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1	Understanding the fate and impact of capsaicin in anaerobic co-digestion of
2	food waste and waste activated sludge
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14 ABSTRACT

15 Anaerobic co-digestion is an attractive option to treat food waste and waste activated sludge, which is 16 increasingly applied in real-world situations. As an active component in *Capsicum* species being 17 substantially present in food waste in many areas, capsaicin has been recently demonstrated to inhibit the 18 anaerobic co-digestion. However, the interaction between capsaicin and anaerobic co-digestion are still 19 poorly understood. This work therefore aims to deeply understand the fate and impact of capsaicin in the 20 anaerobic co-digestion. Experiment results showed that capsaicin was completely degraded in anaerobic 21 co-digestion by hydroxylation, O-demethylation, dehydrogenation and doubly oxidization, respectively. 22 Although methane was proven to be produced from capsaicin degradation, the increase in capsaicin 23 concentration resulted in decrease in methane yield from the anaerobic co-digestion. With an increase of 24 capsaicin from 2 ± 0.7 to 68 ± 4 mg/g volatile solids (VS), the maximal methane yield decreased from 274.6 \pm 25 9.7 to 188.9 \pm 8.4 mL/g VS. The mechanic investigations demonstrated that the presence of capsaicin 26 induced apoptosis, probably by either altering key kinases or decreasing the intracellular NAD⁺/NADH ratio, 27 which led to significant inhibitions to hydrolysis, acidogenesis, and methanogenesis, especially acetotrophic 28 methanogenesis. Illumina Miseq sequencing analysis exhibited that capsaicin promoted the populations of 29 complex organic degradation microbes such as Escherichia-Shigella and Fonticella but decreased the 30 numbers of anaerobes relevant to hydrolysis, acidogenesis, and methanogenesis such as Bacteroide and 31 Methanobacterium.

32 Keywords: Capsaicin; Food waste; Waste activate sludge; Anaerobic co-digestion; Methane production

33 1. Introduction

Food waste (FW) and waste activated sludge (WAS) are two major bio-solids in the world, which are
massively generated. It is documented that more than 1.3 billion tons FW are globally produced each year

36 (Li et al. 2020b, Xu et al. 2018), and the annul amount is estimated to achieve approximately 2.2 billion tons 37 by 2025 (Mehariya et al. 2018). In China, more than 90 million tons of FW is produced each year, 38 accounting for 37-62 % of municipal solid waste (Zhang et al. 2014). As for WAS, its amount in China is 39 over 40 million tons per year, and increases at an annual average rate of 4.75 % (Luo et al. 2020b). The total 40 amount in the world is estimated to increase to 103 million tons by 2025 (Yao et al. 2018).

FW and WAS contain substantial degradable substrates (e.g., proteins, carbohydrates, and lipids) and also 41 42 several recalcitrant or toxic materials such as cellulose, humus antioxidant, antibiotic, and heavy metals (Liu et al. 2020a, Shah et al. 2005, Tao et al. 2020, Wang et al. 2019a). They will pose high risks to the 43 environment if they are not treated appropriately (Li et al. 2020a). As a mature technology to effectively 44 45 prevent pollution and recover energy concurrently, anaerobic digestion attracts much attention (Liu et al. 46 2020b, Luo et al. 2020a). Compared with the mono-digestion, anaerobic co-digestion of FW and WAS offers complementary benefits such as substrate variability, toxicity dilution, and C/N ratio balance (Sole-Bundo et 47 48 al. 2017, Zhao et al. 2016). Therefore, it has been recently thought to be a very promising option and 49 growingly executed in field situations (Nghiem et al. 2017).

50 Capsaicin, a major pungent ingredient in varieties of capsicums, is widely used as food additives

51 throughout the world, especially in South East Asian, Latin-American countries and southwest of China

52 (Kurita et al. 2002, Surh and Lee 1995). For instance, the daily consumption of capsicum spices is 5

53 g/person in Thailand (Monsereenusorn 1983) and 20 g/person (one chili pepper) in Mexico (López-Carrillo et

54 al. 1994). The capsaicin content in capsicums usually ranges from 0.1 to 2.5 mg/g (Parrish 1996). This

55 indicates that capsaicin accumulation in FW could be up to 25 g/kg.

56 It is known that capsaicin has a wide variety of antimicrobial effects and can interact at primary sensory 57 neurons exerting the characteristic actions of excitation, desensitization and neurotoxicity (Kurita et al. 2002). 58 Due to this characteristic, several efforts have been carried out to assess the toxicity of capsaicin to

59 microorganisms. Gu et al. (2019) showed that the minimum inhibitory concentrations of capsaicin on

60 Streptococcus mutans, Actinomyces viscosus, Lactobacillus, and Streptococcus sanguis were 50, 50, 50, 25
 61 µg/mL respectively.

As anaerobic co-digestion is a biological process with varieties of anaerobes being involved, the presence 62 of capsaicin might also affect these microbes. Li et al. (2016) demonstrated that when the pungency degree 63 64 decreased from 1136.1 to 71.5 Scoville Heat Units (i.e., 11.1 to 0.7 g Capsaicin/kg Kitchen Waste), the 65 maximum methane production increased from 9.9 to 13.5 mL/ (g VS h), indicating the detrimental impact of capsaicin on anaerobic digestion. Yue et al. (2020) recently found that N-VanillyInonanamide (one type of 66 67 capsaicin) inhibited anaerobic digestion of glycerol trioleate severely. As N-Vanillynonanamid addition 68 increased from 0 to 40% wt, the methane yield decreased from 780.21 to 142.1 mL/g Total Volatile Solid. The findings obtained by the previous investigations confirmed the detrimental effect of capsaicin and raised 69 70 our concerns in terms of the toxicity of capsaicin to anaerobic co-digestion. Considering the massive 71 quantities of capsaicin-rich wastes treated daily, comprehensive and deep understanding the fate and impact of 72 capsaicin in anaerobic co-digestion is of significance to manipulate the co-digesters in field situations. 73 Despite the excellent work made by Li et al. and Yue et al., details of what happen in capsaicin-rich 74 co-digestion systems remain largely unknown. For example, capsaicin as an organic, it is unclear about the 75 transformation and metabolism of capsaicin in the process of anaerobic co-digestion and its interaction with anaerobes. The contribution of capsaicin degradation to methane yield is also not clear. Moreover, as 76 anaerobic co-digestion contains several processes such as disintegration, hydrolysis, acidogenesis, 77 78 acetogenesis, and methanogenesis, it is also unknown that the mechanism of capsaicin effects on each process. 79 By clarifying these questions, this work aims to deeply understand the fate and impact of capsaicin in

anaerobic co-digestion of FW and WAS. Firstly, the fate of capsaicin in the co-digesters was systematically
assessed. Then, the influence of capsaicin at different concentrations on methane production was
investigated. Finally, details of how capsaicin affects methane production were explored. To our
knowledge, this is the first study revealing the interaction between capsaicin and anaerobic co-digestion.

