peaks at  
211 1435 cm<sup>-1</sup> and 3000-3650 cm<sup>-1</sup>. The broad peak could be attributed to hydrogen bonding  
212 between the polar functional groups of PVA and GO [37]. A less intense peak at 1650 cm<sup>-1</sup>  
213 might be due to the carbonyl group of GO. However, all membranes lack another typical  
214 carbonyl peak at 1720 cm<sup>-1</sup>, which could be due to the partial reduction of GO membranes.  
215 The peaks at 980 cm<sup>-1</sup> and 1370 cm<sup>-1</sup> are attributed to the stretching vibration of the C-O bond  
216 in CNT/GO-PVA composite membranes. Notably, the peaks are weaker than those on GO-  
217 based membranes, owing to the partial reduction of GO during membrane preparation [38].  
218 Mild annealing of GO at 80 °C results in tailored nanosheet spacing while retaining the  
219 majority of the oxygen functionalities of GO. Thus, FTIR indicates that oxygen functional group  
220 linkages are weaker in CNT<sub>15</sub>GO<sub>5</sub>PVA<sub>0.5</sub> and CNT<sub>10</sub>GO<sub>10</sub>PVA<sub>0.5</sub> membranes than in  
221 CNT<sub>5</sub>GO<sub>15</sub>PVA<sub>0.5</sub> and GO<sub>20</sub>PVA<sub>0.5</sub> membranes. Additionally, the acetyl ring exhibits peaks at  
222 2845 and 1110 cm<sup>-1</sup>, corresponding to the stretching vibrations of -CH and C-O-C bonds  
223 (**Figure 3b and c**) [39]. The deconvoluted FTIR spectra confirm the chemical bonding between  
224 GO and PVA for the CNT<sub>5</sub>GO<sub>15</sub>PVA<sub>0.5</sub> membrane (**Figure S4**). These peaks demonstrate the  
225 formation of a covalent bond between PVA and GO. The cross-linking and formation of  
226 covalent bonds between the PVA and GO moieties provide additional stability to the CNT/GO  
227 membrane, allowing it to overcome compaction and hydration effects.

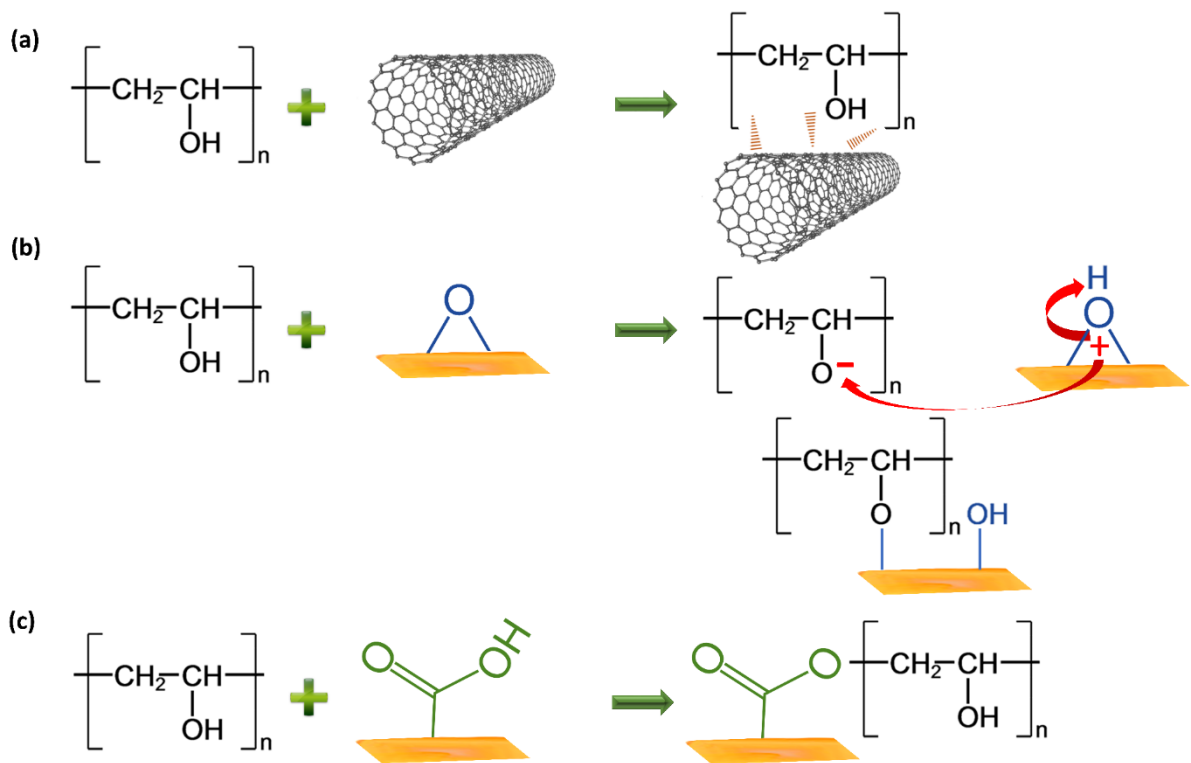
228 The size of ordered domains, bonding nature, and the presence of dopants in the CNT/GO-  
229 PVA composite membranes was investigated using Raman spectroscopy [40]. **Figure 2e** shows  
230 the Raman spectra for CNT/GO-PVA composite membranes. Since membranes are prepared  
231 via pressure-assisted filtration technique, all membranes have a highly ordered structure. The  
232 D and G bands were prominent Raman peaks for all CNT/GO-PVA membranes. The G band  
233 peak at  $1590\text{ cm}^{-1}$  is caused by the C-C bond stretching induced by the  $E_{2g}$  vibrational mode,  
234 whereas defects and disorders cause the D band peak at  $1349\text{ cm}^{-1}$  in the graphite lattice  
235 induced by the  $A_{1g}$  vibrational mode. The relative intensity of the G band is greater for  
236 CNT<sub>10</sub>GO<sub>10</sub>PVA<sub>0.5</sub> and CNT<sub>15</sub>GO<sub>5</sub>PVA<sub>0.5</sub> membranes than for the other membranes, owing to  
237 the low amount of oxygen-containing functional groups. However, the relative intensity of  
238 the D band is greater in CNT<sub>5</sub>GO<sub>15</sub>PVA<sub>0.5</sub> and GO<sub>20</sub>PVA<sub>0.5</sub> due to the presence of more polar  
239 functional groups that create defects at the micro-level. The values of  $I_D/I_G$  for  
240 CNT<sub>15</sub>GO<sub>5</sub>PVA<sub>0.5</sub>, CNT<sub>10</sub>GO<sub>10</sub>PVA<sub>0.5</sub>, CNT<sub>5</sub>GO<sub>15</sub>PVA<sub>0.5</sub>, and GO<sub>20</sub>PVA<sub>0.5</sub> are given 0.269, 0.273,  
241 0.504, and 0.548, respectively. In contrast to standard  $sp^2$  materials, reducing the defects in  
242 GO increases the  $I_D/I_G$  ratio. Hence, the CNT<sub>5</sub>GO<sub>15</sub>PVA<sub>0.5</sub> membrane showed a higher  $I_D/I_G$   
243 ratio compared to CNT<sub>15</sub>GO<sub>5</sub>PVA<sub>0.5</sub> and CNT<sub>10</sub>GO<sub>10</sub>PVA<sub>0.5</sub> membranes. Notably, all CNT/GO-  
244 PVA composite membranes exhibited a transitional behaviour between ordered and  
245 disordered configurations. The CNT<sub>5</sub>GO<sub>15</sub>PVA<sub>0.5</sub> membranes had a Raman spectrum strikingly  
246 similar to that of the GO<sub>20</sub>PVA<sub>0.5</sub> membrane. This indicates that the CNT is distributed  
247 throughout the matrix between the GO layers and around.



