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# 1 Janus membranes for membrane distillation: Recent advances and 2 challenges

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## 7 **Abstract:**

8 Membrane distillation (MD) is a promising hybrid thermal-membrane separation technology  
9 that can efficiently produce freshwater from seawater or contaminated wastewater.  
10 However, the relatively low flux and the presence of fouling or wetting agents in feed solution  
11 negate the applicability of MD for long term operation. In recent years, ‘two-faced’  
12 membranes or Janus membranes have shown promising potential to decrease wetting and  
13 fouling problem of common MD system as well as enhance the flux performance. In this  
14 review, a comprehensive study was performed to investigate the various fabrication,  
15 modification, and novel design processes to prepare Janus membranes and discuss their  
16 performance in desalination and wastewater treatment utilizing MD. The promising potential,  
17 challenges and future prospects relating to the design and use of Janus membranes for MD  
18 are also tackled in this review.

19  
20 **Keywords:** Janus membrane; membrane distillation; desalination; wastewater treatment;  
21 membrane fabrication

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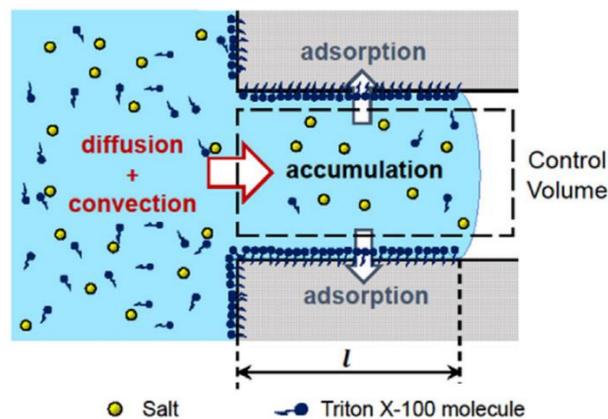
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58

59 **1. Introduction**

60 Global water scarcity, driven by rapid urbanization, population growth and climate change, is  
61 a critical issue nowadays and is expected to get worse in the next decade. As a result,  
62 alternative sources of fresh water such as from seawater and wastewater are being sought  
63 out [1]. The vast amounts of seawater available makes desalination as a viable option for  
64 freshwater extraction. However, the state-of-the-art reverse osmosis (RO) that is widely used  
65 in many countries, still has limitations in treating high salinity brine. In recent years,  
66 membrane distillation (MD) process has driven increased interest due to its ability to treat  
67 hypersaline solutions, challenging wastewaters [2] and even for resource recovery [3]. MD is  
68 a thermal-based membrane separation system which benefits from possible use of low-grade  
69 thermal energy and is a brilliant candidate to treat a wide range of water sources from  
70 common brackish and seawater to hypersaline RO retentate, shale-gas or coal-steam gas  
71 produced water, and highly polluted wastewaters [4, 5]. Though MD has relatively lower  
72 energy efficiency compared to RO [6], it still has some advantages over RO in terms of its  
73 ability to utilize low-grade heat sources such as waste heat and solar energy, is highly suited  
74 for modular system configuration, and can treat hypersaline solutions that is above the  
75 salinity limit of RO [7]. Despite these advantages, industrial application of MD is still limited  
76 due to low flux and wetting issues of currently used membranes. Wetting happens when  
77 liquid water overcomes the entry pressure of the membrane pores starting from the largest  
78 pore size, thus penetrating and reaching the permeate side. Wetting is exacerbated when

79 dealing with challenging wastewaters that contain inorganic salts, humic acid and low surface  
80 tension components such as surfactants, oils, etc.

81 Although different studies generally attributed the wetting mechanism to the change in  
82 hydrophilicity of membrane pores by adsorption of the surfactants on the pore walls (Figure  
83 1) [8], recent studies focusing on the wetting mechanism proved that the main reason for  
84 pore wetting is the reduction of surface tension of the feed stream [9]. These studies also  
85 proved that adsorption of the surfactants on the pore walls can delay the wetting by removing  
86 the surfactants from the water-gas frontier [9-11].



87

88 *Figure 1 Pore wetting schematic in a microporous membrane [10]*

89 Many recent studies have tried on increasing the hydrophobicity of the membranes by  
90 increasing the surface roughness. The rough surfaces can trap the air and decrease the  
91 slipping angle of the membrane, resulting to higher hydrophobicity. The strategies include  
92 nanoparticle (NP) coating or incorporation [12, 13] such as Si [12], Al [14], and Ti [15] NPs, co-  
93 extrusion [16, 17], co-spinning, electrospinning [18], spray-assisted non-solvent induced  
94 phase separation [19], grafting [20], and phase inversion techniques [21, 22]. Though the  
95 superhydrophobic membranes improved their wetting resistivity, however, their oleophilic  
96 characteristics can still lower the durability of the membranes, and fouling is still a drastic

97 problem [23-25]. To address this drawback, omniphobic membranes, which can repel both  
98 water and low surface tension agents have been designed and investigated [26]. This can be  
99 obtained by designing a hierarchical structure or re-entrant surface structure followed by  
100 coating with a low surface energy layer [27, 28]. However, omniphobic membranes are still  
101 prone to fouling issues due to hydrophobic foulants like oil droplets [11, 29]. Thus, continued  
102 efforts are still done to design a membrane that can potentially reduce fouling formation,  
103 while resisting wetting and maintaining adequate flux and rejection.

104 Inspired from nature, especially from sea species like clamshell and sharkskin, many groups  
105 have worked towards designing underwater oleophobic surfaces which can dramatically  
106 decrease fouling problems made by microorganism or by organic fouling for MD application.  
107 Among the various suggested methods, the Janus membrane (multilayer  
108 hydrophilic/superhydrophobic or hydrophilic/omniphobic membrane) or 'two-faced'  
109 membrane (i.e., both sides of the membrane have different wetting properties) is a promising  
110 structure for MD systems for the treatment of challenging wastewaters from food processing,  
111 leather and fabric industries, shale gas well drilling, and domestic sewage [30, 31]. For MD  
112 application, a Janus membrane, which has one side hydrophilic layer and one side omniphobic  
113 or hydrophobic layer can potentially repel most of fouling agents like oil particles [18, 22, 27].  
114 The hydrophilic layer repels the oil droplets and other hydrophobic compounds and prevent  
115 their adhesion on the surface, and the hydrophobic or omniphobic base layer mitigates the  
116 wetting problem [28, 32].

117 Additionally, to enhance the driving force in MD and consequently have high permeate flux,  
118 membranes with low mass transfer resistance and high heat transfer resistance are  
119 favourable. The preferred membrane for MD process to have high flux is a porous and thin

120 membrane. However, this feature can also dramatically decrease the strength of the  
121 membrane, especially if used in vacuum MD (VMD) modules, and can increase the heat loss  
122 through the membrane. As a result, to overcome this problem, the best suggested method is  
123 fabrication of Janus membrane to increase the thickness of the membrane (by adding  
124 hydrophilic layer) without increment in hydrophobic thickness [44]. Studies have reported  
125 that Janus membranes can enhance the flux performance and decrease the heat loss, while  
126 reducing the propensity for wetting and fouling [27, 33]. The hydrophilic layer of the Janus  
127 membranes plays as a fouling barrier. In addition, it works as a heat barrier and decreases the  
128 total heat transfer without sacrificing the mass transfer coefficient [1, 41].

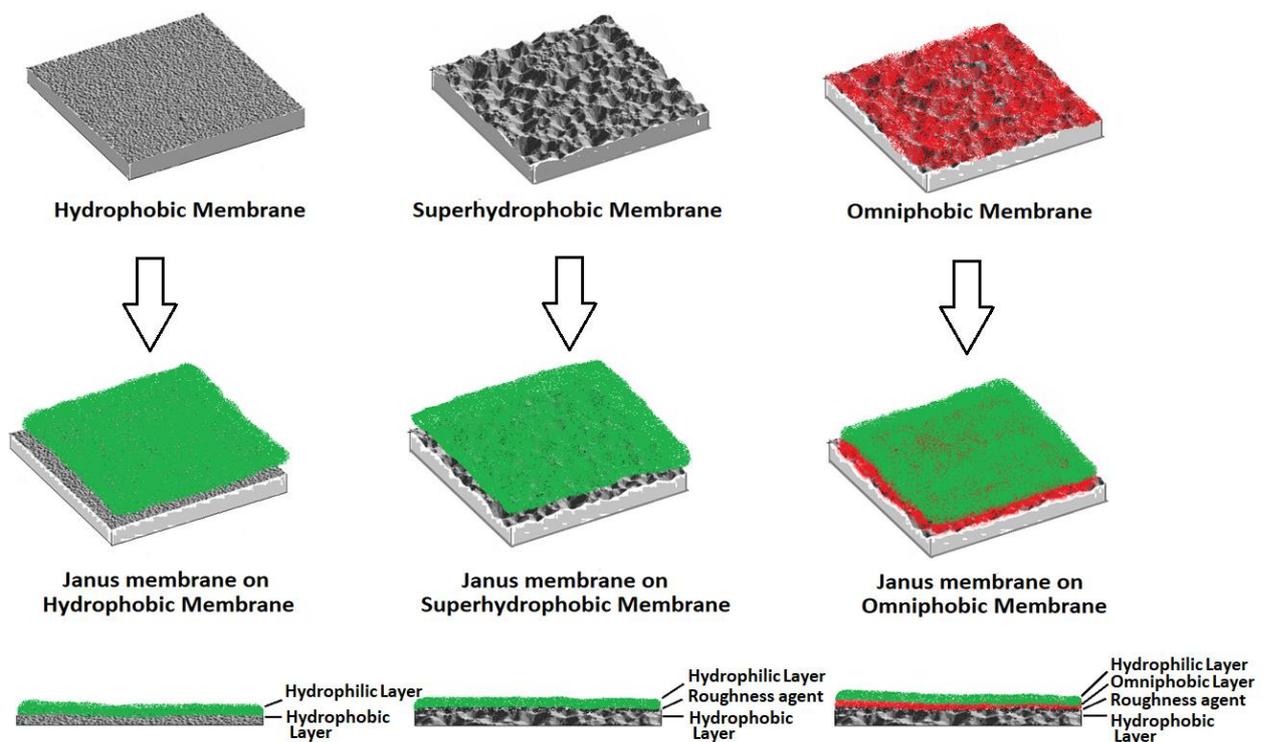
129 This review presents the recent advances progress on the fabrication, challenges and  
130 application of Janus membranes for MD [27, 34-36]. To the authors' knowledge, no review  
131 has been carried out so far focusing only on Janus membranes for MD. We start our discussion  
132 with the fundamentals of Janus membrane design, and then present some innovative  
133 strategies for Janus membrane fabrication and modification. The application and evaluation  
134 of Janus membrane are also elaborated and finally, the effect of Janus membranes in  
135 overcoming fouling and wetting problems as well as flux improvement is thoroughly  
136 elucidated.

137

## 138 **2. Overview and design of Janus membranes**

139 Janus is the name of the ancient Roman god that has two opposite faces; one looks to the  
140 past and the other looks to the future [37, 38]. In material science field, Janus was firstly used  
141 by De Gennes for synthesis of particles that chemically have different hemispheres [39]. The

142 first Janus material have been composed of poly(methyl methacrylate) and polystyrene  
 143 materials. Accordingly, materials with ambivalent properties is called Janus, like Janus  
 144 particles, Janus nanosheets, and Janus membrane. Janus membrane was firstly introduced by  
 145 Cheng and Wiersma in 1982 and since then the number of research focused on improvement  
 146 methods of Janus membrane drastically increased [40]. Janus membrane is a new  
 147 configuration that has asymmetric wettability in both sides. In other words, one side is  
 148 hydrophilic and the other side is hydrophobic or omniphobic [41]. **Figure 2** shows a schematic  
 149 of the various designs of Janus membranes. As shown in this figure, the Janus membrane can  
 150 be fabricated by coating of hydrophilic layer on top of a hydrophobic, superhydrophobic, or  
 151 omniphobic base membrane. The fabricated Janus membrane can be used in both  
 152 configurations, including the hydrophilic layer towards feed stream or vice versa.



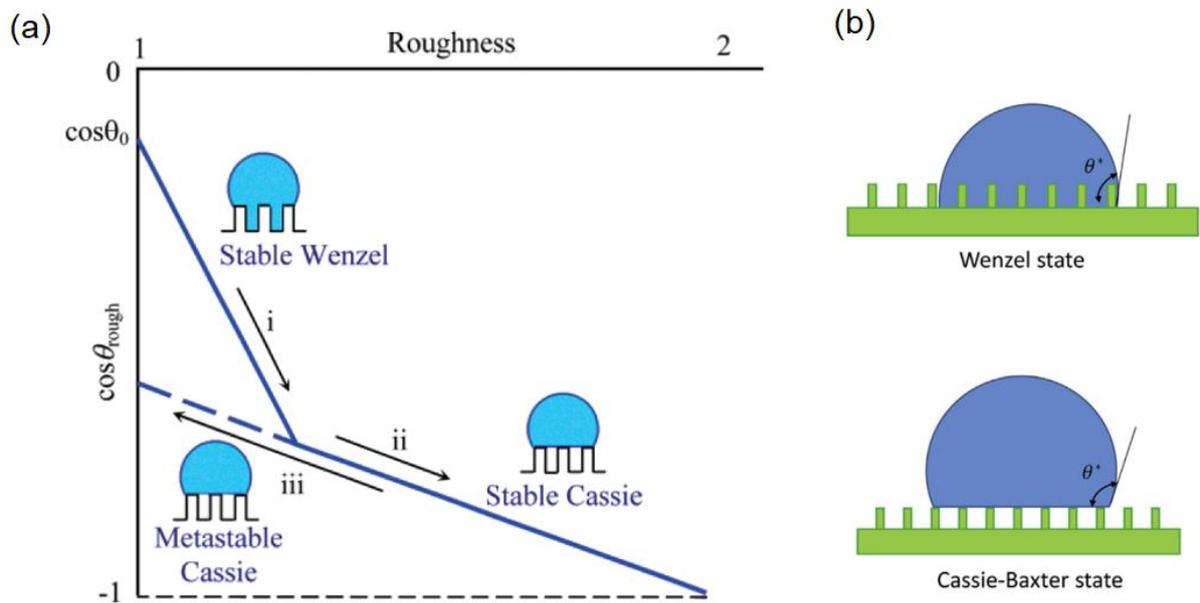
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154

Figure 2. Different types of Janus membrane configurations.

155 According to the mass and heat transfer conflicts in MD systems, the optimum thickness can  
156 be approximately calculated using the pore size and heat conductivity coefficient. For Janus  
157 membrane, the optimum thickness can also be designed accordingly. Reports indicated that  
158 the optimum thickness of the hydrophobic part (with porosity > 70%, thermal conductivity =  
159 0.1-0.3 W/mK) is in the range of 30-60  $\mu\text{m}$  [16][69]. However, most of hydrophobic  
160 membranes have been fabricated having the thickness of around 100-150  $\mu\text{m}$  to compensate  
161 its low mechanical strength [69].

162 Hydrophobicity or hydrophilicity is dependent on both the morphology and surface energy of  
163 the material. These parameters determine the tendency of the surface to adhere or repel the  
164 liquid materials. The wetting properties are dependent to the chemical structure of the  
165 surface and also to the roughness, pore size, and environmental condition. Empirical  
166 correlations can be used to predict the surface affinities of various liquids, but the easiest and  
167 straightforward evaluation method is via measurement of liquid contact angle. In general,  
168 surfaces with water contact angle (WCA) greater than  $90^\circ$  are considered hydrophobic and  
169 less than  $90^\circ$  are hydrophilic [4]. Different liquid types will have varying affinity to a particular  
170 material and surface. For membranes having rough and porous surfaces, the contact angle  
171 can be estimated using Wenzel equation for homogenous and Cassie-Baxter for  
172 heterogeneous types. Figure 3 shows the transition lines for different wetting states versus  
173 the roughness of the surface [42]. In addition, Figure 3b depicts the state of the water droplet  
174 in both Wenzel state and Cassie-Baxter state [43].



175

176 *Figure 3. (a) The transition line from Cassie-Baxter regime to Wenzel regime [42], and (b) the*  
 177 *state of droplets in both Wenzel and Cassie-Baxter states [43].*

178

179 According to the physical and chemical properties of the surface and liquid, different states  
 180 from Wenzel state to metastable and stable Cassie-Baxter state are formed. The Cassie-Baxter  
 181 state shows the low interaction of liquid with the membrane surface that results to higher  
 182 hydrophobicity and lower slippery angle of the membrane, which are suitable for MD  
 183 application. In this condition, upward capillary forces inhibit intrusion of liquid into the  
 184 grooves of membrane surface and preserve the membrane from wetting [44, 45].

