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1 **Aging microplastics in wastewater pipeline networks and**
2 **treatment processes: physicochemical characteristics and Cd**
3 **adsorption**

4
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18 **Abstract**

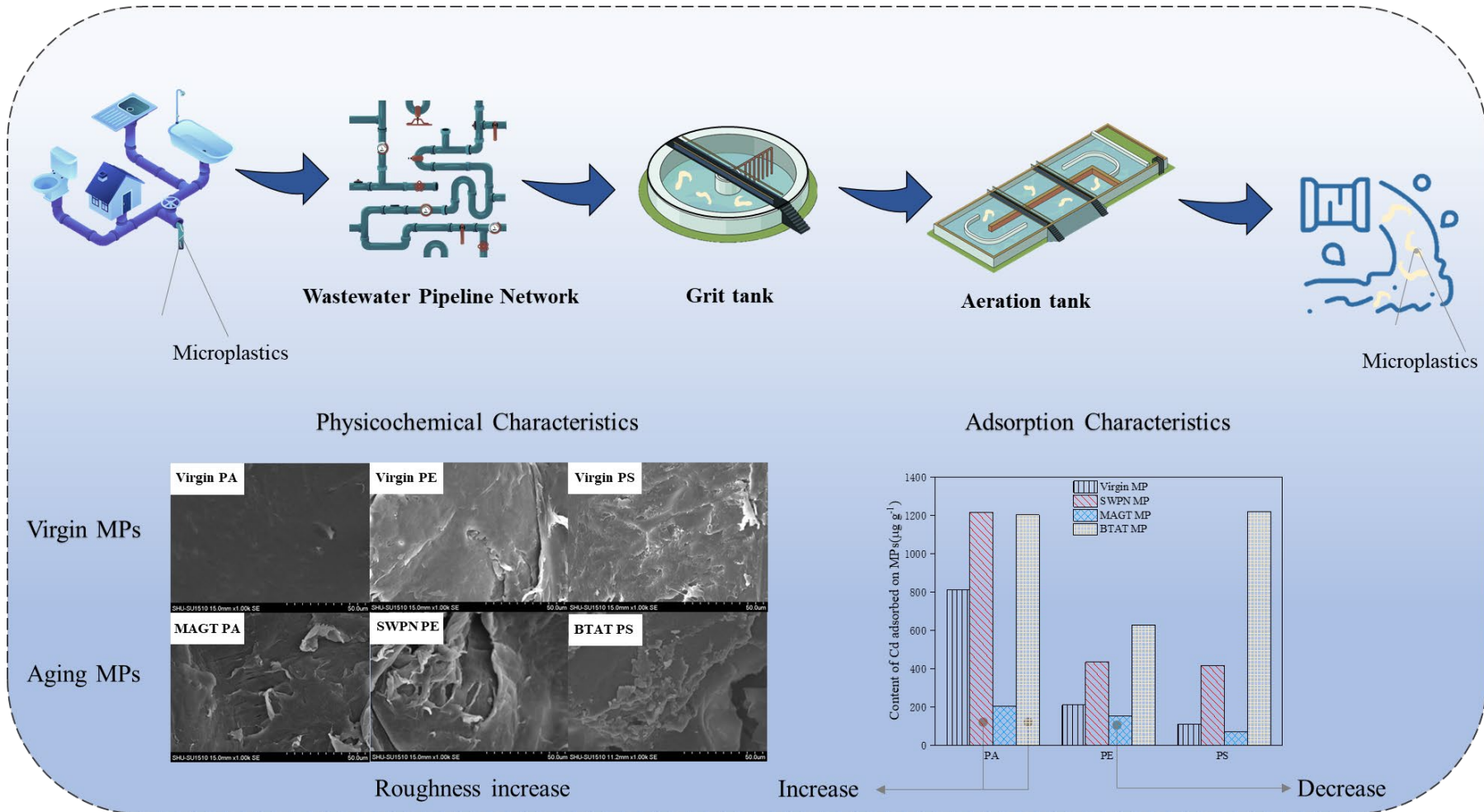
19 Despite a wealth of information on the removal efficiency of MPs during
20 wastewater treatment processes (WWTPs), little attention has been paid to how
21 WWTPs may affect the MPs physicochemical characteristics. In this study, changes in
22 physicochemical characteristics of three MPs, i.e. polyamide (PA), polyethylene (PE)
23 and polystyrene (PS) through the wastewater pipeline, grit and biological aeration tanks
24 were investigated. The results show that sulfidation in the pipeline (SWPN) causes a
25 wavier MP surface, and denser holes are found on the PA surface after biological
26 treatment in aeration tank (BTAT), but the MP surface is insignificantly affected by the
27 mechanical abrasion in grit tank (MAGT), compared with the virgin MP. The MP zeta
28 potentials decrease after treated by SWPN and BTAT, thus causing an increase in the
29 MP adsorption potentials of Cd. The influence on the MP adsorption potentials is higher
30 from BTAT than from SWPN, followed by MAGT, and all treatments lead to the change
31 in the MP adsorption mode from monolayer to multi-layer. 2D-FTIR correlation
32 spectroscopy demonstrates that the N-H bond in the PA plays a more important role
33 than C-H bond in the adsorption of Cd, . The findings provide new insights into the
34 effect of WTPs on the MP aging and physicochemical characteristics.

35 **Keywords:** microplastics; wastewater treatment plant; wastewater treatment; aging
36 characteristics; adsorption potential

37

38

Graphic Abstract



39 **Highlights**

- 40 ➤ Changes in MP characteristics via three treatment processes were investigated
- 41 ➤ The crack and ripples appear on the MP surface after wastewater treatment
- 42 ➤ The SWPN and BTAT treatments cause a decrease in the MP zeta potentials
- 43 ➤ Biological treatment has the highest effect on MP adsorption potentials of Cd
- 44 ➤ N-H bond in PA plays a more important role than C-H bond in Cd adsorption

45

46 **1. Introduction**

47 Microplastics (MPs), often defined as plastic particles <5 mm, as emerging
48 pollutants of environmental concern have gradually raised attention worldwide since
49 they pose threat to aquatic species as well as human beings (Sun et al., 2019; Wang et
50 al., 2016). MPs can be detected in all environmental systems and biota, such as rivers,
51 lakes, oceans, sediments, marine animals and soils (Andrady 2011, Eerkes-Medrano et
52 al. 2015, Rillig 2012, Van Cauwenberghe et al. 2013). MPs may carry organic pollutants
53 as well as heavy metal compounds and transfer them into living organisms, which could
54 have serious toxic effects (Li et al. 2019b). The persistent organic pollutants (POPs)
55 adsorbed to plastics can reach up to 1 million times higher concentrations than ambient
56 and these compounds can be further desorbed inside organisms, exasperating POPs
57 bioaccumulation at higher trophic levels (Browne et al. 2013, Sun et al. 2019, Wang et
58 al. 2018).