248

249 **Figure 2:** Physicochemical characterizations of CNT/GO-PVA composite membranes. (a) Top  
 250 surface morphology of CNT/GO-PVA composite membranes. (b) UV-visible spectra with  
 251 wavelength ranging from 380 to 750 nm. (c) XRD with 2θ ranging from 5 to 50 °. (d) FTIR

252 spectra with wavenumber ranging from 500 to 4000  $\text{cm}^{-1}$ . (e) Raman spectra with Raman shift  
 253 ranging from 1000-2000  $\text{cm}^{-1}$ .



254

255 **Figure 3:** Schematic for the interaction scheme (a) Van der Waals interactions between PVA  
 256 and CNT. (b) and (c) covalent bond formation between PVA and GO.

257 Water contact angle (WCA) studies were performed to determine the wettability of the  
 258 CNT/GO-PVA composite membrane surfaces. The  $\text{CNT}_5\text{GO}_{15}\text{PVA}_{0.5}$  and  $\text{GO}_{20}\text{PVA}_{0.5}$   
 259 membranes showed lower WCA of 44.35 and 42.25, respectively. Hydroxyl, carboxyl, and  
 260 other polar moieties on the membrane surface increase the membrane's hydrophilicity. By  
 261 increasing the amount of CNT in the GO/PVA matrix, the WCA was increased to 48.95 and  
 262 56.42 of the  $\text{CNT}_{10}\text{GO}_{10}\text{PVA}_{0.5}$  and the  $\text{CNT}_{15}\text{GO}_5\text{PVA}_{0.5}$  membranes, respectively. Through Van  
 263 der Waals force and  $\pi$ - $\pi$  stacking interactions, non-polar CNT interacted with the GO/PVA  
 264 matrix and thus occupied the space between the GO nanosheets and their external  
 265 surface. The zeta potential ( $\zeta$ ) describes the charge on the surface of CNT/GO-PVA in their  
 266 aqueous dispersions. It is an important physical parameter that can be used to investigate the  
 267 effect of GO and PVA on the dispersion mechanism and quality of CNT/GO-PVA dispersions.  
 268 **Table 2** shows the measurements of surface  $\zeta$  measurements and water contact angle for  
 269 CNT/GO-PVA composite membranes. For example, the surface  $\zeta$  of  $\text{CNT}_{15}\text{GO}_5\text{PVA}_{0.5}$  was