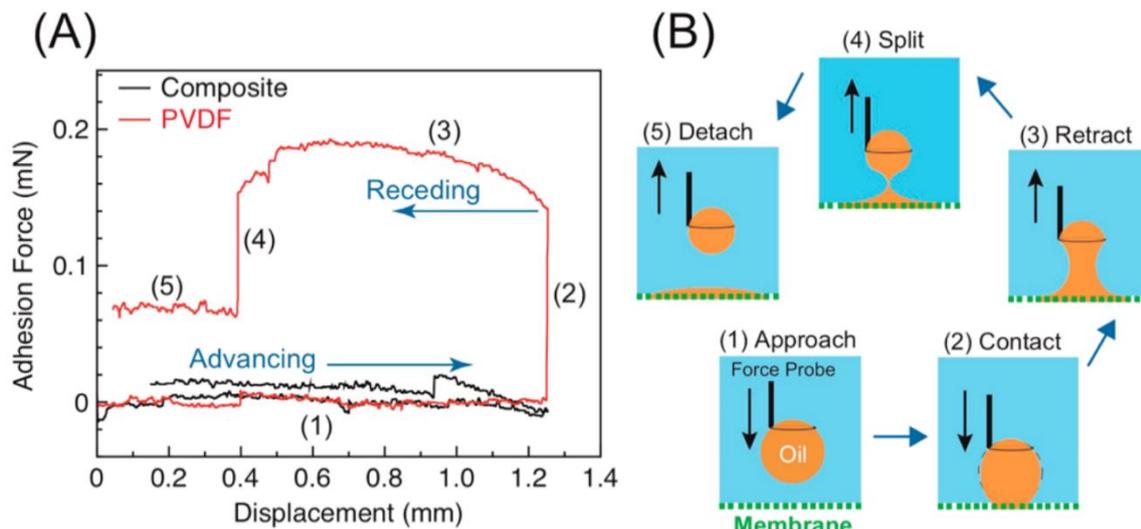
### 185 **2.1. Anti-fouling and anti-wetting properties**

186 Janus membranes, which possess opposite wettability at two sides of the membrane can lead  
 187 to wetting and fouling resistance if properly designed. The combination of two layers with  
 188 distinct surface energy provides a specific wettability condition for Janus membranes [46].

189 When exposed to different types of liquids including water, mineral oil, ethanol, or surfactant-  
190 rich water, Janus membranes can potentially limit their wicking into the membrane compared  
191 to other membranes. For example, superhydrophobic membranes are adequately resistant  
192 to high surface tension liquids but are easily wetted by low surface tension liquids [47, 48].  
193 Omniphobic membranes perhaps are highly regarded for MD processes, as they possess good  
194 resistivity against surfactants and wetting agents, but still suffers from fouling issue in oil-  
195 polluted wastewaters [27, 32]. High volume of oil-containing wastewater produced during  
196 different food and shale gas drilling process make it crucial to find an effective and low cost  
197 process for oil water separation [49, 50]. Oil droplets in feed can lead to quick fouling of the  
198 membrane surface, resulting to decrease in flux, clogging and wetting issues that affect its  
199 long-term operation. Thus, many groups have started to design Janus membranes while  
200 utilizing the positive value of superhydrophobic or omniphobic substrates to deal with these  
201 issues.

202 Several studies have shown that hydrophobic and omniphobic membranes have less  
203 resistance to underwater oil droplet due to the hydrophobic-hydrophobic interaction  
204 between oil droplet and the membrane surface. In the case of hydrophobic membrane, due  
205 to the strong hydrophobic-hydrophobic interaction, oil wicks through the membrane, clogs  
206 the pores and causes fouling of the membrane [29]. For omniphobic membrane, the  
207 membrane surface is also covered by the oil particles due to hydrophobic interaction and foul  
208 the membrane, however the oil particles do not wick into the pores and the fouling is  
209 reversible via commonly used cleaning methods like backwashing [11]. Janus membranes  
210 have thin hydrophilic layer that are hydrated with water, showing underwater oleophobicity,  
211 which can repel oil droplets and avoid oil fouling formation. Furthermore, according to  
212 Wenzel and Cassie theory, an increase in the roughness of the hydrophilic layer can lead to

213 an increase in the area of hydrated top layer and consequently enhances its oleophobicity.  
214 This was proven by study of Huang et al, wherein the hydrophilic layer of the Janus membrane  
215 was coated with silica and chitosan to increase both the wettability and surface roughness of  
216 membrane. This led to the reduction of fouling generated by oil droplets on the Janus  
217 membrane [48, 51]. Another study also demonstrated the effect of hydration of the  
218 hydrophilic layer on repulsion of oil droplets from depositing on the surface [34, 52]. Wang et  
219 al. [52] are the pioneers of using force spectroscopy to analyse the oil fouling of membrane.  
220 In their work, the adhesive force between oil droplet and membrane surface for the hydrated  
221 top layer of Janus membrane was less than 0.02 mN, while that of hydrophobic PVDF  
222 membrane reached to around 0.2 mN (see **Figure 4**). This proportion shows relatively high  
223 repulsive force of Janus membrane for oil droplets. The receding curve also shows dramatic  
224 decrease for hydrophobic membrane (from about 0.18 mN to less than 0.08 mN) which  
225 reveals the presence of high adhesive interaction. In other words, the hydrophobic  
226 membrane attracted the oil droplets at the time of contact and showed higher possibility of  
227 fouling, whereas the change in adhesive force for Janus membrane is zero, demonstrating  
228 that no interaction occurred during the contact and detachment [29, 52]. In addition, DCMD  
229 test results revealed higher fouling resistivity of Janus membranes compared to hydrophobic  
230 or omniphobic membranes.



231

232 *Figure 4. Force-distance curve for dynamic movement of oil droplet into contact of both*  
 233 *Janus and hydrophobic membrane through advancing and receding movement [52].*

234

235 In another study, the wettability performance of Janus membrane prepared by coating of PDA  
 236 on omniphobic PTFE/PP-Teflon was compared with hydrophobic PTFE-PP membrane, under  
 237 various types of liquids. Results showed high interaction of hydrophobic membrane with low  
 238 surface tension liquids but low interaction on Janus membranes. This low interaction is  
 239 attributed to the presence of omniphobic membrane substrate beneath the thin hydrophilic  
 240 layer repelling the low surface tension liquids in the process. This exceptional behaviour  
 241 helped the Janus membrane to work for long term MD operation with stable flux and salt  
 242 rejection, while other tested membranes showed reduction in performance after some hours  
 243 of testing with contaminated and polluted feed water [53]. Li et al. also investigated the effect  
 244 of coating of hydrophilic layer on the wettability of prepared membranes [27]. The results  
 245 proved that Janus membrane enjoyed a near perfect salt rejection and constant flux during  
 246 the treatment of seawater containing all types of wetting and foulant agents. This study also  
 247 demonstrated that the thickness of the hydrophilic layer can have dramatic effect on fouling

248 and wetting resistance of omniphobic membrane, so care must be taken to come up with the  
249 optimum thickness [27].

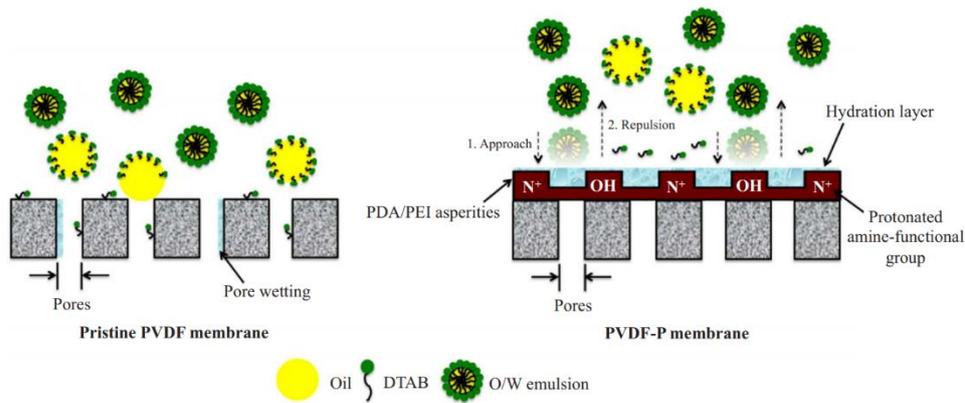
250 Zhu et al. fabricated a Janus membrane by coating hydrophilic PAN layer on F-SiO<sub>2</sub> @PVDF-  
251 HFP/PS omniphobic membrane. The hydrophilic PAN (4 wt%) solution was coated on the  
252 omniphobic membrane by electrospinning, and the formed structure resulted to a dramatic  
253 increase in underwater OCA to more than 164°, proving underwater superoleophobicity of  
254 Janus membrane [33]. Long term MD operation of the Janus membrane demonstrated a  
255 stable flux of 25 LMH and 100% salt rejection for 50 h continuous test, while hydrophobic  
256 PVDF and superhydrophobic PVDF NFM showed quick fouling after only half hour of test. The  
257 dynamic study of the fouling mechanism showed that oil droplets attached and fouled first  
258 on the other two membranes, but could not attach on hydrophilic PAN layer of Janus  
259 membrane. The unattached oil droplets were then aggregated on the surface of Janus  
260 membrane and formed bigger oil droplets and then left the Janus membrane surface without  
261 any fouling problem [33, 54]. The dynamic investigation of wetting and contact angle can  
262 determine the mechanism of fouling and wetting in the membrane and derived data are more  
263 helpful to assess the DCMD experimental results.

264 The effectiveness of Janus membrane for increasing the resistivity of membrane against  
265 fouling and wetting problems also depends on the composition of contaminants in the feed  
266 water. The structure and features of surfactants can change the fouling mechanism in the  
267 Janus membranes. The ionic surfactants can adsorb on the membrane surface via the  
268 electrostatic or hydrophobic forces. Although the negative charge of hydrophobic membrane  
269 (like PVDF membrane) repels the negative side of surfactants, however, it can interact with  
270 the other side of the surfactant and adsorb it. Therefore, the flux reduction in hydrophobic

271 membrane could be attributed to this interaction. In this interaction, the hydrophobic to  
272 hydrophilic ratio of surfactants can determine the power of hydrophobic-hydrophobic  
273 interaction of membrane and surfactants and show stronger adsorption of surfactants on the  
274 membrane [55, 56]. However, the adsorption rate is determined by the diffusion, which is  
275 irrelevant to the strength of the adsorption. In other words, smaller hydrophilic-lipophilic  
276 balance (HLB) of surfactant represents stronger adsorption, but does not show faster  
277 adsorption and does not demonstrate the higher probability of wetting issue in the MD  
278 process [56]. For Janus membranes, the hydrophobic and electrostatic interactions play the  
279 most important roles. For example, in the case of PDA-PEI/PVDF Janus membrane, the  
280 protonated amine functional group can make electrostatic interaction by sulfate groups of  
281 hydrophilic parts of surfactants and induce fouling for the membrane [18, 22, 27].

282 On the other hand, when Janus membrane deals with cationic surfactants like DTAB, the  
283 positive charges of protoned amine-functional groups in the membrane and quaternary  
284 ammonium heads of the DTAB repel each other and the intrinsic structure of Janus membrane  
285 keeps the membrane surface from surfactant fouling. For the case of hydrophobic membrane,  
286 like PVDF, the negative charge of the membrane surface can attract the positive parts of DTAB  
287 and make both electrostatic and hydrophobic interaction and make wetting problem for  
288 hydrophobic membrane. In one fouling study, the surfactant-stabilized oil in water emulsion  
289 was prepared as the fouling agent [57]. The results revealed that the oil-water emulsion has  
290 positive charge and is repelled by positive charge of protonated amine-functional groups on  
291 the Janus membranes and helps the hydrogen-bond in hydrated layer for prevention of oil  
292 fouling on the Janus membranes (as depicted in **Figure 5**) [57, 58]. However, when the feed  
293 water contains free surfactant in addition to surfactant-stabilized oil, the free surfactants  
294 easily pass the hydrophilic layer of the Janus membrane and make wetting beneath the

295 hydrophobic layer [29]. In general, the effectiveness of a modification should be investigated  
 296 case by case and the moieties of the feed water and membrane structure should be  
 297 recognised.



298  
 299 *Figure 5. the anti-fouling procedure of feed water containing surfactant-stabilized oil in Janus membrane [57]*  
 300

### 301 **3. Janus membrane fabrication methods**

302 Depending on the face of the Janus membrane that is on the feed side, the application of the  
 303 Janus membrane varies. In general, in relation to the wettability characteristics of the top face  
 304 of the membrane, the Janus membrane is fabricated for two general applications: lowering  
 305 the fouling or lowering the mass transfer resistance. In former state, the hydrophilic layer is  
 306 in contact with feed stream and the Janus membrane is used for antifouling application (i.e,  
 307 it can repel the foulant). In latter case, the hydrophilic layer of Janus membrane is in contact  
 308 with permeate side and Janus membrane is used for increasing the mass transfer of the MD  
 309 process, without sacrificing the thickness of the membrane that affect its mechanical stability.  
 310 The thickness and other features of hydrophilic and hydrophobic layer varies, depending on  
 311 the application of Janus membrane. In this way, the Janus membrane is fabricated using two  
 312 general methods: deposition of hydrophilic layer on top of hydrophobic membrane or vice

313 versa. In this section, the fabrication process of Janus membrane is categorised according to  
314 the base substrate: incorporation of hydrophilic layer on top of a hydrophobic/omniphobic  
315 substrate or incorporation of hydrophobic layer on top of a hydrophilic substrate.

316

### 317 **3.1. Hydrophilic on top of hydrophobic configuration**

318 The most common method for the fabrication of Janus membrane, which have been widely  
319 used in many studies, is by deposition or incorporation of a hydrophilic layer on top of a  
320 hydrophobic or omniphobic membrane substrate [36]. This method has the advantage of  
321 being generally simple, straightforward, and is a step-wise process [59]. However, the  
322 modification methods in many cases compromise the quality of the substrate membrane by  
323 clogging the pores or changing the hydrophobicity of the membrane. Furthermore, stepwise  
324 preparation increases the material and fabrication costs and increases the delamination  
325 problems [37, 60]. Fabrication of new membranes is usually done by phase inversion, hollow  
326 fiber spinning or by electrospinning. However, these processes in many cases do not directly  
327 create the Janus membrane structure, thus further modification processes are required. The  
328 modification processes include coating, incorporation of nanoparticles or surface modifying  
329 macromolecules (SMM), electrospinning or electrospraying of environmental friendly  
330 hydrophilic materials like PEG, PDA, hydrogels, grafting of hydrophilic functional groups, and  
331 other ways of providing specific wettability and function to the membrane [61-63]. In other  
332 studies, before modification of the membrane surface, some chemical methods such as  
333 plasma treatment were used to prepare the hydrophobic substrate to be more affinitive to  
334 the hydrophilic layer. This section presents the various ways to fabricate and modify Janus  
335 membranes with hydrophilic-hydrophobic structure.

