

# **COMPACT AND ROBUST MEMBRANE BIOREACTOR FOR SOURCE-SEPARATED URINE RESOURCE RECOVERY FOR A CIRCULAR ECONOMY**

**by JIAXI JIANG**

Thesis submitted in fulfilment of the requirements for  
the degree of

**Doctor of Philosophy**

under the supervision of Prof Hokyong Shon and  
Dr Sherub Phuntsho

University of Technology Sydney  
Faculty of Engineering and Information Technology

February 2022

## **Certificate of Original Authorship**

I, Jiayi Jiang declare that this thesis, is submitted in fulfilment of the requirements for the award of Doctor of Philosophy, in the School of Civil and Environmental Engineering, Faculty of Engineering and Information Technology at the University of Technology Sydney.

This thesis is wholly my own work unless otherwise referenced or acknowledged. In addition, I certify that all information sources and literature used are indicated in the thesis.

This document has not been submitted for qualifications at any other academic institution.

This research is supported by the Australian Government Research Training Program.

Production Note:

**Signature:** Signature removed prior to publication.

**Date:** 23/02/2022

## **Acknowledgements**

I would like to express my sincere appreciation to my principal supervisor Prof. Hokyong Shon and co-supervisor Dr. Sherub Phuntsho for their continuous support of my Ph.D. study and encourage me in pursuing my research interests. My deepest thanks to Dr. Pema Dorji, Dr. Ugyen Dorji, Dr. Jiawei Ren, Dr. Federico Volpin, Mr. Umakant Badeti and Mr. Abdulaziz Yousef B Almontashiri for their guidance and collaborations. Thanks to my family for supporting me all the time, always uplift me, comfort me, and bring joy to my soul.

## List of Publications

1. U. Badeti, **J. Jiang**, A. Almuntashiri, N. Pathak, U. Dorji, F. Volpin, S. Freguia, W.L. Ang, A. Chanan, S. Kumarasingham, H.K. Shon, S. Phuntsho, Impact of source-separation of urine on treatment capacity, process design, and capital expenditure of a decentralised wastewater treatment plant, *Chemosphere*, 300 (2022) 134489.
2. **J. Jiang**, S. Phuntsho, N. Pathak, Q. Wang, J. Cho, H.K. Shon, Critical flux on a submerged membrane bioreactor for nitrification of source separated urine, *Process Safety and Environmental Protection*, 153 (2021) 518-526.
3. J. Ren, D. Hao, **J. Jiang**, S. Phuntsho, S. Freguia, B.-J. Ni, P. Dai, J. Guan, H.K. Shon, Fertiliser recovery from source-separated urine via membrane bioreactor and heat localized solar evaporation, *Water Research*, 207 (2021) 117810.
4. F. Volpin, U. Badeti, C. Wang, **J. Jiang**, J. Vogel, S. Freguia, D. Fam, J. Cho, S. Phuntsho, H.K. Shon, Urine treatment on the international space station: current practice and novel approaches, *Membranes*, 10 (2020) 327.
5. F. Volpin, **J. Jiang**, I. El Saliby, M. Preire, S. Lim, M.A. Hasan Johir, J. Cho, D.S. Han, S. Phuntsho, H.K. Shon, Sanitation and dewatering of human urine via membrane bioreactor and membrane distillation and its reuse for fertigation, *Journal of Cleaner Production*, 270 (2020) 122390.

## **Journal Articles Under Review**

1. W. Shon, **J. Jiang**, S. Phuntsho, H.K. Shon. (Under review). Nutrient in a Circular Economy: Role of urine separation and treatment.
2. **J. Jiang**, A. Almuntashiri, W. Shon, S. Phuntsho, Q. Wang, S. Freguia, I, El-Saliby, H.K. Shon. (Under review). Feasibility study of powdered activated carbon membrane bioreactor (PAC-MBR) for source-separated urine treatment: a comparison with MBR.