84 2. Materials and methods

85 2.1 Source and characteristics of FW, WAS, and inocula.

86 FW used in this work, which was mainly composed of rice, noodles, and vegetables, was withdrawn from a cafeteria in Hunan University (Changsha, China). The indigestible substrates (e.g., inorganic 87 particles, bones, and chopsticks) were first removed before FW was crushed into small particles (1-3 mm) for 88 89 further use. The main characteristics of FW are as follows: pH 5.8 \pm 0.1, total solids (TS) 121.3 \pm 5.8 g/L, 90 volatile solids (VS) 116.1 \pm 4.3 g/L, total chemical oxygen demand (TCOD) 142.3 \pm 7.4 g/L, total proteins 91 31.2 ± 1.4 g COD/L, total carbohydrates 123.5 ± 5.7 g COD/L, and capsaicin content 4 ± 1 mg/g FW. In this 92 study, extra capsaicin, with purity being > 98%, was purchased from Hefei Bomei Biotechnology company. 93 WAS used in this work was taken from the secondary tank of a municipal wastewater treatment plant in Changsha, China. WAS was first filtered with a 2 mm \times 2 mm screen and then concentrated in 4 °C 94 95 refrigerator for 24 h before use, and the main characteristics of WAS are as follows: pH 6.9 \pm 0.1, TS 57.3 \pm 2.6 g/L, VS 28.3 \pm 1.2 g/L, TCOD 36.2 \pm 1.6 g/L, total proteins 8.5 \pm 0.3 g COD/L, and total carbohydrates 96 97 1.6 ± 0.1 COD/L.

Inocula applied in this work were harvested from a mesophilic anaerobic reactor in our laboratory, which has been operated 130 days with solid retention time of 30 d and WAS as substrate. The main properties of inoculated sludge are as follows: pH 7.2 \pm 0.1, TS 46.7 \pm 3.5 g/L, and VS 38.6 \pm 2.3 g/L.

101 2.2 Effect of capsaicin on methane production from anaerobic co-digestion.

102	This batch test was performed in six identical serum bottles, and the working volume of each bottle was
103	500 mL. Among them, one was set as the blank, and the other five were operated as the experimental
104	reactors. According to the literature, the mixture ratio of FW to WAS used in this study was set as 1:1 on a
105	VS basis (Mehariya et al. 2018). Firstly, 1.5 L mixture of FW and WAS was evenly divided into the five
106	experimental reactors, respectively. Then, different amounts of extra capsaicin were added into the reactors,
107	which led to the initial capsaic in content of 2 \pm 0.7, 8 \pm 1.2, 20 \pm 2.3, 36 \pm 2.6, or 68 \pm 4.1 mg/g VS. It
108	should be emphasized that no extra capsaicin was added into the first experimental reactor, and 2 ± 0.7 mg/g
109	VS was the background value in the digestion mixture. To improve the uniformity of capsaicin, all the
110	mixtures were pretreated in a water-bath shaker (120 rpm, 60 °C) for 30 min (Huang et al. 2020). When the
111	mixtures were cooled down to room temperature, each reactor received 50 mL same inocula, as mentioned
112	above. The blank reactor, which merely contained 50 mL inocula and 300 mL of Milli-Q water, was also
113	conducted to test the methane productivity from the inocula alone. All the reactors were flushed with high
114	purity nitrogen for 5 min to eliminate oxygen, sealed with rubber stoppers, and placed in an air-bath shaker
115	(120 rpm) at 35 \pm 1°C for 45 d. pH value in all the reactors was maintained at 7.0 \pm 0.1 during the whole
116	digestion period by 4 M hydrochloric acid or 4 M sodium hydroxide with automatic titrators.

In this work, all the tests, unless otherwise described, were operated in triplicate. The data reported below are net values, with the values determined in the blank reactor having been subtracted. During the entire digestion process, the yield of methane produced was determined periodically by releasing the pressure in the serum bottle using a 300 mL glass syringe to equilibrate with the room pressure according to the method documented in the literature (Liu et al. 2019), and the calculation of the cumulative volume of methane was detailed in our previous publication (Wang et al. 2015).

123 2.3 Methane production from capsaicin.

Three replicates serum bottles with a working volume of 500 mL each were carried out to assess whether capsaicin can be served as substrates to produce methane in the anaerobic co-digestion process. Each reactor received 50 mL same inocula. Among them, one bottle receives 300 mL of Milli-Q water and was set as the control, the other two bottles received 300 mL synthetic medium containing either 36 mg capsaicin/g VS or 68 mg capsaicin/g VS as the extra digested substrate. All the operations were the same as depicted in Section 2.2.

130 2.4 Effect of capsaicin on solubilization, hydrolysis, acidogenesis, and methanogenesis.

131 This batch test was performed to assess the effect of capsaicin on digestion steps (i.e., solubilization, hydrolysis, acidogenesis, acetoclastic methanogenesis and hydrogenotrophic methanogenesis) relevant to 132 133 methane production. The effect of capsaicin on WAS solubilization was assessed in real WAS by comparing 134 the variations in soluble proteins and soluble polysaccharides in the presence of different capsaicin 135 concentrations, while the impact of capsaicin on other biological processes was evaluated in synthetic media 136 through comparing the specific degradation rates of the model substrates under different concentrations of capsaicin according to the previous study (Wu et al. 2019). In this test, fifteen replicate serum bottles were 137 138 performed and divided into five groups (namely Test-I, Test-II, Test-III, Test-IV, and Test-V) with three in 139 each.