59 Field investigations showed that the MPs in the natural environment are weathered
60 by environmental factors like wind, sunlight, mechanical abrasion, chemical oxidation
61 and biological degradation in natural environments (Liu et al. 2019, Song et al. 2017,
62 Ter Halle et al. 2016), and the altered (aged) MPs have greater adsorption of pollutants
63 than virgin (untreated) MPs (Holmes et al. 2014, Turner and Holmes 2015, Wijesekara
64 et al. 2018, Zhang et al. 2018). Song et al. (2017) reported that the combination of UV
65 exposure duration and mechanical abrasion leads to the fragmentation of MPs into
66 undetectable submicron particles. Liu et al. (2019) found that advanced oxidation

67 processes such as heat-activated $K_2S_2O_8$ and Fenton treatments are able to accelerate
68 the MP aging reactions. Iniguez et al. (2018) revealed a clear loss of elasticity and an
69 increase in the rigidity of four types of plastics after UV irradiation.

70 In contrast to the natural environments, wastewater treatment plant (WWTP) as a
71 reinforced artificial treatment system might produce similar and even more serious
72 effects on the physicochemical characteristics of MPs (Narancic et al. 2018). Until now,
73 WWTPs are focal points in concentrating large amounts of MPs from urban sources
74 (Freeman et al. 2020). The removal efficiency of MPs after physical and biological
75 progress has been reported in a large number of literature (Blair et al. 2019, Carr et al.
76 2016, Dubaish and Liebezeit 2013, Lares et al. 2018, Talvitie et al. 2017). Few studies
77 have paid attention to the aging behavior and physicochemical changes (e.g. adsorption
78 potentials) of the MPs through the WWTPs (Kelkar et al. 2019). In fact, the MPs
79 derived from the personal care and cosmetic products and washing wastewater have
80 gone through a complex wastewater pipeline before entering the WWTP. There is
81 usually an anaerobic environment in the pipeline network and anaerobic microbial
82 processes are responsible for the formation of reductive compounds such as hydrogen
83 sulfide (H_2S). This hypothesis is that the pristine characteristics of the MPs in
84 wastewater are changed under the chemical effects of the reductive groups.

85 It is well known that the general processes of wastewater treatment include
86 primary and secondary treatments. Some researchers reported that the MPs after
87 wastewater treatment have the distinctive characteristics compared to the primitive

88 MPs. The processes of mixing, pumping or bubbling the wastewater in the “grit and
89 grease” removal stage might bring the mechanical abrasion to the MPs (Li et al. 2019b).
90 The use of treatment processes involving materials harder than MPs such as rapid sand
91 filtration (RSF) can induce the fragmentation of MPs (Enfrin et al. 2019). The
92 fragmentation of MPs into NPs by WWTPs increased the number of NPs/MPs in water
93 by one order of magnitude (Enfrin et al. 2019). Meanwhile, enormous amounts of
94 microorganisms in the activated sludge may cause biological degradation of the MPs,
95 and then change their physicochemical properties in the aeration tank. Zubris and
96 Richards (2005) found that the MPs in the sewage sludge have a high degree of wear
97 or erosion and become fragile compared to the industrially produced nascent MPs.
98 Mahon et al. (2017) implied that anaerobic digestion process may reduce the MP
99 abundances due to the microbial breakdown polymers through the activity of
100 exoenzymes. In addition, high content of organic matter (e.g. humic acid) in wastewater
101 might cause an change in the structures of MPs (Chen et al. 2018). Li et al. (2019a)
102 reported that the adsorption potential of sludge-based MPs is much higher than that of
103 the virgin MPs. The results imply that the wastewater treatment processes can exert a
104 significant influence on the MP physicochemical characteristics and adsorption
105 potentials. However, the specific effect of various WWTPs on the MP properties have
106 not yet been investigated in detail under the controlled conditions.

107 In this study, three potential effects on MP physicochemical characteristics were
108 simulated during the processes that the MPs enter into and then pass through the

109 WWTPs, i.e. sulfidation in wastewater pipeline network (SWPN), mechanical abrasion
110 in grit tank (MAGT) and biological treatment in aeration tank (BTAT). Then, the effects
111 were evaluated using various techniques, such as scanning electron microscopy (SEM),
112 Fourier transform infrared spectroscopy (FTIR), element analysis, zeta potential,
113 adsorption potentials, and 2D FTIR correlation spectroscopy (2D- FTIR COS). The
114 study can provide a theoretical support to understand environmental behavior and risk
115 of wastewater-based MPs before entering the natural environment in terms of the MP
116 aging characteristics in the WWTPs.

117

118 **2. Materials and methods**

119 **2.1 Materials and reagents**

120 Virgin MPs, i.e. polyamide (PA), polyethylene (PE) and polystyrene (PS) ranging
121 from 150 to 300 μm were purchased from the Micro Powders, Inc., Shanghai, China.
122 Cadmium chloride ($\text{CdCl}_2 \cdot 2.5\text{H}_2\text{O}$) was 99.0% pure and obtained from the Sinopharm
123 Group Co. Ltd, Shanghai, China. Metal stock solutions of 1000 mg L^{-1} were prepared
124 using deionized water. Standard metal solution was purchased from the Aladdin
125 Industrial Corporation, Shanghai, China.

126 **2.2 Simulating the effect of wastewater pipeline network and treatment processes**

127 **Sulfidation in wastewater pipeline network (SWPN).** The SWPN effect on the
128 MPs was investigated according to the literature (Kent et al. 2014). Briefly, the ACS
129 grade sodium sulfide nonahydrate (Aladdin reagent) was dissolved in deionized water.

130 5 mmol L⁻¹ sodium bicarbonate buffer was added to the sulfide solution to raise the pH
131 value to 8.6 or higher to limit the effect of H₂S volatilization. All solutions were stored
132 at room temperature (~22 °C) and placed in the dark. In this experiment, 0.1 g of each
133 MP was weighed into a 30 mL glass tube and immersed in 20 mL of 15 mmol L⁻¹ Na₂S
134 solution for 2 days, and then collected for the following analysis. Each treatment was
135 carried out in triplicate.

136 **Mechanical abrasion in grit tank (MAGT).** SiO₂ was used as a representative
137 grit. Both 0.1 g each MP and 0.8 g SiO₂ were added to a glass tube at a mass ratio of
138 1:8, and 20 mL of the configured domestic sewage was added. The glass tubes were
139 flipped and stirred for 24 h. After that, the MPs were extracted for the following analysis.
140 Each treatment was carried out in triplicate.

141 **Biological treatment in aeration tank (BTAT).** The simulated aeration tank was
142 performed in a sequencing batch reactor (SBR) reactor. The reactor body was made of
143 plexiglass with an effective volume of 6 L, as shown in Figure S1 of Supporting
144 Information (SI). Injection and discharge of the wastewater were carried out by a
145 peristaltic pump. The reactor temperature was kept at 25±1 °C. The aeration pump was
146 used for aeration, so that the dissolved oxygen of the system was held at 2-6 mg L⁻¹.
147 The artificial sewage was prepared according to the Table S1 (SI). The SBR preparation
148 and sludge domestication were shown in the SI.

149 1 g of each MP was added to a 2 L of conical flask with the 300 mL domesticated
150 sludge and 700 mL artificial sewage. A running cycle of the SBR flask was 8 h, in which

151 water inflow was carried out for 1 h, aeration for 4 h, settlement for 1 h, drainage for 1
152 h, and idle for 1 h. The experiment was continuously operated for 14 d. After that, the
153 MPs were extracted for the following analysis, and the activated sludge were collected
154 for the microbial community analysis. Each treatment was carried out in triplicate.