### 336 **3.1.1 Vacuum filtration**

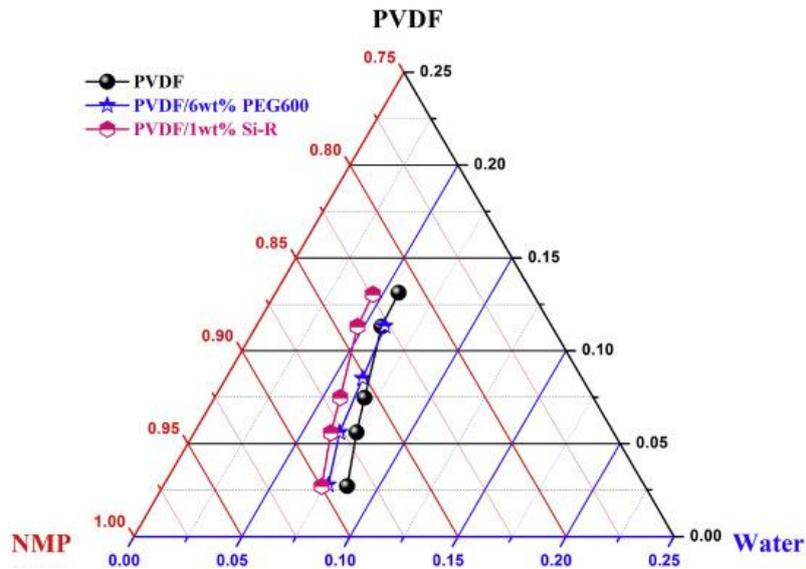
337 Vacuum filtration is a simple and straightforward method for coating of a hydrophilic top layer  
338 on hydrophobic or omniphobic base membrane. In this method, firstly a hydrophobic or  
339 omniphobic microporous flat sheet membrane is fabricated and then a hydrophilic layer is  
340 coated on top layer using vacuum filtration of a solution containing desired hydrophilic  
341 nanoparticles (NPs). The size, dimension, and chemical structure of NPs are very important  
342 parameters in defining the efficiency of the Janus membrane. However, this method suffers  
343 from low stability and delamination problem. For example, one study covered the top layer  
344 of a PVDF membrane by vacuum filtration of solution containing Si NPs which resulted to an  
345 increase in membrane surface roughness [64], while another study added CNT containing  
346 solutions which led to a decrease in roughness for the same type of substrate [65-67]. The  
347 explanation for this modification can be attributed to the size and shape of the nanoparticles  
348 and also the presence of ridge-valley structure on the PVDF membrane surface. This condition  
349 can cause a decrease in porosity, which can led to diminished flux performance [34]. Even  
350 though the CNT containing membrane decreased the pore size distribution of the Janus  
351 membrane by blocking or decreasing the effective area of some pores, its mechanical stability  
352 compared to unmodified membrane has increased. TGA data showed higher thermal stability  
353 and mechanical analysis of modified membrane revealed that imposing strains of PVDF-CNT  
354 membrane was about two-fold compared to unmodified PVDF membrane. However, the  
355 tensile strength obtained similar results to that of neat membrane [34]. The inorganic nature  
356 of CNTs and also the functional groups present on its surface can have interaction with the  
357 substrate and other CNTs to make a strong deposited layer, having sufficient hydrophilic  
358 wettability [60, 68]. Generally, the physical and chemical structure of CNTs make possible  
359 rapid mass transfer of water molecules through outer and inner surface of CNTs via

360 sequential sorption-desorption and can increase water transport to the membrane surface  
361 and simultaneously make a barrier against oil droplets for some special wastewater  
362 treatments like oil-emulsion treatment [34].

### 363 **3.1.2 Coating via co-casting phase inversion**

364 Co-casting is another method wherein both layers are subsequently casted and can be used  
365 to fabricate bilayer or multilayer materials, such as Janus membranes. One important factor  
366 in the investigation of the effect of simple coating procedure is considering the structure of  
367 layers during coating. In phase inversion, the type of polymer, solvent, nonsolvent, and  
368 temperature are important factors of layering. The structure and morphology of casted  
369 solution is formed according to the miscibility of the solvent and nonsolvent and the  
370 difference in chemical and physical properties of matrix polymer may cause delamination  
371 during coagulation process. Therefore, the thermodynamic properties of different mixtures  
372 should be considered to find optimum type of solvent and nonsolvent [61, 69, 70]. The ternary  
373 phase diagram should be used to determine the miscibility of polymers, solvents, and  
374 nonsolvent to estimate the optimum condition to fabricate integrated multi-layer membrane.  
375 For example, in **Figure 6**, the black line shows the binodal curve of PVDF dope solutions  
376 containing three compositions (polymer, solvent, and non-solvent). As indicated in this figure,  
377 addition of PEG or silica nanoparticles to dope solution changed the phase diagram of dope  
378 solution by moving the binodal curves and showed a decrease in power of the solvent in  
379 mixed matrix polymer solution versus neat dope solution. [71]

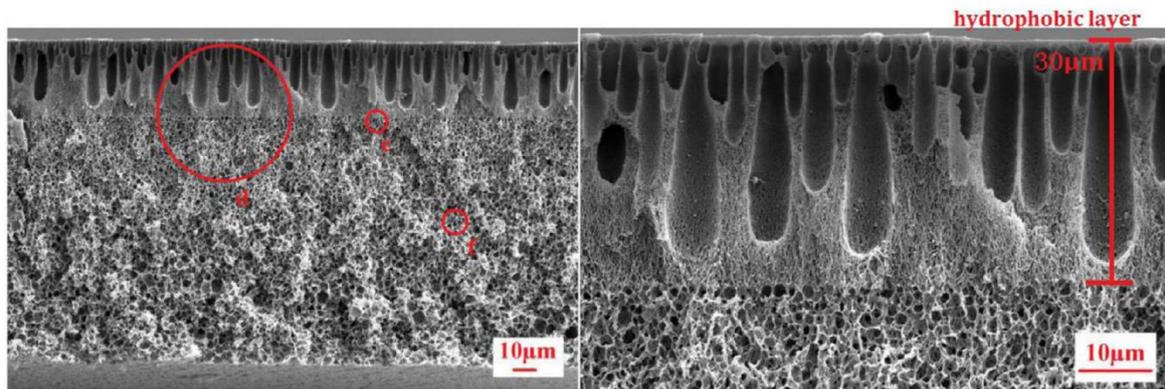
380



381

382 *Figure 6. The Ternary diagram for coagulation of different types of PVDF/NMP solution in*  
 383 *water bath [71].*

384 In another study, in the process of co-casting of PVDF-PVA as hydrophilic layer and PVDF as  
 385 hydrophobic beneath layer, due to difference in solvent replacement, two distinct layers were  
 386 formed (**Figure 7**). Difference in solvents and polymers resulted in the fabrication of  
 387 asymmetric membrane with an obvious boundary between two layers. The difference in rate  
 388 of miscibility of solvents in two phases into nonsolvent coagulant bath formed two distinct  
 389 layers which increased the possibility of delamination [69]. Depending on the type of phase  
 390 inversion process (TIPS or NIPS), the coagulation process has direct influence on the structure  
 391 of the Janus membrane [22, 72, 73].



392

393 *Figure 7. Cross section SEM image of flat sheet bilayer membrane fabricated by PVDF-PVA*  
 394 *on PVDF [69]*

395 **3.1.3 Asymmetric fabrication**

396 Asymmetric fabrication refers to the one-step fabrication of Janus membranes as opposed to  
 397 symmetric fabrication where a hydrophilic layer is subsequently coated on a hydrophobic or  
 398 omniphobic layer. In the asymmetric method, usually the difference in solubility of materials  
 399 is used to fabricate asymmetric structure. In brief, a dope solution containing at least two  
 400 distinct types of materials, like polymers or nanoparticles, is prepared and the dope solution  
 401 is placed in a coagulant environment. Then the asymmetric structures start to form due to  
 402 difference in surface energy of materials and their tendency to reach the low energy surface.  
 403 Also in some cases, the difference in solubility of polymer composite in a coagulant liquid  
 404 causes faster migration of polymer parts toward the outer surface and causes fabrication of  
 405 a membrane with different wettability in both sides [30, 33, 74].

406 Additionally, it is possible to fabricate Janus membranes by internal migration of materials  
 407 through the membrane matrix and make a polar hydrophilic structure. In this method, usually  
 408 a dope solution containing both hydrophilic and hydrophobic materials is prepared and then  
 409 the solution placed in an asymmetric surface energy environment. In this condition, the

410 macromolecules or monomers, which are not yet coagulated, tend to migrate to surfaces with  
411 lower energy, according to their chemical affinities. This movement usually occurs in phase  
412 inversion process. In this process, the nonsolvent tends to remove solvents and replace them,  
413 according to solvent-polymer-nonsolvent interaction in ternary phase diagram. In a  
414 heterogeneous polymer solution containing both hydrophilic and hydrophobic polymers, the  
415 polymer parts tend to migrate to the more-soluble nonsolvent, due to their intrinsic  
416 interactions. For example, if the water is nonsolvent, the hydrophilic parts tend to migrate  
417 toward the outer surface and, as a result, can change the hydrophilicity of outer layers. In this  
418 method asymmetric membrane can be fabricated without delamination problem. For  
419 comparison, in a normal phase inversion, both top and bottom layer become similar in  
420 hydrophilicity, due to simultaneous migration of hydrophilic part of solution towards all sides.  
421 In order to preserve the asymmetric style, novel methods like adhesion of an impermeable  
422 layer to one side of the casting surface should be used [22, 61]. Li et al. utilized glycerol to  
423 coat a nonwoven fabric, then a polymeric solution is casted on the fabric and then immersed  
424 in coagulation bath. As a result, a solution containing copolymer PVP-VTES and PVDF was  
425 prepared. The PVP-VTES has hydrophilic affinity and tends to have interaction with water to  
426 reach lower surface energy. Compared to PVDF, the PVP-VTES had faster migration rate. The  
427 presence of glycerol layer in the bottom side of the membrane makes a barrier against the  
428 solvent-nonsolvent exchange and diminishes the phase separation on the beneath layer.  
429 Therefore, the hydrophilic copolymer cannot penetrate across the bottom layer of the  
430 membrane and the migration occurs only in one side of the casted layer and the difference in  
431 miscibility rate results to an asymmetric hydrophilic-hydrophobic structure [22].

432 The asymmetric modification of hydrophobic membrane to fabricate Janus membrane has  
433 various difficulties like wetting of the substrate pores via hydrophilic layer. MD membranes

434 have microporous structures and the pores usually can be wetted due to capillary force and  
435 interactions between the bulk membrane and coating layer. As a result, if the modification  
436 method does not perform accurately, not only that the wetting and fouling not hindered, but  
437 also the separation performance of the hydrophobic substrate decreases. Some methods  
438 have been suggested to enhance the modification process. One of these methods include  
439 placing a separation interface to prevent the modification layer from intruding into the pores  
440 of the substrate. In this method, usually a thin layer is coated on the surface of the  
441 hydrophobic membrane and then a hydrophilic layer is entangled with this intermediate top  
442 layer and two distinct regions are formed. The intermediate layer plays the role of making  
443 strong adhesion on both hydrophilic and hydrophobic layers and also prevents the pore  
444 clogging by the hydrophilic layer. In another type of method, it is possible to adjust the  
445 reaction time of the polymeric dope solution to make a gradient reaction across the  
446 membrane width. In this method the composition of dope solution is accurately selected to  
447 have different reaction rate and difference in reaction rate make integrated asymmetric  
448 membrane with opposite wettability in both sides [31, 68, 75, 76].

#### 449 **3.1.4 Two-phase interface method**

450 One of the difficulties of Janus membrane fabrication is modification of only one side of the  
451 substrate. It is not so straightforward to modify only one side of a polymeric surface having  
452 only some micron thickness. Therefore, an applicable modification method should have  
453 capability of changing the wettability of one side of the membrane without changing the  
454 characteristics of the other side. The dilemma is the selection of proper solution. A wetting  
455 solution may intrude into the pores and decrease the efficiency of the MD process, while a  
456 non-wetting solution may not interact with the membrane substrate and may delaminate the

457 top layer. Various methods have been proposed to modify the surface of hydrophobic  
458 membrane. Two phase interface method is a novel coating method that can be used to modify  
459 only one side of the membrane, without affecting the other side. In this method the  
460 membrane substrate is soaked in the interface of two immiscible liquids, so that one side of  
461 the membrane is in contact with the surface of the other liquid. Then the desired layer is  
462 reacted with the membrane substrate to form a layer on top of it [22, 59, 77]. For instance,  
463 Yang et al. have floated PP membrane on a solution containing PDA/PEI. This resulted to a  
464 hydrophilic layer of PDA/PEI coated on the hydrophobic PP membrane and a Janus membrane  
465 was fabricated. In this method, it is essential to coat the membrane surface with high viscosity  
466 solution to prevent intrusion of solution into the substrate pores via capillary force [77].  
467 Similar method also can be applied by restricting one side of membrane substrate by sticking  
468 an impermeable layer and then soaking the membrane inside a reaction liquid. In this way,  
469 the solution can react with only one side of the membrane and a hydrophilic layer is coated  
470 on the membrane substrate. The stucked layer preserves the other side of the substrate from  
471 solution reactants. After finishing the reaction, the impermeable coating is peeled-off and  
472 Janus membrane is fabricated. However, the peeling-off step in most of cases destroys the  
473 beneath layer of the Janus membrane and may affect the performance of the membrane for  
474 application in DCMD [60, 78].

### 475 **3.1.5 UV-mediated modification strategy**

476 Another method for the fabrication of Janus membrane is treating one side of the membrane  
477 using photoreaction or photoresist materials. In this method, the membrane substrate can be  
478 soaked in a photoreacted or photoresist solution and then one side of the membrane is  
479 activated by irradiation. After the reaction is carried out, the remained photoresist or

480 photoreacted material is removed and a Janus membrane is fabricated. However, care must  
481 be taken to make sure that the photosensitive or photoreacted material must not affect the  
482 wettability of the membrane substrate after removal from the membrane surface.

483 UV-sensitive reactions are also good way to the modify one side of the membranes. Thiol-ene  
484 click reaction is an example of reaction that is activated by UV-light. This method has benefits  
485 of rapid reaction rate, high yield, easy process, and controllable directional reaction. Li et al  
486 modified different types of substrates by firstly coating of PDA, using mussel-inspired catechol  
487 chemistry, and then silanized it to produce superhydrophobic substrates. The  
488 polycondensation of Trichlorovinylsilane provides photosensitive functional groups.  
489 Afterwards, the superhydrophobic substrate is immersed in thiol-ene click reaction solution  
490 and was irradiated by UV-light, which renders one-side of the membrane surface hydrophilic.  
491 This modification process makes a membrane having asymmetric wettability with 140° WCA  
492 difference between two sides of the membrane. According to the pore size distribution and  
493 thickness of the substrate, this membrane can be used for different water treatment  
494 applications like MD, oil-in-water emulsion, or water-in-oil emulsion separation [80].

### 495 **3.1.6 Multi-step coating method**

496 Wang et al. fabricated a Janus membrane using a multistep method to coat hydrophilic  
497 polyamine in one side and a hydrophobic polymer at the other side. In this study, cotton fabric  
498 was deposited by a compound of PDMS containing light sensitive materials. Then one side of  
499 deposited cotton was irradiated to crosslink the light sensitive material and make a strong  
500 connection with the fibers. Afterward, the remaining deposited material was washed using  
501 hot THF solvent. Then, the other side of the fiber was grafted by propyl methacrylate groups,  
502 using sol-gel method and a catalytic reaction, to increase the hydrophilicity of Janus

503 membrane. Therefore, hydrophilic cotton fibers become hydrophobic/superhydrophilic Janus  
504 membrane after these consecutive process[81] . Furthermore, it is possible to combine multi-  
505 effect of coated layer to enhance effectiveness of prepared Janus membrane for some special  
506 applications, like incorporation of nanoparticles on top of hydrophilic layer of Janus  
507 membrane to cover its microdefects. However, due to change in structure of hydrophilic layer  
508 during hydration process, the stability of coated layer is very challenging and its stability  
509 should be investigated. In order to assess the stability and stiffness of the coated layer,  
510 especially for nanoparticle coating, the first step is to use an ultrasonic instrument. In this  
511 method, the loose bonding is detected and the applicability of the Janus membrane for long  
512 term operation is determined [57]. In this way, it is possible to assess the stability of coated  
513 nanoparticles by placing the used membrane in high frequency ultrasonic bath to determine  
514 the percentage of nanoparticles that remained on the surface of the Janus membrane [32,  
515 82].

516 Generally, the surface energy of PVDF is higher than PTFE, but it has been widely used for MD  
517 process due to its good compatibility with different polymers and solvents, low cost, and  
518 adequate mechanical stability. Therefore, a wide range of polymers that are compatible with  
519 PVDF are used for the fabrication of bilayer or blended Janus membrane. In order to decrease  
520 delamination, it is better to choose polymers with close solubility parameters to make  
521 interactions during coating process. Although PVDF has been widely used as hydrophobic  
522 substrate for MD process, it can be modified to become hydrophilic or superhydrophilic  
523 substrate. In other words, its useful properties can be used in other side of technology to have  
524 high water wettability characteristics [24, 83-86]. In a study, Zhou et al. fabricated a Janus  
525 membrane by changing a hydrophobic PVDF membrane to superhydrophilic membrane by  
526 initiation of vinyltriethoxysilane cross-linking reaction that converted it into a

527 superhydrophilic PVDF substrate. The superhydrophilic PVDF was casted on a PET nonwoven  
528 fabric and after coagulation, it was peeled off to generate micro and nano size rough  
529 structures and then superhydrophobic fluorinated silica nanoparticle solution was sprayed on  
530 these torn surface to coat the substrate and make a superhydrophobic layer. Regarding to the  
531 degree of superhydrophobicity of the top layer, this Janus membrane can be used in different  
532 methods of water treatment, like forward osmosis or MD [87].