Test-I: Three reactors with a working volume of 500 mL each were operated. The three reactors first
received 300 mL mixture of FW and WAS, which capsaicin concentrations were 2 ± 0.7, 8 ± 1.2, 36 ± 2.6
mg/g VS, respectively. After being pretreated at 60 °C for 30 min, each reactor was fed with 50 mL inocula.
All other conditions were the same as those described above. By measuring the concentrations of soluble
proteins and carbohydrates in the initial 2 days, the effect of capsaicin on solubilization could be obtained.
Test-II: Three replicate anaerobic digestion reactors were operated. Each reactor received 50 mL

identical inocula and 300 mL same synthetic wastewater containing 5.3 g dextran. In the anaerobic co-digestion of this study, carbohydrates are the dominate substrate used for hydrolysis, and the carbohydrates in synthetic wastewater were similar to that in the co-digestion substrate. Afterwards, 0, 11 and 18 mg capsaicin were respectively added into the three reactors, which resulted in the initial capsaicin condition of 0, 30 and 50 mg/L, respectively. All other conditions were the same as those described above. By measuring the specific degradation rate of dextran, the effect of capsaicin on hydrolysis process could be indicated. Test-II: This test was operated the same as described in Test-II except that the substrate (i.e., dextran) in

153 synthetic wastewater was replaced by 2.7 g glucose, respectively.

154 Text-IV: The operation of this test was performed with the same approach as described in Test-II except 155 that 1.25 g sodium acetate was employed to replace dextran in synthetic wastewater.

Test-V: In this test, three reactors were operated. Each received 50 mL identical inocula and 300 mL Milli-Q water containing 0, 11 or 18 mg capsaicin. Afterwards, each reactor was flushed with a mixed gas (40% hydrogen, 10% carbon dioxide and 50% nitrogen) for 5 min to ensure that each was full of synthetic hydrogen-containing gas. At last, all these reactors were capped with rubber stoppers, sealed, and placed in an incubator (120 rpm) at $35 \pm 1^{\circ}$ C.

161 2.5 Model-based Analysis.

Methane production was simulated by the modified Gompertz equation (Eq(1)) (Lay et al. 1997), and several kinetic parameters, e.g., Mm (maximum methsane yield potential, mL/g VS or mL/L), Rm (methane production rate, mL/(g VS·d) or mL/d or mL/(L·d)), λ (lag phase time of methane production, d), and t (digestion time, d) were calculated using Origin 7.0 software.

166 — (1)

167

The effect of capsaicin on each process of anaerobic co-digestion can be assessed by the inhibition

168 constant, which is obtained from Eq (2).

169

(2)

170 Where, *X* is the reaction rate, subindex "s" is the substrate, subindex "i" is the inhibitor, *Ii* is the 171 concentration of inhibitor (mg/L), and $K_{s,i}$ is the relevant inhibition constant (mg/L).

172 2.6 Analytical Methods.

The analyses of Total Suspended Solid (TSS), Volatile Suspended Solid (VSS), TCOD, and SCOD were conducted in accordance with Standard Methods. Carbohydrate was measured by phenol-sulfuric method with glucose as the standard. Protein was determined by the Lowry-Folin method with BSA as the standard. The composition in biogas was analyzed by gas chromatograph equipped with a thermal conductivity detector according to the method documented in the literature (Wang et al. 2019b).

178 The concentration of capsaicin was determined using HPLC according to the reference (Hwang et al.

179 2017). The samples were first centrifuged at 6500 rpm at 4 °C for 10 min and dried at 58 °C for 48 h by

180 Vacuum drying oven. Then, 0.2 g dried sample was weighed and dissolved in n-hexane. The dissolved

181 sample was shocked for 5 min before being placed into ultrasonic machine for 10 min. After the sample was

- re-centrifuged at 2500 rpm for 5min, the normal hexane extract was filtered through 0.22 µm filterable
- 183 membrane and then injected into HPLC system (Agilent 1200, USA). The mobile phase was methyl alcohol
- 184 and deionized water (70:30, v/v) with a flow rate 1.0 mL/min. The absorbance was measured at 280 nm.
- 185 The major metabolic products of capsaicin in the digestion process were measured via liquid

186 chromatography-mass spectrometer/mass spectrometer (Jia et al. 2018). The metabolic products were 187 extracted using solid phase NH₂ Cartridge (6 mL, 500 mg sorbent) and then eluted with methanol. The 188 eluant was filtered through 0.22 µm filterable membrane and injected into LC-MS/MS (LC-MS/MS, Agilent 189 1290 series LC, 6460 Triple Quad LC/MS). The metabolic products were separated using a ZORBAX

190	RRHD Eclipse Plus C18 column (2.1 \times 50mm, 1.8 $\mu m)$ and the mass spectrometers were performed in
191	positive electron-spray ionization (ESI+) mode. The samples preparation and determination method of
192	LC-MS/MS were detailed in Supplementary Information (SI).
193	For determining the activity of key enzymes, 25 mL sample was taken out from the reactors, cleaned
194	using 100 mM sodium phosphate buffer (pH 7.4), sonicated at 20 kHz at 4 °C for 10 min, and finally
195	centrifuged at 12000 rpm at 4 °C for 15 min to remove the debris. The extracts were kept on the ice before
196	analyzing. The relative activities of function enzymes (mch, F420, AK, PTA, Coenzyme A, acetyl-CoA
197	decarbonylase/synthase complex (ACDS) and Coenzyme M) relevant to methane production were analyzed
198	using previously reported methods (Grahame and DeMoll 1996, Li et al. 2015, Liu et al. 2015, Wang et al.
199	2018a).
200	The membrane fluidity of microbial cells was determined by flow cytometry using Annexin V-FITC

201 fluorescence dye according to the reference (Luo et al. 2016). Briefly, the samples were centrifuged in a 50 202 mL tube at 6000 rpm for 5 min, with the pellet being suspended by pre-cooled phosphate buffer saline (PBS). 203 Then the suspension was heated at 60 °C in a water bath for 30 min and re-suspended by pre-cooled PBS. 204 After filtering the suspension using 500 Nylon mesh and stained, the samples were determined using BD 205 Biosciences AccuriC6 flow cytometer (Bacton Dickinson Immunocytometry Systems, San Jose, CA, USA), 206 with the staining process being available in SI.

For microbial community analysis, the collected samples were first centrifuged for 5 min at 10000 rpm. 207 208 Then, the total DNA was extracted from the samples using the Fast DNA kit (MoBio Laboratories) according 209 to the instruction from manufacture. The quantity and purity of DNA were analyzed with a Nanodrop spectrophotometer (Thermo Scientific, Wilmington, DE, USA). The high-throughput sequencing (Illumina 210 Ltd. (Shanghai, 211 Miseq) conducted by Majorbio co., China). The primers 515F was

212 (5'-GTGCCAGCMGCCGCGG-3') and 806R (5'-GGACTACHVGGGTWTCTAAT-3') targeting the V4

213 regions of bacterial 16S DNA genes were used.