155 **2.3 MP extraction and analysis**

156 The MP extraction was conducted according to the density separation method
157 reported in our previous work (Li et al. 2018b). MP morphology was measured using
158 scanning electron microscopy (SEM, Hitachi SU-1500, Hitachi High Technologies
159 Corp., Tokyo, Japan). FTIR spectra of the MPs were determined with a FTIR
160 spectrometer (Nicoq 380 MX, Thermo Fisher Scientific, MA, USA). Elemental
161 analysis of the MPs for C, H, N and S was conducted using a macro elemental analyzer
162 (Vario Micro cube, Germany). Oxygen content was determined by difference:
163 $O\% = 100 - (C + H + N + S) \%$. The Zeta potential of MPs was measured by Zetasizer
164 (Malvern Instru, Ltd), before the particle suspensions were ultra-sonicated overnight.

165 **2.4 Batch adsorption experiments**

166 The MP adsorption test was carried out according to the methods described in our
167 previous work (Li et al. 2019a). Cd was used to estimate the changes in adsorption
168 potentials of the MPs for heavy metal pollutants after different treatment stages. The
169 adsorption was conducted in centrifuge tubes, each of which contained 0.05 g MP
170 particles and 5 mL metal solution of 10 mg L^{-1} Cd. All metal solutions were prepared
171 by diluting stock solutions with deionized water and adjusting the pH value with 0.1

172 mol L⁻¹ HCl and 0.1 mol L⁻¹ NaOH. The tubes were placed on an end-over-end shaker
173 at 30 rpm at room temperature for 24 h. The control group was made in the same metal
174 solution using the same procedure but without MP particles. Each test including the
175 control was run in triplicate.

176 To further investigate adsorption isotherm of the MPs to Cd, the Cd concentrations
177 were set to 1, 2, 3, 4, 5, 10, 20 and 40 mg L⁻¹ as required, respectively. After 24 h of
178 sorption, the MP particles were extracted, and the solutions were filtered using 0.45 µm
179 membrane filter. The metal concentrations in the filtrates were measured using
180 inductively coupled plasma optical emission spectrometer (ICP-OES), and the metal
181 contents adsorbed on the MPs were calculated by determining the difference between
182 the control and sample filtrate. Detailed description of the ICP-OES analysis is shown
183 in the SI.

184 **2.5 2D-FTIR COS analysis of MPs Cd interactions**

185 The MP particles that adsorbed different Cd concentration were dried for the 2D
186 FTIR COS analysis, to further reveal the mechanism that these treatments affected the
187 Cd adsorption on MPs to. The FTIR spectra were normalized by summing the
188 absorbance from 4000–400 cm⁻¹ and multiplying by 1000 (Li et al. 2015a, Li et al.
189 2014). Subsequently, the normalized data set were transformed into a new spectral
190 matrix using principal component analysis (PCA) in Matlab R2012b (The Mathworks,
191 Natick, USA) to reduce the level of noise (Babamoradi 2013), and then 2D FTIR COS
192 maps were conducted using 2D Shige software (Kwansei Gakuin University, Japan)

193 and re-plotted by Origin 9.0 software (OriginLab Corp., Northampton, MA, USA) .

194 **2.6 Microbial community analysis of activated sludge in aeration tank**

195 Microbial community genomic DNA was extracted from the activated sludge
196 samples using the E.Z.N.A.® soil DNA Kit (Omega Bio-tek, Norcross, GA, U.S.)
197 according to manufacturer's instructions. Gene amplicons (16S rRNA gene) were
198 carried out using PCR with primers 27F and 519R. Each primer was pre-pended with a
199 8-base barcode sequence and a unique barcode was applied for each sample (Li et al.
200 2015b). Purified amplicons were pooled in equimolar and paired-end sequenced on an
201 Illumina MiSeq PE300 platform/NovaSeq PE250 platform (Illumina, San Diego, USA)
202 according to the standard protocols by Majorbio Bio-Pharm Technology Co. Ltd.
203 (Shanghai, China). Sequencing data were demultiplexed, quality-filtered on
204 Trimmomatic, and merged according to the criteria. The quality filtered sequences were
205 clustered into operational taxonomic units (OTUs) at 97% thresholds (Edgar 2013).
206 Taxonomy of each 16S rRNA gene sequence was analyzed by RDP Classifier against
207 the Silva 16S rRNA database with a confidence threshold of 70%. Finally, microbial
208 community composition was run on the free online platform of the Major bio I-Sanger
209 Cloud Platform (Shanghai, China).

210

211 **3. Results and discussion**

212 **3.1 Changes in MP physicochemical characteristics**

213 **3.1.1 Microscopic features of MPs**

214 As shown in Fig. 1, the cracks and pores are found on the surfaces of the PE and
215 PS treated by SWPN, in comparison to virgin MPs, implying that the chemical
216 treatment generated in the wastewater pipeline has an impact on the MPs, consistent
217 with previous studies (Liu et al. 2019, Wu et al. 2020). Liu et al. (2019) and Wu et al.
218 (2020) reported that the cracks and pits are gradually generated on the surfaces of MP
219 in the heat-activated $K_2S_2O_8$ system. The surface of PS after BTAT becomes rougher
220 and tends to be fragmented (Fig. 1). It indicates that the MPs are susceptible to
221 biological erosion during biological aeration progress, possibly due to the hydrolysis
222 and oxidation in the activated sludge system where a large number of bacteria live
223 (Mahon et al. 2017, Rom et al. 2017). Narancic et al. (2018) demonstrated that strong
224 microbial activity under artificial biological systems may cause MP oxidation or
225 degradation. Compared with other treatment, MAGT causes hardly any change in the
226 micrographs of the MP surface, indicating that it has little effect on the surface
227 morphology of the MPs. Studies showed that the MPs are rubbed due to the shearing
228 forces, attributed to mechanical mixing during the “gravel and grease” removal stages
229 (Li et al. 2019a). Song et al. (2017) showed that fragmentation of MPs occurs after
230 prolonged friction in the presence of silica sand (Song et al. 2017). In this study, the
231 exposure time between MPs and inorganic particles was short (only 24 h), and thus no
232 detectable change is found in the MPs.

233 PE spectra display the peaks at around 2916, 2849, 1471, and 718 cm^{-1} (Cooper
234 and Corcoran 2010). The absorption peaks of PS are observed at 3083, 3061, 3024,

235 2923 and 2849 cm^{-1} , due to the C-H vibration of aromatic rings (Mao et al. 2020). The
236 PA spectra possess characteristic absorption peaks of amide I band at about 1638 cm^{-1} ,
237 amide II band at about 1542 cm^{-1} , amine group at about 3300 cm^{-1} , and methylene at
238 3070, 2938, and 2867 cm^{-1} (Tang et al. 2009). As shown in Figure S2 (SI), FTIR spectra
239 of the MPs after SWPN and MAGT show no significant difference in the surface
240 functional groups from the virgin MPs, while minor changes in peak intensity of the
241 MPs after BTAT are observed, indicating that biological treatment has higher impact
242 on MP surface functional composition, than the other two treatments. In the activated
243 sludge systems, the MPs come into contact with the inorganic particles and organic
244 matter, as well as the microorganisms (Fred-Ahmadu et al. 2020). The colonization of
245 these microorganisms with different sizes and types form the biofilms on the surface of
246 MPs (Fu et al. 2019, Zhang et al. 2020), thus modifying the surface functional groups
247 of the MPs (Rummel et al. 2017).