### 533 **3.2 Hydrophobic on top of hydrophilic configuration**

534 Although most of the Janus membranes are fabricated by coating of hydrophilic layer on top  
535 of hydrophobic or superhydrophobic membrane, it is possible to do the opposite fabrication  
536 method: coating of hydrophobic layer on top of hydrophilic layer [93]. The following are  
537 different methods used for this type of fabrication method.

#### 538 **3.2.1 Liquid-liquid interface**

539 In a novel method, liquid-liquid interface was used for the incorporation of a hydrophobic  
540 layer on top of a hydrophilic substrate. For this purpose, firstly the hydrophilic cotton  
541 membrane was soaked in dopamine solution for deposition of intermediate layer. Then the  
542 DA-coated cotton membrane was floated on the water – dichloroethane containing  
543 octadecylamine ( $C_{18}NH_2$ ) two phase beaker. The membrane is placed at the liquid-liquid  
544 interface, according to a range of densities. The amine groups of  $C_{18}-NH_2$  has hydrophilic  
545 tendency and stay orientated toward water interface. Therefore, this intrinsic property  
546 caused interaction of amine group with dopamine molecules deposited on the surface of  
547 cotton membrane. The deposition of PDA on the hydrophilic cotton fiber prepared the  
548 medium for attachment of  $C_{18}-NH_2$  hydrophobic layers. The water-oil interface prepares the

549 exchanging area for this attachment. After interaction, the prepared Janus membrane has a  
550 relatively thin hydrophobic C<sub>18</sub>-NH<sub>2</sub> layer beneath a thick hydrophilic layer [35]. However, this  
551 technique is only possible to perform on flat sheet membranes. In another study, Vanagamudi  
552 et al. have fabricated Janus membrane by casting of hydrophobic PVDF layer on the  
553 electrospun nanofibers made of hydrophilic nylon/chitosan blend. The presence of hydroxyl  
554 and amine functional groups give high hydrophilicity to the electrospun nanofiber. Although  
555 the Janus membrane showed reduced pore size, the flux and rejection increased compared  
556 to neat PVDF membrane [88].

### 557 **3.2.2 Electrospinning deposition**

558 Yan et al. have used a novel method by deposition of hydrophobic electrospun nanofiber on  
559 superhydrophilic non-polymeric substrate. The substrate was constructed from porous  
560 copper mesh having nanosize needles. This substrate was prepared by immersion of smooth  
561 copper mesh into NaOH solution having (NH<sub>4</sub>)<sub>2</sub>S<sub>2</sub>O<sub>8</sub> [89, 90]. This process changed the  
562 wettability of the substrate from hydrophobic to superhydrophilic feature (WCA changes  
563 from 114° to 0°). The nanosized needles can intrude into the deposited nanofibers and  
564 enhance coating interaction and decrease the possibility of delamination and, in general,  
565 increased the entanglement of deposited hydrophobic layer with the substrate. Furthermore,  
566 the formed interface roughness increases the hydrophobicity and hydrophilicity of Janus  
567 membrane. The top layer was deposited using electrospinning of polymer solution containing  
568 different PVDF concentration. The change in the concentration of the PVDF solution, changed  
569 the properties of nanofibers. While beads were formed on the nanofibers fabricated at lower  
570 concentration, the beads disappeared at higher PVDF concentration. In addition, Tijing et al.  
571 have fabricated a dual-layer membrane for DCMD application by electrospinning of PVDF-HFP

572 on PAN microfibers. In this method, the PAN nanofibers firstly was electrospun on the drum  
573 and then the PVD-HFP nanofibers was electrospun on the PAN substrate. The prepared  
574 membrane showed superb porosity of 90% and WCA of 150° at the feed side and complete  
575 salt rejection, completely suitable for DCMD application [91].

### 576 **3.2.3 Surface Modifying Macromolecules (SMM)**

577 In general, Janus membranes can have two configurations: asymmetric wettability in a  
578 distinct layer or having gradient wettability from top to bottom layer. The former type has a  
579 separating layer that connects the hydrophilic and hydrophobic layers together. The latter  
580 usually is formed by migration of materials having opposite wettability through the dope  
581 solution during coagulation or processing time and the concentration gradient makes the  
582 wettability gradient across the membrane. Application of surface modifying macromolecules  
583 (SMM) in the fabrication of Janus membrane provides a gradient change in wettability across  
584 the membrane [92, 93]. SMMs are a group of active additives that tend to move toward the  
585 lower surface energy surfaces and can migrate in non-solidified phase to reach to lower  
586 interfacial energy. In other words, the SMMs in a dope solution have the ability to move to  
587 all-sideward to reach the surfaces and to have minimum interfacial energy. The small  
588 percentage of SMMs are sufficient to make a heterogeneous layer. Therefore, the application  
589 of SMMs has shown great potential for the fabrication of Janus membrane, especially for  
590 integrated membrane for MD application. The promising point of SMM is about the possibility  
591 of one step fabrication, which decreases the commercial costs. SMMs are usually fluorinated  
592 polymer segments produced by fluorination of polymers like polyurethane, PVDF, and PES  
593 and are dissolved in a solution containing hydrophilic polymer solution. The dope solution is  
594 casted and placed in an air environment phase inversion process. The waiting time lets the

595 SMMs to migrate toward the surface having low surface energy and make an asymmetric  
596 Janus membrane with a gradient wettability: hydrophobic top layer and hydrophilic bottom  
597 layer [94]. The type of blended polymer, SMM polymer and fluorocarbon, and dope solution  
598 solvent are important parameters affecting the mechanical, physical, and chemical properties  
599 of Janus membrane. Zhang et al. reported the use of different types of solvents like  $\text{CHCl}_3$ ,  
600  $\text{CH}_3\text{CN}$ , THF and acetone for the fabrication of SMM-based Janus membrane. Their results  
601 indicated that the best condition was achieved by using  $\text{CH}_3\text{CN}$  solvent achieving the highest  
602 wettability difference between the two sides [90, 94].

603 The incorporation of SMM in hydrophilic membranes increases the chemical, mechanical, and  
604 thermal stability of the membranes and covers the delamination drawbacks for application of  
605 Janus membrane in different wastewater treatment application. One of the most important  
606 challenges is due to the all-directional movement of SMMs in dope solution, while the  
607 preferred movement direction is only one side migration. The derived membrane after phase  
608 inversion process usually have hydrophobic surface and hydrophilic bulk. In order to  
609 efficiently use the migration behaviour of SMM, the fabrication process needs to be modified  
610 using methods for controlling the directional migration. The covering of one side of the  
611 membrane is a possible method that have been used to direct the SMMs toward only one  
612 surface [22]. Before focusing on application of SMMs in Janus membrane, SMMs were used  
613 for enhancement of the hydrophobicity of the base membrane. In some research, hydrophilic  
614 PEI membrane was modified with SMM to fabricate Janus membranes for MD application [94,  
615 95]. Also, in a series of studies performed by Khayet's group, fluorinated SMMs were blended  
616 with hydrophilic PEI to enhance the LEP of the membrane [17, 96].

617 **3.2.4 Other methods**

618 Other researchers also have used hydrophilic porous substrate like cellulose acetate or  
619 cellulose nitrate and coated hydrophobic layers like styrene or vinyltrimethylsilicon  
620 compounds to fabricate bilayer Janus membranes. However, these researches have used  
621 radiation graft or plasma polymerization methods that are relatively complicated and  
622 expensive for large scale fabrication [16, 97]. Also, most of studies were performed in flat  
623 sheet module and more research on other commercial modules like hollow fiber is necessary.

624 Perfluoropolyether (PFPE) compounds, like PTFE, are polymeric materials that have high  
625 content of fluorine in its structure. The fluorine content increases the chemical and thermal  
626 resistivity of the polymers and form a superhydrophobic compound. Beside this outstanding  
627 properties, fabrication of porous PTFE membrane is so complicated and expensive. On the  
628 other side, PVDF, a fluorine-containing polymer that are being used as MD membrane, has  
629 lower hydrophobicity compared to PTFE. Therefore, applying novel methods to use the  
630 benefits of PTFE and decreasing the complicity and cost of process for MD application is  
631 favourable [2-4]. In a study performed by Figoli et al, a UV-sensitive PTFE layer was coated on  
632 commercial hydrophilic polyamide membrane. In this work, commercial microfiltration PI  
633 membrane was dip coated in PTFE oligomer solution and then one side of coated layer was  
634 cured by UV light. The UV-process stabilized PTFE on one side of the PI membrane and the  
635 remaining PTFE from other side was washed out to produce a Janus membrane. The derived  
636 membrane had high hydrophobicity, owing to the PTFE layer, and was fabricated simpler than  
637 commercial PTFE microporous membranes. Additionally, it had the advantages of being a  
638 Janus membrane [98].

## 639 **4. Surface modification strategies towards Janus membrane fabrication**

### 640 **4.1. Plasma treatment**

641 Gas plasma technology is a chemical-energy modification method, which changes the  
642 structure of the material to the phase other than three regular solid, liquid, and gas phases.  
643 In this technology, usually high voltage is applied to the materials to ionize them and the  
644 materials are brought to the plasma phase. In this phase, a controlled reaction on a narrow  
645 and thin layer can be performed, according to the properties of used gas and also substrate  
646 surface. Plasma technology is widely used in membrane technology to change the properties  
647 of the surface layer to desired property, mostly to prepare surface for adopting of a coating  
648 layer [26]. Plasma etching can scratch a very thin layer of the membrane substrate and  
649 prepare condition for making interaction with coating layer [99, 100].

650 For a Janus membrane, the membrane substrate has hydrophobic or omniphobic properties  
651 and the top layer has hydrophilic wettability. The opposite wettability characteristics of these  
652 layers make challenges in the adhesion process. Therefore, gas plasma method can be used  
653 to ionise the hydrophobic or omniphobic substrate surface and change the structure for  
654 hydrophilic attachment. For example, Li et al. treated the surface of PP substrate via plasma  
655 for two minutes (at 200 W) to coat a hydrophilic top layer. The treated surface effectively  
656 accepted the coating of a Teflon layer for increasing hydrophobicity of the substrate and also  
657 attachment of hydrophilic PDA layer [53]. Zuo et al. have used plasma technology to modify  
658 the surface of PEG and TiO<sub>2</sub>-coated PVDF membrane. The etching technique modified the  
659 surface of a hydrophobic PVDF membrane to graft with PEG functional groups. The FTIR  
660 spectrum showed a decrease in both asymmetrical and symmetrical stretching bond of CF<sub>2</sub> at  
661 1178 and 1275 cm<sup>-1</sup> and increase in OH stretching bond at 3400 cm<sup>-1</sup>, which is a sign of a

662 successful modification process. This grafting process caused changing in the wettability of  
663 the membrane to hydrophilic and fabrication of Janus membrane. However, the grafting  
664 approximately halved the average pore size of the membrane, which is beneficial for  
665 decreasing the wettability, but also decreases the flux of the membrane.

666 In another study performed by Lee et al, a Janus membrane was successfully fabricated by  
667 soaking of porous hydrophilic alumina substrate in photoresist AZ 5214 and then etching one  
668 side of the membrane by air plasma. Afterwards, the etched surface was silanized using low  
669 surface energy perfluorodecyltrichlorosilane to make an omniphobic thin layer. The presence  
670 of photoresisted material makes a barrier against infiltration of the membrane pores with  
671 silane groups preserving its hydrophilicity during the modification process. Afterwards, the  
672 remaining photoresist was washed out and removed. This fabrication procedure produced a  
673 Janus membrane with top hydrophobic coating and bottom substrate hydrophilic structure.  
674 This novel method also can be used for other modification techniques. After etching one side  
675 of the membrane, it is possible to coat-etch the surface of the substrate by other polymeric  
676 hydrophobic layer using methods like vapour deposition or interfacial layer deposition [101].

#### 677 **4.2. Nanoseeding technique**

678 Nanoseeding is a novel technology for changing the structure of the surface by increasing the  
679 surface roughness and its physical and chemical characteristics. In this method, first, the  
680 nanoseeds are stabilized on the substrate surface and then the nanorods are grown on the  
681 activated sites of the substrate. This modification method also can be used to increase the  
682 hydrophobicity of the substrate by growing of hydrophobic nanorods. Furthermore, due to  
683 barbed morphology of the surface, it is possible to immobilize a layer containing opposite  
684 wettability to fabricate Janus membrane. The combination of bumped rods with chemical

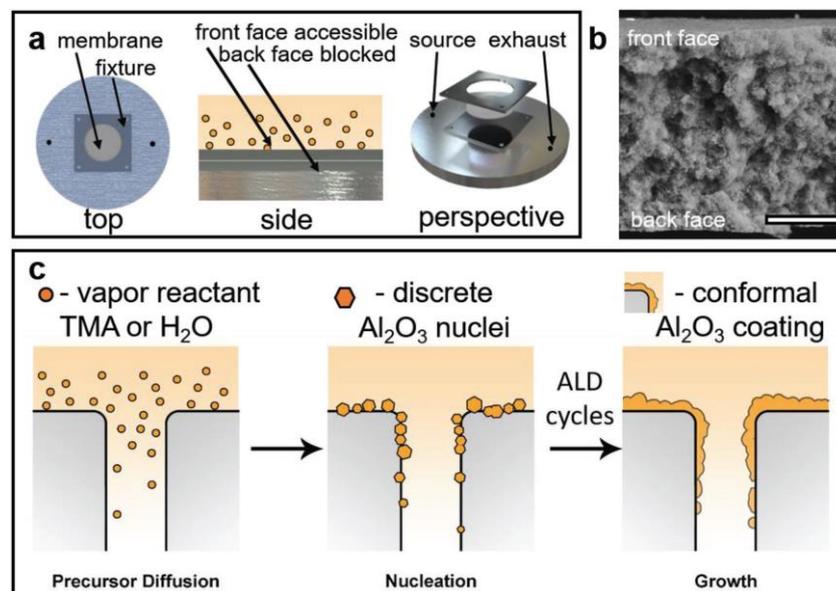
685 interaction provided by thermal and mechanical treatment can fix the top layer on the  
686 superhydrophobic substrate [102, 103]. In a study, ZnO nanorods were grown on a hydrophilic  
687 cellulose acetate fiber in arrays and then superhydrophobic layer was made by immersion in  
688 sodium laurate solution. Afterwards, hydrophilic MnO<sub>2</sub> nanowires were coated on one side  
689 of the substrate via vacuum filtration and hydrothermal treatment. The modified membrane  
690 has shown superb properties like high porosity, asymmetric wettability and highly stabilized  
691 coated layer. The substrate showed superhydrophobic characteristic with WCA of 153° and  
692 sliding angle of 3°. However, the OCA of the substrate is 0° that shows oleophilicity of the  
693 substrate, which indicates that it is susceptible to rapid fouling. The asymmetric modification  
694 process makes a surface oleophobic and substrate hydrophobic that provides condition for  
695 treatment of foulant-rich contaminated wastewater, using MD method. Additionally, the  
696 stability of the coated layer was tested by immersion of the membrane in a hot water/ethanol  
697 solution. This solution swells both layers and provide maximum layer stress. The results  
698 showed no detachment of MnO<sub>2</sub> nanowires that prove high interaction of coated layer [97].

### 699 **4.3. Atomic layer deposition method**

700 Layering technology also can be used to fabricate a Janus membrane via atomic layer  
701 deposition (ALD) method (see **Figure 8**). ALD is a precise technique used in semiconductor  
702 fabrication process for layer by layer conformal growth. In this method, a metal oxide layer  
703 having molecular-sized thickness is deposited on desired surface without changing the  
704 structure of the pores. Therefore, this method can be used to precisely coat an oxide metal  
705 having hydrophilic features on the surfaces of hydrophobic or superhydrophobic substrate.  
706 Waldman et al. have modified the surface of hydrophobic PP membrane by deposition of  
707 hydrophilic aluminium oxides to fabricate Janus membranes. The results demonstrated that

708 Janus membrane having high wettability difference was fabricated without considerable  
 709 change in porosity and pore size distribution of the substrate. Also, it was revealed that the  
 710 coating depth and degree of hydrophilicity can be tuned by controlling exposure dose and  
 711 time of the process. Also, molecular precision of ALD makes it possible to provide sharp  
 712 wettability difference across a narrow line in one side of the substrate. [36]

713



714

715 *Figure 8. Atomic Layering Deposition Technique used for changing the characteristics of top*  
 716 *Layer [36]*

#### 717 4.4. Other methods

718 Other novel methods like laser modification are also possible for surface modification and  
 719 fabrication of Janus membrane. However, these methods are expensive and time consuming  
 720 and only has justification in some special applications. In this method, both sides of  
 721 hydrophilic substrate are roughened and coated with low surface energy material to produce

722 superhydrophobic membrane. Then, one side of the surface is treated with laser to scratch  
723 fluorinated or low surface energy coating [75].