214 2.7 Statistical Analysis.

All the batch experiments were performed in triplicate. An analysis of variance (ANOVA) with least significant difference test was used to assess the significance of results, and p < 0.05 was considered statistically significant.

218 3. Results and discussion

219 3.1 Capsaicin variation in anaerobic co-digestion.

220 Fig. 1A shows the variations in HPLC chromatogram of extracted mixtures taken from the reactor fed 221 with 68 ± 4.1 mg/g VS capsaic at different digestion times. According to HPLC chromatogram tested with 222 the standard capsaicin, the absorption peak of capsaicin appears at near 4.5 min (Fig. S1). It can be seen that 223 the absorption peak gradually declined with the digestion time, which indicates that capsaicin was degraded in 224 the anaerobic co-digestion process. Quantitative calculation exhibits that the concentration of capsaicin in digestion mixture also decreased with the digestion. With the digestion time increase from 0 to 9 d, 225 capsaicin concentration decreased from 68 ± 4.1 to 14.2 ± 2.4 mg/g VS. On 12 d digestion, less than 1 mg/g 226 227 VS capsaicin was measured in the system, suggesting that capsaicin was almost degraded in the co-digestion 228 completely. The results further suggests that the specific degradation rate of capsaicin in this co-digestion 229 system is 4.1 mg/(g VS)·d. Similar observations were also made on other reactors fed with other capsaicin 230 levels.

It is reported that capsaicin could be metabolized by crude enzyme preparations from body, midgut and
Malpighian tubule of *Helicoverpa armigera* and *H. assulta* (Zhu et al. 2020). Through a CO₂ Evolution Test,
Wang et al. (2014) demonstrated that capsaicin could be biodegraded by microbes and bio-converted to CO₂

and H₂O under aerobic conditions. When a filamentous fungus i.e., *Aspergillus oryzae*, was incubated with red pepper powder in potato dextrose broth, Lee et al. (2015a) found that capsaicin was degraded with five metabolites being obtained. Despite these significant researches, this is the first study proving the degradation of capsaicin in anaerobic co-digestion of FW and WAS.

3.2 Identification of the Main Metabolites of Capsaicin Degradation.

239 LC-MS/MS was used to identify the metabolites of capsaicin in anaerobic co-digestion process. Since 240 the fragment ions of MS/MS spectrometry occurred at 10.496 min are the same to those produced from 241 standard capsaicin (Fig. S2), the peak occurred at 10.496 min is considered to be capsaicin. On 0 d, one peak 242 was detected at 10.496 min (M) in LC/MS chromatogram extracted the sample withdrawn from the digester 243 fed with $68 \pm 4.1 \text{ mg/g VS}$. On 9 d, this peak decreased largely, and meanwhile three new peaks occurred, 244 with their retention time being 6.708 min (M1), 8.362 min (M2), and 12.331 min (M3), respectively (Fig. 2). 245 This confirms again that capsaicin was degraded in the anaerobic co-digestion and suggests that three major 246 metabolic products were generated from capsaicin degradation. The proposed structure and details of 247 metabolites are shown in Table S1.

To understand capsaicin biodegradation and identify these three metabolites, the precursor ions $[M + H]^+$, $[M1 + H]^+$, $[M2 + H]^+$, $[M3 + H]^+$, and their fragmentation patterns were further determined. The precursor ion peak of $[M + H]^+$ at m/z 306 indicates that the molecular weight of capsaicin was 305 (Fig. 3A). Besides, three fragment ions at m/z 137, 170, and 182 were also found in Fig. 3A. The fragment ion at m/z137 was reported to be vanillyl portion of capsaicin resulting from cleavage of C7-N8, while the product ions at m/z 170 and 182 were respectively derived from fragmentation of alkyl chain at C7-N8 and C1-C7 (Reilly et al. 2003).

255	Analogous to capsaicin (M), the molecular weight of M1 was 321 due to the precursor ion peak of
256	$[M1+H]^+$ at m/z 322 (Fig. 3B). Apart from the precursor ion peak, there are other four fragment ions being
257	observed in Fig. 3B. The presence of fragment ion at m/z 137 indicated that vanilloid ring of capsaicin was
258	not modified. Shifts in the product ions at m/z from 182 and 170 to 198 and 186 may be owing to addition of
259	oxygen atom (16 amu) to the alkyl chain. The product ion at m/z 181 was likely due to loss of hydroxyl
260	group from fragment ion at m/z 198 while the appearance of fragment ion at m/z 304 was probably due to loss
261	of terminal CH ₂ O from m/z 322. Based on these analyses, M1 (m/z 322) was inferred to alkyl hydroxylated
262	metabolite of capsaicin, with its molecular structure being detailed in Fig. 3B. It was reported that the alkyl
263	side chain of capsaicin was susceptible to enzymatic oxidation (Reilly and Yost 2006), and M1 was also
264	detected as a capsaicin metabolite by Aspergillus oryzae (Lee et al. 2015a).
265	Four fragment ions were observed in the MS/MS spectrum of M2 (Fig. 3C). The precursor ion peak at
266	m/z 292 [M2+H] ⁺ indicated that the molecular weight of M2 was 291. The appearance of fragment ion at
267	m/z 123 was probably owing to a net loss of 14 amu from the vanilloid ring (m/z 137) through demethylation
268	of methoxy group. Gonzalez-Gil et al. (2019) demonstrated that tramadol and trimethoprim can transformed
269	to O-desmethyltramadol and 4-desmethyltrimethoprim by demethylation of methoxy groups in anaerobic
270	digestion. The existences of fragment ions at m/z 170 and 182, however, suggested that the alkyl chain was
271	not modified. Therefore, M2 was inferred to be an O-demethylation metabolite of capsaicin, which was
272	previously detected in capsaicin degradation catalyzed by P450 enzyme as well (Reilly et al. 2003).
273	The precursor ion peak at m/z 336 [M3+H] ⁺ indicated the molecular weight of M3 being 335 (Fig. 3D),
274	which was 30 amu larger than that of capsaicin. It can be seen that the fragment ion at m/z 170 still existed,
275	suggesting that the alkyl chain at C7-N8 was unchanged. However, the fragment ion at m/z 137 disappeared,
276	which suggested that the vanilloid portion of capsaicin was modified. Two new fragment ions at m/z 184

and 140 were detected. The fragment ion at m/z 184 was likely produced by cleavage of alkyl chain at
N8-C9 of capsaicin, while the fragment ion at m/z 140 may be due to loss of -CH₂NO from the fragment ion
m/z 184. Thus, M3 was probably a doubly oxidized metabolite of dehydrogenated capsaicin, and this was
also determined in capsaicin bioconversion by *H. armigera* (Tian et al. 2019).