## Conferences

1. The 11th International Membrane Science and Technology Conference (IMSTEC 2022), 4-8 December 2022. Australia & online. Poster presentation
2. 2022 Rich Earth Summit, 1- 3 November 2022. USA & online. Oral presentation
3. The International Workshop on Membrane in Kobe (IWMK 2021), 18-19 November 2021 online. Poster presentation
4. 2021 Rich Earth Virtual Summit, 3-5 November 2021 online. Attended
5. North American Membrane Society (NAMS 2020), 18-21 May 2020 online. Attended
6. The 2021 International Conference on the "Challenges in Environmental Science and Engineering" (CESE-2021), 6-7 November 2021 online. Oral presentation
7. The 4th International Conference on capacitive Deionization and Electrosorption (CDI&E 2019), 20-23 May China. Poster presentation

# Table of Contents

Certificate of Original Authorship .....	i
Acknowledgements .....	ii
List of Publications .....	iii
Journal Articles Under Review .....	iv
Conferences.....	v
List of Figures .....	x
List of Tables .....	xiii
Abstract .....	xiv
1 Introduction.....	1
1.1 Research background.....	1
1.2 Contribution to the existing knowledge.....	2
1.3 Research aims and objectives. ....	4
1.4 Thesis structure outline.....	5
2. Literature review.....	7
2.1 Urine composition and properties.....	7
2.2 Why reusing the nutrients in the urine.....	9
2.3 Types and Implementations of Urine Diversion.....	12
2.3.1 Urine-Diverting Flush Toilet (UDFT) .....	13
2.3.2 Urine-Diverting Dry Toilet (UDDT) .....	18

2.4	Review of current membrane technologies for urine resource utilization....	19
2.4.1	Pressure driven membrane process .....	20
2.4.2	Forward osmosis (FO) .....	21
2.4.3	Electrodialysis (ED).....	22
2.5	Review of alternative membrane-based process for source-separated urine resource utilization .....	24
2.5.1	Forward osmosis-reverse osmosis (FO-RO).....	24
2.5.2	Membrane bioreactor (MBR) and MBR-combined treatment process ....	25
2.5.3	Membrane distillation (MD).....	28
2.6	Nitrification.....	29
3.	Critical flux on a submerged membrane bioreactor for nitrification of source separated urine .....	32
3.1	Abstract.....	32
3.2	Introduction.....	33
3.3	Materials and methods .....	36
3.3.1	MBR set-up and operation.....	36
3.3.2	Characteristics of stored source separated urine .....	39
3.3.3	Determination of critical flux and the critical flux for irreversibility.....	40
3.3.4	Analytical methods .....	42
3.4	Results and discussion .....	44
3.4.1	UF-MBR start-up and operation .....	44
3.4.2	Effect of step length and height on critical flux.....	49



3.4.3	Effect of aeration intensity on critical flux .....	50
3.4.4	Effect of sludge concentration on critical flux.....	51
3.4.5	Fouling reversibility .....	52
3.5	Conclusions.....	56
4	Effects of PAC concentration in membrane bioreactor (MBR) for source-separated urine treatment .....	57
4.1	Materials and methods.....	57
4.1.1	Laboratory scale PAC-MBR operation.....	57
4.1.2	Analytical methods .....	59
4.2	Results and discussion .....	61
4.2.1	Effect of PAC dosage on membrane permeate water quality .....	61
4.2.2	Effect of PAC dosage on organic matter removal .....	62
4.2.3	Effect of PAC dosage on micropollutant removal .....	64
4.2.4	Effect of PAC dosage on sludge mixture properties.....	65
4.3	Conclusions.....	66
5.	Feasibility study of powdered activated carbon membrane bioreactor (PAC-MBR) for source-separated urine treatment: a comparison with MBR .....	67
5.1	Abstract.....	67
5.2	Introduction.....	68
5.3	Materials and methods .....	69
5.3.1	Experimental setup.....	69
5.3.2	Water quality analysis .....	72