248 **3.1.2 Elemental analysis**

249 Compared with the corresponding virgin MPs, C, H and N contents of the treated
250 MPs decrease, while the O content and O/C ratios increase (Table 1), showing that the
251 treatment processes cause an increase in oxidation degree of the MPs. Compared with
252 the SWPN and MAGT, C and H contents of the MPs after BTAT increase more
253 drastically, implying that biological treatment has more considerable effect on the MP
254 elemental composition, in accordance with the FTIR results. The possible reason is that
255 the presence of some plastic-degrading bacteria on the surface of MPs causes their

256 chain scission and oxidation, and thus a decrease in the C and H contents (De Tender
257 et al. 2017). During BTAT, the changes in C and O contents of the PS are higher than
258 that of PA and PE, implying that the PS might be more easily aged than the PA and PE,
259 corresponding to the SEM results. In contrast to the secondary carbon in the PE, the
260 carbon atom bonded to the benzene ring in the PS is more susceptible to erosion,
261 resulting in rapider oxidation of PS (Gewert et al. 2015). In addition, Fig. 2 shows
262 microbial community composition of the activated sludge tank mixed with the three
263 MPs at genus level. The most abundant microorganism is *Saccharibacteria* for both of
264 the PA and PE, but *Flavobacterium* for the PS, which may supply an additional
265 explanation for the result that the biological treatment generates higher impact on the
266 PS, compared with the other two MPs.

267 **3.1.3 Surface zeta potentials**

268 Zeta potentials are associated with the adsorption potentials of chemicals on the
269 MP surface controlled by electrostatic interactions (Guo et al. 2018). As shown in Table
270 2, zeta potential of the virgin PA is 0.55 ± 0.01 mV. After SWPN and BTAT, zeta potential
271 of the PA drops to -0.16 ± 0.24 mV and -0.57 ± 0.52 mV, respectively, indicating that their
272 surface negative charges increase. A decrease in surface charge of the PA after SWPN
273 might be resulted from the combination of S^{2-} and N-H. Previous literature reported that
274 most hydrophobic MPs in water enhance the adsorption of hydroxide ions, thus
275 negatively charging the microparticle surface (Fotopoulou and Karapanagioti 2012,
276 Tampio et al. 2016). A decrease in surface charge of the PA after BTAT might be resulted

277 from the attachment of organic matter in the activate sludge. The humus in the sludge
278 is usually negatively charged, and easy to attach to the MPs, resulting in an increase in
279 negative charge on the surface of PA after BTAT (Li et al. 2018a, Lu et al. 2018). Initial
280 colonization of PA by microorganisms occurs within minutes to hours (McGivney et al.
281 2020, Zettler et al. 2013), also resulting in an increase in the negative charge on the
282 surface of MPs (Rummel et al. 2017, Tribedi and Sil 2013, Zettler et al. 2013). In
283 addition, zeta potential of the PE slightly increases after SWPN, and there is no obvious
284 change in other treatments. The results therefore implied that different MPs may have
285 different response to the chemical treatment in term of zeta potential due to their
286 different monomeric composition, which deserves to be further investigated.

287 **3.2 Changes in MP adsorption characteristics**

288 **3.2.1 Adsorption potential of MPs for Cd**

289 As shown in Fig. 3, compared with the virgin MPs, adsorption potential of the
290 MPs for Cd decreases after MAGT, but increases after SWPN and BTAT. In aquatic
291 environments, the MPs show electrostatic interaction toward organic and inorganic
292 cations (Guo et al. 2018, Holmes et al. 2012, Xu et al. 2018). It is reported that the
293 adsorption of metal by MPs is mainly resulted from the electrostatic interactions (Zou
294 et al. 2020). SWPN and BTAT may cause an increase in the negative charges on MP
295 surface, which potentially enhance the role of electrostatic interactions in sorption
296 process. Such results of a decrease in zeta potentials of the PA after SWPN and BTAT
297 provide an evidence supporting the increase in the adsorption potentials.

298 Adsorption potential of the MPs treated by the processes presents a decreasing
299 order as following: BTAT > SWPN > MAGT. The result shows that the biological
300 treatment causes the highest enhancement of the MP adsorption potentials, in
301 accordance to the FTIR and elemental results. In biological aeration tanks, due to the
302 large specific surface area of MPs, biofilms are easily formed on the surface (Kaiser et
303 al. 2017, Rummel et al. 2017). Biofilm can affect the sorption behavior of MPs by
304 modifying their physical properties, including the decreased surface hydrophobicity
305 and increased heterogeneity (Johansen et al. 2019, Johansen et al. 2018, Rummel et al.
306 2017). Johansen et al. (2019) reported that biofilm can enhance the adsorption of strong
307 and weak cations onto the MPs. Holmes et al. (2012) revealed that the sorption
308 capacities of metals on weathered plastics are enriched 1.5-25 times higher than virgin
309 MPs due to the adhesion of biofilms and precipitates, consistent with our results that
310 adsorption potential of the three MPs after the biological treatment increases by 1.6-11
311 times.

312 After SWPN, the adsorption capacities of the PA, PE and PS increase by 1.6, 2
313 and 3 times, respectively, compared with the corresponding virginal MPs (Fig. 3).
314 Similarly, the adsorption capacities of the PA, PE and PS increase by 1.6, 3 and 11 times
315 after BTAT, respectively. The results show that the effect of the treatment processes on
316 PS is higher than PE, followed by PA. Higher amount of Cd adsorbed on PS in contrast
317 to PE implies that the glassy PS are possibly more susceptibly aged than rubbery PE.
318 Every other carbon atom in the PS main chain that is bonded to the benzene ring is

319 more susceptible to chemical attack than the secondary carbon in PE, possibly resulting
320 in more aging of PS (Liu et al. 2019), and thus enhancing its ability to adsorb pollutants.
321 Compared with PE and PS, increase in the PA adsorption potential after the treatment
322 may be resulted from higher Cd adsorption by virgin PA.

323 3.2.2 Adsorption isotherms

324 To further clarify the adsorption characteristics, the Freundlich and Langmuir
325 isotherm models were used to fit Cd adsorption data on MPs (Guo et al. 2020). The
326 adsorption isotherm models can be described by Equations (1) and (2), respectively.

$$\frac{C_e}{q_e} = \frac{1}{k_L q_{\max}} + \frac{C_e}{q_{\max}} \quad (1)$$

$$\ln q_e = \ln k_F + \frac{1}{n} \ln C_e \quad (2)$$

327 In which C_e (mg L^{-1}) is the Cd concentration remaining in the solution at equilibrium,
328 q_e ($\mu\text{g g}^{-1}$) is the amount of Cd adsorbed per mass unit of adsorbent at equilibrium, q_{\max}
329 ($\mu\text{g g}^{-1}$) is the maximum adsorption capacity, k_L (L mg^{-1}) is the Langmuir binding
330 constant, k_F ($\text{mg}^{1-n} \text{L}^n \text{g}^{-1}$) and n are the Freundlich constants related to the adsorption
331 capacity and the adsorption intensity, respectively.