281 3.3 Could methane be produced from capsaicin degradation?

282 The analyses above showed that in anaerobic co-digestion, capsaicin was first degraded into M1, M2, 283 and M3 by hydroxylation, O-demethylation, dehydrogenation and doubly oxidization, respectively. According to the literature, these three metabolites would be further hydrolyzed into amino and carboxyl 284 285 compounds by amidases, with the possible degradation pathway of capsaicin being proposed in Fig. 4 (Cho et 286 al. 2014, Wang et al. 2018, Yue et al. 2020). However, it remains unknown whether these metabolic hydrolysates could be used for methane production in anaerobic co-digestion, requiring to be further clarified. 287 288 To figure out this possibility, one batch test was operated using either inocula or inocula + capsaicin as 289 the digestion substrate, with the experimental details being shown in Section 2.3. It was found that about 290 31.0 ± 0.9 mL methane was produced from the sole inocula whereas the corresponding value was 44.3 ± 1.3 291 mL from inocula + 36 mg capsaicin/g VS and 59.9 ± 1.8 mL from inocula + 68 mg capsaicin/g VS (Fig. S3). 292 This indicates that capsaicin could be served as substrate for methane production in anaerobic digestion. 293 According to Eq (3), it can be calculated that 0.59 g (or 826 mL) of methane will be produced from 1 g capsaicin if it is completely digested, suggesting that 60 and 87 mL methane should be generated from inocula 294 295 + 36 mg capsaicin/g VS and inocula + 68 mg capsaicin/g VS, respectively. However, the measured data 296 from the two inocula + capsaicin digesters were much lower than the theoretical values. The possible reasons might be due to 1) incomplete utilization of capsaicin degradation intermediates and 2) inhibition of 297 298 capsaicin to the activity of inocula.

299
$$C_{18}H_{27}NO_3 + 10.5 H_2O \rightarrow 11.25 CH_4 + 6.75 CO_2 + NH_3$$
 (3)

300 3.4 Effect of capsaicin on methane production.

301 The cumulative methane yield during anaerobic co-digestion in the presence of capsaicin at different 302 concentrations is shown in Fig. 5. It can be observed that methane yield in the reactor without extra 303 capsaicin addition (i.e., 2 ± 0.7 mg/g VS capsaicin reactor) increased with the digestion time from 1 to 34 d, 304 and no signification increase was observed after that day 34 (p > 0.05). The optimum digestion time for this 305 reactor was therefore 34 d, with the maximum methane yield of 274.6 ± 9.7 mL/g of VS being measured. 306 From Fig. 5, it was also found the increase of capsaicin affected methane production obviously. With an 307 increase of capsaicin concentration from 2 ± 0.7 to 68 ± 4.1 mg/g VS, methane yield decreased from $274.6 \pm$ 308 9.7 to 188.9 ± 8.4 mL/g VS. Apart from methane yield, the optimum digestion time was also affected by 309 capsaicin. For example, $68 \pm 4.1 \text{ mg/g VS}$ of capsaicin increased the optimum digestion time to 58 d. 310 To further understand the effect of capsaicin on anaerobic digestion from the aspect of model, the

modified Gompertz equation was employed to estimate three kinetic parameters, i.e., maximum methane yield potential (*Mm*), methane production rate (*Rm*), and lag phase time (λ). It can be found that the Gompertz equation described the experimental data well, with R² > 0.99 in all the scenarios (Fig. 5). When capsaicin concentration increased from 2 ± 0.7 to 68 ± 4.1 mg/g VS, the determined *Mm* and *Rm* decreased respectively from 257.4 mL/g VS and 17.8 mL/(g VS·d) to 189.9 mL/g VS and 6.6 mL/(g VS·d), whereas the calculated λ increased from 6.7 to 14.7 d. This indicates that the increase of capsaicin not only decreased biochemical methane potential but also inhibited the rate of methane production.

According to the analyses above, it was demonstrated that the addition of capsaicin reduced rather than improved methane yield, though the addition of capsaicin provided extra substrate for anaerobes to produce methane. This suggests that anaerobic co-digestion from original substrates was largely inhibited by 321 capsaicin, which was in accordance with the results reported previously (Yue et al. 2020). Based on the

322 experimental data obtained in the current work, it was estimated that 50% inhibitory concentration of

capsaicin to anaerobic co-digestion was around 36.26 mg capsaicin/g VS (Fig. S4). Since anaerobic
 co-digestion includes several processes such as solubilization, hydrolysis, acidogenesis, and methanogenesis,

325 the mechanism of how capsaicin affects methane production were explored in the following text.

326 3.5 Mechanism of How Capsaicin Inhibits Anaerobic Co-digestion.

327 It was found that the concentrations of soluble proteins and carbohydrates increased with capsaicin

328 concentration (Fig. 6A and Fig. 6B). For example, the concentrations of soluble proteins and carbohydrates

in the reactor fed with 2 ± 0.7 mg/g VS capsaicin were respectively 882.7 ± 23.2 and 2695.4 ± 25.5 mg

330 COD/L, while the corresponding concentrations in the reactor fed with $68 \pm 4.1 \text{ mg/g VS}$ capsaicin were 331 1505.8 ± 29.1 and 5530.2 ± 53.2 mg COD/L, respectively. According to the literature, an increase in the 332 fluorescence intensity indicates an increase in soluble organics in digestion liquid (Fig. 6C) (Xu et al. 2017). 333 There are two peaks, which are respectively located at Ex/Em of 200-250/290-320 and 250-280/<380 nm, 334 being found in all the samples (Fig. 6C). The fluorescence intensity of both the peaks increased with the 335 addition of capsaicin, suggesting that an increase of capsaicin enhanced increases in soluble organics. All 336 these facts confirmed that the presence of capsaicin improved rather than reduced solubilization, indicating 337 that capsaicin may inhibit the bio-processes involved in anaerobic co-digestion.