724 In one study, Ghalehi et al. modified PVDF flat sheet membrane with concentrated KOH to  
725 graft hydrophilic functional groups on the membrane surface. During the reaction, the high  
726 alkaline condition breaks the carbon-hydrogen and carbon-fluorine bonds and generate  
727 carbon hydroxyl bonds. The zeta potential analysis performed on the modified membrane  
728 showed that the surface became more negatively charged, compared to unmodified  
729 membrane, owing to its hydrophilic structure that adsorbs more anions like OH<sup>-</sup> or Cl<sup>-</sup> from  
730 the electrolyte [61]. Some studies also used facile fabrication of Janus membrane by simply  
731 putting hydrophobic mesh filters on top of hydrophilic substrates, usually hydrophilic fabrics  
732 like cotton. This method can be used for special applications like fog harvesting, but due to  
733 low adhesion interaction and also large pore sizes of hydrophobic meshes cannot be used for  
734 applications like MD or oil-water separation [31]. Also, it is possible to premodify the  
735 membrane surface to increase the efficiency of prepared Janus membrane. For instance, The  
736 Si nanoparticles, which have been widely used to increase the roughness of the membrane,  
737 has negative charges and in the membrane surface should have positive charge to make  
738 possibility of interaction of Si NPs with membrane surface. Therefore, charge modifiers like  
739 TEOS or CTAB can be used to change the charge of membrane surface to positive. After  
740 deposition of roughening materials like silica nanoparticles, the surface of rough membrane  
741 is coated with low surface energy coating like fluorine materials to make in air omniphobic  
742 membrane. Now, the hydrophilic layer like composition of Si NP/chitosan/  
743 perfluorooctanoate can be coated to make a superb Janus membranes. If the attachment  
744 process is carried out perfectly, a high performance Janus membrane is achieved with  
745 mentioned layer characteristic [48].

746 Layer-by-layer assembly is another technique for modifying the surface of hydrophobic  
747 membrane for fabrication to Janus membrane. In this method, one side of the hydrophobic  
748 membrane (like PVDF) is sealed and then the membrane is periodically immersed in various  
749 solutions containing intermediate and hydrophilic solutions. This subsequent immersions is  
750 termed as layer-by-layer coagulation of dope solutions [104].

## 751 **5. Configurations of Janus membranes**

### 752 **5.1. Flat sheet Janus membrane**

753 The easiest structure to prepare for MD application is flat sheet membranes and they have  
754 been widely fabricated to investigate the performance of various Janus membranes [68]. In a  
755 study, the effect of changing the solvent of PVDF-based membrane on delamination was  
756 investigated by fabrication of flat sheet Janus membrane [69]. This simple membrane  
757 structure besides ease of production process provides a condition for fast analysis of the  
758 effect of various parameters on the property of bi-layer Janus membrane. Li et al. also  
759 fabricated a flat sheet Janus membrane comprising of an omniphobic layer composed of  
760 PVDF-silica NPs coated with FDTES low surface energy as substrate and hydrophilic layer by  
761 coating of atom-transfer radical-polymerization (ATRP) on the plasma-etched substrate. The  
762 flat sheet structures helped in the investigation of the effect of low thickness coating of  
763 hydrophilic layer on both foulant and wetting resistivity of prepared Janus membrane. Also,  
764 the effect of operating condition on flux and salt rejection was easily studied [27].

765 In general, the layer deposition is the simplest modification method for fabrication of Janus  
766 membrane. In this method, which is commonly applicable for flat sheet membranes, a thin  
767 layer of desired coating solution is coated on the surface of the substrate. Due to low viscosity

768 of the solution at the time of casting, pore wetting may be an issue for this method. Also, high  
769 viscosity solution may clog the pores of the membrane. The interaction of coating layer with  
770 the membrane substrate also is another important factor that affects the performance of the  
771 membrane for long term operation. In a study, the glutaraldehyde-PVA solution was  
772 prepared, coated, and incubated on the surface of PVDF membrane. The substrate pores  
773 were preserved from wetting by controlling the physical condition of the solution. The derived  
774 flat sheet membrane showed good coating with low pore wetting and high water productivity  
775 [105]. In some studies, before coating of the main hydrophilic layer, the top surface of the  
776 membrane is pre-treated to prepare conditions for strong interaction of hydrophilic layer with  
777 the substrate. Plasma etching or coating with intermediate polymer solutions like PDA is some  
778 examples of this intervention. Although some of these methods showed superb layer  
779 interactions and great separation performance, the applicability of suggested method for  
780 large scale and commercial system is not satisfied. In general, flat sheet membrane is  
781 generally thought as not a favourable module for industrial application. Furthermore, multi-  
782 step fabrication technique increases the cost of membrane and decreases its  
783 commercialization potential[105].

## 784 **5.2. Hollow fiber Janus membrane**

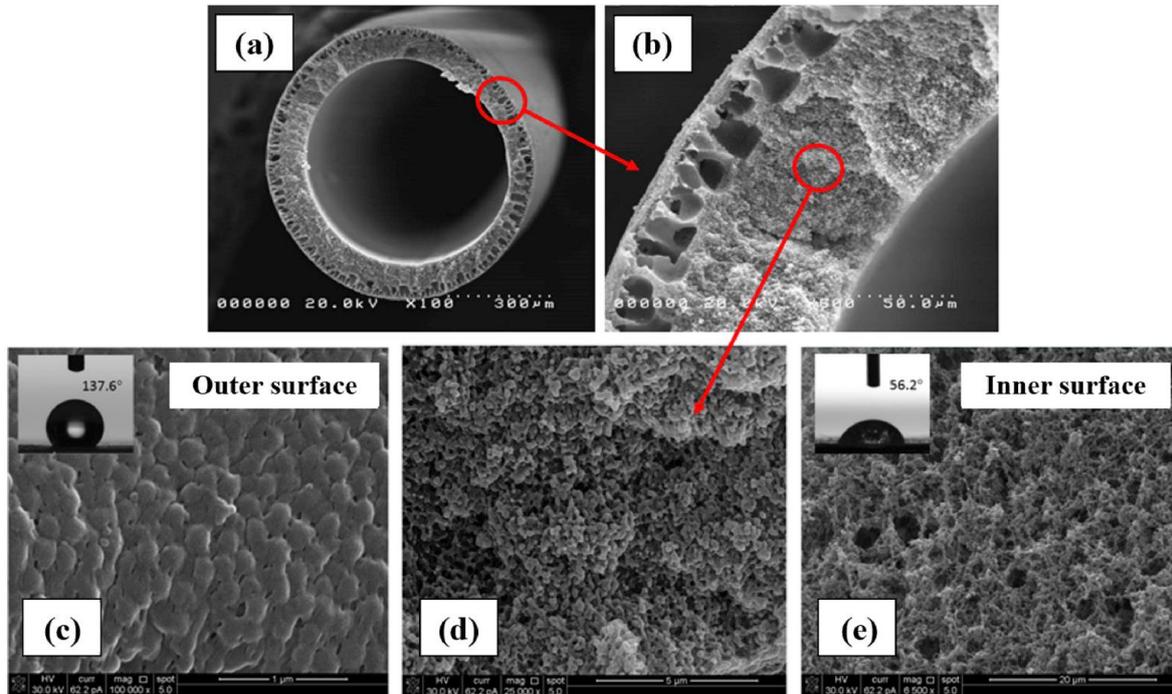
785 One of the most optimum modules for commercialization of water treatment application is  
786 hollow fiber membranes. This structure has relatively high aspect ratio and low facility volume  
787 per volume of produced permeate water. Although its fabrication in lab scale is more difficult  
788 than flat sheet membranes, it is favourable for industrial and large-scale production.  
789 Therefore, the most facile and straightforward modification methods should be applied on  
790 hollow fiber membranes to find shortcut path for commercialization [106]. A negative point

791 of the hollow fiber membranes is having high-pressure drop along the membrane that  
792 increases the working pressure of membrane and as a result, the wetting possibility of the  
793 membrane. Furthermore, due to exponential correlation of vapour pressure with  
794 temperature, temperature decrease in the module and as a result, the flux dramatically  
795 decreases in the end of the membrane. Therefore, the optimum condition is to have a low  
796 length hollow fiber membrane with feed inlet through the shell side with higher contact  
797 surface area and permeate gathered through the lumen side of the membrane [16, 107-110].

798 Regarding high promising potential of hollow fiber membrane for wastewater treatment  
799 applications, different studies have focused to modify or fabricate hollow fiber Janus  
800 membrane. Various types of methods have been proposed including vapour deposition,  
801 lumen coating, outer surface coating, and co-extrusion. Among these methods, coating  
802 process is simplest method, but the homogeneity and lamination are two main problems  
803 during fabrication and operation of this type of Janus membrane. The one-step fabrication  
804 of Janus membrane is desirable to simultaneously save the time and cost. For this purpose, it  
805 is possible to use triple orifice spinneret to co-extrusion of two polymeric solution with  
806 opposite wettability characteristics. From large-scale production point of view, the co-  
807 extrusion is most efficient and applicable method for production of membrane modules. With  
808 respect to other modification methods, co-extrusion method decreases the possibility of  
809 delamination of distinct layers. However, the proper selection of dope solution and coagulant  
810 bath condition are crucial section of production process. The type and category of solvents  
811 used for preparation of both dope solutions and their interaction during extrusion and  
812 coagulation are determining the quality of the hollow fibers and the possibility of  
813 delamination. Therefore, the co-extrusion has shown great flexibility through dope  
814 preparation and fabrication process [17, 96]. Zou et al. fabricated Janus hollow fiber

815 membrane by co-extrusion of PVDF/PEG and PVDF Si-R dope solution and NMP/water as bore  
816 fluid. One advantage of this method is the use of NMP as solvent for both dope solutions.  
817 Therefore, the unique solvent helped the preparation of integrated membrane without  
818 separable layer. The presence of Si nanoparticles also increased the roughness of the outer  
819 hydrophobic layer and PEG increased the hydrophilicity of inner layer. As depicted in **Figure**  
820 **9**, the composition difference make two different morphologies for inner and outer part of  
821 the membrane; PVDF-Si NP formed a thin hydrophobic outer surface with WCA of  $137^\circ$  and  
822 PVDF-PEG formed thick hydrophilic inner layer with WCA of  $56^\circ$  [108]. This difference can be  
823 attributed to the difference in inner and outer coagulation bath condition and difference in  
824 dissolving rate of polymers in coagulant solution. The presence of NMP in the bore fluid  
825 decreases the exchanging rate of solvent-nonsolvent and produce porous structure with small  
826 pore sizes, whereas the pure water coagulant bath in outer surface prepared high dissolution  
827 rate and finger-like structure during phase inversion process is formed. The  
828 superhydrophobicity properties of Si-R was also effective on formation of such configuration,  
829 which prevent extensive distribution of water molecules through dope solution for NMP-  
830 water exchanging. As a result, instead of liquid-liquid mixing, solid-liquid mixing occurred and  
831 porous and triangle structure is formed. The interface of two dope solution is obvious in the  
832 SEM images (Fig 7), however the similar solvent make strong uniformity between two phases  
833 and decreased the possibility of delamination.

834 Although these studies proved the benefits of co-extrusion process, it has some limitation in  
835 the selection of polymer and solvent and the tolerance in degree of hydrophilicity and  
836 hydrophobicity of Janus membrane layers. In other words, co-extrusion method compromises  
837 the wettability difference between top and bottom layers for overcoming of lamination  
838 challenge.



839

840 *Figure 9. SEM images of Janus membrane fabricated using co-extrusion technique (a, b) and*  
 841 *the inner and outer morphology and their surface WCA (c, d, e)[108]*

842 The surface modification of hollow fiber membrane is another attractive method for  
 843 modification of currently industrialised hollow fiber membranes. The advantage of this  
 844 method is on the modification of a standard hollow fiber membrane that have uniform and  
 845 applicable substrate structure. However, the drawbacks of coating procedures are still  
 846 challenging for this modification process. One of the commonly used procedure is using  
 847 mussel-inspired technique to adhere hydrophilic layer in inner or outer surface of  
 848 hydrophobic hollow fiber membrane. However, the modification of lumen is more  
 849 straightforward. For example, Yang et al. have modified the lumen side of PP hollow fiber  
 850 membrane by coating of PDA/PEI dope solution. In this method, the dope solution is stepwise  
 851 intruded through the pores of the substrate and changed the wettability of inner layer to  
 852 hydrophilic ones. The thickness of hydrophilic layer can be adjusted by changing deposition  
 853 time. The presence of dopamine in the coating dope made a tough and strong hydrophobic

854 adhesion by substrate and a uniform structure was formed. The depth of penetration and  
855 thickness of hydrophilic layer of Janus membrane is measured by using EDX scan. PDA can  
856 chelate silver ions and make bond via its catechol groups. Therefore, Ag solution was  
857 circulated through the lumen of hollow fiber and after chelating, EDX scan is taken from the  
858 cross section of membrane to evaluate the terrace of silver ions, which is equivalent to  
859 thickness of hydrophilic layer. The results showed that about 20% of thickness of hydrophobic  
860 membrane was coated by hydrophilic layer (about 90  $\mu\text{m}$  out of 450  $\mu\text{m}$ ) [107]. In another  
861 study, Zuo et al. have focused to fabricate a Janus hollow fiber membrane by co-extrusion of  
862 PVDF and Ultem dope solutions. The bilayer Janus membrane showed more than four times  
863 higher tensile strength and high flux, compare to conventional one-layer PVDF membrane  
864 [111]. Polyetherimide also is a good substrate for dual layer Janus membrane fabrication for  
865 MD application, owing to its mechanical strength, hydrophilicity, and compatibility with PVDF.  
866 Even though the Polyetherimide Ultem is immiscible with PVDF, the solubility parameters of  
867 both are so close, which can make tough molecular interaction between two connected  
868 layers.

869 Another important point in the fabrication of bilayer Janus membrane is the concentration of  
870 polymers in dope solution. Regarding to the fact that after coating process, the dope solutions  
871 start to shrink, the relative concentration of inner and outer layer has direct influence on the  
872 quality of interface layer. In hollow fiber membranes, the shrinkage direction is towards the  
873 centre. Therefore, if the concentration of outer layer is less than the inner layer, the shrinkage  
874 process causes the outer polymer solution to be firm around the lumen polymer solution. This  
875 transition makes a tough and tight interface layer. However, the physical properties of both  
876 layers can improve this adherence. More integrated polymeric bilayer is achieved in the case  
877 of choosing polymers with high mechanical strength for inner layer and polymer with high

878 stretching property for outer layer. This combination stretches the outer layer on the tough  
879 support surface [71, 112, 113].

880 The porosity of both layers is a crucial point for fabrication of a high flux Janus membrane.  
881 Due to the fact that most of polymeric layer are fabricated through phase inversion process,  
882 the coagulation bath condition is the most important parameter to adjusting the porosity of  
883 the membrane. In this state, the composition of coagulation bath, its distance from the  
884 spinneret, and also its temperature should be properly adjusted in an optimum value.  
885 Coagulation bath containing a mixture of nonsolvent (water) and polymer solvent reduces the  
886 rate of phase inversion and directs the transition phase towards more porous structure.  
887 However, very slow phase inversion causes more dense structure in inner sides of the polymer  
888 layer and achieves opposite result.

889 Bonyadi et al. fabricated a Janus membrane by co-extrusion of PVDF and PAN solution in the  
890 outer and inner orifice layers of hollow fiber spinneret. The membrane showed no obvious  
891 defects in the layering and morphology. Due to the difference in expansion coefficient and  
892 also loosing of interactions after swelling of both layers, they were delaminated during the  
893 DCMD test and separation process was interrupted. In another attempt to modify this  
894 drawback, they fabricated a bilayer Janus hollow fiber membrane by using PVDF as main  
895 polymer and hydrophobic and hydrophilic clays in both dope solutions. In this study, PVDF  
896 solution containing hydrophobic cloisite nanoparticles have been used as outer layer and  
897 PVDF-PAN dope solution containing hydrophilic cloisite NA as the inner solution. The  
898 presence of PVDF in both layers caused strong adhesion through co-extruding process. In this  
899 study the effect of coagulant bath composition was studied and results demonstrated that a  
900 dense and smooth surface is obtained by using a nonsolvent with strong exchange rate, like

901 water. But using a moderate coagulant bath like mixture of methanol and water made a rough  
902 membrane with more porous membrane structure. The optimum membrane porosity was  
903 achieved for coagulant bath comprising of water/methanol with concentration of 20/80 wt%,  
904 having contact angle of 140° and 50° for two sides [16].