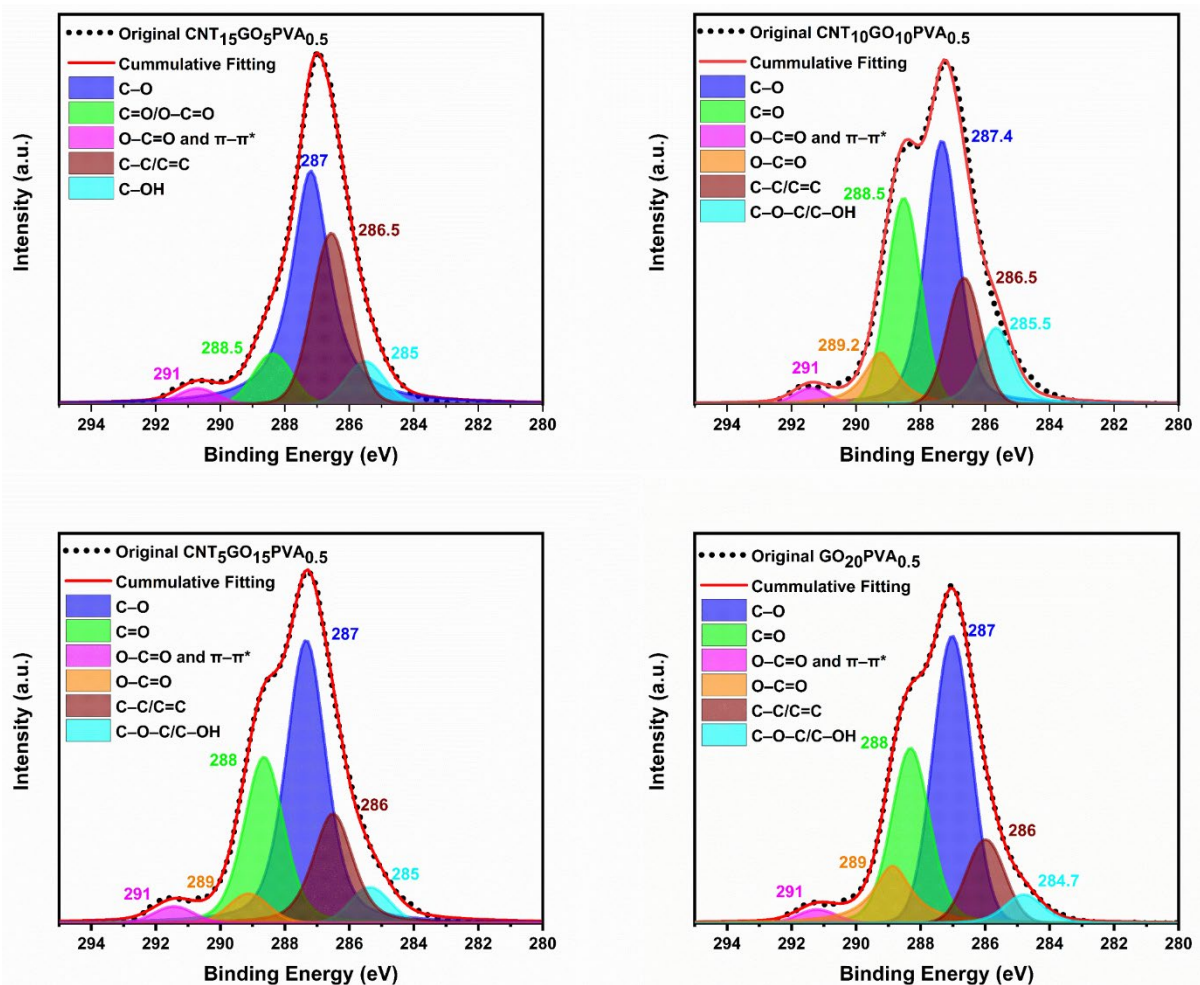
270 reduced to -11.9 mV. The surface  $\zeta$  of the CNT<sub>5</sub>GO<sub>15</sub>PVA<sub>0.5</sub> and GO<sub>20</sub>PVA<sub>0.5</sub> membranes was -  
 271 26.1 and -30.3 mV, respectively, confirming the presence of polar functional groups on the  
 272 membrane surface. However, pristine GO membranes show a surface  $\zeta$  of up to -70 mV but  
 273 suffer mechanical stability [18]. Therefore, PVA was used in this study to improve the stability  
 274 of the CNT/GO membrane. The negative surface  $\zeta$  of all the CNT/GO-PVA composite  
 275 membranes is caused by deprotonation of carboxylic acid (-COOH) and hydroxyl groups (-  
 276 OH) on the membrane surface derived from GO and PVA, respectively. As a result, resonance  
 277 stabilization helps to stabilize the GO and PVA conjugate base [18]. Given this property, that  
 278 resonance enables delocalization, the system's overall energy decreases as its electrons  
 279 occupy a larger volume, thereby stabilizing the system. Whereas CNT can be classified into  
 280 two distinct zones: i) end caps (hemispherical fullerene) and ii) sidewalls (folded graphene  
 281 sheet). Usually, the GO polar functional groups interact with the end caps of CNT, and this  
 282 process is driven by the release of strain energy [41, 42]. Also, the value of the acid  
 283 dissociation constant fall in the range of 3.93-3.96 for GO; as a result, the  $\zeta$  of CNT changes  
 284 with the addition of GO solution [43]. The addition of CNT and PVA in between GO nanosheets  
 285 reduces the availability of polar functional groups on the surface of the composite  
 286 membranes. Thus, the surface  $\zeta$  decreases with an increase in CNT concentration.  
 287 Additionally, the surface  $\zeta$  decreased due to the formation of covalent bonds between the GO  
 288 and PVA moieties, as covalent bond formation consumes the extra electrons during the  
 289 functionalization reaction (**Figure 3b** and **c**). The detailed interaction between CNT, PVA, and  
 290 GO is shown in **Figure 3**.

291 **Table 2:** Surface zeta potential and water contact angle studies of CNT/GO-PVA composite  
 292 membranes.