Table 1 summarizes the experiment value and model-simulation value of inhibition of capsaicin on dextran, glucose, acetate and H₂. It can be seen that the specific degradation rates of dextran, glucose, acetate, and hydrogen in the blank (i.e., 0 mg/L capsaicin) were respectively 8.07 ± 0.26 , 7.00 ± 0.30 , 2.85 ± 0.14 , and 0.24 ± 0.01 mg/g VS·h, and these values were considered the original activities of microbes relevant to hydrolysis, acidogenesis, acetotrophic methanogenesis, and hydrogenotrophic methanogenesis, respectively. 343 When 50 mg/L capsaicin was added, these values decreased respectively to 6.19 ± 0.62 , 3.30 ± 0.66 , $1.12 \pm$

344 0.03, and 0.17 \pm 0.02 mg/g VS·h. This suggests 50 mg/L capsaicin reduced the relative activities of

microbes (expressed as % of the original) relevant to hydrolysis, acidogenesis, acetotrophic methanogenesis,
and hydrogenotrophic methanogenesis by 23%, 27%, 61%, and 29%, respectively. Similar observations
were also made at 30 mg/L capsaicin.

From Table 1, it was also found that inhibition constant ($K_{s,i}$) of capsaicin to the degradation of these substrates was in the order of acetate > H₂ > glucose > dextran, suggesting that the inhibition of capsaicin to these bioprocesses was in the sequence of acetotrophic methanogenesis > hydrogenotrophic methanogenesis > acidogenesis > hydrolysis. All the results showed that although capsaicin enhanced solubilization, it significantly inhibited the bioprocesses of hydrolysis, acidogenesis, and methanogenesis, especially acetotrophic methanogenesis. It can be understood why capsaicin inhibited methane production from anaerobic co-digestion.

355 It was reported that capsaicin could induce apoptosis by either altering key kinases (Pramanik and Srivastava 2012), or decreasing the intracellular NAD⁺/NADH ratio by binding to quinone binding site of 356 357 NADH dehydrogenase 1 (NDH-1) (Lee et al. 2015b, Yagi 1990). Furthermore, Torrecillas et al. (2015) 358 found capsaicin molecule could establish a molecular interaction with cell membrane, where the nine-carbon 359 alkyl chain of capsaicin was aligned with the phospholipid acyl chains, perturbing the cooperative behavior of the phospholipid and inducing apoptosis. When capsaicin entered into the anaerobic co-digestion systems, it 360 361 could contact with the membrane and key enzymes of anaerobes, or even enter into the intracellular cells. These behaviors may result in inactivation of functional enzymes, reduction in conversion between NAD⁺ and 362 363 NADH, or even cell lysis (Fig. 7A).

364	This deduction can be supported by flow cytometry, which is usually used to reflect the cell functional
365	state. The physiological status of microorganism cells can be divided into four regions. Among them,
366	viable cells are shown in AV-/PI (Q4), early apoptotic cells are shown in AV+/PI (Q3), necrotic (or late
367	apoptotic) cells are shown in $AV^+/PI^+(Q_2)$, and debris and damaged cells are shown in $AV^-/PI^+(Q_1)$. It can be
368	seen that with an increase of capsaicin from 0 to 50 mg/L the fluorescence percentage of viable cells
369	decreased from 96.7% to 78.7%, while the fluorescence percentage of early apoptotic cells increased from 0.9%
370	to 16.0% (Fig. 7B). This is the major reason for capsaicin enhancing solubilization but reducing hydrolysis,
371	acidogenesis and methanogenesis.
372	According to the data shown in Table 1, it can be found that the inhibition of capsaicin to acetotrophic
373	methanogenesis, one major pathway responsible for methane production, was much severer than that to
374	hydrogenotrophic methanogenesis, the other methane production pathway. Thus, one might want to know
375	why capsaicin caused different inhibitions to these two methane production pathways. In acetotrophic
376	methanogenesis, acetate can be either converted into acetyl-phosphate and acetyl-CoA catalyzed by AK and
377	PTA in turn or directly degraded to acetyl-CoA catalyzed by CoA. The generated acetyl-CoA is then
378	converted into 5-methyl-THMPT under the catalysis of ACDS. In hydrogenotrophic methanogenesis, H ₂ and
379	CO_2 can be converted into 5-methyl-THMPT, with mch and F_{420} being as the key enzymes (Fig. 8A). As the
380	same intermediate in the two pathways, 5-methyl-THMPT then undergoes the succession steps of
381	5-methyl-THMPT \rightarrow methyl-CoM \rightarrow CH ₄ . It was found that although the presence of capsaicin inhibited
382	the activity of all these enzymes in acetotrophic and hydrogenotrophic methanogenesis, its inhibition to CoA
383	and ACDS was much severer than that to others (Fig. 8B). This may explain why capsaicin caused severer
384	inhibition to acetotrophic methanogenesis than hydrogenotrophic methanogenesis.

385 When ACDS catalyzes the step of acetyl-CoA to 5-Methyl-THMPT, two electrons would be generated 386 (Grahame and DeMoll 1996). In anaerobic digestion, the generated electrons are generally transferred to ferredoxin by 4Fe-4S clusters ligands on ACDS (Ferry 2011). Previous publication demonstrated that 387 388 capsaicin could be activated to an electrophilic intermediate, and this intermediate could compete for the electrons available for ferredoxin utilization (Fig. 8C) (Surh and Lee 1995). This causes reductions in the 389 390 electrons transferred by 4Fe-4S clusters ligands on ACDS, which might be the reason for capsaicin severely 391 inhibiting the activity of ACDS. Moreover, it is reported that the amino group of capsaicin can be subjected 392 to dehydration condensation reaction with carboxyl group of CoA, inhibiting the metabolic activity of CoA 393 (Yue et al. 2020).

394 3.6 Effect of capsaicin on microbial community.