### 905 **5.3. Electrospun Janus nanofiber membrane**

906 Electrospinning is a nanofiber fabrication method that uses electrostatic forces to produce  
907 ultrafine nanofibers, with high tolerance in tunability of the structure of produced mat [114,  
908 115]. Also, the process can be easily controlled and different polymeric solutions or  
909 compositions can be used for the process. Having these features and also advantages of fast  
910 laboratory fabrication that increases the rate of optimising of the effective parameters made  
911 electrospinning and electrospraying as attractive methods for the fabrication of membranes.  
912 A bilayer electrospun Janus membrane can be fabricated by consecutive electrospinning of  
913 substrate and top layer. In this type of membrane, the special structure and morphology of  
914 electrospun membrane make good entanglement of electrospun nanofiber mats and produce  
915 a tough and strong bilayer composite [116]. It should be noticed that the composition of both  
916 substrate and top layer should be accurately chosen to find highest available interaction  
917 during layering and decreasing the possibility of delamination [117].

918 Some studies were performed using this method and usually a similar type of polymer for  
919 both layers is used. In other words, prepared composite dope solution for both layers have at  
920 least one similar polymer in its composition. Yue et al. fabricated a bilayer electrospun  
921 nanofiber firstly by electrospinning of PVDF-PVAc as hydrophilic substrate and then coated  
922 with electrospun PVDF nanofibers containing SiO<sub>2</sub> nanoparticles modified by hexamethyl  
923 disilazane, as hydrophobic layer. In the prepared membrane, the presence of modified SiO<sub>2</sub>

924 enhanced the hydrophobicity of the coated layer, but decreased the interaction of ENFs with  
925 the substrate layer. Therefore, in order to increase the layer interaction, it is possible to  
926 stepwise increase the concentration of modified SiO<sub>2</sub>. At first dope solution having lower  
927 nanoparticle percentage makes stronger interaction with substrate and then dope solution  
928 having higher percentage of nanoparticles is electrospun, which increases the hydrophobicity  
929 of outer surface. Membrane analysis showed WCA increment to 170° and sliding angle  
930 decrement to 3° by increase in nanoparticle concentration to 2 wt% [117]. The advantage of  
931 electrospun nanofibers is its intrinsic surface roughness that formed due to the cylindrical  
932 shape of nanofibers and multilevel structures of mats. This structure naturally increases the  
933 resistivity of the membrane against wetting problem by decreasing the interaction area and  
934 transferring the wettability state of the membrane toward the Cassie-Baxter state.  
935 Furthermore, coating of the membrane surface by nanoparticles can enhance its roughness  
936 by formation of a multilevel re-entrant geometry and decreases the wetting challenge and  
937 makes electrospun nanofibers a good candidate for MD process [118].

938 Electrospinning is a novel fiber fabrication technique that has the advantage of great aspect  
939 ratio. The nanoscale diameter of the nanofibers increases the processibility of the fibers for  
940 various applications. This feature makes possible to adjust the pore size of produced mat for  
941 special applications. Due to micron-size pores of fabricated mats, electrospun nanofibers can  
942 be used in MD application. Also, the layer by layer fabrication process increases the roughness  
943 of produced mats, which is highly favourable for fouling and wetting resistivity of the  
944 membranes in MD operation. This configuration can be effectively applied in fabrication of  
945 Janus membrane. The electrospinning process gives the option to coat hydrophilic  
946 electrospun nanofiber on top of superhydrophobic substrate. Also, by changing the applied  
947 voltage and physical condition of solution, it is possible to electro spray the solution on top of

948 the membrane substrate. Electrospinning can also produce a uniform, stable, and tough  
949 covering layer and it can be used for the implantation of microsphere structures on the  
950 surface of membranes to increase their roughness to produce omniphobic or  
951 superhydrophobic membranes. Electrospinning or electrospaying can also cover a uniform  
952 and even coating on the membrane surface and decrease the presence of defects on the  
953 membrane surface. These defects are places for intrusion of oil pollutants or surfactants that  
954 decrease the efficiency of the membrane for long term operation. Regarding these privileges,  
955 electrospinning and electrospaying have been widely used for fabrication of Janus  
956 membrane for water treatment application [103, 119-121].

957 Zhu et al. used both electrospinning and electrospaying methods for the fabrication of  
958 breathable asymmetric Janus membrane for MD application [33]. In his study, PVDF  
959 nanofibers was first spun as membrane substrate and then Si and low surface energy agent  
960 (FAS) were added to the solution containing PVDF and polystyrene and electrospayed to  
961 transfer the omniphobicity to the membrane surface. Afterwards, SiO<sub>2</sub>-PAN solution was  
962 electrospayed on the omniphobic substrate to fabricate Janus membrane. Proper selection  
963 of solution mixtures is an important aspect of this method. The microspheres coated for  
964 increment of roughness and decreasing of surface energy in first electrospaying step and  
965 coating of hydrophilic layer in second electrospaying stage should have adequate adhesion  
966 and durability. The attachment of polymer on top of solid polymeric layer is not very strong  
967 and it needs to consider the process of adhesion of coating layer on membrane substrate. The  
968 type of solvent used on the dope solution and its interaction with substrate polymer are  
969 important factors for increasing the stability of the coated layer. The solvent should have the  
970 ability to make a medium for interaction of quest polymer with substrate polymer.  
971 Furthermore, as much as the produced microspheres are smaller, the stability, robustness,

972 and roughness of the coating layer is higher. Therefore, when electro spraying technique is  
973 used for membrane fabrication, the process is affected by polymeric dope composition,  
974 applied voltage, tip-substrate distance, and other operational parameters that should be  
975 adequately adjusted to produce smaller size microstructures. Studies revealed that the  
976 addition of nano or micro size particles can break-up the production of larger-size  
977 microspheres during electro spraying process [122]. In an example, aerogel was added to the  
978 PVDF dope solution for electro spraying process. The hydrogel particles in high voltage  
979 electro spraying condition can disrupt the PVDF solution and distribute through the solution  
980 and make nano-sized spheres sprayed on the surface of substrate. Lower weight and higher  
981 contact area of sprayed microspheres helped increasing the interaction with substrate and  
982 enhanced durability and roughness of produced membranes.

983 Therefore, some additives or a mixture of some polymers should be used to simultaneously  
984 attain the desired property and strong adhesion and long durability. For example, LiCl was  
985 added to the PVDF solution of substrate to increase its conductivity that ease facile fabrication  
986 of electro spun nanofibers. Also, polystyrene have been added to PVDF-HFP-Si NPs to produce  
987 fibers having stabilized microsphere shape beads [122]. In a study, Wu et al used subsequent  
988 electro spinning method for fabrication of Janus membrane by deposition of hydrophilic PVA  
989 on PU substrate. PVA has the hydrophilic nature and PU has hydrophobic and their  
990 combination resulted to a high performing Janus membrane with  $120^\circ$  contact angle  
991 difference between two sides. The processibility of electro spinning can also give the option  
992 to analyse the performance of Janus membrane having different coating thickness, by  
993 changing deposition time [123, 124].

994

## 995 **6. MD performance of Janus membranes**

### 996 **6.1 Hydrophilic-Hydrophobic/Omniphobic Janus membrane configuration**

997 In a study carried out by Li et al., neat hydrophobic and Janus membranes were fabricated  
998 and their performance was compared. While Janus membranes with hydrophobic PVDF  
999 substrate showed highest flux, its salt rejection was lower than Janus membranes with  
1000 omniphobic substrate. The covering of the PVDF substrate with fluorinated layer enhanced  
1001 the salt rejection of the Janus membrane. Also, the comparison of the flux of Janus  
1002 membranes with hydrophobic and omniphobic membrane showed that the Janus membrane  
1003 has higher separation performance for both flux and salt rejection [53]. Experimental results  
1004 showed that while the flux of hydrophobic membrane was 15 LMH and it decreased to 14  
1005 LMH for omniphobic membrane, the Janus membrane showed flux of about 20 LMH without  
1006 compromising the salt rejection. These characteristics can be attributed to the presence of  
1007 hydrophilic layer, which helps bring the hot feed water into the pores of the omniphobic  
1008 membrane substrate for evaporation. Furthermore, in the case of using low concentration of  
1009 hydrophilic solution, these materials can intrude into the beneath pores without blocking of  
1010 the pores and decrease the thickness of hydrophobic or omniphobic layer and therefore  
1011 increase the mass transfer ratio. On the other side, higher concentration of the coating layer  
1012 can block the pores and decrease the flux [32, 69]. The blockage of the pores by top layer  
1013 should be recognised on the reasons for flux decrement. For example, in one study, the flux  
1014 of the fabricated membrane decreased from 29 LMH to 17.5 LMH by covering of the  
1015 hydrophobic membrane by a hydrophilic layer. Though the permeate conductivity of the  
1016 Janus membrane remained constant during the 600 min test, the hydrophobic membrane lost  
1017 its salt rejection performance and permeate conductivity reached from zero to 200  $\mu\text{S}/\text{cm}$

1018 [27]. However, the comparison of different experimental studies have demonstrated that the  
1019 value of flux decreasing is dependent on the coating procedure and also the type of used  
1020 materials and in some cases the flux of Janus membrane have enhanced [30, 33, 53]. Zhu et  
1021 al. have shown that while the flux of the Janus membrane is relatively equal to the  
1022 hydrophobic ENF PVDF (28 LMH), its salt rejection is stable for long term application and  
1023 permeate conductivity remained approximately zero during 50 hrs test experiment. This value  
1024 for hydrophobic ENF PVDF reached to 75  $\mu\text{S}/\text{cm}$  after 50 hrs [33].

1025 Generally, the explanation of any process for fabrication of Janus membrane should be  
1026 assessed case by case. Although the presence of thin hydrophilic layer can improve the  
1027 thermal efficiency of the MD module, increment of the hydrophilic layer thickness above an  
1028 optimum value can have opposite influence. In this case, temperature polarization worsens  
1029 and thick solid layer decreases the rate of water passage and, as a result, the flux decreases.  
1030 Furthermore, the heat from the feed side cannot easily transfer to the boundary layer of  
1031 evaporation and this barrier decreases the driving force of vapour transport. In general, the  
1032 degree of hydrophilicity of the top layer is an important factor for determination of the  
1033 influence of the Janus membrane in separation of wastewater. Hydrophilic layer of Janus  
1034 membranes with lower hydrophilic affinity has less feed transport rate and consequently the  
1035 amount of water reached to the surface of hydrophobic layer for vaporization decreases and  
1036 the flux of the membrane decreases. Therefore, the selection of top layer with high  
1037 wettability is desired. Also, the saturation time for the top layer is an important factor during  
1038 lab work and the experimental data should be reported after saturation of top layer [50, 60].  
1039 In this way, during recent years, various materials have been used in different studies and a  
1040 broad experimental data of the performance of fabricated Janus membranes was obtained.  
1041 A general comparison of different studies performed by different coating materials showed

1042 relatively higher effectiveness of zwitterionic hydrophilic layer for decreasing of fouling  
1043 problem and increasing separation performance. In other words, the zwitterionic made  
1044 strong adhesion on omniphobic membrane without compromising the omniphobicity of  
1045 substrate layer [27]. A brief comparison of different Janus membrane fabricated for MD  
1046 application is shown in Table 1.

Table 1. Comparison of different membrane optimization methods in terms of MD permeate flux.

Hydrophilic layer	Substrate type	Hydrophobic Layer	Method	$\Delta T$	Flux LMH	Advantages	Dis-advantages	Module	Hydrophobic WCA	Hydrophilic WCA	Ref
CTAB/PVDF-HFP	Nano Fiber	SiNP/CTS/PFO Spray	ENF/Dip coating	50				DCMD	150	10	[48]
Dopamine-self polymerization (L)	FLAT SHEET	PTFE/PP (B)	Dip coating	50	19.7	Long term performance Low fouling and wetting	Fabrication difficulty (3 step)	DCMD	128	30	[64]
Zwitterionic	HOLLOW FIBER	Omniphobic Quartz fiber		40	15.5	High antifouling and antiwetting	Fabrication difficulty (3 step)	DCMD	121	25	[27]
SiO <sub>2</sub> /PAN	Nano Fiber	PVDF ENF	Elstrospinning Electrospraying	40	25	excellent breathability	Low mechanical	DCMD	170	10	[33]

		(F:SiO <sub>2</sub> /PAN, M: SiNP FAS PVDF PS, P: PVDF-HFP)				high antifouling					
PDA-AgNO <sub>3</sub>	HOLLOW FIBER	PDA-AgNPs	HF-Coating	40	17	Antibacterial Long term operation	Presence of Ag in permete	DCMD	109	7.6	[82]
PVA-CNT	FLAT SHEET	PVDF	spraying	40		High fouling resistence	CNT stability	DCMD	115	33	[34]
PVA-GA	FLAT SHEET	PVDF	Dip Coating	40	25	Anti-Scaling characteristic	lower flux	DCMD	151	56	[105]
PDA-PEI	HOLLOW FIBER	PVDF	Dip Coating	40	15	one-step fabrication	pore blockage	DCMD	109	25	[57]
PI	FLAT SHEET	PTFE	Dip Coating	40	8	low cost, one step,	Low Flux	DCMD	145	45	[98]
KOH- Modification	FLAT SHEET	PVDF	grafting	50	45	Simple Process	low durability	DCMD	150	62	[61]

Cotton Fabric	FLAT SHEET	PDMS	grafting			high wettability difference,	complicated process		153		[87]
PVDF-PAN-Cloisite	HOLLOW FIBER	PVDF-cloisite	CO-extrusion	90	55	High Flux		DCMD	50	140	[16]
Hydrogel	FLAT SHEET	Teflon (PTFE)	Coating	40	30	High wetting resistivity	Low stability	DCMD			[55]
PDADMAC/PAA	FLAT SHEET	PVDF		45	5	long-term robustness	Low flux	DCMD	125	50	[63]
DA	FLAT SHEET	PTFE		50	89	High flux, Antifouling resistivity		VMD	134	59	[125]
cellulose acetate	FLAT SHEET	PTFE	Electrospinning	40	20	Antifouling, Mechanical strength		DCMD	135	39	[126]
graphene oxide	FLAT SHEET	PVDF	dip-coating	40	25	Antifouling and antiwetting	Low stability	DCMD	145		[127]

PU	FLAT SHEET	PTFE	Dip coating	40	23	Antifouling and antiwetting		DCMD	130	15	[128]
EDA/PEI	FLAT SHEET	PVDF	Electrospinning and dip-coating	35	5	High oil-fouling resistivity	Low flux		127	40	[78]

1110 Always, nature is the best reference for the production of most optimum and environmental  
1111 friendly materials and instruments. Mussels have the ability to make a strong, rapid and tough  
1112 adhesion to different underwater places and preserve themselves from high pressure water  
1113 forces. This tough adhesive that has the ability to adhere to various surfaces has dopamine-  
1114 based structure and as a result, mussels as inspired from nature have been utilized for the  
1115 fabrication of materials to render attachment of different surfaces having opposite wettability  
1116 tendency. In fact, dopamine has the ability to be used as an interface for attachment of  
1117 hydrophilic layer on top of hydrophobic membrane substrates [30, 107]. Polydopamine is a  
1118 biological adhesive inspired from mussels and formed through self-polymerization of  
1119 dopamine at room condition via autoxidation in an aqueous media containing dissolved  
1120 oxygen [59, 129]. The presence of catechol, quinone and amine functional groups gives  
1121 hydrophilic nature to dopamine and also make it possible to make various types of  
1122 interaction, including hydrogen bond, covalent bond, pi-interaction, charge transfer  
1123 interaction and metal chelation, with substrate materials. This wide range of interaction made  
1124 dopamine an attractive material for adhesion to substrates having various condition like wet,  
1125 dry, organic, or inorganic. This ability caused PDA play the role of main or intermediate for  
1126 covering of top layer of hydrophobic, superhydrophobic, or omniphobic membranes for  
1127 fabrication of Janus membranes in MD applications [12, 59, 129]. For example, Chew et al.  
1128 have co-deposited a hydrophilic layer of PDA/PEI on the outer surface of PVDF hydrophobic  
1129 substrate. The novelty in this work is in the co-deposition of hydrophilic layer on top of  
1130 hydrophobic substrate. The hydrophilic layer made strong bond with water molecules and  
1131 become hydrated and this hydrated layer prevent membrane fouling and enhance the  
1132 separation performance of the membrane [57]. In this work, the permeate flux for Janus  
1133 membrane (11 LMH) was slightly lesser than hydrophobic ones (4 LMH), but the permeate

1134 conductivity for Janus membrane was close to zero during 80 hr test (~100 % rejection) and  
1135 for hydrophobic membrane it stepwise increased until it reached to more than 1000  $\mu\text{S}/\text{cm}$   
1136 after 20 hrs.