Membrane Code	Surface zeta potential (mV)	Water contact angle (°)
CNT <sub>5</sub> GO <sub>15</sub> PVA <sub>0.5</sub>	-26.1 ± 0.8	44.35 ± 2.1
CNT <sub>10</sub> GO <sub>10</sub> PVA <sub>0.5</sub>	-16.4 ± 1.3	48.95 ± 1.8
CNT <sub>15</sub> GO <sub>5</sub> PVA <sub>0.5</sub>	-11.9 ± 0.7	56.42 ± 0.5
GO <sub>20</sub> PVA <sub>0.5</sub>	-30.3 ± 1.2	42.25 ± 1.4

293

294 XPS was used to analyse the surface chemistry and chemical state of CNT/GO-PVA composite  
 295 membranes after mild annealing. **Figure 4** shows the deconvoluted C1s spectra of CNT/GO-  
 296 PVA composite membranes, confirming the presence of CNT, GO, and PVA in the matrix. The  
 297 C1s spectra are composed of several characteristics peaks with the typical peaks observed at  
 298 291 eV (O–C=O and  $\pi$ - $\pi^*$ ), 289 eV (O–C=O), 288 eV (C=O), 287 eV (C–O), 286 eV (C–C/C=C),  
 299 and 284 eV (C–O–C/C=O) confirms the presence of oxygen functionality in all membranes  
 300 [44]. Since less GO was used in the CNT<sub>15</sub>GO<sub>5</sub>PVA<sub>0.5</sub> membrane, it contained a higher  
 301 concentration of graphitic carbon, primarily C–C, as compared to others. The intensity of the  
 302 sp<sup>2</sup> and sp<sup>3</sup> hybridized graphitic carbon (C–C) peak (286 eV) decreases in the following order  
 303 CNT<sub>15</sub>GO<sub>5</sub>PVA<sub>0.5</sub> < CNT<sub>10</sub>GO<sub>10</sub>PVA<sub>0.5</sub> < CNT<sub>5</sub>GO<sub>15</sub>PVA<sub>0.5</sub> < GO<sub>20</sub>PVA<sub>0.5</sub>. This could be because of  
 304 the intercalation of CNT between consecutive GO nanosheets. Additionally, the  
 305 CNT<sub>15</sub>GO<sub>5</sub>PVA<sub>0.5</sub> membrane had a lower intensity of the oxidised carbon peak due to the low  
 306 concentration of GO in the matrix. Further, the peak for oxidized carbon at 287 eV (C–O) and  
 307 288 eV (C=O) of CNT<sub>5</sub>GO<sub>15</sub>PVA<sub>0.5</sub> membrane is identical to GO<sub>20</sub>PVA<sub>0.5</sub> membrane.



308

309 **Figure 4:** Deconvoluted C1s spectra of CNT/GO-PVA composite membranes.