Illumina Miseq 16S-rRNA genes sequencing was performed to investigate the effect of capsaicin on microbial community by comparing the structure and abundance of microbial community between the control and experimental reactors. The control reactor was fed with 2 mg/g VS capsaicin co-substrates, while the experimental reactor was fed with 68 mg/g VS capsaicin co-substrates. The number of operational taxonomic units was 1074 in the control reactor and 1050 in the experimental digester, with 886 being shared

400 (Fig. S5). The Alpha diversity results (Table S2) showed that PD index was similar in the two reactors,

401 while Chao index in the control was greater than that in the experiment reactor, suggesting that the increase of

- 402 capsaicin reduced the microbial diversity but did not change largely the microbial structure.
- 403 At the phylum level, the most predominant bacteria in the two reactors were *Firmicutes*, *Bacteroidetes*,
- 404 *Proteobacteria*, and *Actinobacteria* (Fig. S6). It is reported that several anaerobes in these phyla can degrade
- 405 organic compounds (e.g., proteins and carbohydrates) (Wei et al. 2019), and many bacteria affiliated to
- 406 *Firmicutes* and *Proteobacteria* were volatile fatty acid producers (Wang et al. 2017). *Euryarchaeota* was the

407 only archaeal phylum in the two reactors (Fig. S6), which was known as methanogens and detected in several
408 anaerobic digesters (Wei et al. 2019).

409	Fig. 9 displays the genus-level distributions of bacteria and archaea abundances in the two reactors.
410	Seven genera of bacteria, which were responsible for hydrolysis and acidogenesis, were detected in the two
411	reactors. For example, the abundance of Bacteroide, which was reported to degrade carbohydrates and
412	organic acids (Pang et al. 2020), was measured to be 17.6% in the control, but it was completely washed out
413	in the experiment reactor. The abundances of Dysgonomonadacea, Petrimonas, and Macellibacteroides,
414	which were able to degrade various polysaccharides and proteins (Maspolim et al. 2015, Murakami et al. 2018,
415	Xu et al. 2019), reduced from 6.5%, 5.3%, and 7.9% in the control to 3.2%, 2.4%, and 1.2% in the experiment
416	reactor, respectively (Fig. 9A). Further calculation showed that the total abundance of these genera was 42.6%
417	in the control and 14.8% in the experiment reactor, indicating that capsaicin reduced largely the number of
418	anaerobes relevant to hydrolysis and acidogenesis.
419	It can be also seen from Fig. 9A that the abundance of Escherichia-Shigella, a resistant genus having
420	ability to degrade aromatic organic pollutants (Cui et al. 2017, Vasiliadou et al. 2018), increased from 1.0% in
421	the control to 10.7% in the experiment reactor. Moreover, the abundance of several other contaminant
422	degradation microbes such as Fonticella, Pirellulaceae, Enterococcus and Herbinix (Cao et al. 2018, Fraj et al.
423	2013, Koeck et al. 2016, Tong et al. 2017), increased with capsaicin addition as well. The total abundance of
10.1	

425 experiment reactor, suggesting that these microbes might be capsaicin decomposers in such anaerobic426 co-digestion systems.

424

potential complex organic degradation microbes increased from 20.7% in the control to 42.4% in the

Fig. 9B shows the distribution of archaea community in the two reactors. The total sequences of
methanogens decreased from 16313 in the control to 7592 in the experiment reactor, suggested that the

429	addition of capsaicin reduced the total archaea populations. Among them, the abundance of					
430	Methanobacterium, decreased from 73.4% in the control to 64.7% in the experiment reactor. However, the					
431	abundances of Methanobrevibacter and Methanosphaera increased from 2.0% and 0.2% in the control to 9.1%					
432	and 2.2%, respectively. This suggest that the effect of capsaicin on different types of archaea is different,					
433	and manipulation of co-digesters to enrich Methanobrevibacter and Methanosphaera could effectively					
434	mitigate the inhibition of capsaicin to methane production. The accurate reason for this different impact is					
435	unclear at the current stage, more efforts are required in the future.					
436	4. Conclusions					
437	This study evaluated the degradation of capsaicin in anaerobic co-digestion of FW and WAS and					
438	explored the effect of capsaicin on methane production as well as the underlying mechanisms of capsaicin					
439	affecting methane yield. The findings obtained not only advance the understanding of capsaicin-involved					
440	digestion but also guide engineers to develop effective strategies in the future to manipulate anaerobic					
441	co-digestion of FW and WAS. The main conclusions are:					
442	(1) Capsaicin can be degraded by some microbe and used as substrate to produce methane.					
443	HPLC-MS/MS analysis that hydroxylation, O-demethylation, dehydrogenation and doubly					
444	oxidization are involved in capsaicin degradation.					
445	(2) The presence of capsaicin not only slowed the process of anaerobic co-digestion but also decreased					
446	methane yield. With the increase of capsaicin from 2 ± 0.7 . to 68 ± 4 mg/g VS, the maximal methane					
447	yield decreased from 274.6 \pm 9.7 to 188.9 \pm 8.4 mL/g VS, while the methane production rate					
448	decreased from 17.76 to 6.63 mL/(g VS·d).					

449	(3) Mechanism investigations revealed that the presence of capsaicin induced apoptosis, which led to
450	significant inhibitions to hydrolysis, acidogenesis, and methanogenesis, especially acetotrophic
451	methanogenesis.
452	(4) The presence of capsaicin enhanced the populations of complex organic degradation microbes such
453	as Escherichia-Shigella and Fonticella but decreased the numbers of anaerobes relevant to hydrolysis,
454	acidogenesis, and methanogenesis such as Bacteroide and Methanobacterium.
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458	Appendix A. Supplementary data
459	This file contains Text S1-S3, Table S1-S2 and Fig. S1-S6.

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1 Table 1

2 Experiment and model values of capsaicin inhibition to dextran, glucose, acetate and H₂ conversions.

	Experiment values ^a			Model values			
Substrate	0 mg/L	30mg/L	50 mg/L	Xs,o ^b	Xs,i ^c		Ks,i ^d
					30 mg/L	50 mg/L	
Dextran	8.07±0.26	5.99±0.19	6.19±0.62	3.01	1.98	1.39	48.5
Glucose	7.00±0.30	5.56±0.35	5.12±0.66	2.00	1.41	1.05	35.9
Acetate	2.85±0.14	1.44±0.13	1.12±0.03	0.79	0.35	0.33	13.7
H_2	0.24±0.01	0.19±0.02	0.17±0.02	1.90	1.45	1.34	33.4

^a Results are the average and their standard deviations of triplicate tests, and the unit is mg/gVS·h

4 ^b $X_{s,0}$ is the degradation of the substrate without capsaicin addition, and the unit is g/(L·d) or g/L.

5 ^c $X_{s,i}$ is the degradation of the substrate when different capsaicin are added, and the unit is $g/(L \cdot d)$ or g/L.

6 ${}^{d}K_{s,i}$ is the related inhibition constant of capsaicin calculated by Eq (2), and the unit is mg/L.