332 Fitting results of the isothermal adsorption of the Freundlich and Langmuir models
333 are shown in Fig. 4. The isotherms of virgin PA, PE and PS fit the Langmuir model
334 well, implying that the adsorption is monolayer (Table 3). The Langmuir model
335 assumes that the surface of the adsorbent is absolutely uniform with monolayer
336 adsorption of only one molecule per adsorption site (Foo and Hameed 2010). However,
337 adsorption isotherms of the PE and PS after SWPN, the PA after MAGT, and the PA

338 and PS after BTAT fit the Freundlich model well. The Freundlich isotherm is based on
339 the assumption regarding surface heterogeneity and can be used to model multi-layer
340 adsorption (Sintim and Flury 2017, Yang 1998). These results indicate that the
341 treatments cause the change in adsorption mode of the MPs for Cd pollutants from the
342 monolayer to the multi-layer. The possible reason is that the embrittlement and
343 fragmentation of aged MPs after the treatment increase the adsorption sites and lead to
344 the change in the MP adsorption behavior.

345 **3.2.3 2D-FTIR COS maps**

346 The 2D-FTIR COS was carried out to further understand the role of functional
347 groups of the ageing MP surfaces in the Cd adsorption. Significant spectral variations
348 are found in the ranges of 700-1700 cm^{-1} .

349 As shown in Fig. 5, three major auto-peaks are found in all the synchronous map
350 of the aged PA by the three treatment processes. The intensities at 1638 cm^{-1} and 1542
351 cm^{-1} are higher than that at 1470 cm^{-1} , implying that the N-H functional group plays a
352 greater role in the aging PA adsorption to Cd, compared with C-H functional groups.
353 An asynchronous map is about diagonal antisymmetry, and thus there are only cross-
354 peaks (Mao et al. 2020). Based on Noda's rules (Jin et al. 2018), asynchronous
355 correlation spectroscopy can reveal the change order of the chemical bonds in the
356 adsorption of the aging MPs to Cd. As shown in Fig. 5a and 5b, the cross-peak at
357 1638,1470 cm^{-1} for the SWPN and MAGT PA is positively correlated, suggesting that
358 the adsorption of N-H functional groups to Cd was faster than that of C-H functional

359 groups. However, the cross-peak at 1638,1470 cm^{-1} for the BTAT PA shows the negative
360 correlation, implying that the adsorption of C-H functional groups was faster than that
361 of N-H functional groups, which is the opposite of the results of the SWPN and MAGT
362 PA. The possible reason is that the attachment of organic matter and microorganism on
363 the PA surface during BTAT causes the enhancement of the adsorption of C-H
364 functional group to Cd, and thus promotes an increase in the adsorption potential. The
365 results complement and confirm the findings from FTIR spectra that biological
366 treatment has the greatest effect on the physical and chemical properties of PA. In
367 addition, two major auto-peaks and one major auto-peak representing C-H functional
368 group are found in synchronous map of the aged PE and PS, respectively (Figs S3 and
369 S4, SI), indicating that the C-H functional group plays a major role in the Cd adsorption
370 process.

371 **3.3 Limitation and further work**

372 The limitation of this study is that the MPs used in this study were virgin
373 commercial plastics, which may be different from the real wastewater-based MPs
374 (Waldman and Rillig 2020). The real MPs entering the WWTPs are affected by a variety
375 of complex factors, such as varying degrees of physical and microbial wear-and-tear in
376 the pipeline network (Bakir et al. 2014, Enfrin et al. 2019). In addition, this study only
377 focuses on the changes in physical and chemical properties of the wastewater-based MP,
378 but it is reported that a large amount of MPs with different weathered characteristics
379 are present in sewage sludge (Li et al. 2020, Mahon et al. 2017, Wei et al. 2019).

380 However, the effects of sludge treatment on MPs property and their potential risk are
381 still not clearly understood. Therefore, further investigation is needed on the changes
382 in the MPs properties during the real WWTPs and during sludge treatment process in
383 WWTPs such as anaerobic digestion, aerobic composting, dehydration, dewatering and
384 thermal drying.

385

386 **4. Conclusions**

387 The three wastewater treatment processes cause the MP aging to different degree.
388 Compared to SWPN and MAGT, BTAT has a greater impact on the microscopic
389 features and elemental composition of MPs, due to the attachment of organic matter
390 and microorganisms and the formation of biofilm on the MPs. SWPN and BTAT cause
391 a decrease in zeta potential of the PA, implying an increase in the surface negative
392 charge of PA. Compared with virgin MPs, the adsorption potential of the MPs for Cd
393 decreases after MAGT, but increases after SWPN and BTAT. The treatment processes
394 produce more significant effects on adsorption potential of PS than PE and PA, possibly
395 because other carbon atoms in the PS main chain that are bonded to the benzene ring
396 are more susceptible to chemical attack. Meanwhile, the treatments cause the change in
397 the adsorption mode of the MPs from monolayer to multi-layer. 2D-FTIR COS analysis
398 shows that the N-H functional groups play a great role in the Cd adsorption of the aging
399 PA, while the C-H functional groups are more important for PE and PS. Further
400 investigations need to explore the changes in the MPs properties during the commercial

401 WWTPs and sludge treatment process in WWTPs.

402

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408

409 **Appendix A. Supplementary data**

410 Additional tables and figures as mentioned in the main text. This supporting
411 information is available free of charge via the Internet.

412

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626 211.

627

628

629 Table 1. Elemental composition of the virgin and treated MPs

Samples`	C	H	N	S	O	Elemental ratio	
	(%)	(%)	(%)	(%)	(%)	C/H	O/C
Virgin PA	64.30±0.30	9.60	13.00	ND ^d	13.10	0.56	0.15
SWPN ^a PA	62.95±1.00	9.51±0.20	11.93±0.10	ND	15.61	0.56	0.19
MAGT ^b PA	62.19	9.21	10.99	ND	17.61	0.57	0.21
BTAT ^c PA	56.33±0.50	8.54±0.20	10.83±0.06	0.30±0.22	24.00	0.55	0.32
Virgin PE	86.32±0.80	13.66±0.10	0.02±0.01	ND	ND	0.53	ND
SWPN PE	85.25±1.80	13.60±0.30	0.02±0.01	ND	1.14	0.52	0.01
MAGT PE	82.55	13.42	0.04	ND	4.00	0.51	0.04
BTAT PE	73.14	11.89	0.32	ND	14.65	0.51	0.15
Virgin PS	92.36±0.70	7.64±0.04	ND	ND	ND	1.01	ND
SWPN PS	91.89 ±1.70	7.61±0.14	ND	ND	0.50	1.01	0.004
MAGT PS	91.20	7.91	0.00	ND	0.89	0.96	0.007
BTAT PS	69.09±0.18	6.10±0.03	0.68±0.18	0.05±0.01	24.08	0.94	0.26

630 ^a, SWPN, sulfidation in wastewater pipeline network; ^b, MAGT, mechanical abrasion in grit tank; ^c,

631 BTAT, biological treatment in aeration tank; ^d, not detectable

632 Table 2. Zeta potential of the virgin and treated MPs

MP samples	PA	PE	PS
Virgin MP	0.55±0.01	-2.02±0.32	-2.04±0.44
SWPN MP ^a	-0.16±0.24	-1.13±0.11	-2.16±0.66
MAGT MP ^b	0.95±0.45	-3.26±0.51	-2.82±0.86
BTAT MP ^c	-0.57±0.52	-2.48±0.22	-3.04±0.58

633 ^a, SWPN, sulfidation in wastewater pipeline network; ^b, MAGT, mechanical abrasion in grit tank; ^c,

634 BTAT, biological treatment in aeration tank

635 Table 3. Adsorption isotherm constants defining Cd adsorption on the virgin and treated MPs

636 according to the isotherm model.