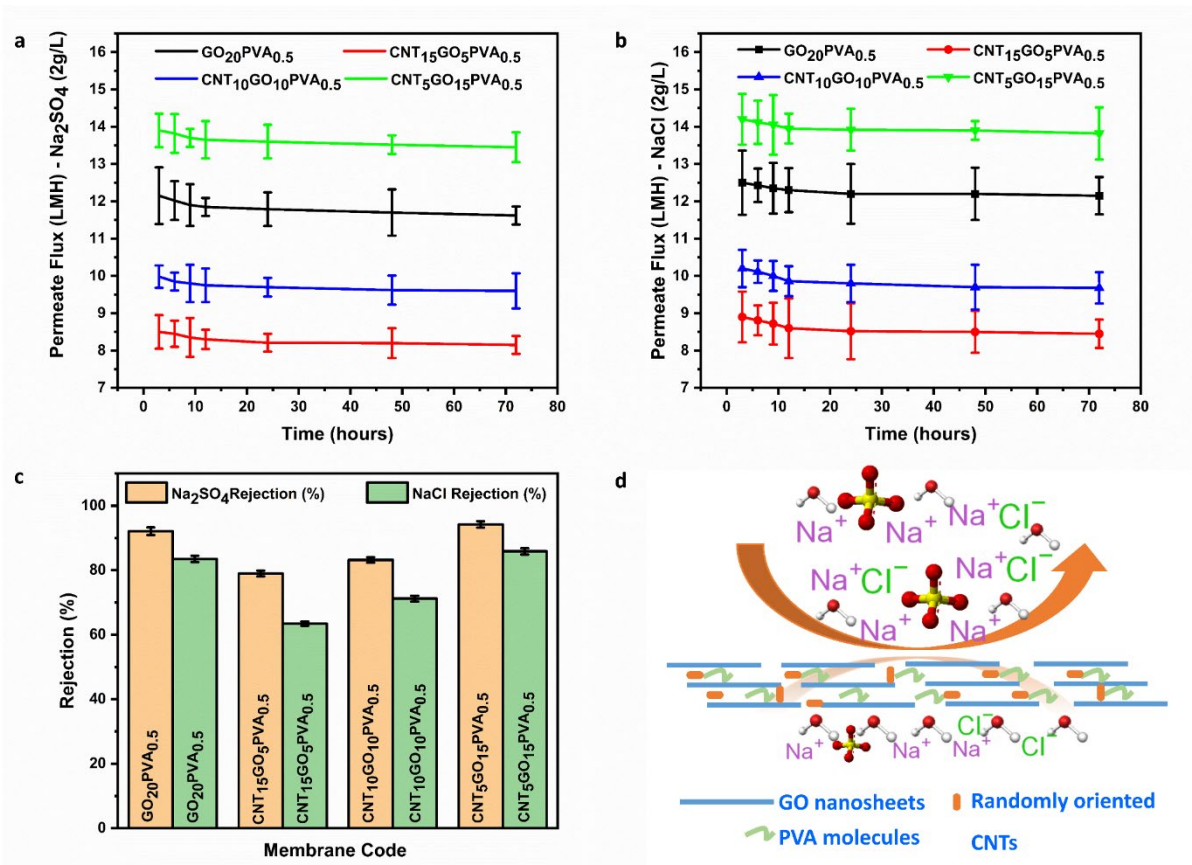
### 310 **3.2. Performance Studies**

311 The permeability and selectivity of CNT/GO-PVA composite membranes for salt rejection  
312 were investigated using Na<sub>2</sub>SO<sub>4</sub> and NaCl feed solutions at 2000 mg/L concentration. The  
313 permeation rate for Na<sub>2</sub>SO<sub>4</sub> and NaCl solutions are shown in **Figures 5a** and **5b**, respectively.  
314 Water permeation rate for membranes is in the following order: CNT<sub>15</sub>GO<sub>5</sub>PVA<sub>0.5</sub> (8.9-8.15  
315 LMH) < CNT<sub>10</sub>GO<sub>10</sub>PVA<sub>0.5</sub> (10.2-9.6 LMH) < GO<sub>20</sub>PVA<sub>0.5</sub> (12.5-11.62 LMH) < CNT<sub>5</sub>GO<sub>15</sub>PVA<sub>0.5</sub>  
316 (14.2-13.45 LMH). The rapid water transport in all membranes is due to the combined effect  
317 of CNT, GO, and PVA. CNT's hydrophobic walls accelerate the flow of water molecules through  
318 the tube by causing them to "slip" whenever they come in contact with the walls [45, 46]. As  
319 the water molecules pass through the tube, they form a chain-like network with one another  
320 due to the presence of strong intramolecular hydrogen bonding [47, 48]. This improves the  
321 flow of water through the tubes and causes water molecules to be dragged forwards by the  
322 one ahead of them. Thus, a higher permeation rate is observed for the CNT<sub>5</sub>GO<sub>15</sub>PVA<sub>0.5</sub>  
323 membrane compared to the GO<sub>20</sub>PVA<sub>0.5</sub> membrane. The combined effect of CNT and GO helps  
324 to get the desired permeation flux. In contrast, water transport in GO membranes occurs via  
325 the Grotthuss mechanism due to large oxygen-containing functional groups. Unlike CNT,  
326 water molecules follow a tortuous path between GO layers [10]. It is worth noting that a slight  
327 decrease in water flux was observed for all the membranes since the salt rejection  
328 experiments were performed using 2000 ppm of Na<sub>2</sub>SO<sub>4</sub> and NaCl.

329 The rejection percentages for Na<sub>2</sub>SO<sub>4</sub> and NaCl solutions are shown in **Figure 5c**. CNT/GO-PVA  
330 composite membranes rejects Na<sub>2</sub>SO<sub>4</sub>, and NaCl ions in the following decreasing order:  
331 CNT<sub>15</sub>GO<sub>5</sub>PVA<sub>0.5</sub> < CNT<sub>10</sub>GO<sub>10</sub>PVA<sub>0.5</sub> < GO<sub>20</sub>PVA<sub>0.5</sub> < CNT<sub>5</sub>GO<sub>15</sub>PVA<sub>0.5</sub>. The highest rejection  
332 rates of 94.2% and 85.86%, respectively, for Na<sub>2</sub>SO<sub>4</sub> and NaCl, were achieved with the  
333 CNT<sub>5</sub>GO<sub>15</sub>PVA<sub>0.5</sub> membrane. In contrast, pristine GO<sub>20</sub>PVA<sub>0.5</sub> membrane rejection rate was  
334 92.1% for Na<sub>2</sub>SO<sub>4</sub> and 83.5% for NaCl ions. The desalination performance of CNT/GO-PVA  
335 composite membranes (**Figure 5d**) is mainly attributed to i) size-exclusion mechanism, ii)  
336 electrostatic interactions between negatively charged CNT/GO-PVA composite membranes  
337 and feed salt solutions, and iii) ion adsorption on the surface of CNT/GO-PVA composite  
338 membranes.



339 In this study,  $\text{Na}_2\text{SO}_4$  has a higher rejection rate than  $\text{NaCl}$  for two primary reasons that may  
 340 seem counterintuitive. Firstly,  $\text{Na}_2\text{SO}_4$  has a higher molecular weight, and the sulphate ion  
 341 ( $\text{SO}_4^{2-}$ ; 0.258 nm) has a larger ionic radius than the chloride ( $\text{Cl}^-$ ; 0.175 nm) ion. Thus,  
 342 technically, it is more difficult for the  $\text{SO}_4^{2-}$  to pass through the membrane. Second, the  
 343 membranes are negatively charged, as shown in surface zeta potential measurements, and  
 344 the  $\text{SO}_4^{2-}$  has a greater negative charge than the  $\text{Cl}^-$ . Thus, long-range interactions such as  
 345 electrostatic repulsions between the negatively charged  $\text{SO}_4^{2-}$  and the negatively charged  
 346 membrane surface are higher than those with  $\text{Cl}^-$  ion. Similar results were reported by Hung  
 347 et al. for GO-graphene membranes [18]. The addition of graphene improved the water  
 348 permeability of the GO membrane and salt rejection in the following order  $\text{NaCl} < \text{magnesium}$   
 349  $\text{chloride} (\text{MgCl}_2) < \text{magnesium sulphate} (\text{MgSO}_4) < \text{Na}_2\text{SO}_4$ .