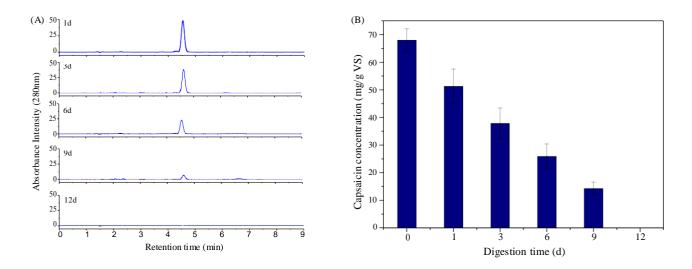
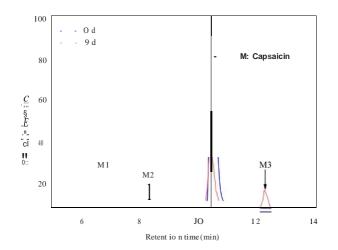


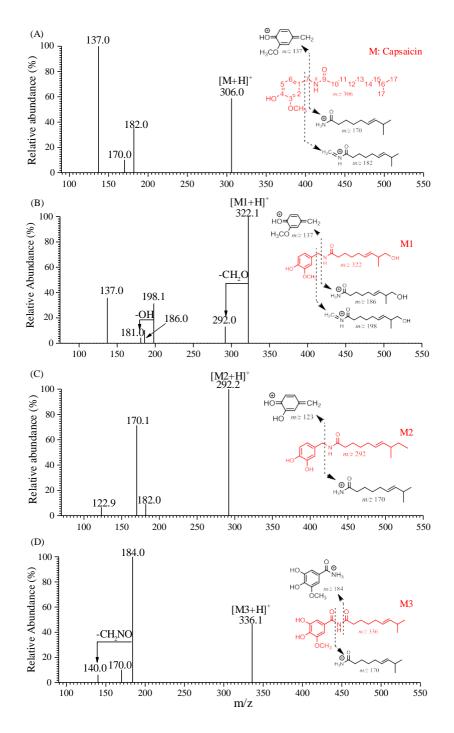
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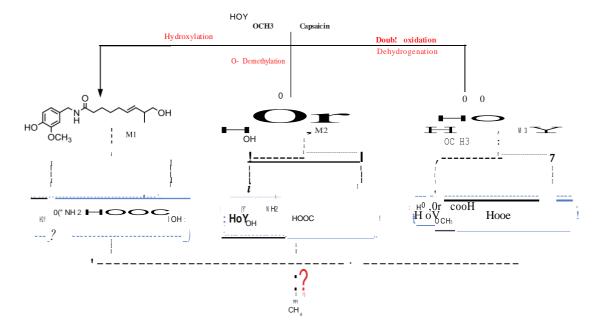




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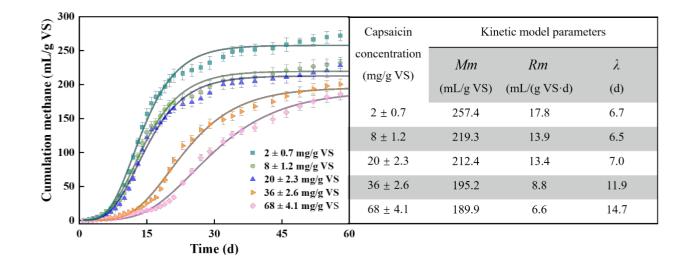


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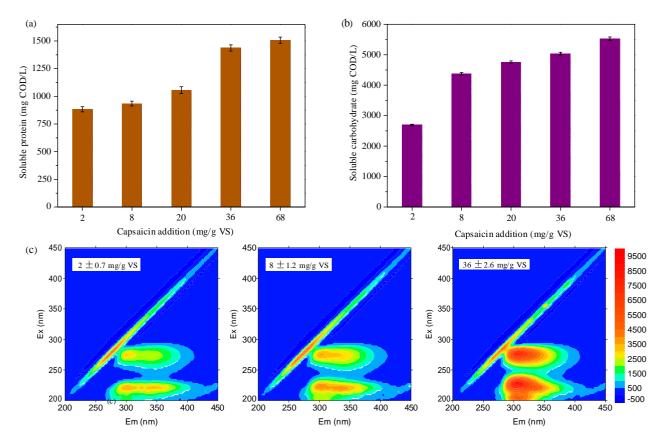


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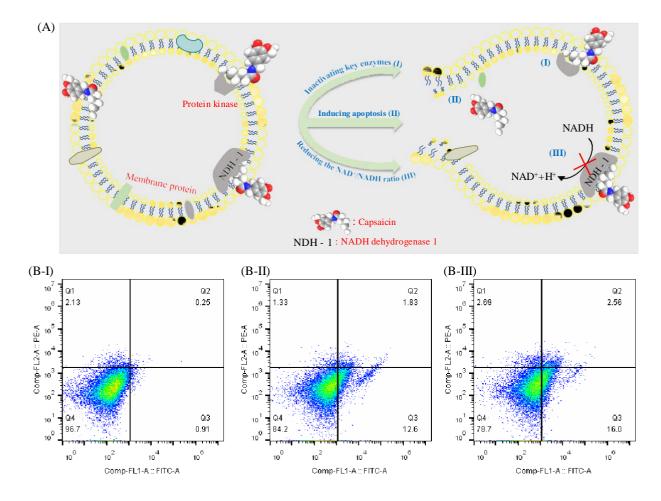


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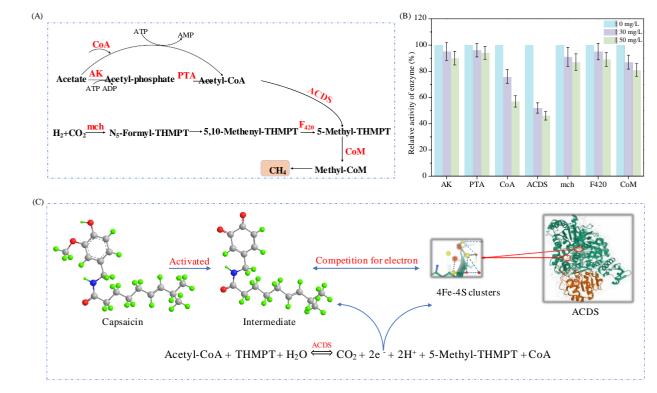


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