5.3.3	Micropollutant analysis.....	73
5.3.4	Fouling models analysis.....	75
5.4	Results and discussion .....	78
5.4.1	Comparison of permeate water quality.....	78
5.4.2	Comparison of organic matter removal .....	79
5.4.3	Comparison of biomass growth.....	80
5.4.4	Membrane performance.....	82
5.4.5	Removal of micropollutants by MBR.....	87
5.5	Conclusion.....	91
6	Conclusions and recommendations .....	92
6.1	Conclusions.....	92
6.2	Limitations and recommendations.....	93
	Bibliography.....	95
	Appendix A Code for fouling model simulations and automatically calculating sum of squared error (SSE) and model fitting constants.....	111
	Appendix B Theoretical fouling models results (Control MBR).....	123
	Appendix C Theoretical fouling models results (Hybrid PAC-MBR) .....	127

## List of Figures

Figure 2.1 World and regional potential nutrient balance between 2016 and 2020. Modified from FAO (2017). .....	10
Figure 2.2 Scheme of flow streams separation, treatment, and reuse for urine diversion flush toilets (UDFT) with sewerage system and urine diversion dry toilets (UDDT). Adapted with permission granted by the copyright holder Tilley et al. (2014).....	16
Figure 2.3 Two-phase collaborative project for implementation of novel sanitation systems in an urban office, funded by the Federal Ministry of Education and Research, Germany. Modified from Winker and Saadoun (2011).....	17
Figure 2.4 Pressure driven membrane filtration types .....	21
Figure 2.5 Schematic diagram of forward osmosis.....	22
Figure 2.6 Schematic diagram of membrane capacitive deionization (MCDI) .....	23
Figure 2.7 Schematic diagram of hybrid forward osmosis-reverse osmosis (FO-RO) system.....	24
Figure 2.8 Schematic diagram of two common MBR configurations. (a) side-stream MBR, (b) submerged MBR.....	26
Figure 2.9 Schematic diagram of MD system.....	29
Figure 3.1 Schematic diagram of the lab scale UF-MBR .....	37
Figure 3.2 Pure water flux (PWF) of potted UF membrane module at different TMP...	37
Figure 3.3 Typical flux profile in (a) continues and (b) improved flux-step method. ....	41
Figure 3.4 (a) pH profile during the MBR start-up and stable operation stages. (b) all-time concentration of inorganic nitrogen compounds in feed urine and MBR permeate .....	46
Figure 3.5 Concentration of FA and FNA during the MBR start-up period and stable operation, and corresponding nitrite accumulation phenomenon. ....	48

Figure 3.6 Effects of various flux step length and step height on critical flux when aeration intensity at 0.2 m <sup>3</sup> h <sup>-1</sup> , biomass concentration at 3.5 g. L <sup>-1</sup> , initial flux rate at 4 Lm <sup>-2</sup> h <sup>-1</sup> , and reference flux rate at 0.5 Lm <sup>-2</sup> h <sup>-1</sup> .....	50
Figure 3.7 Effects of various aeration intensity and biomass concentration on critical flux when initial flux rate at 4 Lm <sup>-2</sup> h <sup>-1</sup> , reference flux rate at 0.5 Lm <sup>-2</sup> h <sup>-1</sup> , flux step length at 15 min, and step height at 6 Lm <sup>-2</sup> h <sup>-1</sup> .....	51
Figure 3.8 Profile of TMP, total fouling rate (FTotal), irreversible fouling rate (FIrr) and critical fouling rate (FCrit) on membrane determined by the improved flux-step method among various aeration intensity (a) 0.1 m <sup>3</sup> h <sup>-1</sup> , (b) 0.2 m <sup>3</sup> h <sup>-1</sup> , and (c) 0.4 m <sup>3</sup> h <sup>-1</sup> . The biomass concentration at 3.5 g.L <sup>-1</sup> , initial flux rate at 4 Lm <sup>-2</sup> h <sup>-1</sup> , reference flux rate at 0.5 Lm <sup>-2</sup> h <sup>-1</sup> , flux step length at 15 min, and step height at 6 Lm <sup>-2</sup> h <sup>-1</sup> .....	55
Figure 4.1 Schematic diagram of proposed hybrid PAC-MBR.....	59
Figure 4.2 Variation of COD removal efficiencies in (a) low PAC-MBR and (b) high PAC-MBR overtime .....	63
Figure 4.3 Overall micropollutants removal rate in low PAC-MBR and high PAC-MBR .....	64
Figure 4.4 Variation of MLSS concentration and MLSS/MLVSS ratio in (a) low PAC-MBR and (b) high PAC-MBR overtime .....	66
Figure 5.1 Schematic diagram of (a) control MBR and (b) hybrid PAC-MBR.....	71
Figure 5.2 Variation of COD removal efficiencies in (a) control MBR, and (b) hybrid PAC-MBR in 73 days .....	80
Figure 5.3 Variation of MLSS concentration and MLSS/MLVSS ratio in (a) control MBR and (b) hybrid PAC-MBR in 73 days .....	81