350

351 **Figure 5:**  $\text{Na}_2\text{SO}_4$  (a), and  $\text{NaCl}$  (b) flux of CNT/GO-PVA composite membranes. (c) The  
 352 rejection rate of  $\text{Na}_2\text{SO}_4$  and  $\text{NaCl}$  for CNT/GO-PVA composite membranes. (d) Illustration for  
 353 the desalination performance of CNT/GO-PVA composite membranes.

354 **Table 3** shows the comparison between CNT/GO-PVA composite membranes and previously  
355 reported GO-based membranes. Parsamehr and colleagues cross-linked GO with  
356 polyethyleneimine (PEI) to improve the membrane's stability and achieved a rejection rate of  
357 37.5% for NaCl [49]. Similarly, tannic acid (TA), 1-Ethyl-3-(3-dimethylaminopropyl)  
358 carbodiimide (EDC), and N-Hydroxysuccinimide (NHS) are added to GO to improve separation  
359 performance [49, 50]. We previously investigated the effect of molybdenum disulphide as a  
360 nanospacer and PVA as a cross-linker on NaCl rejection and achieved up to 89 % rejection  
361 [11]. Additionally, the low permeability of 4.19 LMH for GO/MoS<sub>2</sub>-PVA membranes precludes  
362 application at a larger scale [11]. Recently, Li et al. investigated the effect of annealing on GO  
363 membranes and concluded that mild annealing enables more ordered laminar channels in GO  
364 membranes. Additionally, the authors reported a high permeability of 29.48 LMH and a  
365 moderate rejection for Na<sub>2</sub>SO<sub>4</sub> of 57.73% [51]. In another study, researchers used single-  
366 walled CNT (SWCNT) between GO nanosheets achieved a 97.5% rejection rate of an organic  
367 dye. However, the operation time and membrane stability remained an issue [30]. Although  
368 numerous simulation studies confirmed carbon nanotubes' superior desalination  
369 performance, experimental validation is still pending [46, 52]. In the present study, optimized  
370 CNT is used as a nanospacer to increase permeability up to 14.2 LMH, with a high rejection  
371 rate of 94.2% and 85.86% of Na<sub>2</sub>SO<sub>4</sub> and NaCl, respectively. **Table 3** shows that  
372 CNT<sub>5</sub>GO<sub>15</sub>PVA<sub>0.5</sub> membrane in this study achieved the highest rejection rate and moderate  
373 permeation flow rate.

374 Overall, the CNT/GO-PVA membranes showed over 85.86% rejection of NaCl, the ionic radii  
375 of Na<sup>+</sup> (0.102 nm) and Cl<sup>-</sup> (0.175 nm). The membranes are also expected to have higher  
376 rejection for ions of larger ionic radii, such as sulfate. In other words, the membranes will  
377 exhibit higher rejection to divalent or large molecular weight ions that the membrane can  
378 reject by size exclusion or electrostatic repulsion. Notably, a lower rejection rate was  
379 observed for NaCl than Na<sub>2</sub>SO<sub>4</sub> due to the higher ionic radii of sulfate anion (SO<sub>4</sub><sup>2-</sup>) compared  
380 to chloride ion (Cl<sup>-</sup>). Additionally, the SO<sub>4</sub><sup>2-</sup> anion exhibits greater electrostatic repulsion with  
381 CNT/GO-PVA composite membranes than the Cl<sup>-</sup> anion does due to the additional negative  
382 charge. Therefore, the selectivity of CNT/GO-PVA composite membranes is due to the  
383 combined effect of molecular size and charge density.

384 **Table 3:** Comparison of CNT/GO-PVA composite membrane performance with others  
 385 reported in the literature.

Membrane code	Substrate	Permeability (LMH)	Rejection	Reference
Pristine GO	CA	10	37.5% NaCl	[49]
Activated GO-PEI	CA	7	55% NaCl	[49]
GO/MoS <sub>2</sub> -PVA	CA	4.19	89.93% NaCl	[11]
TA-GO-PEI	CA	15	64% NaCl	[50]
GO-PEI (layer-by-layer)	PP	4.2	38% NaCl	[53]
Base-Refluxing Reduced GO	MCE	22.82	40% NaCl	[54]
Mild annealed GO	PES	29.48	57.73% Na <sub>2</sub> SO <sub>4</sub>	[51]
Hybrid rGO-CNT	AAO	20-30	97.13% MO	[32]
FCNT-GONR	polymeric support	138	100% organic dyes	[55]
Hybrid rGO-GONR	Nylon support	161-327	95.13% MO >99% MR	[56]
CNT <sub>5</sub> GO <sub>15</sub> PVA <sub>0.5</sub>	MCE	13.45- 14.2	94.2% Na <sub>2</sub> SO <sub>4</sub> 85.86% NaCl	Present work
GO <sub>20</sub> PVA <sub>0.5</sub>	MCE	11.62- 12.5	92.1% Na <sub>2</sub> SO <sub>4</sub> 83.5% NaCl	Present work