MP samples	Langmuir isotherm	Freundlich isotherm
Virgin PA	$k_L=0.320 \text{ L } \mu\text{g}^{-1}$ $q_{\max}=0.3396 \text{ mg g}^{-1}$ $R^2=0.89$	$k_F=5.28 \mu\text{g}^{1-1/n} \text{ g}^{-1} \text{ L}^{1/n}$ $n=2.58$ $R^2=0.83$
SWPN ^a PA	$k_L=0.53 \text{ L } \mu\text{g}^{-1}$ $q_{\max}=2.13 \text{ mg g}^{-1}$ $R^2=0.97$	$k_F=102.35 \mu\text{g}^{1-1/n} \text{ g}^{-1} \text{ L}^{1/n}$ $n=13.35$ $R^2=0.80$
MAGT ^b PA	$k_L=6.27 \text{ L } \mu\text{g}^{-1}$ $q_{\max}=25.74 \mu\text{g g}^{-1}$ $R^2=0.63$	$k_F=1.79 \mu\text{g}^{1-1/n} \text{ g}^{-1} \text{ L}^{1/n}$ $n=2.07$ $R^2=0.87$
BTAT ^c PA	$k_L=4.588 \text{ L } \mu\text{g}^{-1}$ $q_{\max}=543.5 \mu\text{g g}^{-1}$ $R^2=0.70$	$k_F=9.67 \mu\text{g}^{1-1/n} \text{ g}^{-1} \text{ L}^{1/n}$ $n=1.98$ $R^2=0.92$
Virgin PE	$k_L=0.414 \text{ L } \mu\text{g}^{-1}$ $q_{\max}=0.2345 \mu\text{g g}^{-1}$ $R^2=0.92$	$k_F=4.53 \mu\text{g}^{1-1/n} \text{ g}^{-1} \text{ L}^{1/n}$ $n=3.7$ $R^2=0.89$
SWPN PE	$k_L=8.80 \text{ L } \mu\text{g}^{-1}$ $q_{\max}=360.9 \mu\text{g g}^{-1}$ $R^2=0.75$	$k_F=10.41 \mu\text{g}^{1-1/n} \text{ g}^{-1} \text{ L}^{1/n}$ $n=2.4$ $R^2=0.99$
MAGT PE	$k_L=7.97 \text{ L } \mu\text{g}^{-1}$ $q_{\max}=126.5 \mu\text{g g}^{-1}$ $R^2=0.97$	$k_F=6.68 \mu\text{g}^{1-1/n} \text{ g}^{-1} \text{ L}^{1/n}$ $n=10.50$ $R^2=0.24$
BTAT PE	$k_L=0.745 \text{ L } \mu\text{g}^{-1}$ $q_{\max}=614.48 \mu\text{g g}^{-1}$ $R^2=0.87$	$k_F=20.03 \mu\text{g}^{1-1/n} \text{ g}^{-1} \text{ L}^{1/n}$ $n=5.01$ $R^2=0.45$
Virgin PS	$k_L=0.516 \text{ L } \mu\text{g}^{-1}$ $q_{\max}=0.0699 \mu\text{g g}^{-1}$ $R^2=0.81$	$k_F=1.11 \mu\text{g}^{1-1/n} \text{ g}^{-1} \text{ L}^{1/n}$ $n=2.23$ $R^2=0.66$
SWPN PS	$k_L=3.062 \text{ L } \mu\text{g}^{-1}$ $q_{\max}=34.64 \mu\text{g g}^{-1}$ $R^2=0.62$	$k_F=7.20 \mu\text{g}^{1-1/n} \text{ g}^{-1} \text{ L}^{1/n}$ $n=1.83$ $R^2=0.97$
MAGT PS	$k_L=31.81 \text{ L } \mu\text{g}^{-1}$	$k_F=3.25 \mu\text{g}^{1-1/n} \text{ g}^{-1} \text{ L}^{1/n}$

	$q_{\max}=57.48 \mu\text{g g}^{-1}$	$n=5.43$
	$R^2=0.97$	$R^2=0.45$
	$k_L=0.798 \text{ L } \mu\text{g}^{-1}$	$k_F=15.05 \mu\text{g}^{1-1/n} \text{ g}^{-1} \text{ L}^{1/n}$
BTAT PS	$q_{\max}=1029.3 \mu\text{g g}^{-1}$	$n=2.43$
	$R^2=0.80$	$R^2=0.89$

637 ^a, SWPN, sulfidation in wastewater pipeline network; ^b, MAGT, mechanical abrasion in grit tank; ^c,

638 BTAT, biological treatment in aeration tank

639 Figure Caption

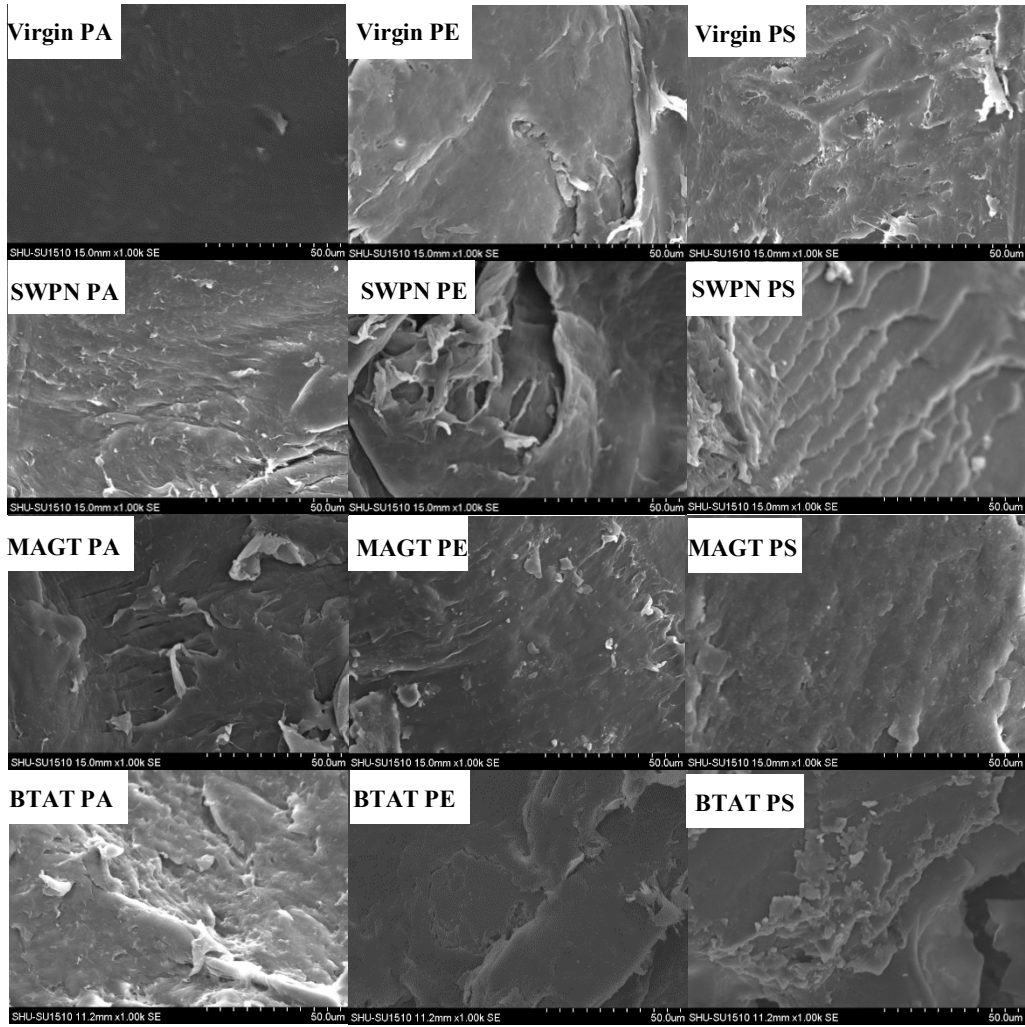
640 Fig. 1. Scanning electron micrograph of virgin and treated MPs. SWPN, sulfidation in wastewater
641 pipeline network; MAGT, mechanical abrasion in grit tank; BTAT, biological treatment in
642 aeration tank