Figure 5.4 Theoretical and experimental Pt/P0 versus time profiles and corresponding SSE values for single and combined membrane fouling models in (a) control MBR and (b) hybrid PAC-MBR..... 86

Figure 5.5 Targeted micropollutant removal rate and logD<sub>6.2</sub> value in control MBR and hybrid PAC-MBR ..... 88

## List of Tables

Table 2.1 The composition of fresh and stored human urine (Udert et al., 2006, Rose et al., 2015, Udert and Wachter, 2012) .....	8
Table 2.2 World and regional potential balance of ammonia as N, phosphate as P, potash as K between 2016 and 2020 (million tonnes). Modified from FAO (2017) .....	10
Table 3.1 Properties of the potted UF membrane module .....	38
Table 3.2 Composition and corresponding ion concentrations in each 40 L stored raw urine at room temperature .....	39
Table 3.3 Proposed experimental operation conditions and control parameters for membrane critical flux study.....	41
Table 3.4 The linear relationship between various aeration intensity and its corresponding critical flux value.....	52
Table 4.1 Composition and corresponding ion concentrations in source-separated urine, low PAC-MBR permeate and high PAC-MBR permeate.....	61
Table 5.1 Composition and corresponding ion concentrations in source-separated urine, control MBR permeate, and hybrid PAC-MBR permeate.....	71
Table 5.2 MRM table for proposed LC-MS/MS analysis.....	74
Table 5.3 Membrane fouling models and corresponding equations at constant flux.....	76
Table 5.4 Theoretical model fitting results and SSE values for the single and combined membrane fouling modules.....	84
Table 5.5 Physicochemical properties of targeted micropollutants and their corresponding removal efficiencies .....	89

## **Abstract**

Human urine contains essential nutrient – nitrogen (N), phosphorus (P) and potassium (K) - for crop cultivation. However, using raw human urine as a direct agricultural fertilizer source is limited, due to its distinct odour, high pH condition, pathogen risk associated with faecal cross-contamination, and the possible presence of high concentrations of pharmaceuticals. Biological nitrification, a two-step biological oxidation process, is therefore a promising technology to covert volatile and odorous ammonia into stable odour-free nitrate, while still preserving all the nutrients. Although biological nitrification is a well-understood process, only a few research groups have studied the application of this process with undiluted human urine, and the experiences to optimize the nitrification of source-separated urine without addition of alkalinity are even less.

In addition, micropollutants such as pharmaceuticals and personal care products are a group of emerging environmental contaminants, which are structurally complex and can cause adverse physiological effects on human health even at low concentration when exposed for long-term. However, the current wastewater treatment technologies are not designed to remove these compounds, and hence most of these residual pharmaceuticals and hormones remain in the treated effluent. Therefore, it is very important that we remove the residual micropollutants by a natural biological process.

The combined processes of powdered activated carbon - microfiltration membrane bioreactor (PAC-MF-MBR) is thereby proposed in this work to optimize the efficiency

of biological nitrification, control membrane fouling, improve organic removal efficiency from 88% to 96%, achieve greater than 99% removal efficiency among all targeted micropollutants (metronidazole, acetaminophen, naproxen, ibuprofen carbamazepine and estriol), promote more rapid biomass growth, increase sludge floc size growth by 17% and achieve complete nutrient recovery from source-separated urine. This study demonstrates the potential application of full-scale PAC-MF-MBR plant in treating source-separated urine at building level for complete nutrient recovery.

Keywords: membrane bioreactor (MBR); powdered activated carbon (PAC); source-separated urine; circular economy; resource recovery; nitrification; micropollutant; fouling