386 GO: graphene oxide; PEI: polyethyleneimine; MoS<sub>2</sub>: molybdenum disulfide; PVA: polyvinyl  
 387 alcohol; TA: tannic acid; CNT: carbon nanotube; CA: cellulose acetate; PP: polypropylene; MCE  
 388 mixed cellulose esters; AAO: anodic aluminium oxide; GONR: graphene oxide nanoribbon;  
 389 FCNT: functionalized carbon nanotube; PES: polyethersulfone; NaCl: sodium chloride; Na<sub>2</sub>SO<sub>4</sub>:  
 390 sodium sulphate; MR: methyl orange and MO: methyl orange

#### 391 4. Conclusion

392 In conclusion, the pressure-assisted filtration technique successfully prepared stable covalent  
 393 cross-linked CNT/GO-PVA composite membranes. The prepared membranes had excellent  
 394 performance for the salt rejection with permeation rate at low operating pressure. Covalent  
 395 cross-linkage between GO and PVA prevents the GO nanosheets from swelling and

396 disintegration. In contrast, mild annealing and CNT improved the CNT/GO-PVA membranes  
397 water permeability. FTIR, Raman, XRD, XPS, and surface zeta potential analysis discussed  
398 chemical bonding and structural properties. CNT/GO-PVA composite membranes are highly  
399 stable under dead-end filtration tests for 72 hours with enhanced permeability and  
400 selectivity. CNT<sub>5</sub>GO<sub>15</sub>PVA<sub>0.5</sub> membrane achieved over 94% rejection rate to Na<sub>2</sub>SO<sub>4</sub> and 13.45  
401 LMH water flux, and for the NaCl, the rejection rate was 85.86%, and water flux was 14.2  
402 LMH. The combination of 1D-CNT and 2D-GO nanosheets proved to be an attractive strategy  
403 to prepare next-generation membranes.

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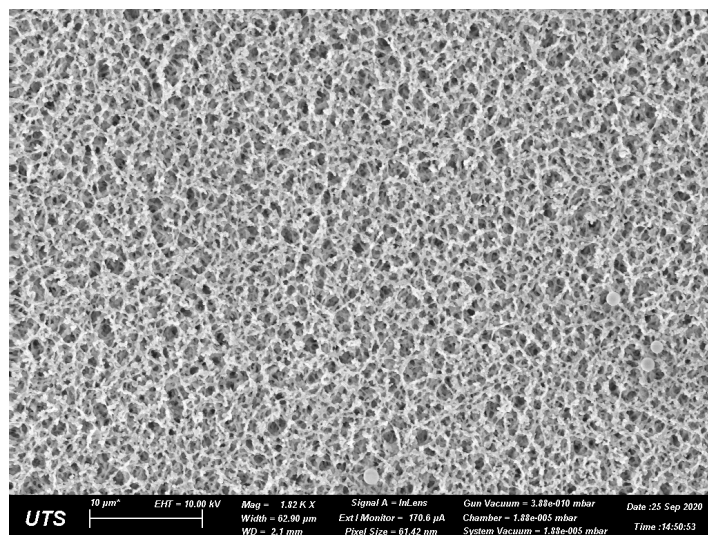
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### Supplementary Information

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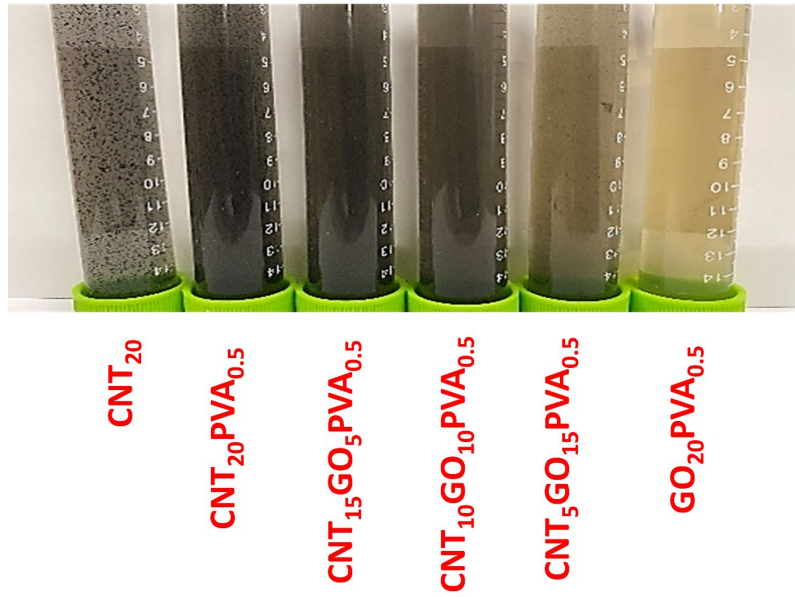


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**Figure S1:** FESEM image for hydrophilic mixed cellulose esters (MCE) substrate.