643 Fig. 2. Microbial community composition in activated sludge from aeration tank after the addition
644 of the MPs for 14 days at genus level

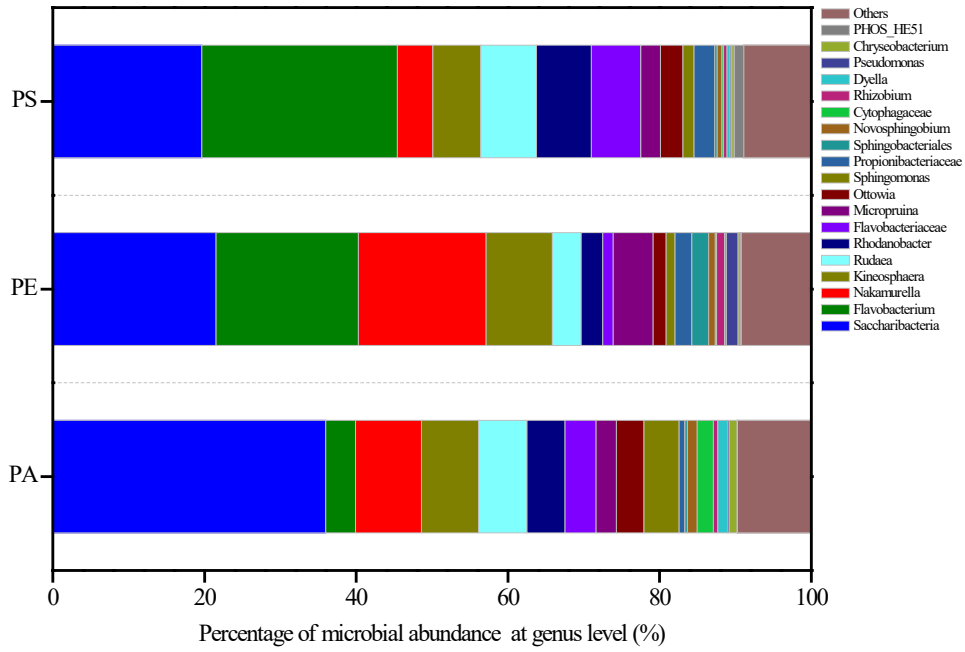
645 Fig. 3. Changes in adsorption potentials of virgin and treated MPs to Cd. SWPN, sulfidation in
646 wastewater pipeline network; MAGT, mechanical abrasion in grit tank; BTAT, biological
647 treatment in aeration tank

648 Fig. 4. Adsorption isotherms of virgin and treated MPs to Cd. SWPN, sulfidation in wastewater
649 pipeline network; MAGT, mechanical abrasion in grit tank; BTAT, biological treatment in
650 aeration tank

651 Fig. 5. Synchronous (left) and asynchronous (right) 2D correlation maps generated from the 700–
652 1700 cm^{-1} region of the FTIR spectra of treated PA samples with the Cd adsorption. a,
653 sulfidation in wastewater pipeline network (SWPN); b, mechanical abrasion in grit tank
654 (MAGT); c, biological treatment in aeration tank (BTAT).



655 Fig. 1. SEM of virgin and treated MPs. SWPN, sulfidation in wastewater pipeline network; MAGT,
656 mechanical abrasion in grit tank; BTAT, biological treatment in aeration tank