1137 In another study, Wu et al also deposited PDA/PEI on the surface of PP membrane. In this  
1138 work, Janus membrane was fabricated by floating of a PP membrane on solution containing  
1139 dopamine and PEI. As a result, the hydrophilic layer was deposited on the substrate using  
1140 mussel-inspired catechol groups of dopamine. This asymmetric configuration obtained 130°  
1141 wettability difference between two sides of the membrane [59]. The SEM images proved the  
1142 presence of microchannel which helped the transport of water molecules using hydrophilic  
1143 moieties and capillary forces. Also, the MD experimental results showed that while the pore  
1144 size of the outer surface of the Janus membrane compared to neat hydrophobic membrane  
1145 decreased, the flux did not decrease. This result proved that the proper selection of type and  
1146 method of top hydrophilic layer cover its drawbacks. In addition, long-term experimental  
1147 results in high SDS feed water better determined the effectiveness of the prepared Janus  
1148 membrane. While the neat hydrophobic PVDF membrane encountered severe wetting and  
1149 fouling by increment in permeate conductivity and decrement in flux after 90 h of test, the  
1150 Janus membrane continued its good flux and salt rejection. This result demonstrated that the  
1151 grafted hydrophilic layer can positively prevent the importation of surfactant and oil droplets  
1152 and can prevent the Janus membrane from fouling and wetting [59].

1153 Furthermore, in another study, a one-step fabrication of Janus membrane was tried by using  
1154 SMM. In a series of experiments, SMMs were fluorinated and then mixed with polyetherimide  
1155 to fabricate Janus membranes. The results showed that the derived composite membrane  
1156 reached LEP greater than 2.9 bar. However, both liquid and gas flux of the membrane

1157 decreased due to lower pore sizes of modified membrane. In addition, the DCMD results of  
1158 Janus membranes prepared by PEI and SMM in different studies showed equivalent or higher  
1159 flux compared to commercial PTFE membrane [17, 96]

1160 The treatment of wastewaters with high microorganisms content is always challenging. For  
1161 this type of wastewater, it is applicable to use some nanoparticles that have antibacterial  
1162 activity to simultaneously improve separation performance of MD membrane and decrease  
1163 bacterial growth on the surface of the membrane. In an experiment, hydrophilic PDA layer  
1164 was coated on top of hydrophobic PVDF hollow fiber to fabricate a Janus membrane.  
1165 Afterwards, to increase both antibacterial activities and fouling resistivity of the membrane,  
1166 silver nanoparticles were used as top layer coating. The experimental study on the prepared  
1167 membrane proved the lower adhesion of fouling agents on the membrane surface. In  
1168 addition, the proliferation of sulphur-containing proteins or thiol groups of enzymes was  
1169 restrained in the silver-containing Janus membrane, which proves its antibacterial activities  
1170 [82].

1171

## 1172 **6.2 Hydrophobic-hydrophilic Janus membrane configuration**

1173 Though most of research on Janus membrane were performed to investigate the effect of  
1174 hydrophilic layer on feed side of the MD system, some studies have investigated the impact  
1175 of hydrophilic layer on permeate side of the MD modules. In these works, the hydrophilic face  
1176 of the Janus membrane was placed toward permeate side. In a study performed by Zou et al,  
1177 a hydrophilic layer containing PEG was coated on hydrophobic substrate and separation and  
1178 energy performance of prepared Janus membrane was investigated by placing its hydrophilic  
1179 side toward permeate side of the module, while the feed side of the membrane was

1180 hydrophobic. The change in energy performance of the Janus membrane was compared to  
1181 neat hydrophobic membrane and results proved that co-extruding of a thin PVDF/PEG  
1182 hydrophilic layer on the PVDF hollow fiber substrate enhanced the energy efficiency of the  
1183 membrane from 55% to 72%. This increase can be attributed to the presence of highly porous  
1184 and hydrophilic layer on permeate side that improves the condensation rate of evaporated  
1185 layer. Also, the hydrophilic layer prevents the intrusion of permeate water into the pores and  
1186 decrease the wetting possibility. Experimental results revealed that the salt rejection, flux and  
1187 heat efficiency of the membrane have decreased in long term test and wetting problem  
1188 occurred after 200 h of operation [71]. In general, in this type of Janus membranes, the  
1189 bottom layer should have high heat conductivity to easily transfer the released heat of  
1190 condensation and maintain the driving force of water transport. In this type of configuration,  
1191 the hydrophilic layer plays the role of increasing the mass transfer, decreasing the heat loss,  
1192 and increasing the mechanical strength of the membrane [60, 89, 130].

1193

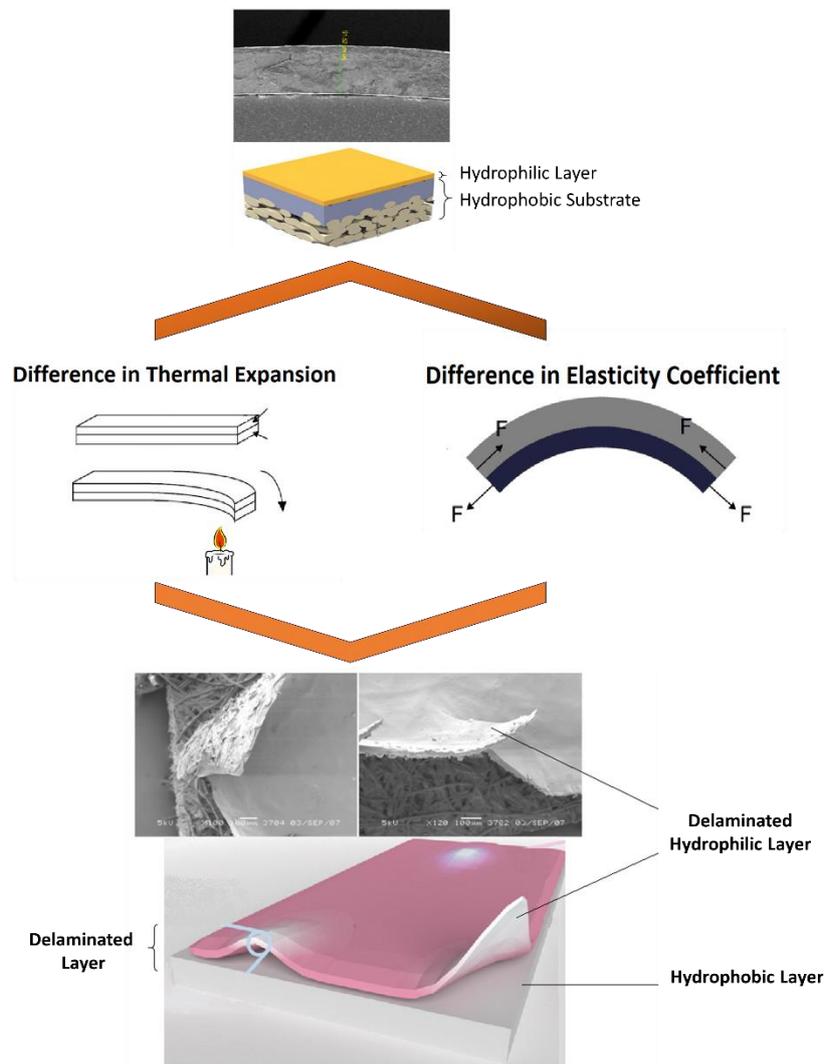
## 1194 **7. Challenges facing Janus membranes in MD**

1195 Regardless of the type of method used for fabrication, Janus membranes have encountered  
1196 two main challenges, which make problems in the way of its performance and potential  
1197 commercialization. First, due to different chemical structure of hydrophobic and hydrophilic  
1198 layers, Janus layers have weak interaction with each other and have been delaminated after  
1199 a period of time of operation. This poor compatibility is a crucial point for long term  
1200 application of Janus membranes. Second, only the hydrophilic layer can repel hydrophobic  
1201 foulant and low surface compounds, like surfactants, and if these foulant can pass through

1202 the hydrophilic layer, they can cause wetting of the hydrophobic layer beneath [22, 30, 33,  
1203 71].

#### 1204 **7.1. Delamination**

1205 Delamination is one of the main issues facing the use of Janus membranes. As per design  
1206 structure of a Janus membrane, it consists of two layers with opposing wettability, which  
1207 means that the layers could be made of different materials that are not affinitive with each  
1208 other without proper modification. For example, in general Janus membrane fabrication, the  
1209 hydrophobic substrate is firstly modified to form re-entrant structure on the surface and  
1210 coated with low surface energy materials converting it into omniphobic membrane. The  
1211 omniphobic membrane then becomes the substrate to coat a hydrophilic layer on top to form  
1212 the Janus membrane, but the low surface energy coating on the omniphobic membranes  
1213 decreases the interaction of coated hydrophilic layer and a weak adhesion is formed that  
1214 make it less robust and stable. This problem is exacerbated during the water treatment  
1215 process when the top layer becomes hydrated. Due to difference in wettability of the  
1216 contacted layer, the swelling of hydrophilic layer increases interaction conflicts and may cause  
1217 membrane delamination problems. Therefore, high attention should be paid to  
1218 simultaneously improve layer adhesion and separation performance of Janus membrane [32,  
1219 37, 38]. The schematic of delamination process is shown in **Figure 10**.



1220

1221

*Figure 10. The schematic of delamination process for Janus membrane*

1222

Although the fabrication of multi-layer polymers has been widely progressed in recent years,

1223

delamination still remained as an issue in this process. In general, the difference in physical

1224

and chemical properties of both layers make it a balancing challenge between attachment

1225

and detachment forces. Also in some studies, in order to increase the accuracy and quality of

1226

the top layer, the hydrophilic layer was coated using layer-by-layer method and through some

1227

steps. This layering coating causes distribution of exerted stress across the coated layer and,

1228

in real operational condition, sequential detachment takes place for a multilayer surface (as

1229

shown in **Figure 10**). The delamination in coating process generally refers back to one of

1230 following two mechanisms: (1) difference in phase inversion process during coagulation step,  
1231 and (2) difference in shrinkage coefficient of layers in both sides of coating layer. In order to  
1232 decrease the delamination, the best choice is by selecting dope solution coming from similar  
1233 solvents and/or the same polymer family. Using similar solvent helps adhesion of distinct  
1234 layers to form an integrated coating. For example, in a study,  $\epsilon$ -Caprolactam was used as  
1235 solvent for both PVDF hydrophobic substrate layer and PVDF-PVA hydrophilic top layer. The  
1236 results demonstrated that using water-soluble solvent improved the fabrication of  
1237 delamination-free Janus membrane for MD application. The presence of same solvent and  
1238 PVDF polymer in both hydrophobic and hydrophilic layer and also the solubility of  $\epsilon$ -  
1239 Caprolactam in the water resulted in the fabrication of an integrated Janus membrane [67].  
1240 However, MD test results for some experiments indicated that this method compromised the  
1241 wettability of coated or substrate layers. As a result, the separation performance is lower  
1242 compare to Janus membranes having high wettability difference between two layers.

1243 Another issue during phase inversion process of Janus membranes is that the structure and  
1244 phases of layers can change. If the two layers are formed with different coagulation rates,  
1245 two separate layers are formed that have low attachment with each other. Therefore, besides  
1246 the selection of dope compositions and their compatibility, the ternary phase inversion of  
1247 both layers should be compared to find the difference in phase inversion rates. Furthermore,  
1248 Janus membranes operated in temperatures below or beyond the ambient temperature has  
1249 led to shrinkage or expansion during the process. This indicates that one has to consider the  
1250 differences in shrinkage coefficient that can amplify the stress and strains on the polymers  
1251 and on the coated layer that further exacerbate layering and delamination problem [41, 131].  
1252 To address this drawback, many groups have used various new fabrication techniques, like  
1253 co-extrusion for hollow fiber membranes, co-casting for flat sheet membranes, addition of

1254 diluents or additives, and proper selection of polymers according to their phase diagram [14,  
1255 132-134].

1256 In general, the quality and robustness of coated layers to avoid delamination problem are  
1257 tested via exposing them to harsh conditions. One way is by immersing the membrane in an  
1258 ultrasonic bath for a long time, which exposes it to constant stress and strain from ultrasonic  
1259 waves. Analysis is then carried out to determine the condition and amount of the coated layer  
1260 with respect to its previous condition. One study utilized FTIR to determine the functional  
1261 groups on a coated PVDF Janus membrane after exposing to ultrasonication for 10 minutes.  
1262 The results showed the presence of functional groups that make strong attachment between  
1263 layers, which were corroborated by the EDX and DCMD results [32, 82].

1264 To enable good interaction of the hydrophilic layer with the substrate for strong adhesion,  
1265 some groups used a pre-treatment process to prepare an omniphobic substrate for strong  
1266 coating step [59, 82]. Studies have shown that a hydrophilic dope solution needs active sites  
1267 on the omniphobic layer to attach to it. Direct coating of top hydrophilic layer will not render  
1268 it effective due to the absence of active sites on the previously generated omniphobic surface.  
1269 This is because omniphobic substrates naturally repels almost all types of liquid and do not  
1270 let the solvents to make active sites. Forming fluorocarbon sites on the omniphobic surface is  
1271 a good strategy but it needs high activation energy, equivalent to a temperature of 90°C. The  
1272 plasma etching technique is a good pre-treatment method to effectively produce active sites  
1273 on the omniphobic surface prior to coating of hydrophilic layer. A study has utilized such pre-  
1274 treatment strategy and strong interaction between the coating layer and the omniphobic  
1275 layer was observed, and no delamination was found after DCMD test. Compared to other

1276 fabricating techniques of Janus membranes, high and stable MD separation performance was  
1277 observed for this Janus membrane [74].

## 1278 **7.2 Reduced vapour transport**

1279 Another challenge for Janus membranes, which usually comes along with delamination  
1280 problem, is dense interface morphology issue that provides resistance against vapour  
1281 transport across the membrane for MD application. The compactness at the interface of  
1282 coating layer generally decreases the effective surface area, and as a result decreases the flux  
1283 of the membrane. For example, Lin et al. coated a porous hydrophobic PTFE membrane by  
1284 hydrophilic hydrogel to enhance its antifouling and anti-wetting performance, but the  
1285 compactness and blockage of the pores decreased the flux of the membrane for DCMD  
1286 application from 30 LMH to 23 LMH [55]. In another study, Wang et al utilized chitosan to  
1287 modify hydrophilic PVDF membrane and results showed 15% flux decline with respect to neat  
1288 PVDF membrane (reached to 26 LMH from 31 LMH) [52]. However, the modified membranes  
1289 showed significantly better antifouling and antiwetting performance. One potential way to  
1290 address both delamination and dense interface morphology problems is by manipulation of  
1291 the concentration and composition of dope solution and also fabrication using co-extrusion  
1292 method. Zuo et al. have used this method and fabricated a membrane with different dope  
1293 compositions to find the most optimum point for decreasing the delamination [111]. The  
1294 dense interface morphology was overcome by addition of alumina nanoparticles to the inner  
1295 layer of co-extruded orifice. In this condition, alumina nanoparticles made some defects on  
1296 the polymeric matrix layer and increased the porosity and, consequently, decreased the  
1297 dense morphology. This resulted to enhanced flux performance. However, overuse of  
1298 nanoparticles also decreased the mechanical strength, the separation performance, and the

1299 top-layer attachment to the membrane [111]. Thus, balance must be performed when  
1300 designing a Janus membrane material with regards to the structure of the coating layer while  
1301 maintaining strong adhesion to the substrate material.