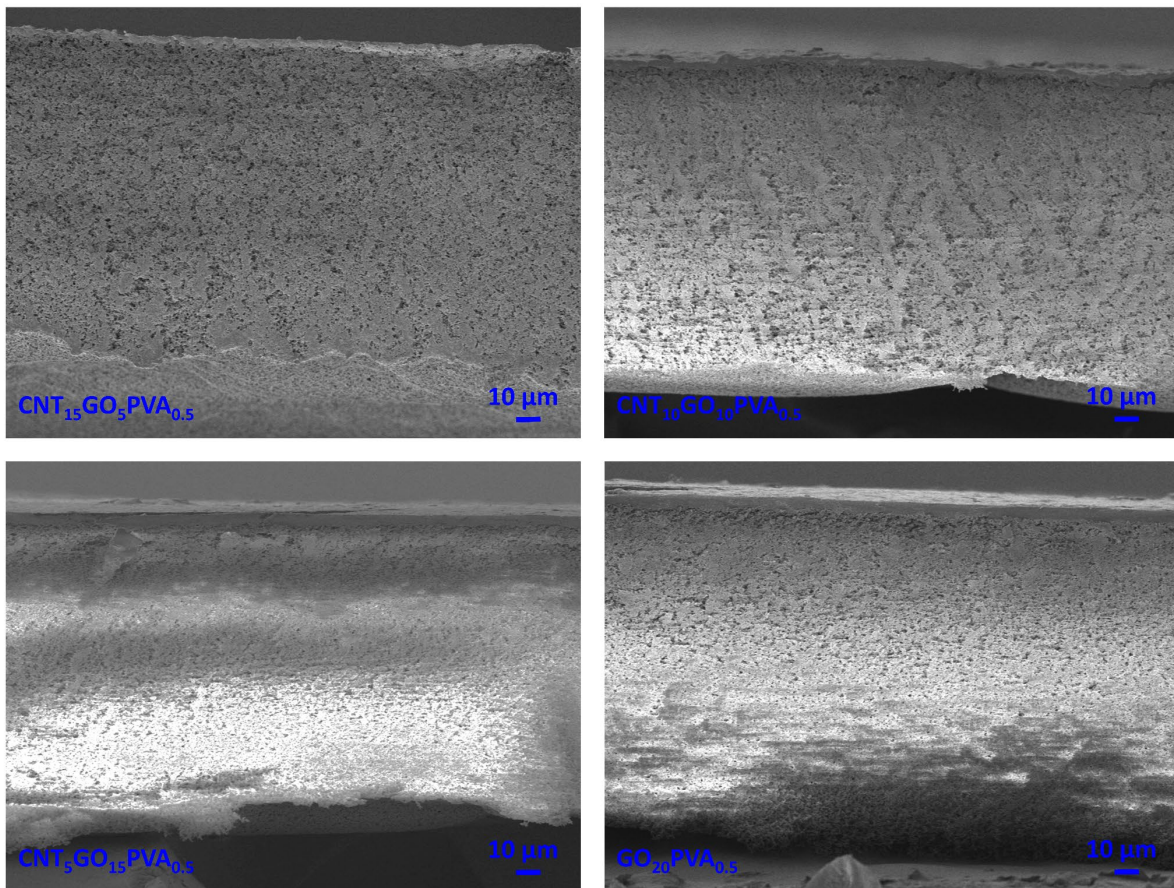


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561 **Figure S2:** Aqueous suspensions of CNT/GO-PVA used for the membrane fabrication.

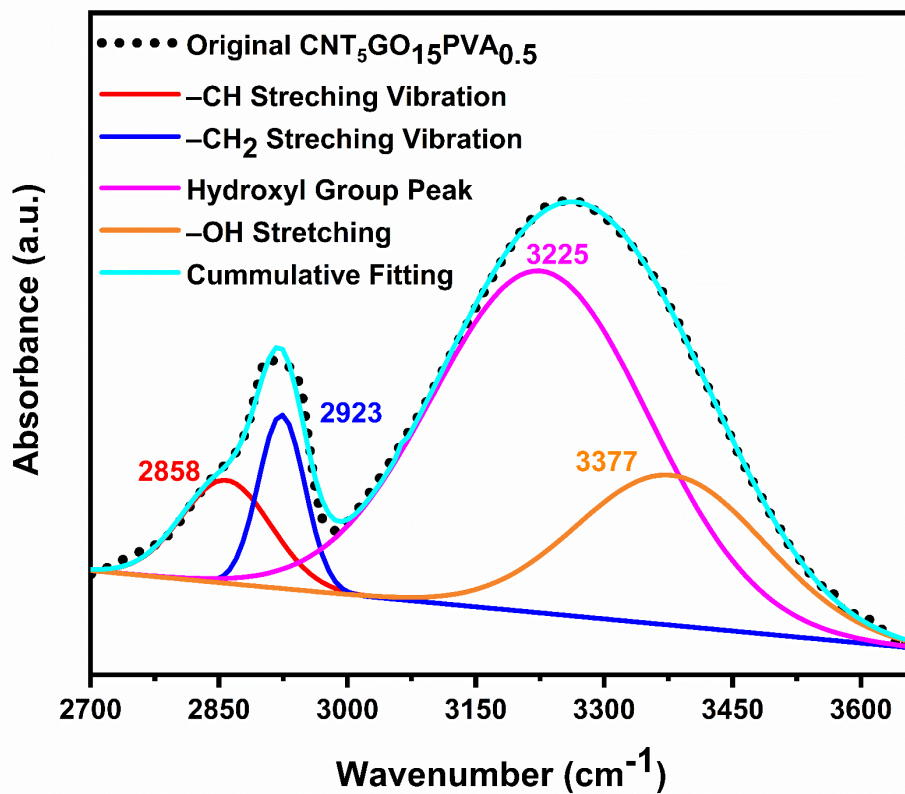
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565 **Figure S3:** Cross-sectional morphology of CNT/GO-PVA composite membranes.



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**Figure S4:** Deconvoluted FTIR spectra of CNT<sub>5</sub>GO<sub>15</sub>PVA<sub>0.5</sub> membrane.