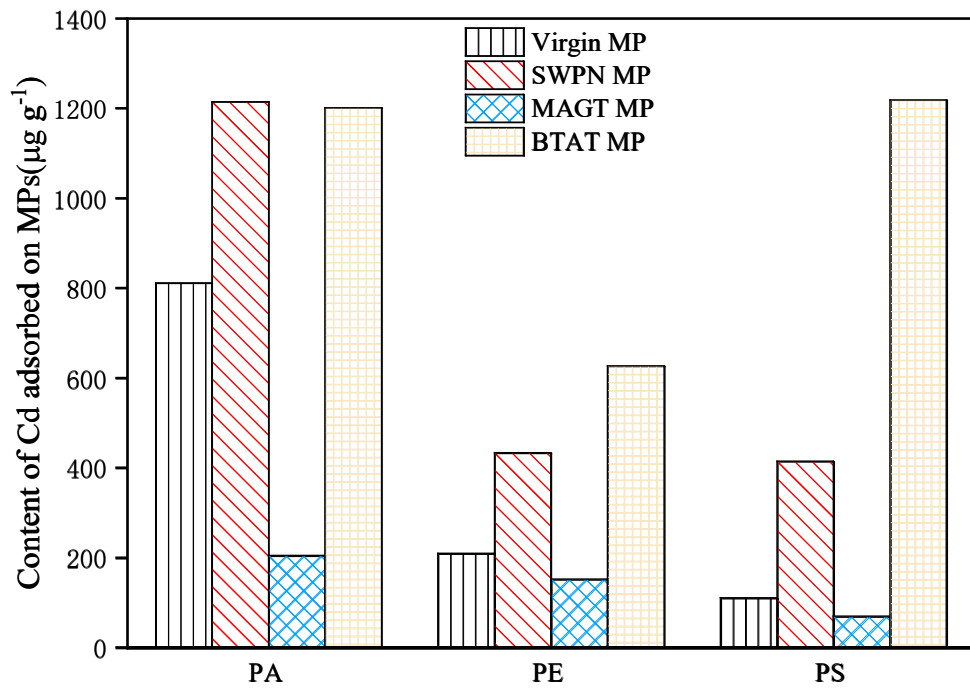
657

658 Fig. 2. Microbial community composition at genus level in activated sludge from aeration tank after

659 the addition of the MPs for 14 days

660

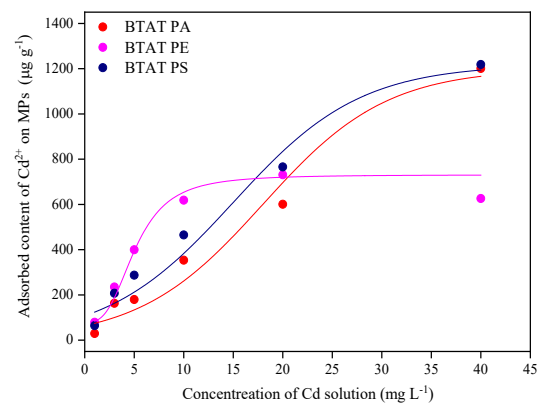
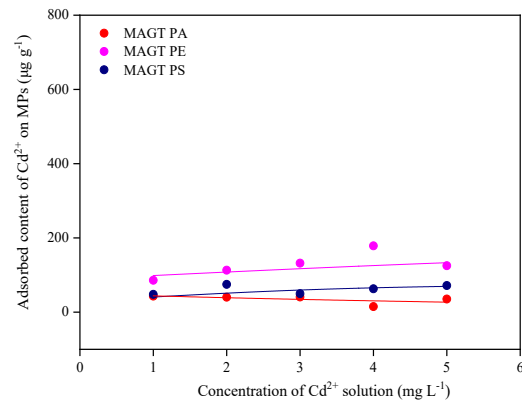
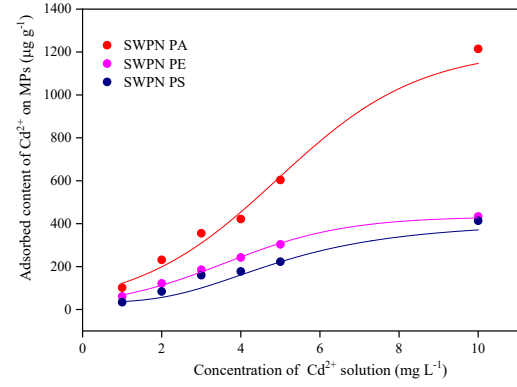
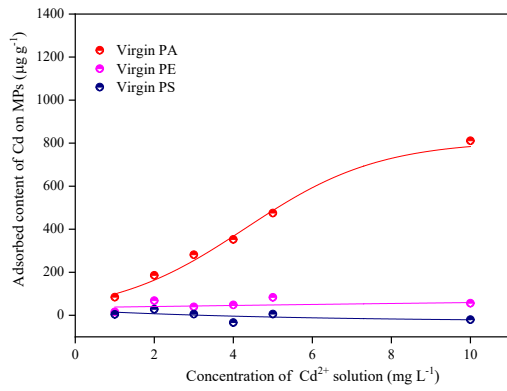
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662

663 Fig. 3. Changes in adsorption potentials of virgin and treated MPs for Cd. SWPN, sulfidation in
 664 wastewater pipeline network; MAGT, mechanical abrasion in grit tank; BTAT, biological treatment
 665 in aeration tank

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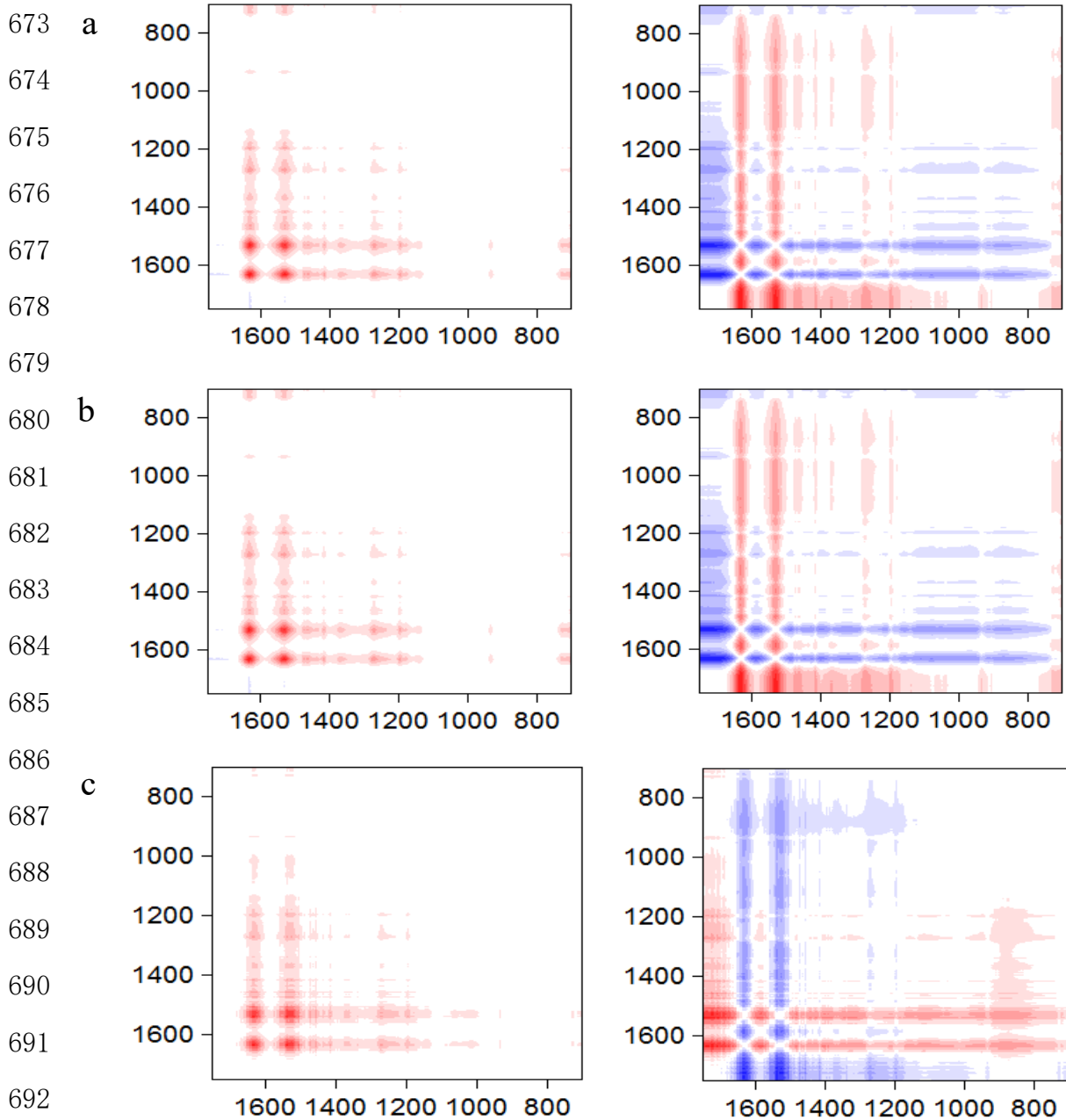
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669 Fig. 4. Adsorption isotherms of virgin and treated MPs for Cd. SWPN, sulfidation in wastewater

670 pipeline network; MAGT, mechanical abrasion in grit tank; BTAT, biological treatment in aeration

671 tank

672



693 Fig. 5. Synchronous (left) and asynchronous (right) 2D correlation maps generated from the 700–
694 1700 cm^{-1} region of the FTIR spectra of treated PA samples with the Cd adsorption. a, sulfidation
695 in wastewater pipeline network; b, mechanical abrasion in grit tank; c, biological treatment in
696 aeration tank.

697