### 1302 **7.3 Scaling problem in Janus membrane**

1303 In the DCMD process, during water vaporization and vapour transport across the pores, the  
1304 salt concentration in the membrane-feed water interface increases. Additionally, due to heat  
1305 loss through the membrane matrix and also latent heat conversion, the temperature of feed  
1306 layer close to the surface decreases and is lower than the temperature of the bulk. This  
1307 situation transfers concentrated water into supersaturated zone and prepares condition for  
1308 formation of mineral scaling by deposition of excess minerals at the interface layer. Therefore,  
1309 due to intrinsic hydrophilicity of the formed scales, the hydrophobicity of the membrane  
1310 surface decreases, that can increase the probability of wetting and diminish LEP of the  
1311 membrane. Also, further increase in scales can block the membrane pores and simultaneously  
1312 decrease the flux of the membrane. Therefore, scale formation, which has separate  
1313 characteristic from fouling problem, should be observed for long-term operation of the MD  
1314 membranes [71, 135]. One of the commonly used method for cleaning the scaling on the  
1315 surface of the membranes is membrane regeneration. In this method, after a period of time,  
1316 the scales are physically or chemically removed from the membrane surface. Although the  
1317 membrane regeneration increases the operability of the membrane, but in general, due to  
1318 potential change in physical and chemical structure of the membrane pores, the performance  
1319 of the regenerated membrane is not similar to the neat membrane. All in all, the most cost  
1320 effective method is preventing of formation of scales on the membrane surface [71].

1321 Due to high salinity and contamination of feed water in MD process, scaling is highly  
1322 susceptible to form and is one of the major problems of MD modules. According to nature of  
1323 feed water, different types of scales may be formed. The most common types of MD scales  
1324 are calcite, gypsum, and silica. Gypsum and NaCl scales form through crystallization  
1325 mechanism, while silica scale is formed by polymerization of silica acid, a non-crystallization  
1326 method. Anti-scalants are widely used to mitigate the crystallization and formation of scales,  
1327 but due to amorphous structure of silica minerals, most of used anti-scalants showed weak  
1328 performance for decreasing silica scale formation [60, 136]. Presence of silica scales have  
1329 been reported in long-term application of MD for treatment of RO, Brackish, and shale gas  
1330 wastewaters [137, 138].

1331 In general, the scaling can be formed through two pathways: homogenous or heterogeneous  
1332 nucleation. In homogenous nucleation scaling, by supersaturating of minerals in small liquid  
1333 parts, the scale particles re spontaneously formed on that place. By increasing the  
1334 concentration of minerals by evaporation of liquids, the homogenous scaling continues to  
1335 form and formed scales deposit on the surface of membranes. Heterogeneous scaling is  
1336 another type of scales that are formed at the liquid-solid interface. In this type of scaling, the  
1337 interaction between dissolved minerals and membrane surface play the main role for scale  
1338 formation. Therefore, the physical and chemical characteristics of the membrane surface  
1339 determine the level of scaling [58, 139].

1340 Until now, different studies have focused on mitigation of fouling and wetting in MD process,  
1341 usually by organising roughness of the surfaces and coating with low surface energy materials.  
1342 Though these modification methods could effectively diminish fouling and wetting problems,  
1343 but the scaling challenges still need additional attention for commercialization of MD

1344 membranes [105, 139]. In order for deep investigation of the scaling issue, the composition  
1345 of fresh and used membranes should be analysed by EDX to investigate the type of crystals  
1346 formed on the surface of the membrane after wastewater treatment by MD. In a study  
1347 performed by Zou et al., the new peaks were observed in the used membrane, which were  
1348 relevant to the oxygen, irons, calcium, and magnesium. The results demonstrated that sulfate,  
1349 carbonate, and hydroxide scales are formed on the membrane surface. Comparison of the  
1350 intensity of the peaks revealed that the calcium carbonate is one of the main scales formed  
1351 on the surface of membrane. However, the membrane used for treatment of RO brine usually  
1352 have large proportion of sodium chloride scales and the composition of wastewater  
1353 determine the most dominant scales formed on the membrane surface [71, 140].

1354 Additionally, the silica formation is another major scaling problem in application of MD  
1355 process. Although the formation of homogenous nucleation depends on the characteristics  
1356 of feed water, the main challenge of scaling is formation of heterogonous nucleation that  
1357 attach to the membrane surface and gather homogenous silica scales and increase the  
1358 volume of scales on the surface. For this reason, different studies were carried out to decrease  
1359 the side effect of scale formation by enhancement of membrane surface geometry and  
1360 structure to decrease slippery angle of the membrane, which directly cause decrease in  
1361 formation and attachment of heterogeneous nucleation on the membrane surface [141, 142].  
1362 In a study, Yin et al. performed a DCMD test to investigate the behaviour of Janus and  
1363 hydrophobic membranes during scale formation in a high SDS feed water. The feed solution  
1364 containing different concentration of amorphous silica, NaCl, and gypsum scales was  
1365 prepared and the test was performed on three different membranes: hydrophobic PVDF  
1366 membrane, PVDF-SiNP-FAS superhydrophobic, and PVA/PVDF-SiNP-FAS Janus membrane.  
1367 The sliding test was performed on the membranes and results show that while hydrophobic

1368 membrane showed high WCA, the water droplet did not slide from the membrane surface.  
1369 Furthermore, water droplet starts to slide at sliding angle of  $17^\circ$  for superhydrophobic  
1370 membrane [105].

1371 Also, dynamic light scattering (DLS) test was used to determine the hydrodynamic diameters  
1372 of the scales formed during the MD test. All membranes showed perfect separation  
1373 performance during DCMD test for feed water with initial saturation index of -0.82. In this  
1374 condition, only small heterogeneous silica scales were formed on the membrane surface,  
1375 without affecting the performances of the membranes and structures of the pores. For the  
1376 feed water with silica saturation index of 0.55, gel-like silica scales with the size of 100-200  
1377 nm were formed in all membranes and the flux decreased for all of them, but Janus  
1378 membrane experienced lower decrease in performance. In this condition, due to high  
1379 concentration of silica, the homogenous nucleation of silica particles can react with silica acids  
1380 and form a cross-linked structures which can attach to the membrane surfaces. Continuous  
1381 formation and attachment of this particles can clog the membrane pores and also change the  
1382 wettability of membrane surface. As a result of this silica-silica interaction and formation of  
1383 both heterogeneous and homogenous silica nucleation, the flux of the membrane decreased  
1384 and the conductivity of permeate increased. The results of this experiments showed that the  
1385 formation of scales decreased the flux of Janus membrane, similar to hydrophobic and  
1386 superhydrophobic ones, by clogging the membrane pores. Eventhough the scale formation  
1387 changed the wettability of the hydrophobic or superhydrophobic membranes, it did not  
1388 change the wettability of the Janus membranes [61, 105]. All in all, the flux decline in  
1389 superhydrophobic membrane was less than others, but the Janus membrane derived the  
1390 highest water productivity. In order to remove the formed scales on the membrane surface,  
1391 the Janus membrane can be regenerated using custom backwashing method. Zou et al

1392 regenerated the Janus membrane and then analysed the membranes for evaluation of its  
1393 performance. The experimental results showed that after 16 h of test, the water recovery of  
1394 the membrane became about half of the fresh membrane after three days of continuous test.  
1395 This result proved that the formation of scales on the Janus membrane deformed the  
1396 structure of the pores and the stability and the shape of the membrane changed and lost its  
1397 high salt rejection and water recovery in long term operation [71].

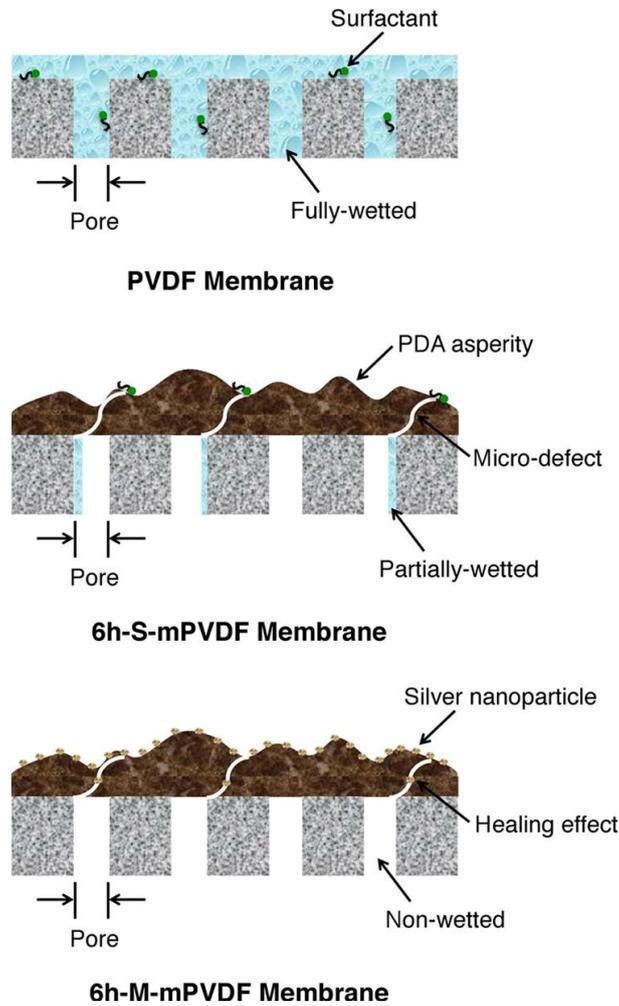
#### 1398 **7.4. Formation of microdefects on hydrophilic layer**

1399 Besides the delamination problem, the coating of a hydrophilic layer on top of an omniphobic  
1400 or a hydrophobic layer can face another challenge: the formation of microdefects during  
1401 formation or polymerization of hydrophilic layer, which can produce microchannels, resulting  
1402 to a decrease in salt rejection of the membrane. To address this challenge, the coated  
1403 hydrophilic layer using common methods is usually exposed to drying and hydration steps  
1404 before their application in real wastewater treatment. Also, sometimes during the real test,  
1405 the membrane may go to a recovery or maintenance mode and get dried. The changes in  
1406 hydration (consecutive drying and wetting) can affect the structure of the hydrophilic layer  
1407 and produce some defects that decrease the performance of the membrane. For covering this  
1408 deficiency, in some studies production of multilevel structure was suggested. Also according  
1409 to Wenzel theory, similar to hydrophobic surfaces that higher roughness increases  
1410 hydrophobicity of the membrane, roughness increment in hydrophilic layer can increase the  
1411 hydrophilicity of the top layer. For example, Chew et al. fabricated a Janus membrane by  
1412 coating of self-polymerized PDA layer on top of PVDF porous hydrophobic substrate. The  
1413 wetting and fouling tests on the prepared membrane was carried out using 500 mg/L Tween  
1414 20-stabilized petroleum-in-water emulsions and results showed better performance for Janus

1415 membrane with respect to neat PVDF membrane. The neat PVDF membrane encountered  
1416 severe wetting and fouling after 20 h operation, but the Janus membranes showed slight  
1417 wetting and fouling after 50 h of experimental test. The analysis was carried out to determine  
1418 the source of decrease in the efficiency of Janus membrane. In this way, the SEM images  
1419 showed presence of microvoids that work like channels to transmit fouling and wetting agents  
1420 to the hydrophobic layer beneath hydrophilic top layer and, therefore, decrease in the  
1421 performance of the membrane can be attributed to these voids.

1422 In order to heal these features, Janus membrane can be coated with nanoparticles to cover  
1423 the formed microchannels or prevent the formation of these microvoids during hydration  
1424 stresses. In a study, the surface of hydrophilic layer was coated with Ag nanoparticles using  
1425 immersion techniques (**Figure 11**). The experimental DCMD results showed perfect  
1426 performance even after 96 hr test without compromising the flux or salt rejection. The Ag  
1427 nanoparticles could effectively cover the microchannels and prevent entrance of low surface  
1428 energy compounds or oil droplets, even in high oil and surfactant contaminated feed water  
1429 [82].

1430



1431

1432 *Figure 11. the effect of dispersion of silver NPs on the wetting resistance of Janus membrane*

1433

[82]

1434

## 1435 **8. Conclusions and future perspectives**

1436 This review focused on the investigation of different aspects of fabrication, modification, and  
 1437 application of Janus membranes for membrane distillation (MD). Various methods for  
 1438 modification of the surface of the hydrophobic or omniphobic membranes were investigated  
 1439 and the benefits and challenges of methods were explored. Furthermore, different possible  
 1440 membrane configurations in various types of modules like flat sheet and hollow fiber have

1441 been introduced. The antiwetting and antifouling performance of the prepared Janus  
1442 membranes in different types of feed water was investigated and the results were compared  
1443 to neat hydrophobic membranes. The results showed higher efficiency of Janus membranes  
1444 for treatment of feed waters having high concentration of contaminants and pollutants and  
1445 proved potential of the Janus membrane for long-term application in MD systems.

1446 However, Janus membrane still is dealt with some challenges that impede its overall  
1447 performance and potential commercialization. First of all, Janus membranes is fabricated by  
1448 modification of MD membranes that are microporous hydrophobic membranes, suitable for  
1449 microfiltration process. These membranes still have some problems for commercialization  
1450 and the first step is fabrication of a special type of membrane for MD. The second challenge  
1451 refers to the types of materials used for modification of the membranes, which should be  
1452 cheap, environmentally friendly, and easily processed. Furthermore, some preparation  
1453 methods give good laboratory results but they do not have bright prospect for large scale  
1454 production. Therefore, researches should be directed to prepare a more ecofriendly and  
1455 producible Janus membrane. The mechanical stability of the Janus membrane is another  
1456 important matter that needs to be recognised for enhancement of tolerability of the  
1457 membrane for long-term working on harsh condition. Additionally, the mechanism of the  
1458 transport of the liquid through the hydrophilic layer and phase change to vapour in Janus  
1459 membrane have not been properly investigated and a detailed modelling or simulation is  
1460 necessary.

1461 Regarding attractive results derived from experimental research, the Janus membranes  
1462 showed high potential to be a candidate for treatment of highly polluted, challenging  
1463 wastewaters in MD systems. For this reason, the direction of the future researches should be

1464 accurately determined to cover the available deficiency of the membranes. The overview of  
1465 the current researches on Janus membrane declared the void points in the research  
1466 environment. The most important point for fabrication of defect-free Janus membrane is  
1467 solving the delamination issues. Also, the change in configuration of the layers can be helpful  
1468 to cover current deficiency of the Janus membranes. In this way the following suggestion are  
1469 made as future prospects for the preparation and design of Janus membranes for MD:

- 1470 • Using compatible materials that have good chemical integrity, but different  
1471 hydrophobicity
- 1472 • Fabrication of trilayer membrane that has hydrophilic affinity in both side but  
1473 hydrophobic affinity in middle, which theoretically shows attractive configuration for  
1474 enhancement of both heat and mass transfer efficiency
- 1475 • Using dual-electrospinning technique that can bring asymmetric and high porosity  
1476 membrane
- 1477 • Using economic and non-fluorinated materials that has low environmental issues and  
1478 low cost
- 1479 • Focusing on one-step fabrication methods to ease fabrication process and decrease  
1480 the processing costs like improvement of SMM based Janus membranes
- 1481 • Most of studies were performed in flat sheet module and more research on other  
1482 commercial modules like hollow fiber is necessary.

1483

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1491

1492 **List of abbreviations**

1493	ALD	Atomic Laser Deposition	
1494	CNT	Carbon Nanotubes	
1495	DTAB	Dodecyl Trimethyl Ammonium Bromide	
1496	ENFM	Electrospun Nanofiber Membrane	
1497	FAS	(Heptadecafluoro-Tetradecyl) Trimethoxysilane	HLB
1498		Hydrophilic–Lipophilic Balance	
1499	LEP	Liquid Entrance Pressure	
1500	MD	Membrane Distillation	
1501	NIPS	Nonsolvent Induced Phase Inversion	
1502	NP	Nanoparticle	
1503	OCA	Oil contact angle	

1504	PDA	Polydopamine
1505	PDMS	Polydimethylsiloxane
1506	PEG	Polyethylene Glycol
1507	PEI	Polyethylenimine
1508	PES	Polyethersulfone
1509	PET	Polyethylene Terephthalate
1510	PI	Polyimide
1511	PP	Polypropylene
1512	PTFE	Polytetrafluoroethylene
1513	PVA	Polyvinyl Alcohol
1514	PVDF	Polyvinylidene Difluoride
1515	PVP-VTES	Poly(Vinylpyrrolidone-Vinyltriethoxysilane)
1516	RO	Reverse osmosis
1517	SMM	Surface Modified Macromolecules
1518	TGA	Thermogravimetric Analysis
1519	TIPS	Temperature Induced Phase Inversion
1520	WCA	Water Contact Angle
1521		

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